



Electrical Capacitance Volume Tomography: An Imaging Tool for Multiphase Flow Systems

Qussai Marashdeh^{1,2}, Fei Wang², and L.S. Fan²

¹Tech4Imaging LLC ²The Ohio State University Department of Chemical and Biomolecular Engineering



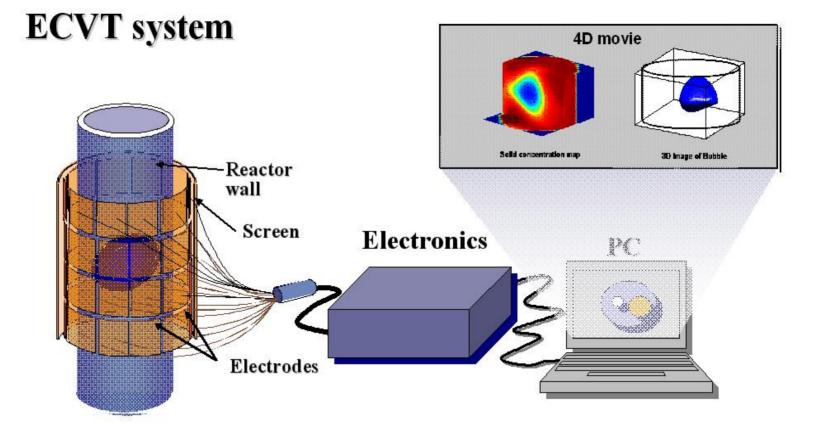
Introduction

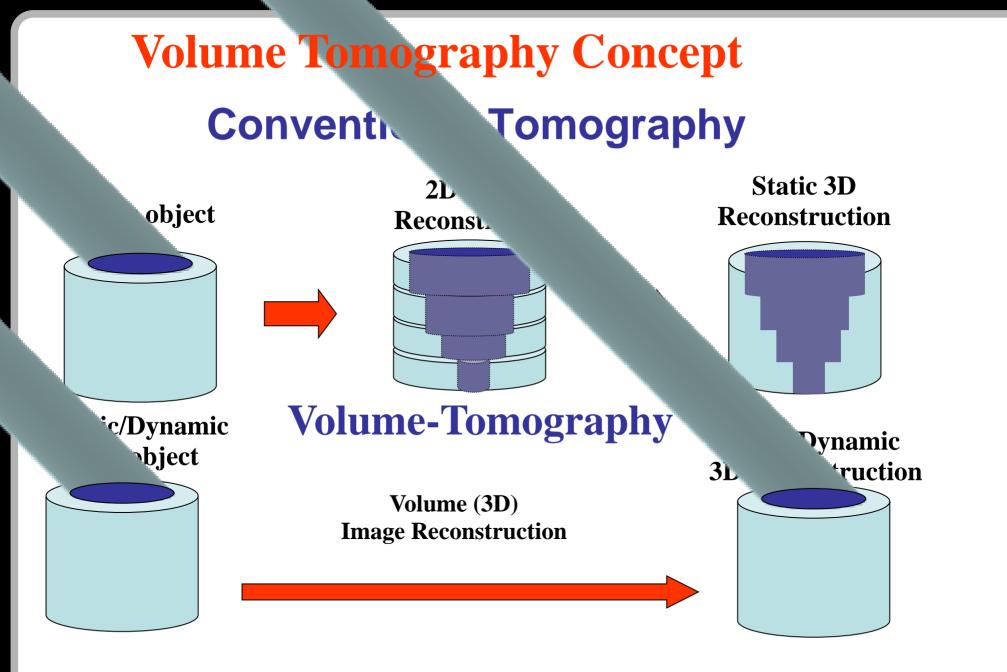
- Electrical Capacitance Volume Tomography (ECVT) is a 3D imaging technique for viewing cold flow processes. It can potentially be applied to hot units too.
- ECVT is among few know non-invasive imaging tool that can be used for commercial applications (low cost, suitable for scale-up, fast, and safe)
- Tech4Imaging LLC is a spin-off company from The Ohio State University to develop and commercialize imaging technologies, including ECVT.
- Tech4Imaging, with DOE support, is developing a complete system of acquisition hardware, sensors, and reconstruction software for.

Preface

- 1. ECVT Technology
- 2. Verification
- 3. Jet Example
- 4. Velocimetry
- 5. Sensors and Scale up Application
- 6. Complex geometries







ECVT technique

Reconstruction	Methodology	Characteristics	Example
Single Step Linear Back Projection	The sensor system is linearized (usually by constructing a sensitivity matrix). The image is obtained by back projecting the capacitance vector using the sensitivity matrix.	Fast, low image resolution, and introducing image artifacts	LBP
Iterative Linear Back Projection	The mean square error between the capacitance data and forward solution of the final image is minimized by iterative linear projections using the sensitivity matrix.	Slower than Single Step Linear. Providing better images than Single Step	Landweber ILBP
Optimization	A set of objective functions are minimized iteratively to provide the most likely image. Different optimization algorithms and objective functions can be used.	Slower than Iterative Linear Back Projection. Providing better images than Iterative Linear Back Projection	3D-NNMOIRT

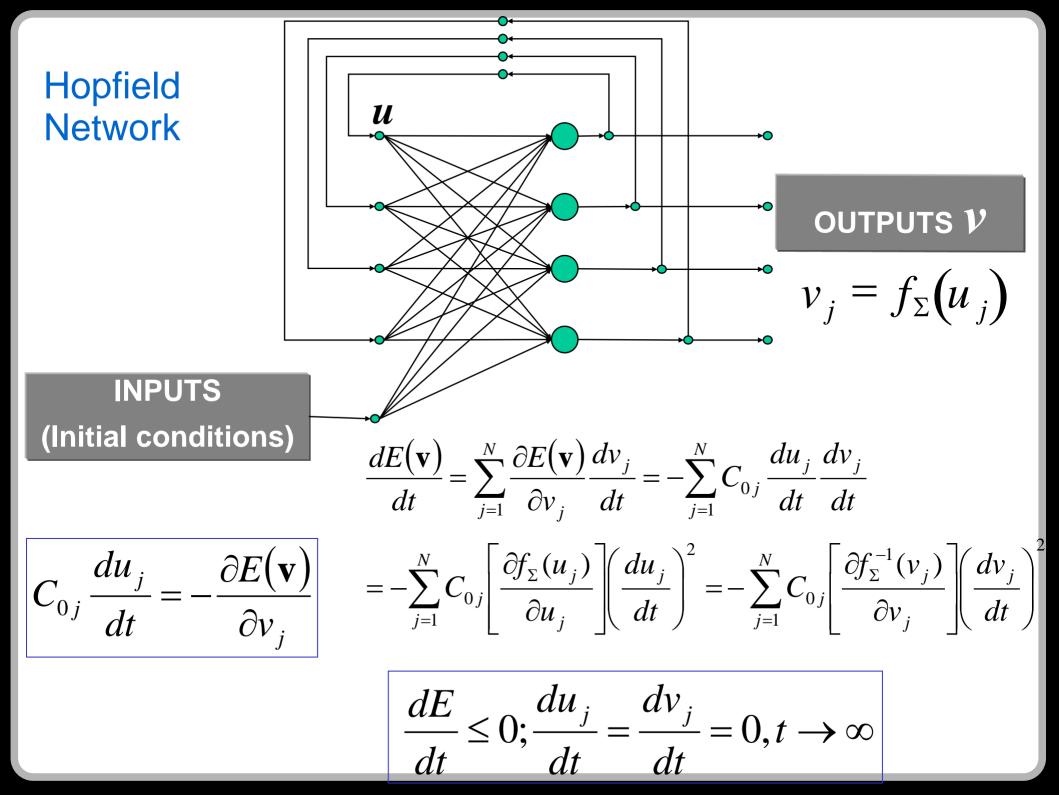
3D-NNMOIRT

Objective functions

Negative entropy function $f_1(\mathbf{G}) = \gamma_1 \sum_{j=1}^N G_j \ln G_j$ Error function $f_2(\mathbf{G}) = \frac{1}{2} \gamma_2 \|\mathbf{S}\mathbf{G} - \mathbf{C}\|^2 = \gamma_2 \sum_{i=1}^M \left(\sum_{j=1}^N S_{ij}G_j - C_i\right)^2$ 3-D Smoothness function $f_3(\mathbf{G}) = \frac{1}{2} \gamma_3 \left(\mathbf{G}^T \mathbf{X}\mathbf{G} + \mathbf{G}^T \mathbf{G}\right)$

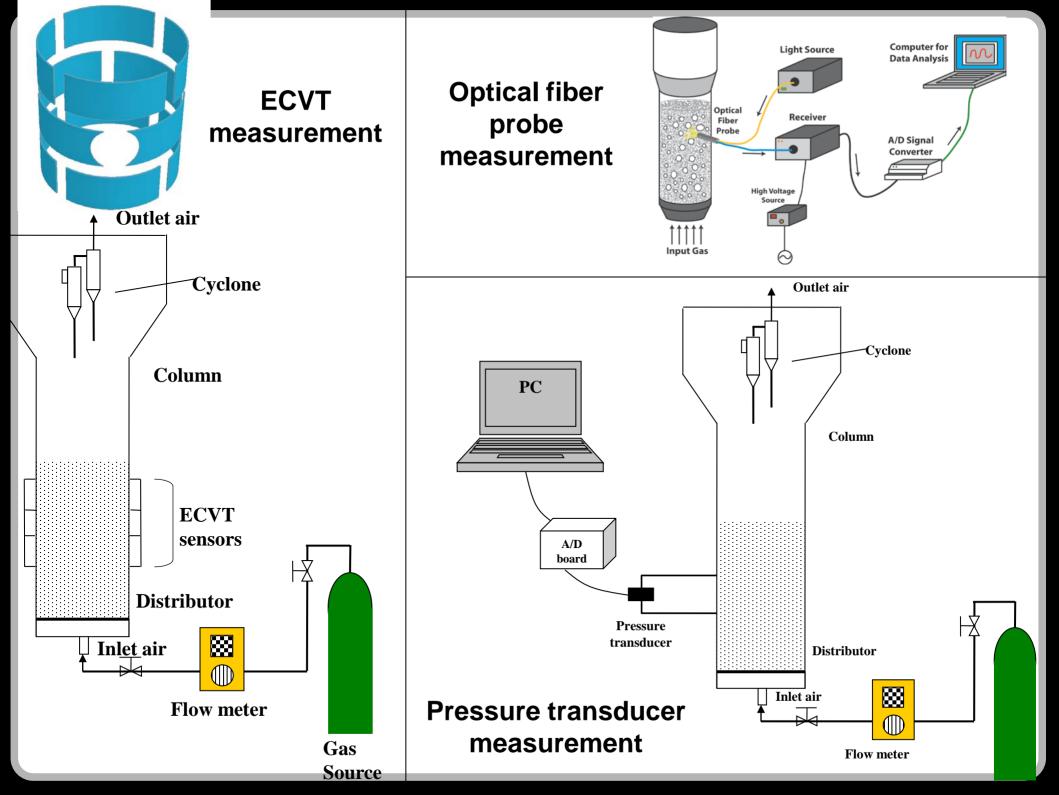
3-to-2D and 3-to-1D matching function for 3-D imaging

$$f_{4}(\mathbf{G}) = \frac{1}{2} \gamma_{4} \left\{ \left\| \mathbf{H}^{1} \mathbf{G} - \mathbf{G}_{2D}^{1} \right\|^{2} + \left\| \mathbf{H}^{2} \mathbf{G} - \mathbf{G}_{2D}^{2} \right\|^{2} \right\}$$
$$= \frac{1}{2} \gamma_{4} \left\{ \sum_{j=1}^{N_{1D}} \left(\sum_{k=1}^{N} H_{jk}^{1} G_{k} - G_{1D,j} \right)^{2} + \sum_{j=1}^{N_{2D}} \left(\sum_{k=1}^{N} H_{jk}^{2} G_{k} - G_{2D,j} \right)^{2} \right\}$$



2. ECVT Verification

- 1) Comparison of the local time-averaged solids concentrations by *ECVT*, *ECT*, and *optical fiber probe*
- 2) Comparison of the time-averaged cross-sectional solids concentrations by *ECT* and *optical fiber probe* and the time-averaged volume solids concentration obtained by *ECVT* and *pressure transducer*
- 3) Comparison of ECVT and MRI



Experimental Conditions

FCC particle: Particle size: 60 μm Particle density: 1400 kg/m³

Fluidized bed:

ID: 4 inch Total height: 2.5 m Two-stage cyclone

Distributor:

Porous plate with a pore size of 20 μ m Fractional free area: 60%

Gas:

1

Air density:1.225 kg/m³ Air viscosity: 1.8x10⁻⁵ Ns/m² 2

FCC particle:

Particle size: 60 μm Particle density: 1400 kg/m³

Fluidized bed:

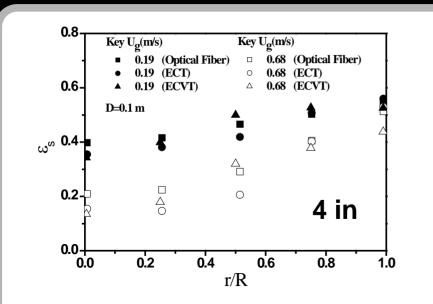
ID: 12 inch Disengagement section: 0.5 m Total height: 2.3 m Two-stage cyclone

Distributor:

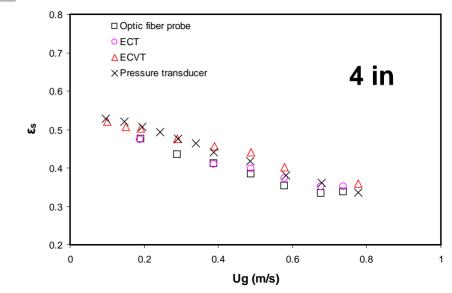
Porous plate with a pore size of 20 μ m Fractional free area: 60%

Gas:

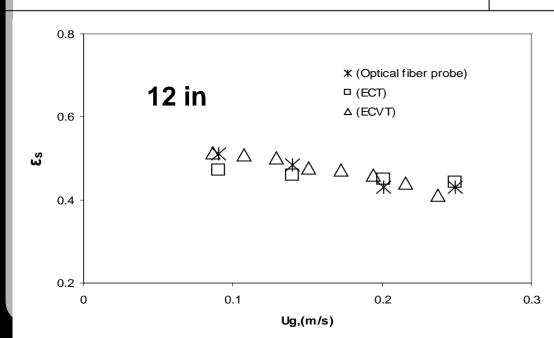
Air density:1.225 kg/m³ Air viscosity: 1.8x10⁻⁵ Ns/m²



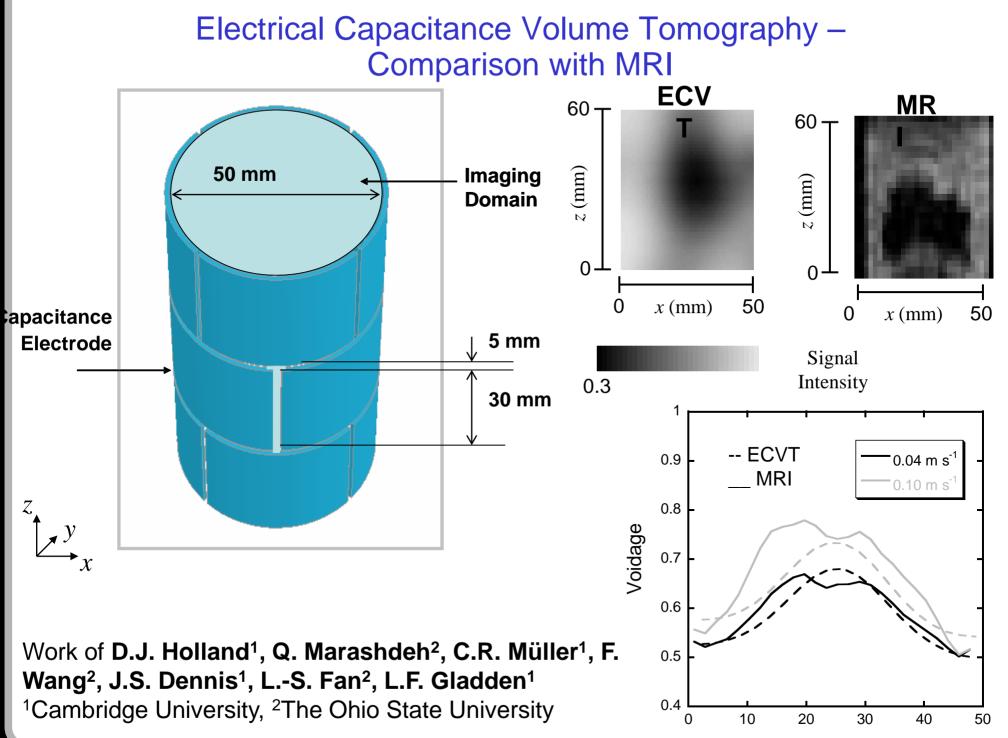
Radial profiles of time-averaged solids concentration in a 4-in gas-solid fluidized bed with FCC particles $(d_p = 60 \ \mu m; \ \rho_p = 1400 \ \text{kg/m}^3)$ obtained by ECVT, ECT and optical fiber probe



Comparison of the time-averaged cross-sectional solids concentrations obtained by *ECT* and *optical fiber probe* and the time-averaged volume solids concentration obtained by *ECVT* and *pressure transducer* for a 4-in gassolid fluidized bed with FCC particles ($d_p = 60 \mu m$; $\rho_p =$ 1400 kg/m³)

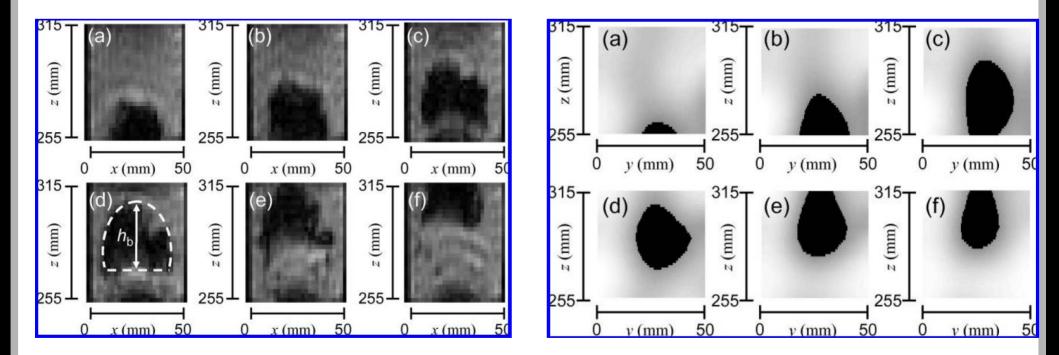


Comparison of the time-averaged crosssectional solids concentrations obtained by the *ECT* and the *optical fiber probe* and the time-averaged volume solids concentration obtained by the *ECVT* for a 12-in gas-solid fluidized bed with FCC particles ($d_p = 60 \ \mu m$; $\rho_p = 1400 \ kg/m^3$)



Horizontal Position (mm)

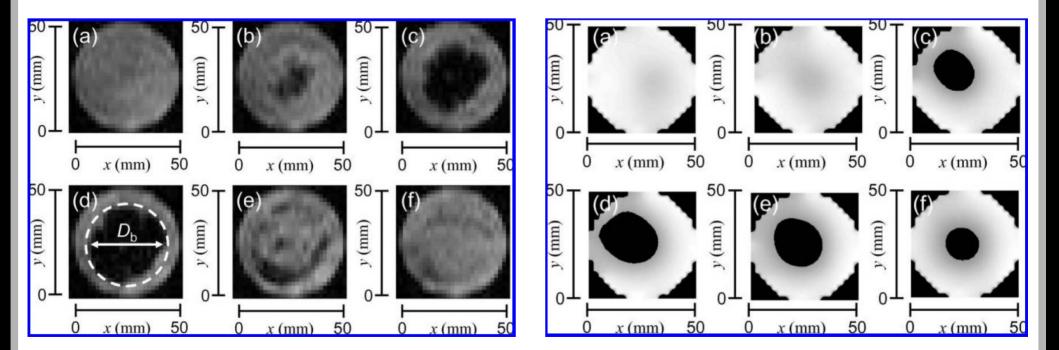
Electrical Capacitance Volume Tomography – Comparison with MRI



Superficial Gas Velocity: 0.04 m/s; MRI: every frame (26 ms) ECVT: every 2nd frame (25 ms)

Work of **D.J. Holland¹**, **Q. Marashdeh²**, **C.R. Müller¹**, **F. Wang²**, **J.S. Dennis¹**, **L.-S. Fan²**, **L.F. Gladden¹** ¹Cambridge University, ²The Ohio State University

Electrical Capacitance Volume Tomography – Comparison with MRI

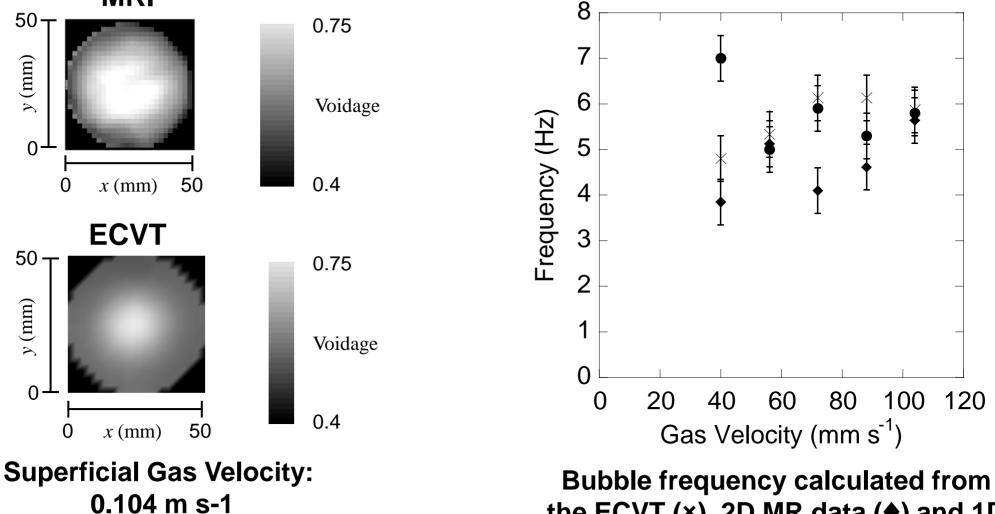


Superficial Gas Velocity: 0.04 m/s; MRI: every frame (26 ms) ECVT: every 2nd frame (25 ms)

Work of **D.J. Holland¹**, **Q. Marashdeh²**, **C.R. Müller¹**, **F. Wang²**, **J.S. Dennis¹**, **L.-S. Fan²**, **L.F. Gladden¹** ¹Cambridge University, ²The Ohio State University

Electrical Capacitance Volume Tomography – Comparison with MRI

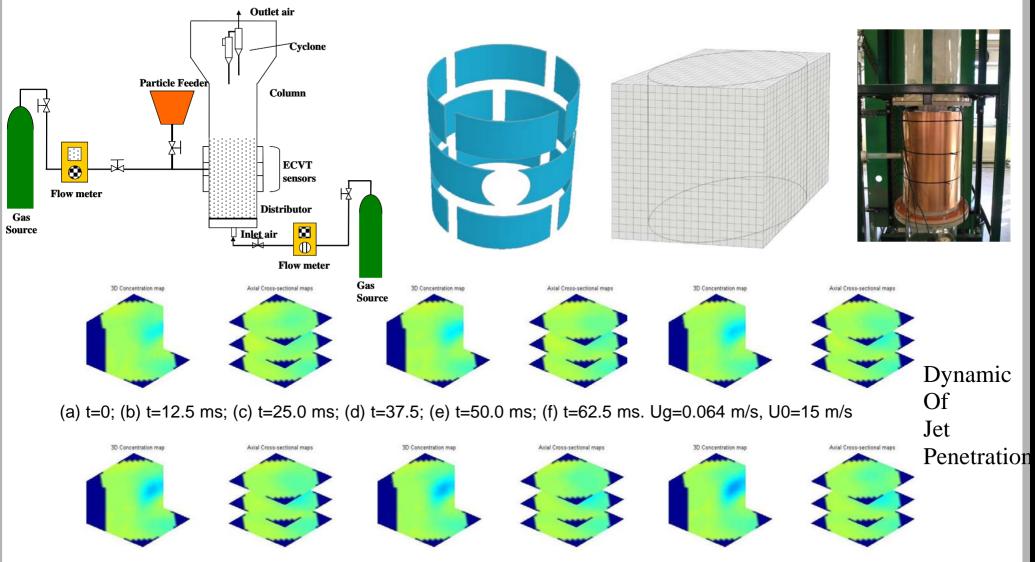
MRI



the ECVT (×), 2D MR data (♦) and 1D ¹ F MR data (●).

Work of **D.J. Holland¹**, **Q. Marashdeh²**, **C.R. Müller¹**, **F. Wang²**, **J.S. Dennis¹**, **L.-S. Fan²**, **L.F. Gladden¹** ¹Cambridge University, ²The Ohio State University

3. Horizontal gas jet penetration in a gas-solid fluidized bed



Fei Wang, Zhao Yu, Qussai Marashdeh, Liang-Shih Fan * "Horizontal gas and gas/solid jet penetration in a gas–solid fluidized bed" *Chemical Engineering Science* 65 (2010) 3394–3408

Experimental Conditions

FCC particle:

Particle size: 60 μm Particle density: 1400 kg/m³

Fluidized bed:

ID: 12 inch Disengagement section: 0.5 m Total height: 2.3 m Two-stage cyclone

Distributor:

Porous plate with a pore size of 20 μ m Fractional free area: 60%

Gas:

Air density:1.225 kg/m³ Air viscosity: 1.8x10⁻⁵ Ns/m²

Sensors and Experimental Setup





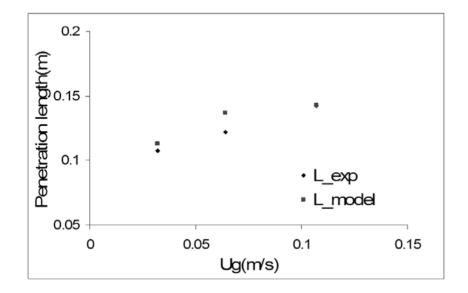
Horizontal gas jet penetration in a gassolid fluidized bed

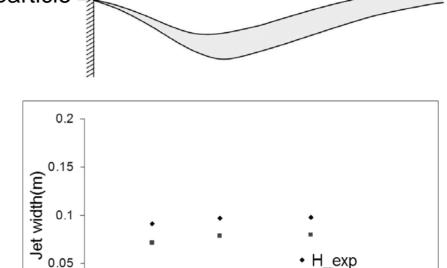
0

0

Horizontal jet in a gas-solid fluidized bed:

- solid particle holdup varies in the radial and axial directions
- particles entrain into the jet
- momentum is transferred from the jet to the solid particle
- the closure of the jet is due to the momentum loss





H model

0.15

0.1

 $\varepsilon_{\alpha} = 0$

Bulk ε_s^0 u = 0

Gas Core

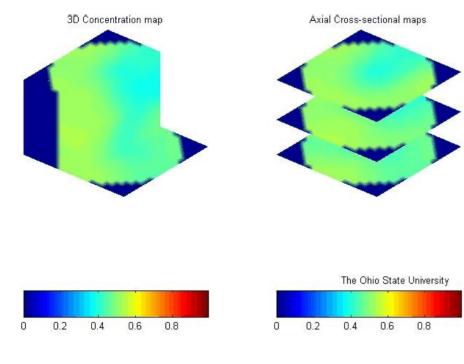
Boundary Layer $\varepsilon_s = \varepsilon_s^0$

Comparison of the maximum penetration lengths of the horizontal gas jet obtained by ECVT experiments and model prediction for the 0.3 m gas-solid fluidized bed

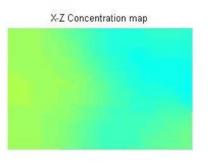
Comparison of the maximum width of the horizontal gas jet obtained by ECVT experiments and model prediction for the 0.3 m gas-solid fluidized bed

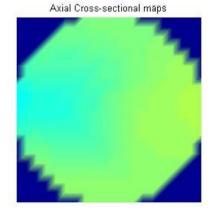
Ug(m/s)

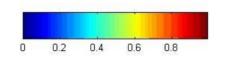
0.05

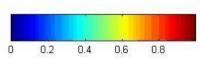


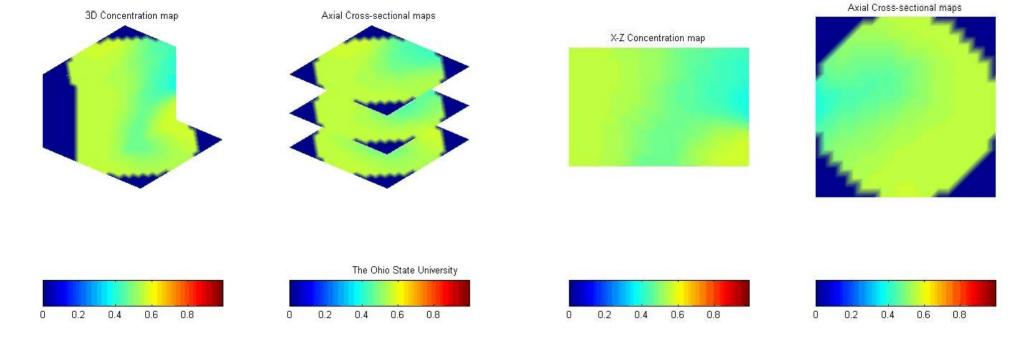
Superficial gas velocity: Ug=0.108 m/s Side gas velocity: Ug_side=15.5 m/s Side solids velocity: Us_side=0



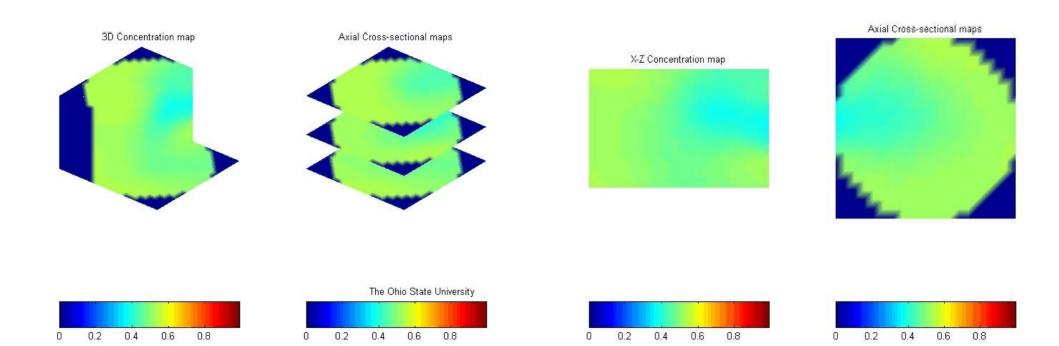






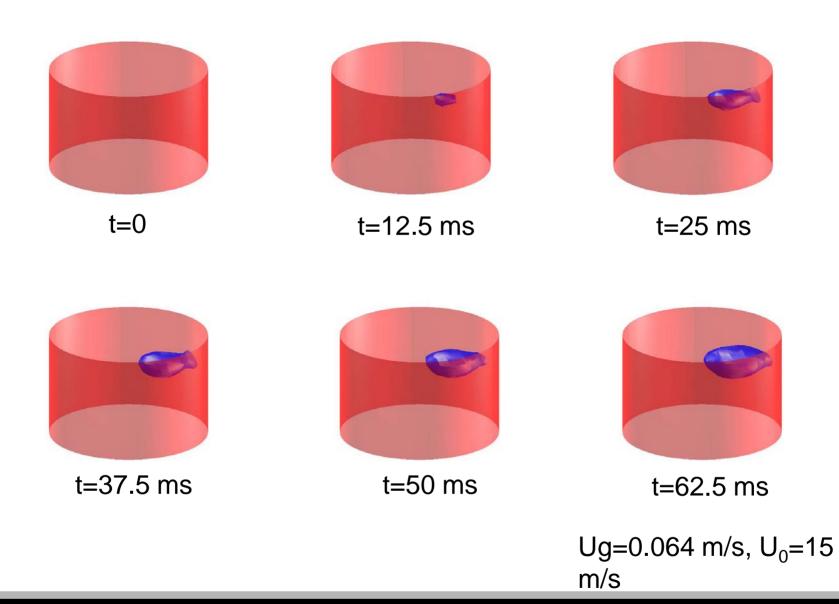


Superficial gas velocity: Ug=0.032 m/s; Side gas velocity: Ug_side=15.5 m/s; Side solids velocity: Us_side=0 Superficial gas velocity: Ug=0.032 m/s; Side gas velocity: Ug_side=16.3 m/s; Side solids velocity: Us_side=16.3 m/s

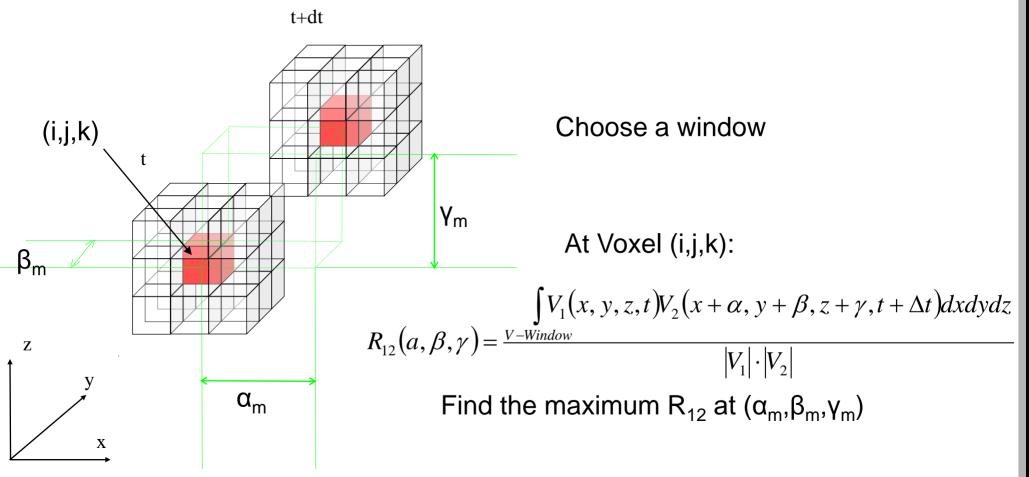


Jet shape from ECVT images

(Maximum jet penetration)

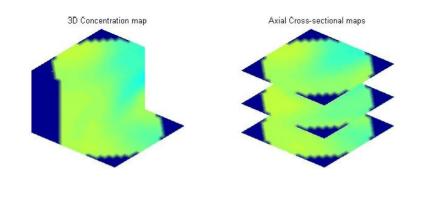


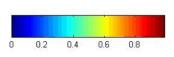
4. Velocimetry



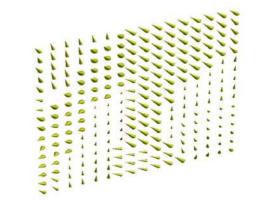
Voxel volume averaged phase velocity at Voxel (i,j,k):

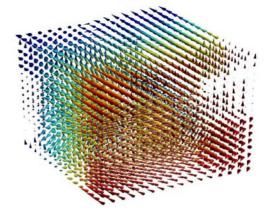
$$v_x = \frac{\alpha_m - i}{\Delta t} \Delta x$$
 $v_y = \frac{\beta_m - j}{\Delta t} \Delta y$ $v_z = \frac{\gamma_m - k}{\Delta t} \Delta z$





		The Ohio State University				
0	0.2	0.4	0.6	0.8		

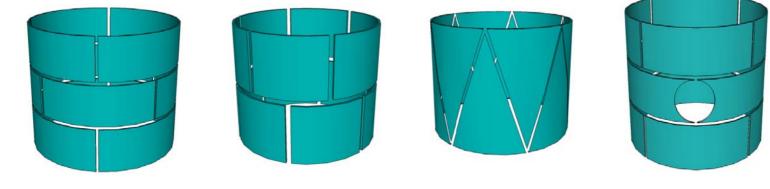




Ug=0.064 m/s, U₀=15 m/s

5. ECVT Sensor Applications

Cylindrical shape sensor

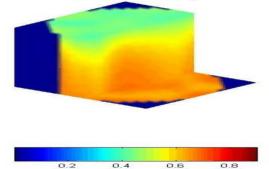








3D Concentration map

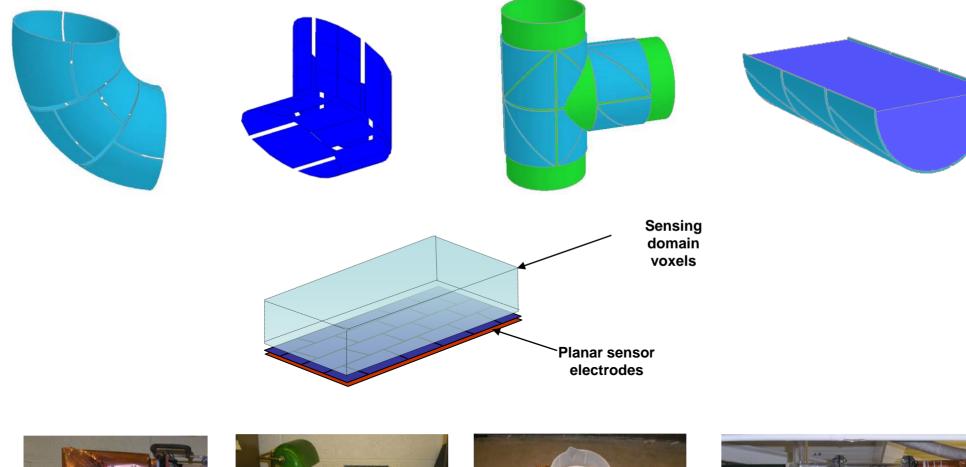


Axial Cross-sectional maps

SCR12-25

ECVT sensor design

Sensors with complex geometries











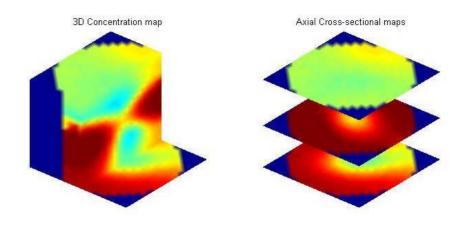
ECVT sensor design

Comparison of different sensor geometries in terms of symmetry, axial resolution and radial resolution

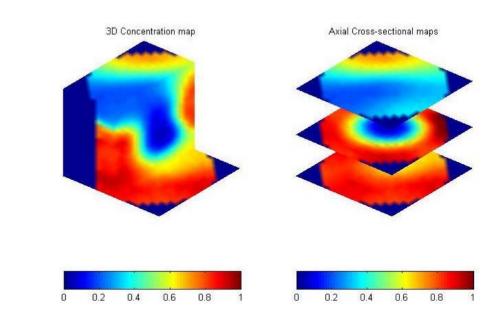
Sensor Type	Sensor Symmetry	Axial Resolution	Radial Resolution
Cylindrical sensor with 1 layer	High	Low, sensitivity decreases toward center.	High, sensitivity decreases toward center.
Cylindrical sensor with 2 shifted layers	Moderate	Moderate, sensitivity decreases toward center.	Moderate, sensitivity decreases toward center
Cylindrical sensor with 3 shifted layers	Moderate	High, sensitivity decreases toward center.	Moderate-High, sensitivity decreases toward center.
Planar sensor with shifted planes	Moderate	Low, sensitivity decreases away from sensor.	High, Sensitivity decreases away from sensor.
Bent sensor	Low	Depends on sensor plate arrangement	Depends on sensor plates arrangement

Fei Wang, Qussai Marashdeh, Liang-Shih Fan * and Warsito Warsito "Electrical Capacitance Volume Tomography: Design and Applications" *Sensors* **2010**, *10*, 1890-1917;

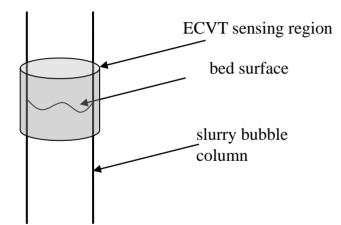
Surface of Slurry Bubble Columns







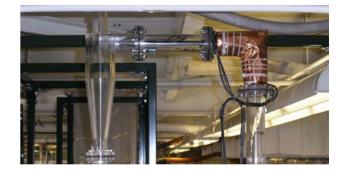
Snapshots of bubble bursting at the surface of a slurry bubble column by ECVT: (a) 3D image before bubble bursting; (b) 3D image after bubble bursting



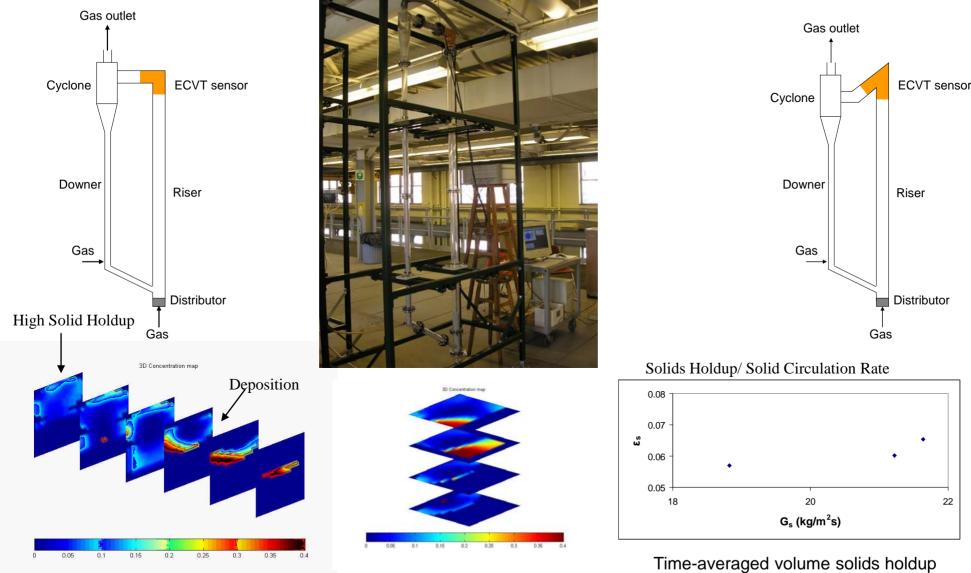
6. Complex Geometries Examples





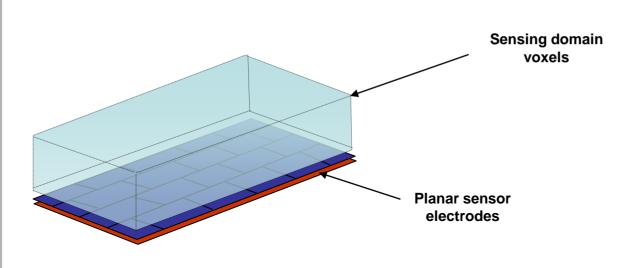


3-D gas-solid flow patterns in the exit region of a gas-solid CFB riser



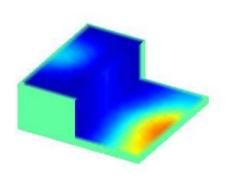
Solids holdup distribution in the bend of the CFB riser at Ug=1.36 m/s and Gs=21.2 kg/m²s:vertical slices and horizontal slices

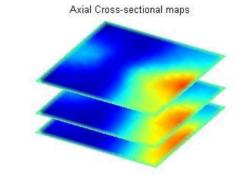
Time-averaged volume solids holdup at the top wall region at the start of the horizontal duct of the bend at Ug=1.16 m/s

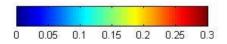


3D Concentration map







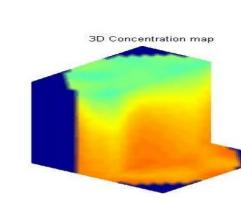


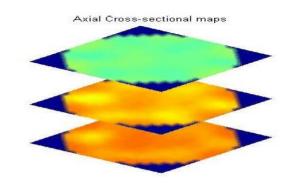
Scale-Up ECVT Sensors

60 inch ID \rightarrow



←12 inch ID







SCR12-25

Concluding Remarks

 ECVT is a non-invasive imaging technology that can be applied to image processes vessels of various diameters.

 ECVT is a unique imaging technology with its potential for commercial scale-up

 Tech4Imaging LLC is developing a commercial ECVT system for imaging multi-phase flow systems.

Acknowledgement

- The support of US. Department of Energy under Grant # DE-NT0006564 is gratefully acknowledged
- Dr. W. Warsito, Dr. Bing Du, Dr. Zhao Yu, and all students who worked or are working on ECVT technology are also acknowledged.

