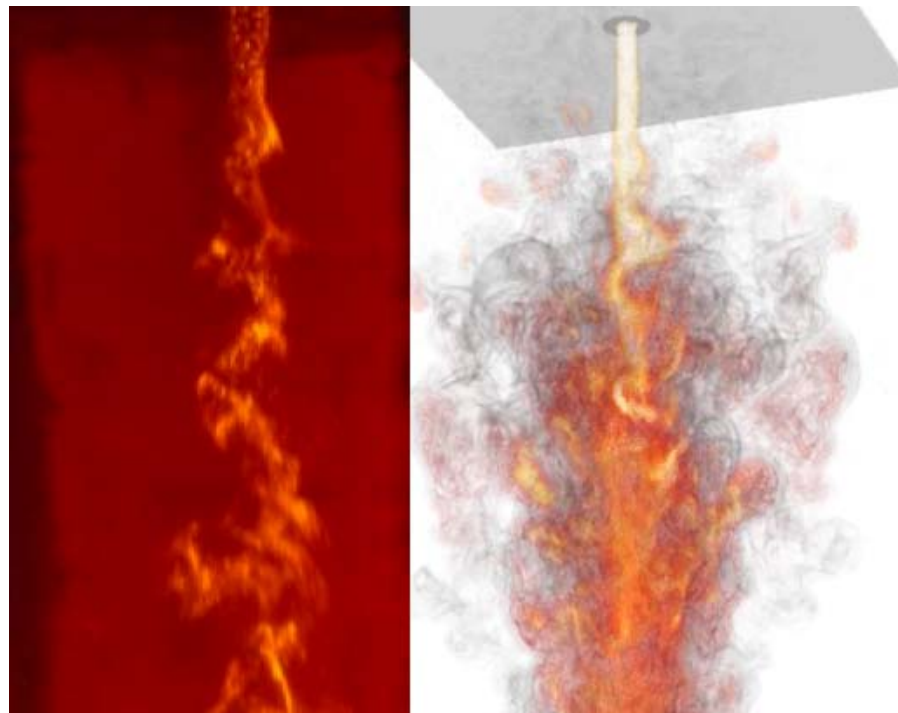




Simulation of Coal Gasification Using Large Eddy Simulation & Direct Quadrature Method of Moments



Charles M. Reid, Jeremy N. Thornock,
Philip J. Smith

Institute for Clean and Secure Energy
Chemical Engineering Department, University of Utah

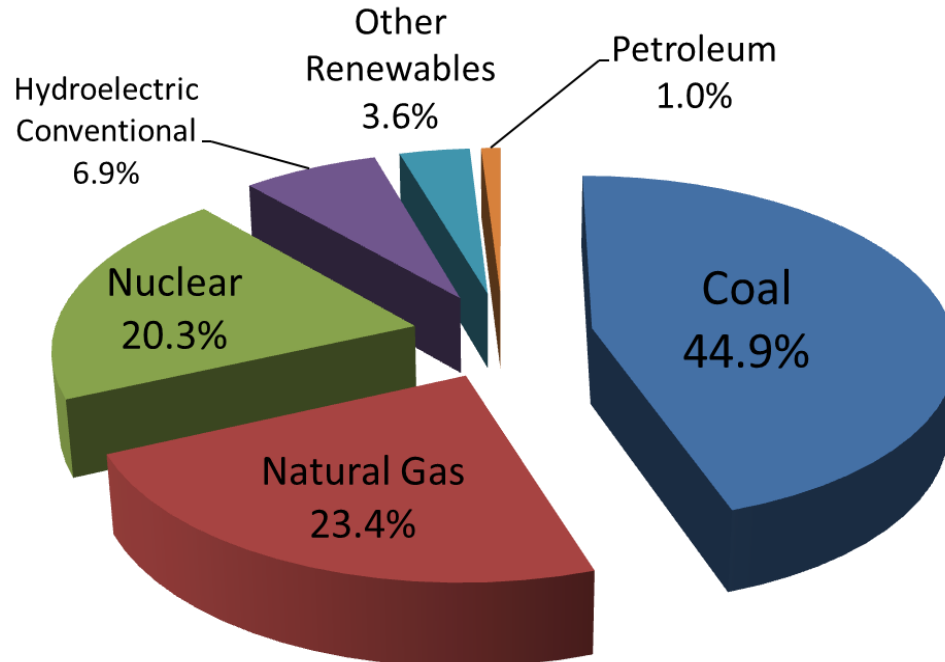




Motivation



2009 U.S. Electricity Generation by Source





Motivation

- U.S. has biggest coal reserves in the world
- 28% of the world's coal!
- Energy has big implications:
 - Environmental
 - Economic
 - Geopolitical
 - Social & Health





Motivation

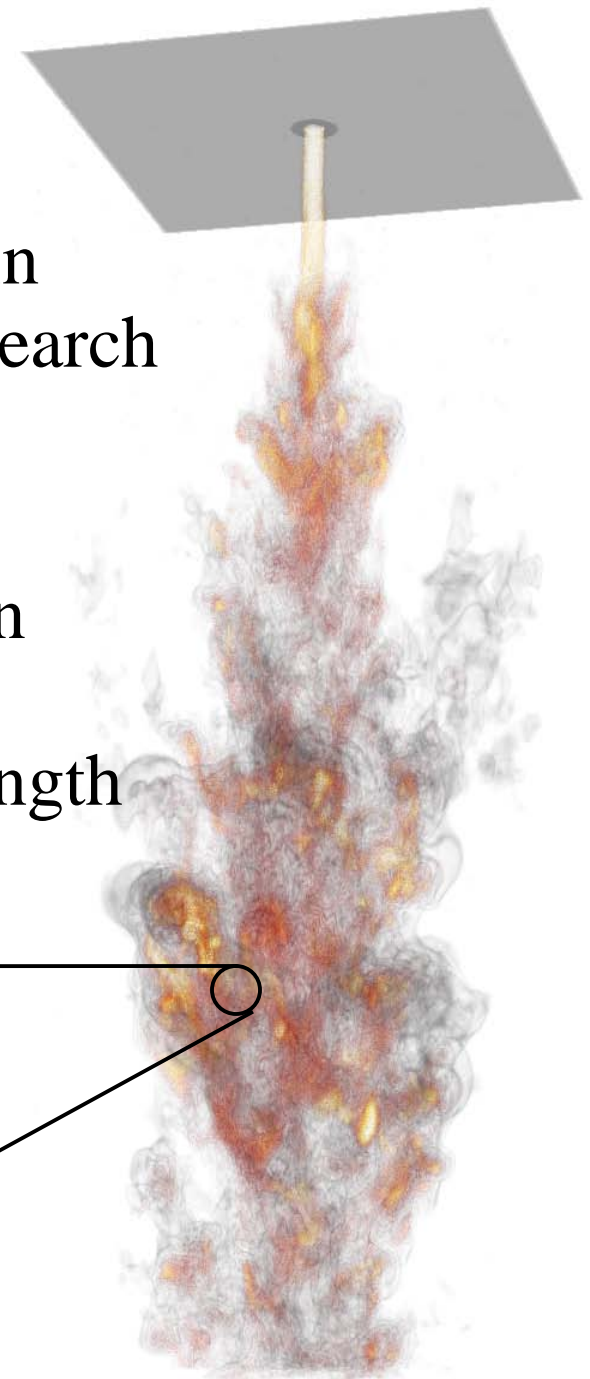
- Increasing environmental scrutiny
- Greenhouse gases
- Industry has a need for:
 - Retrofit of existing plants
 - Evaluation of new technology





Simulation

- Simulation - has potential to join experiments and theory as a research methodology
- Large-scale simulation tools can tackle difficult multi-physics problems with wide range of length and time scales





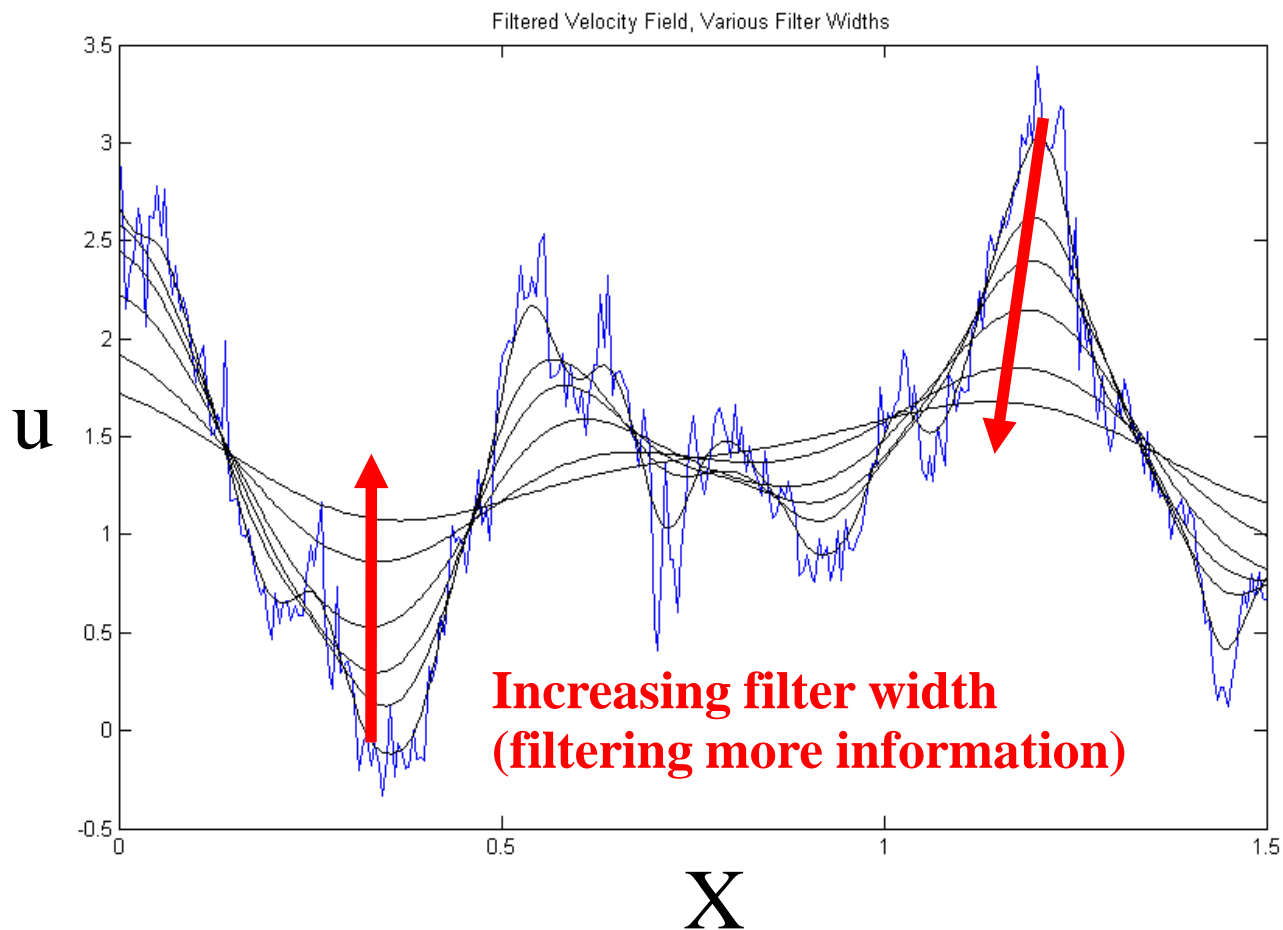
Outline/Overview

- Large eddy simulation (LES)
- Solid-Phase Models
 - Direct quadrature method of moments (DQMOM)
- Application to coal gasification
- Results & Discussion
- Conclusions



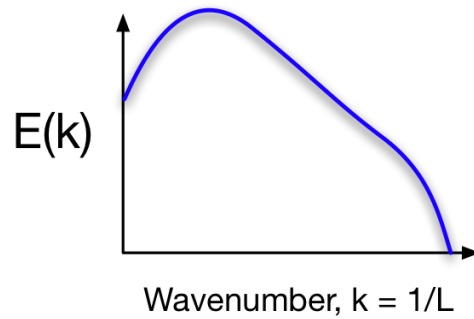
Large Eddy Simulation

- Low-pass filtering: spatial averaging

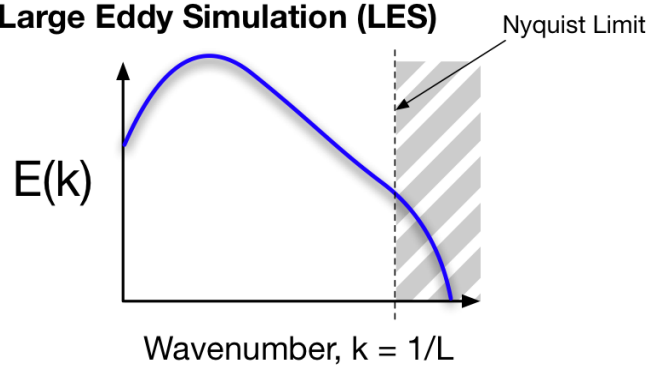




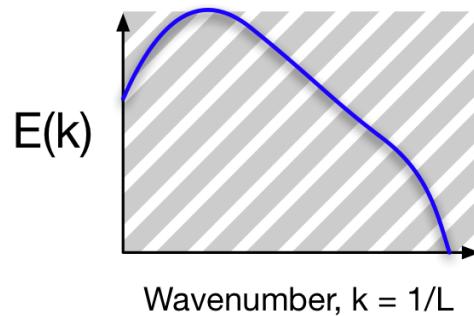
(a) **Direct Numerical Simulation (DNS)**



(b) **Large Eddy Simulation (LES)**



(c) **Reynolds-Averaged Navier Stokes (RANS)**

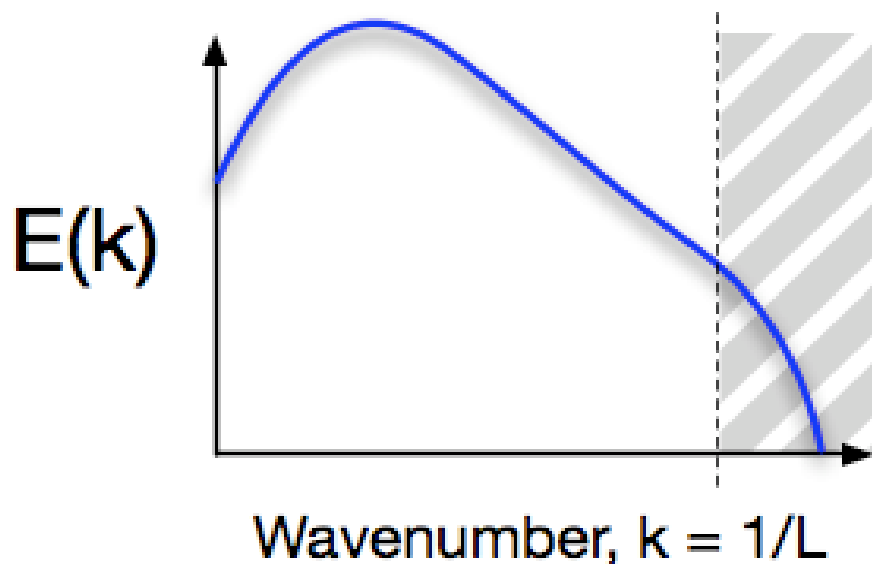


 = Modeled  = Resolved



Large Eddy Simulation

Scalar/Particle Energy Spectrum



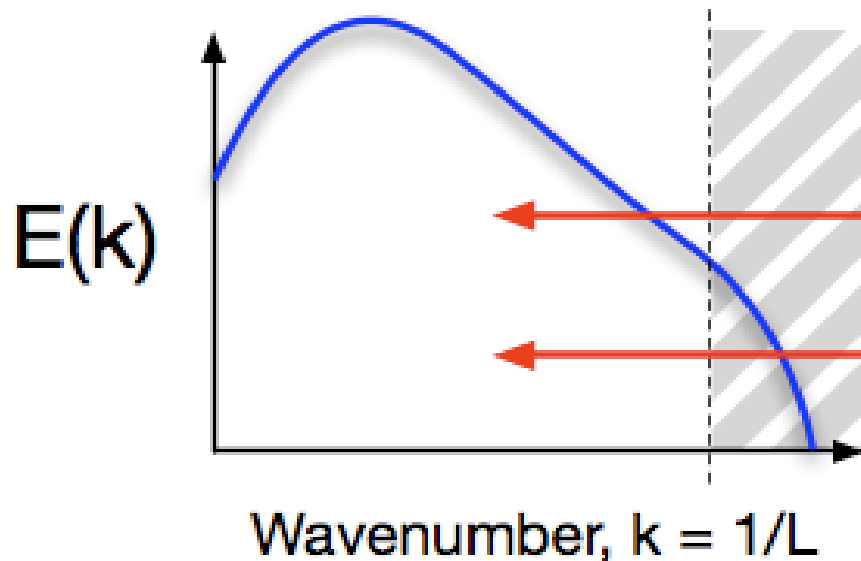
$$Da = \frac{\tau_{mixing}}{\tau_{reaction}}$$

$$St = \frac{\tau_{particle}}{\tau_{fluid}}$$



Large Eddy Simulation

Scalar/Particle Energy Spectrum



Decreasing
Damköhler Number

Increasing
Stokes Number

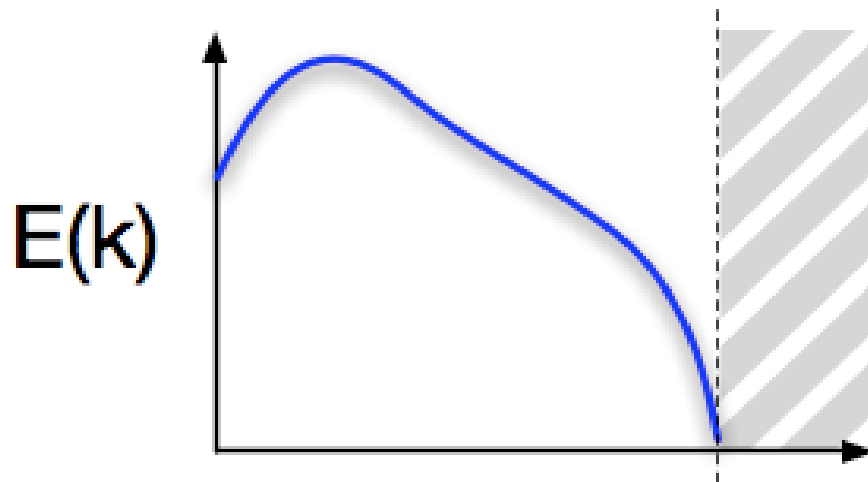
$$Da = \frac{\tau_{mixing}}{\tau_{reaction}}$$

$$St = \frac{\tau_{particle}}{\tau_{fluid}}$$



Large Eddy Simulation

Scalar/Particle Energy Spectrum



Wavenumber, $k = 1/L$

$\left\{ \begin{array}{l} \text{if } \tau_{\text{eddy crossover}} < \tau_{\text{eddy lifetime}} \\ \text{else} \end{array} \right.$

Damköhler Nyquist Limit:

$$\Delta \lesssim Da^{-\frac{1}{2}} Sc^{-\frac{3}{4}} \eta$$

Stokes Nyquist Limit:

$$\Delta \lesssim \left(\frac{\tau_p \nu}{St} \right)^{1/2}$$

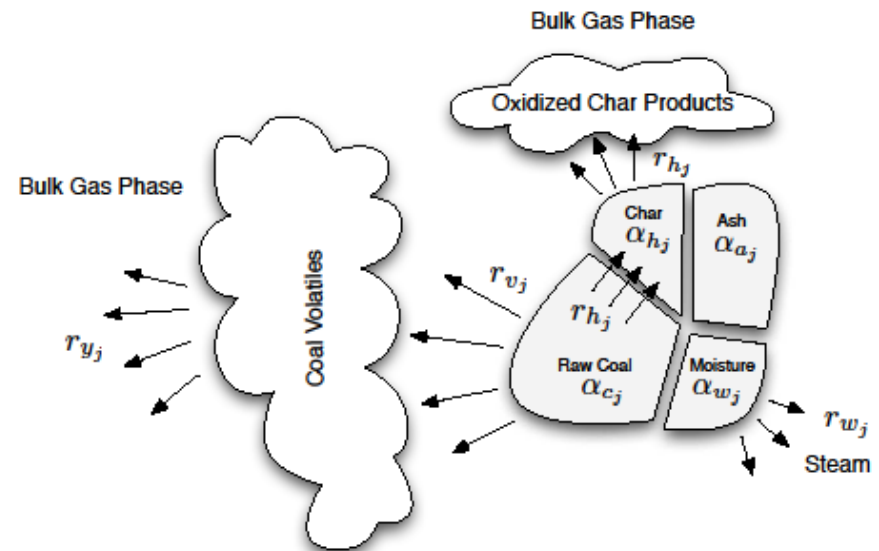
$$\Delta \lesssim \frac{\tau_p^2 g}{St}$$



Solid Phase Models

- Characterization of particles:
- Internal coordinates = particle independent variables
(Denoted ξ)

- Lagrangian models
- Eulerian models





Solid Phase Models

- Lagrangian: ODEs

$$\frac{d\mathbf{x}}{dt} = S_{\mathbf{x}} \qquad \frac{d\xi}{dt} = S_{\xi}$$

- Eulerian: NDF transport equation

$$\frac{\partial f(\xi; \mathbf{x}, t)}{\partial t} + \frac{\partial}{\partial x_i} (\langle u_i | \xi \rangle f(\xi; \mathbf{x}, t)) + \sum_{j=1}^{N_{\xi}} \frac{\partial}{\partial \xi_j} (\langle G_j | \xi \rangle f(\xi; \mathbf{x}, t)) = h(\xi; \mathbf{x}, t)$$

$$u_i = \frac{dx_i}{dt}$$

$$G_j = \frac{d\xi_j}{dt}$$



Solid Phase Models

- Lagrangian: ODEs

$$\frac{d\mathbf{x}}{dt} = S_{\mathbf{x}}$$

$$\frac{d\xi}{dt} = S_{\xi}$$

- Eulerian: NDF transport equation

$$\frac{\partial f(\xi; \mathbf{x}, t)}{\partial t} + \frac{\partial}{\partial x_i} (\langle u_i | \xi \rangle f(\xi; \mathbf{x}, t)) + \sum_{j=1}^{N_{\xi}} \frac{\partial}{\partial \xi_j} (\langle G_j | \xi \rangle f(\xi; \mathbf{x}, t)) = h(\xi; \mathbf{x}, t)$$

$$u_i = \frac{dx_i}{dt}$$

$$G_j = \frac{d\xi_j}{dt}$$

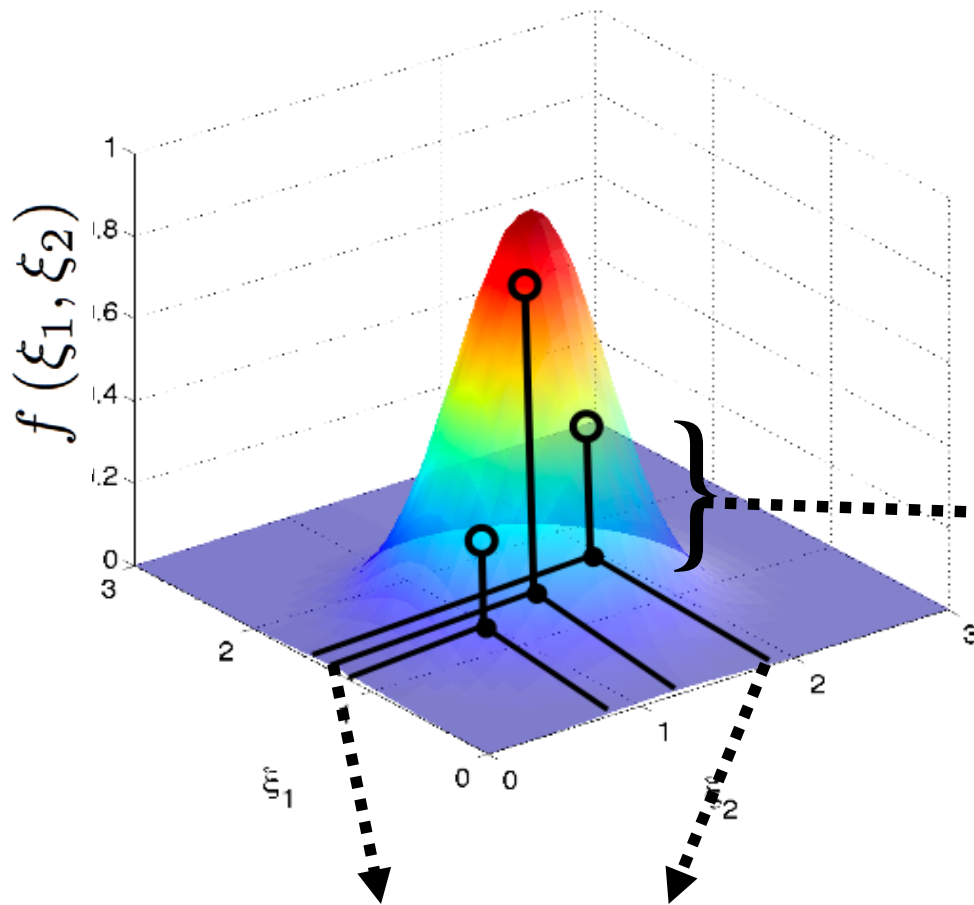


Moment Methods

- Moment definition: $m_k = \int_{-\infty}^{+\infty} \xi^k f(\xi) d\xi$
- Multi-fluid method
 - Solids = "fluid" phase
 - Zeroth, first moments
 - What about adding another "fluid" phase?
- Multi-environment models



Direct Quadrature Method of Moments (DQMOM)



Abscissas (i.e. what values of ξ
the particles have)

Weights
(i.e. how many
particles are in
that environment)



Direct Quadrature Method of Moments (DQMOM)

- Weight/weighted abscissa transport equations

$$\frac{\partial w_\alpha}{\partial t} + \frac{\partial}{\partial x_i} (\langle u_i | \boldsymbol{\xi} \rangle w_\alpha) = a_\alpha$$
$$\frac{\partial s_{j,\alpha}}{\partial t} + \frac{\partial}{\partial x_i} (\langle u_i | \boldsymbol{\xi} \rangle s_{j,\alpha}) = b_{j,\alpha}$$

- Source terms come from solution to linear system

$$\mathbf{Ax}=\mathbf{B}$$

- Linear system comes from moment transform of NDF transport equation



DQMOM Implementation

- Numerical issues solving $Ax=B$
 - Abscissas overlapping
 - Linearly dependent moments
 - Small weights
 - Large values of $G_j = \frac{d\xi_j}{dt}$
- For > 2 environments, A always ill-conditioned (condition number $\sim 10^{16}$)
- Contamination of one cell means contamination of all cells
- LU solvers, QR solvers, SVD solvers, Lapack solvers, Numerical Recipes solvers.....



Optimized Moments Approach

- Professor Rodney Fox, "Optimal Moment Sets for Multivariate DQMOM", Ind. Chem. Eng. 2009.
- Replace abscissas in moment transform terms with optimal abscissas (star script)
- Because moment transform is linear, linear transform matrix (M^*) can be factored out on bot

$$\mathbf{A}\mathbf{x} = \mathbf{B}$$

$$\mathbf{A}(\mathbf{A}^*)^{-1}\mathbf{A}^*\mathbf{x} = \mathbf{B}$$

$$\mathbf{M}^*\mathbf{A}^*\mathbf{x} = \mathbf{M}^*\mathbf{B}^*$$

$$\mathbf{A}^*\mathbf{x} = \mathbf{B}^*.$$



INSTITUTE FOR CLEAN
& SECURE ENERGY

Implementation of DQMOM in Large Eddy Simulation



Arches LES Code

- Finite volume
- 2nd Order Runge-Kutta, Strong Stability-Preserving
- Dynamic local similarity SGS model
- DOM Radiation calculation
- Object-Oriented C++
- Part of the Uintah Computational Framework (UCF)





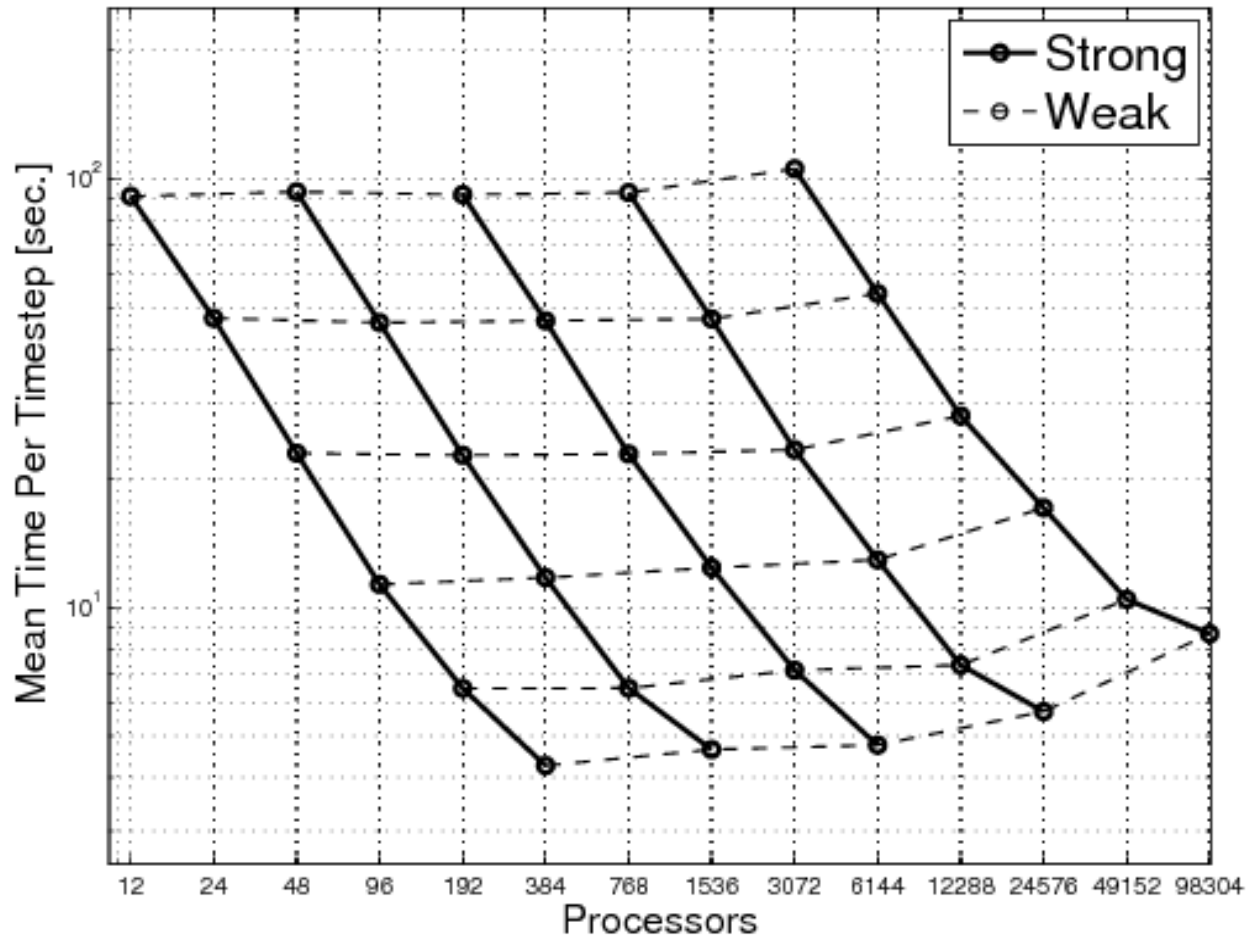
Uintah Framework

- Component-based
- Structured grid
- Load balancing
- Taskgraph to schedule tasks and manage resources/data
- Provides parallelization to thousands of processors



Uintah Framework

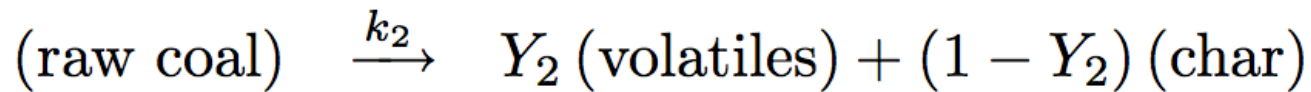
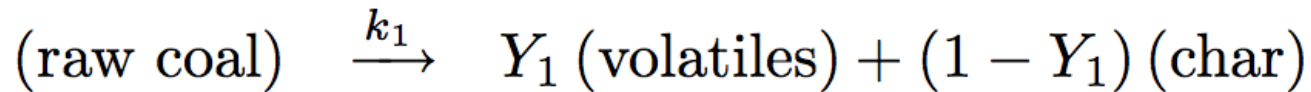
AMR-ICE Scaling





Coal Models

- Equilibrium chemistry
- Kobayashi 2-step devolatilization



$$A_1 = 3.7 \times 10^5 \text{ s}^{-1}$$

$$A_2 = 1.46 \times 10^{13} \text{ s}^{-1}$$

$$E_1 = -17,600 \text{ kcal/kmol} \quad \text{Ubhayakar (1976)}$$

$$E_2 = -60,000 \text{ kcal/kmol}$$

- Particle heat transfer: radiation, convection
 - DOM, 2 ordinates
 - Nusselt # convection model



Coal Models

- Fast equilibrium Eulerian particle velocity model (Balachandar 2008)

$$\frac{(u_{particle} - u_{gas})}{u_k} \approx (1 - \beta) \left(\frac{\tau_{particle}}{\tau_k} \right)^{1/2}$$

$$\beta = \frac{3}{\frac{2\rho_p}{\rho_f} + 1}$$

$\beta = 3$ Buoyant particles (bubbles)

$\beta = 0$ Heavy particles

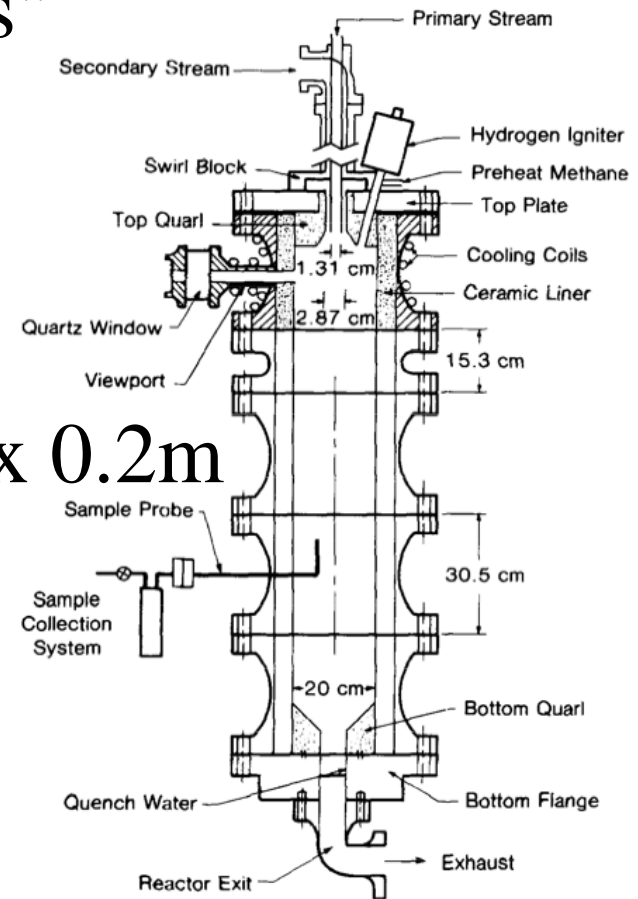


- Soelburg et al. 1984, "Entrained Flow Gasification of Coal 1: Evaluation of Mixing and Reaction Processes"

- Simulation: No walls

- Domain: 0.7m x 0.2m x 0.2m

- 350 x 100 x 100
(resolution of 2 mm)

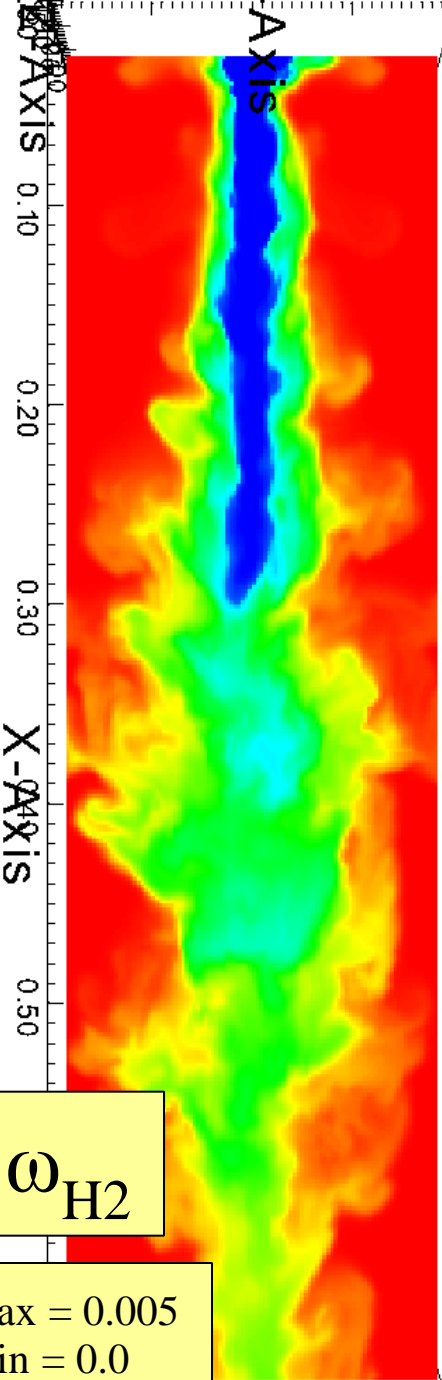




DQMOM + LES

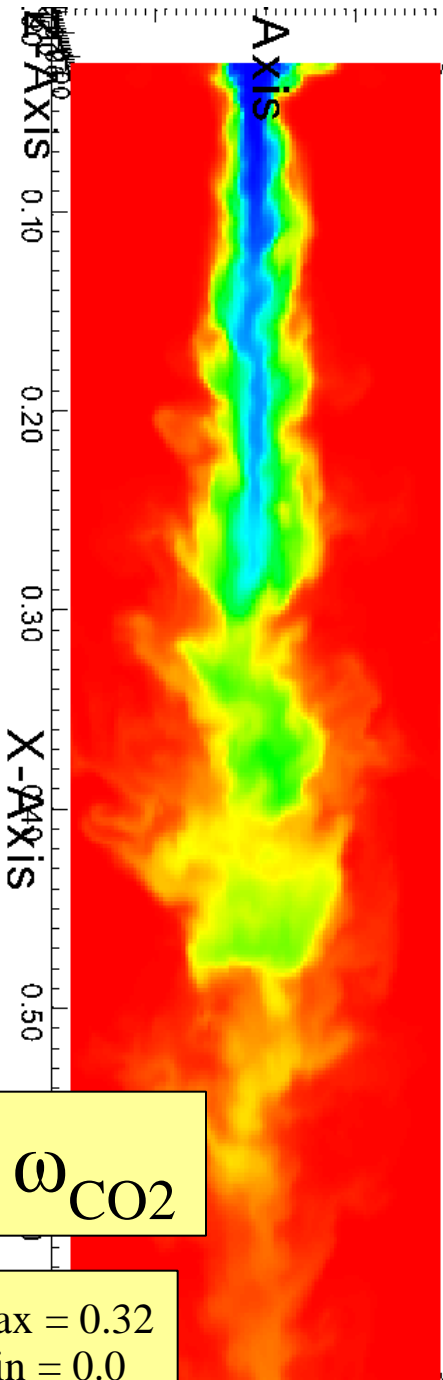
Coal Gasification Results

Max: 2.278e-17
Min: 0.005423



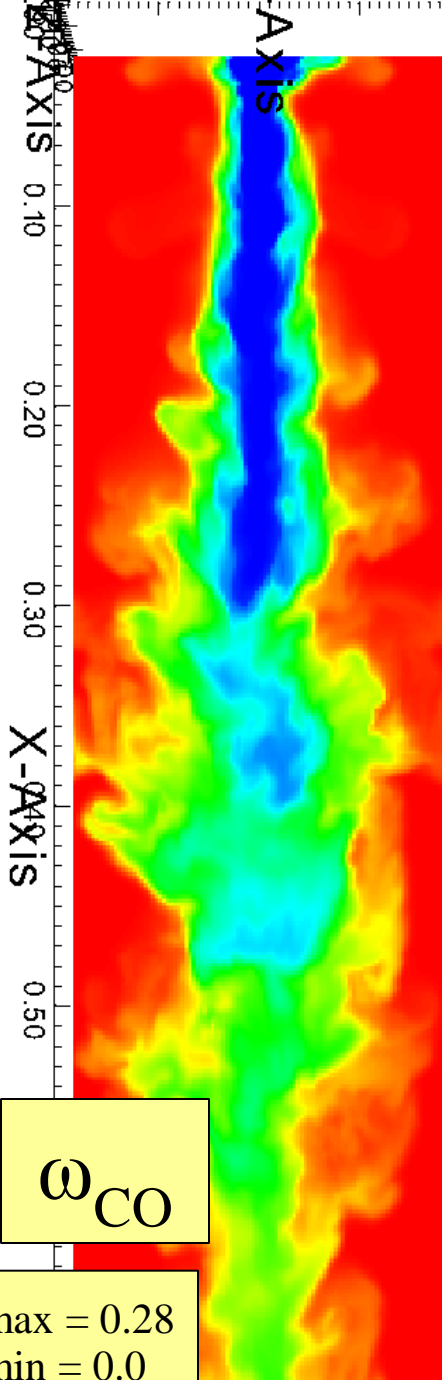
ω_{H_2}
max = 0.005
min = 0.0

Max: 3.855e-06
Min: 3.855e-06



ω_{CO_2}
max = 0.32
min = 0.0

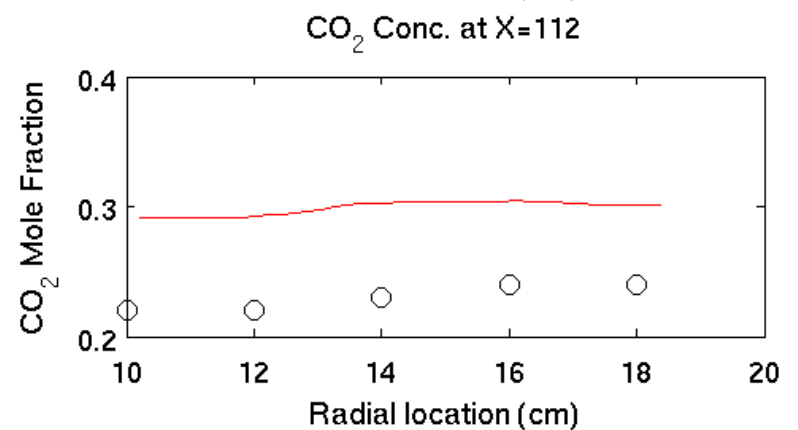
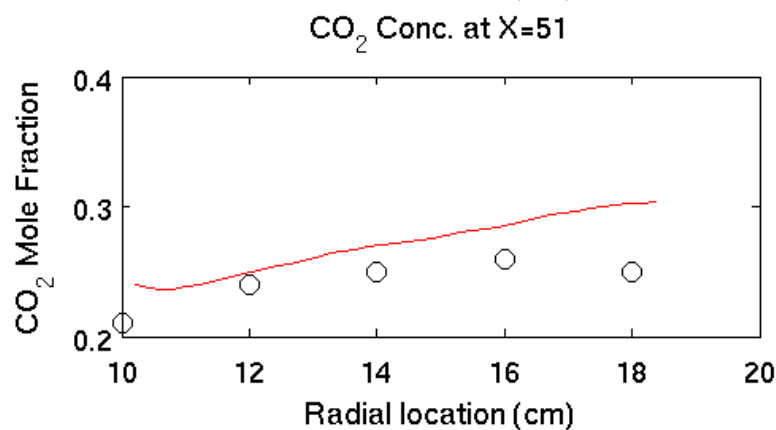
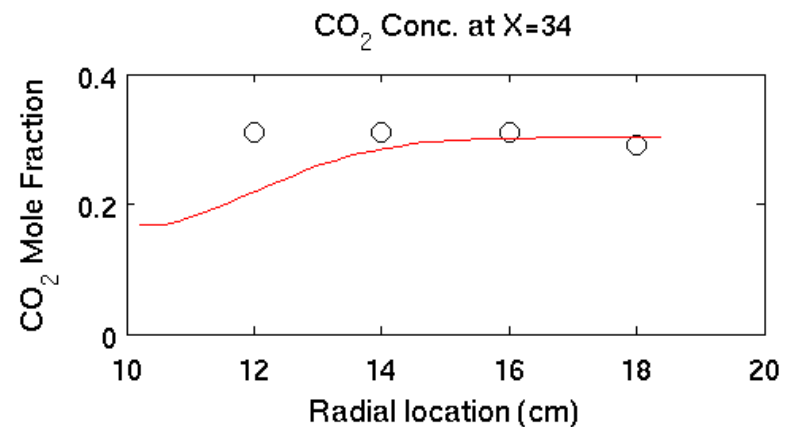
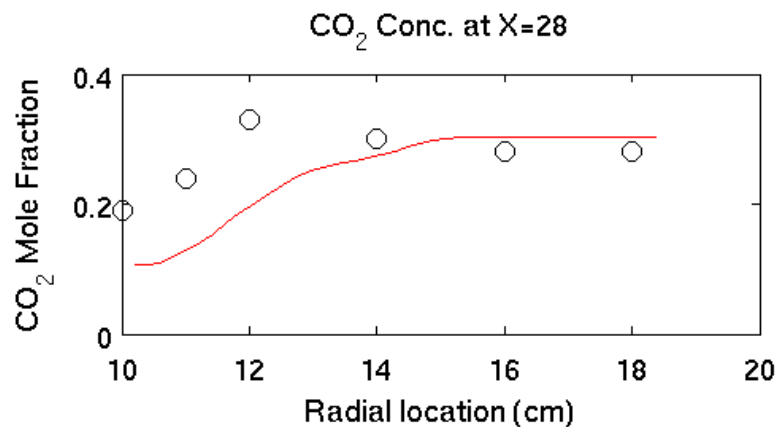
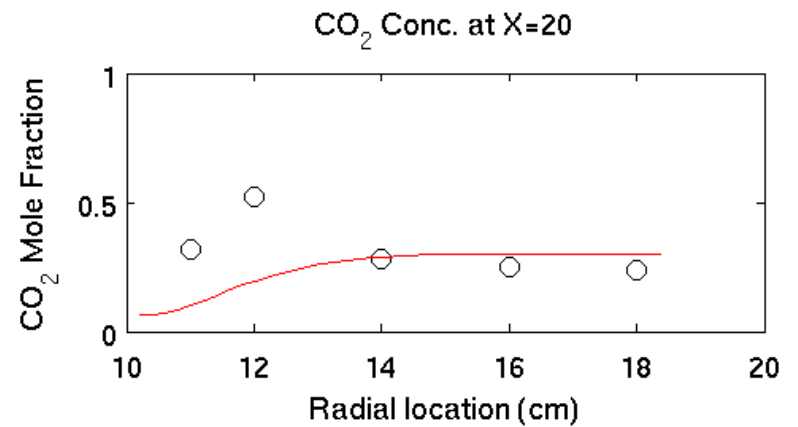
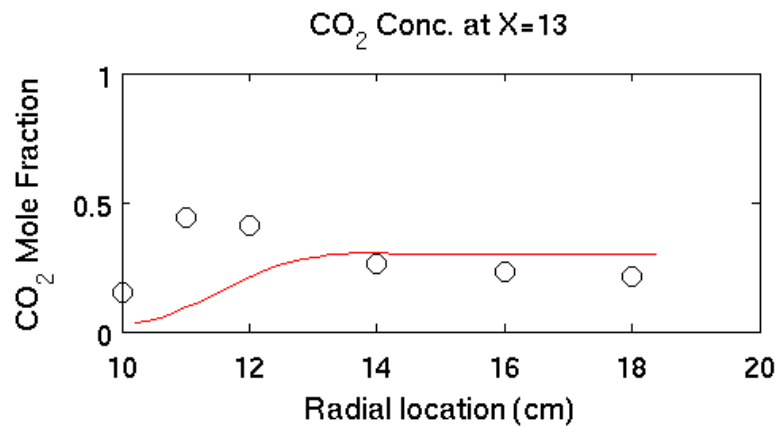
Max: 0.3139
Min: 1.650e-16

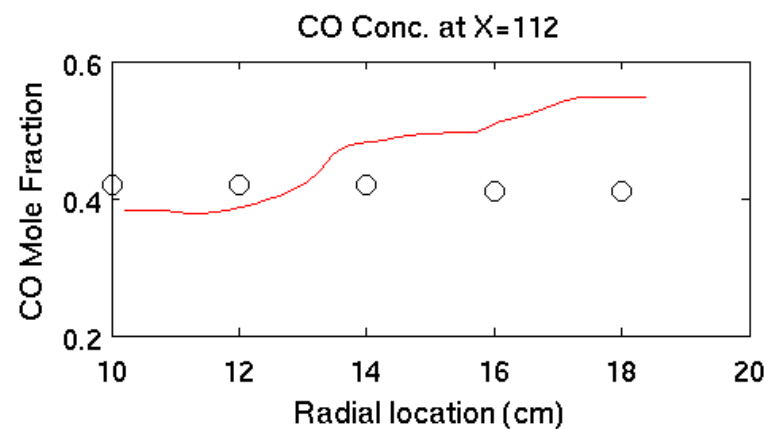
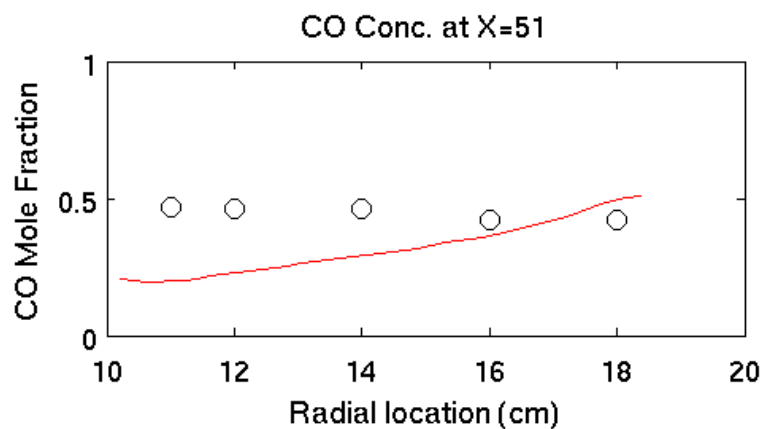
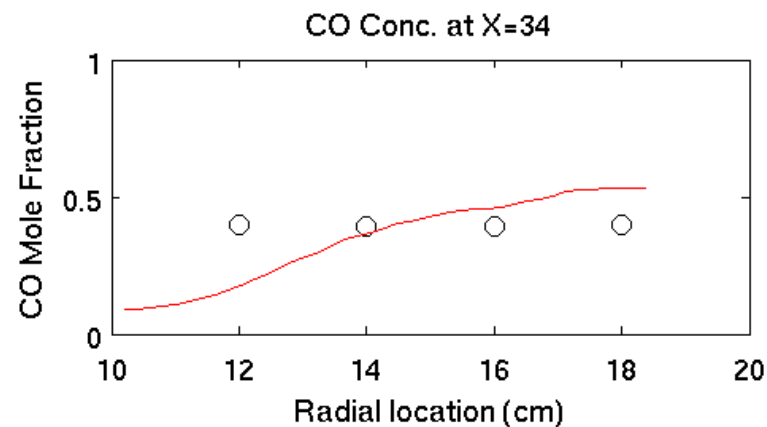
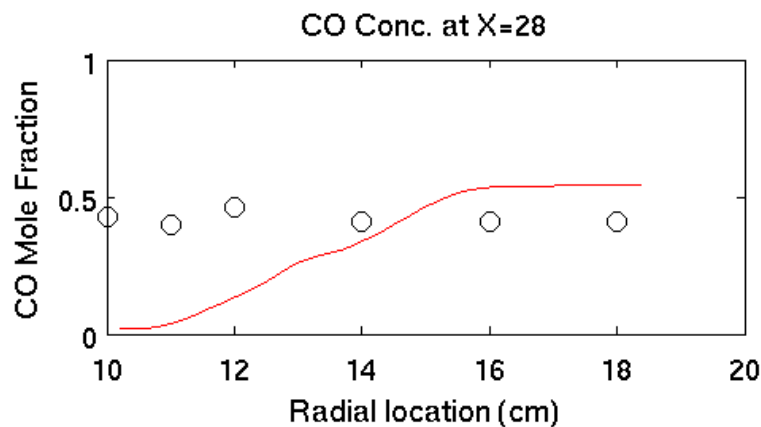
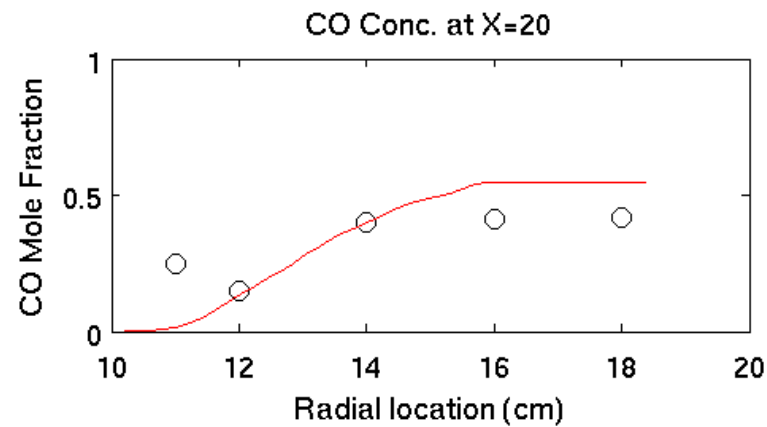
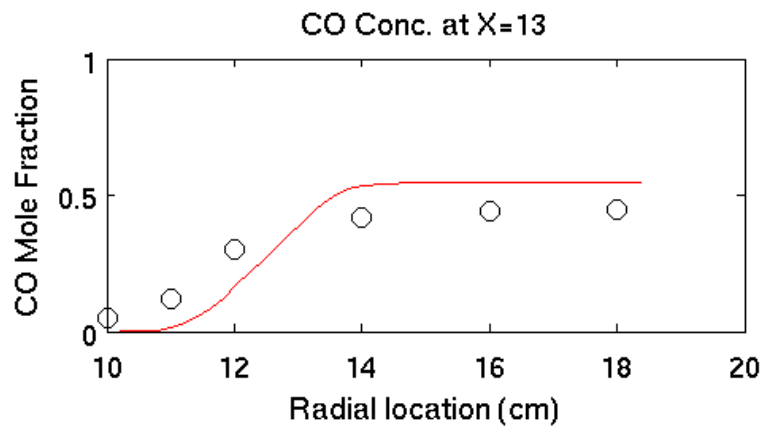


ω_{CO}
max = 0.28
min = 0.0

Max: 0.2792
Min: 1.650e-16

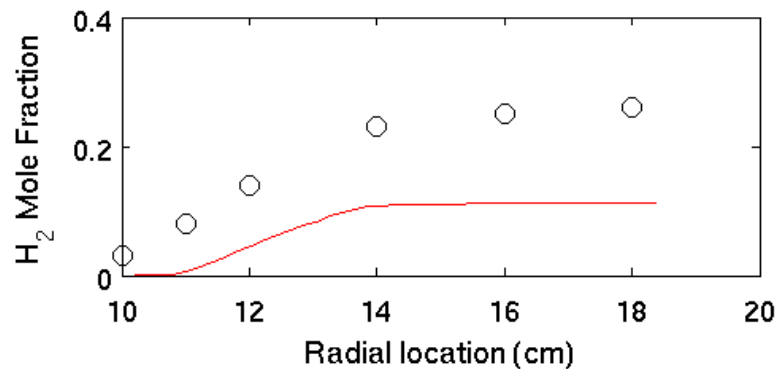




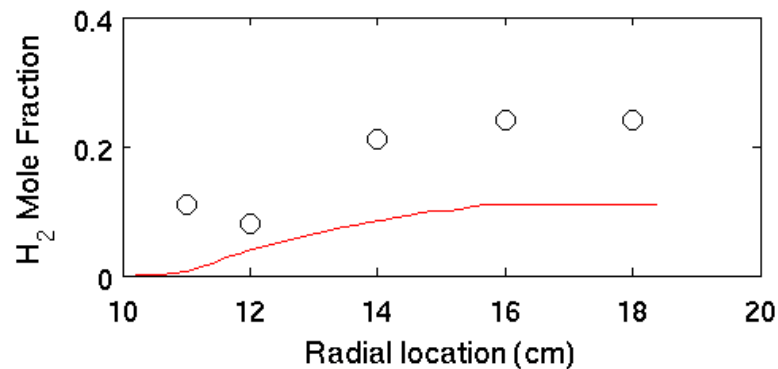




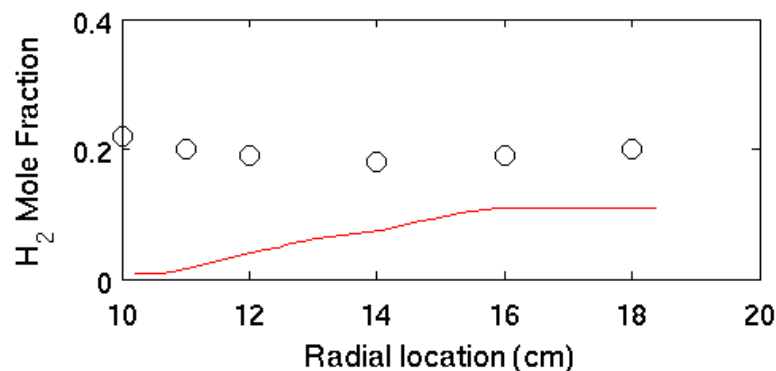
H₂ Conc. at X=13



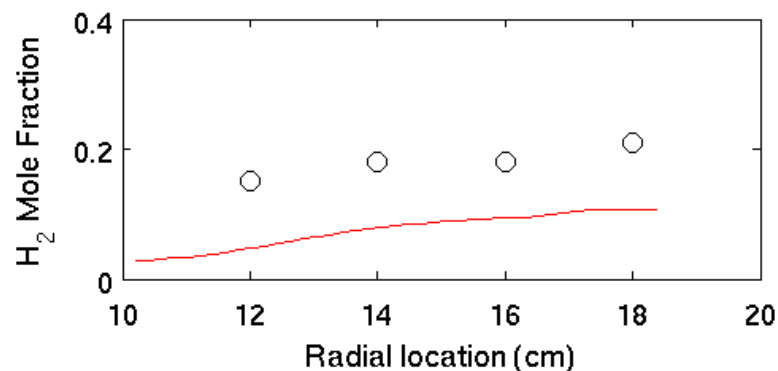
H₂ Conc. at X=20



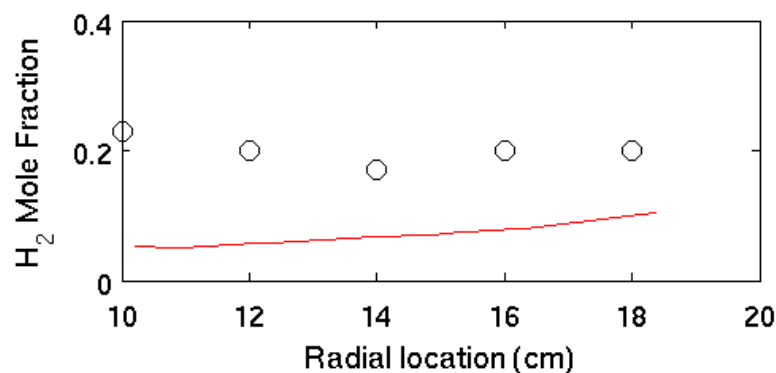
H₂ Conc. at X=28



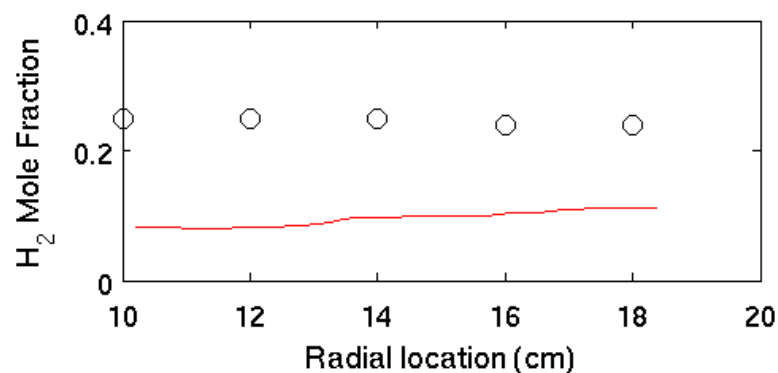
H₂ Conc. at X=34

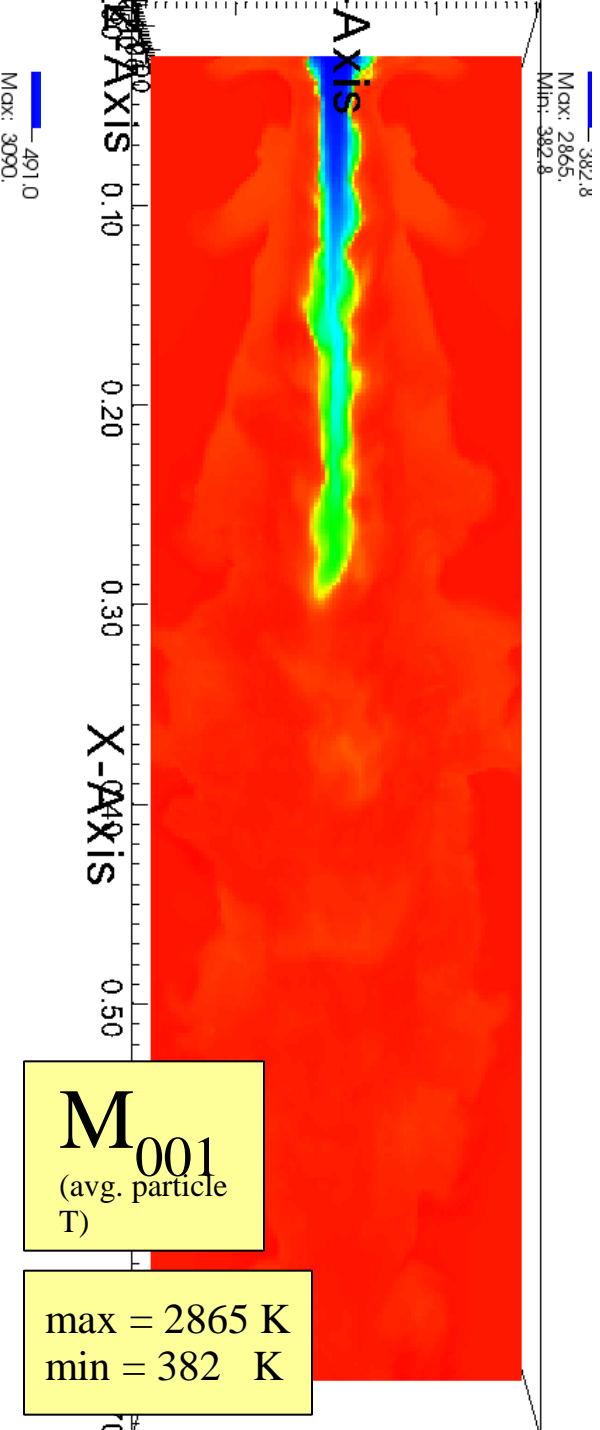
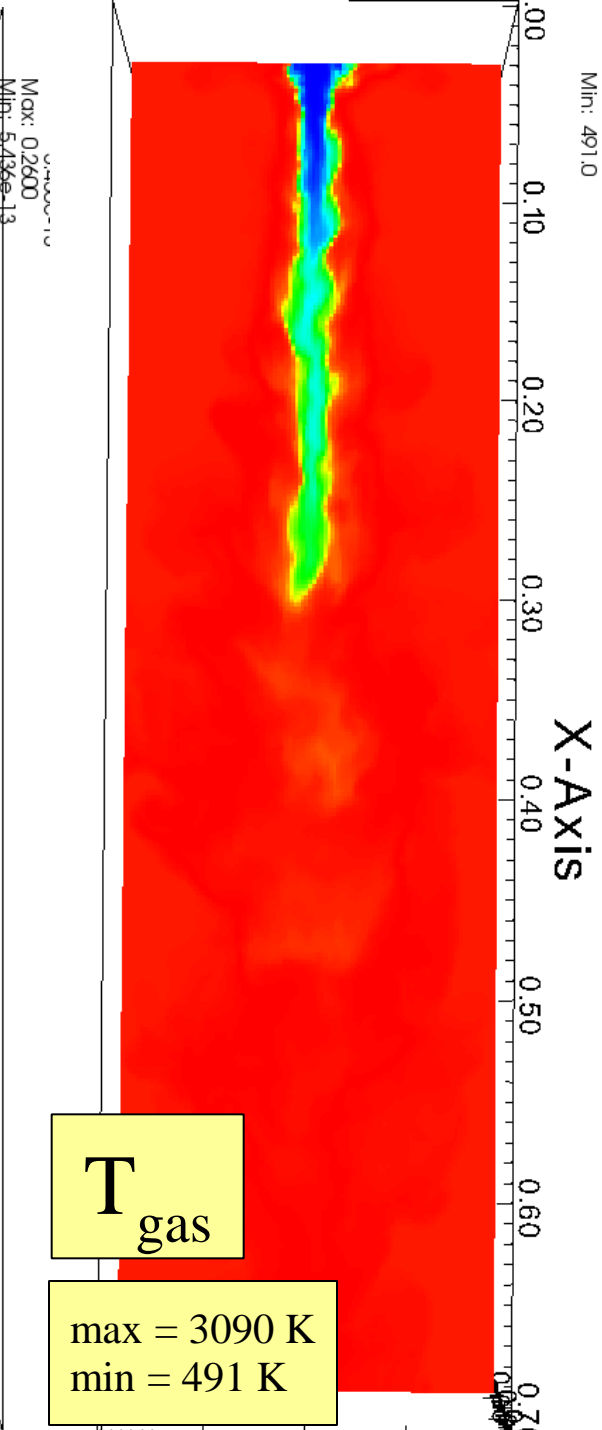
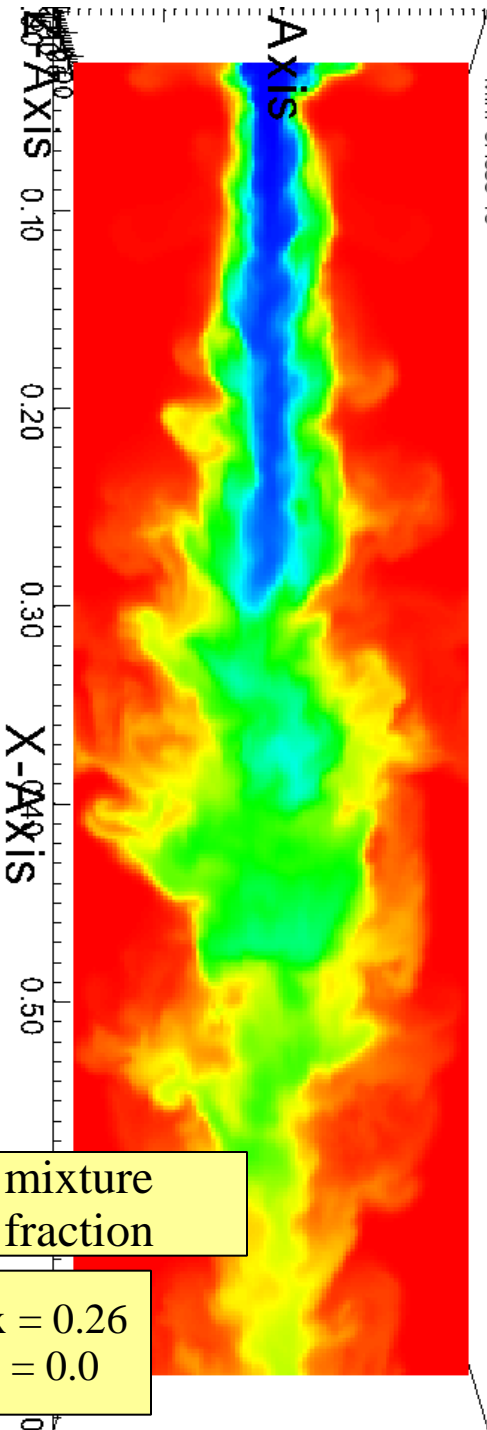


H₂ Conc. at X=51



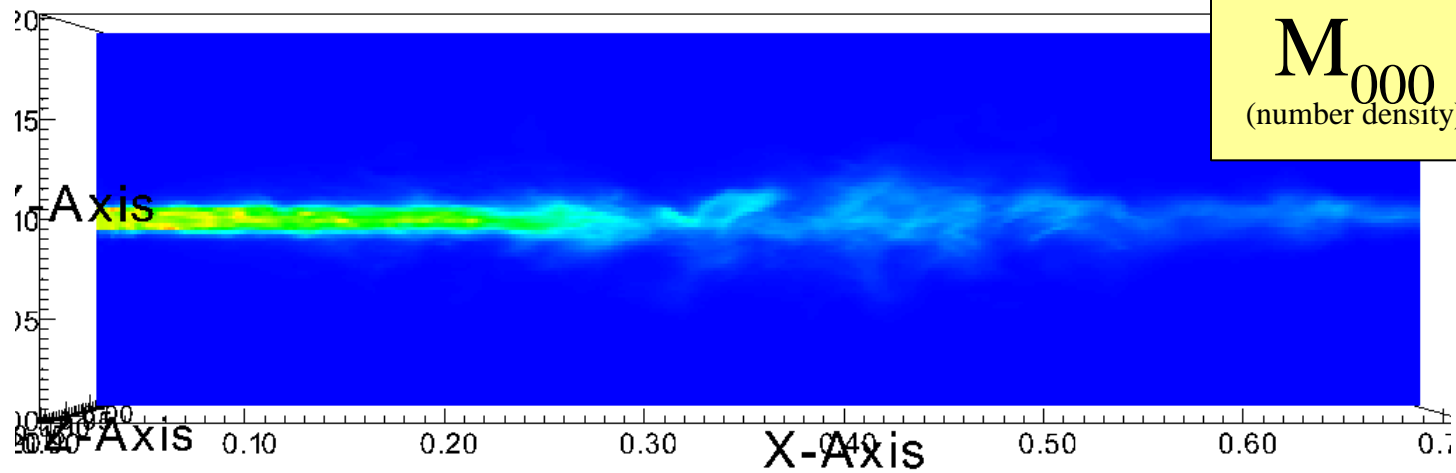
H₂ Conc. at X=112



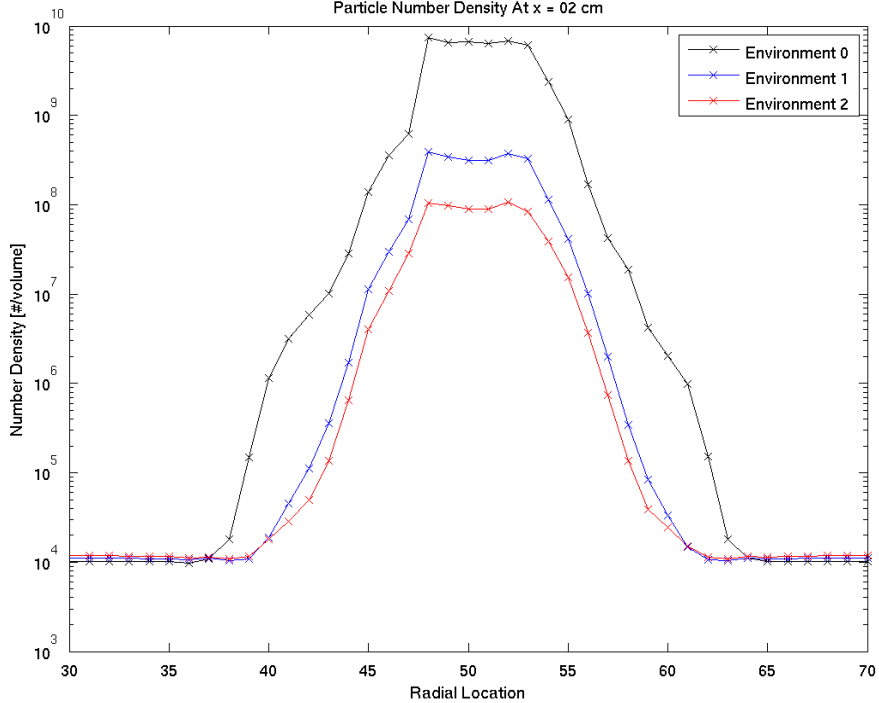




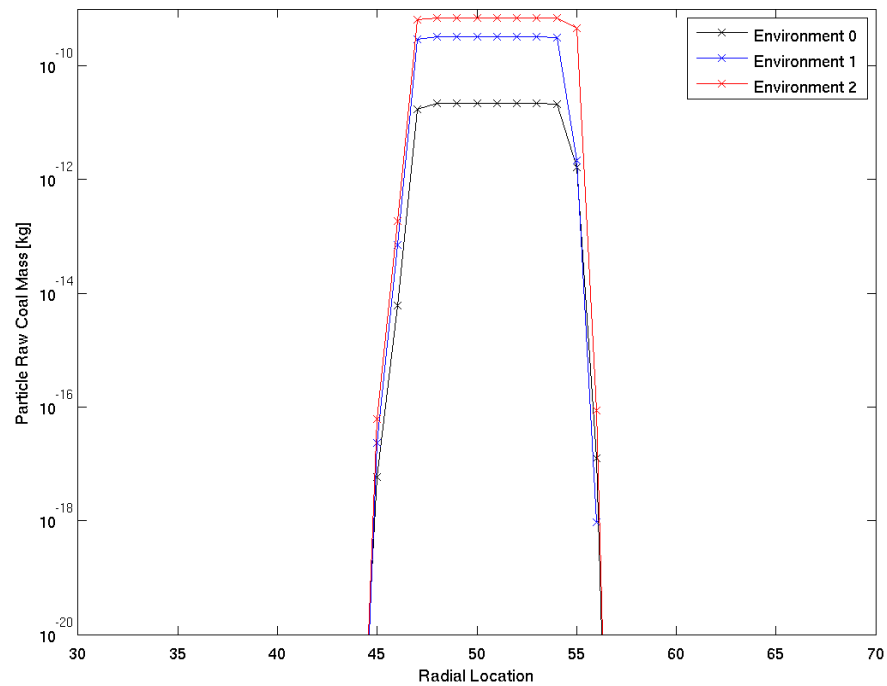
Max: 9.797e+09
Min: 1.525e+04



Particle Number Density At x = 02 cm

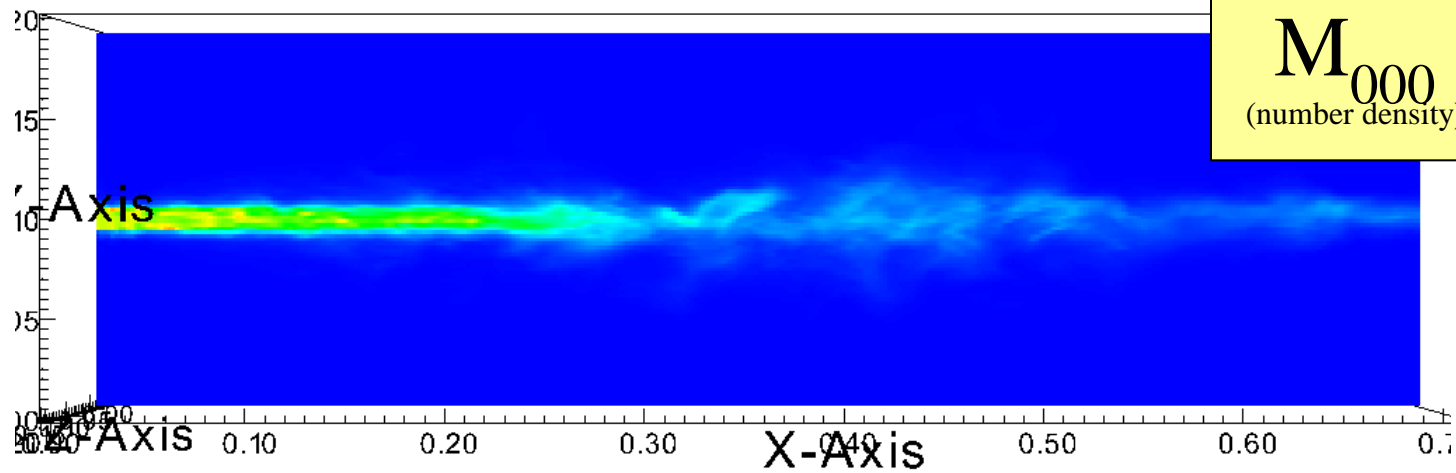


Particle Raw Coal Mass At x = 02 cm

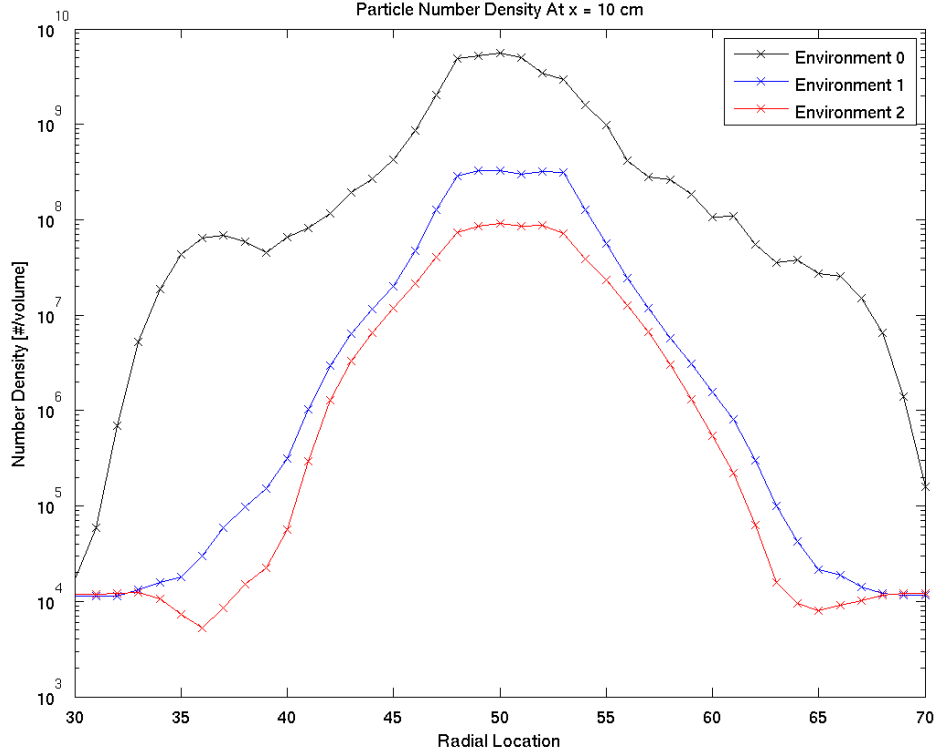




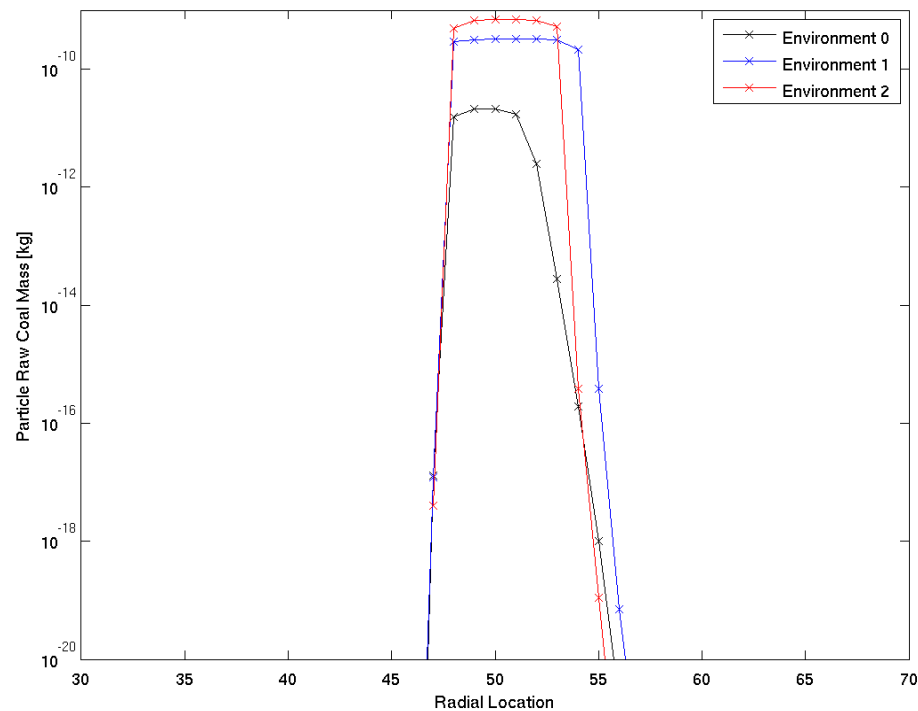
Max: 9.797e+09
Min: 1.525e+04



Particle Number Density At x = 10 cm

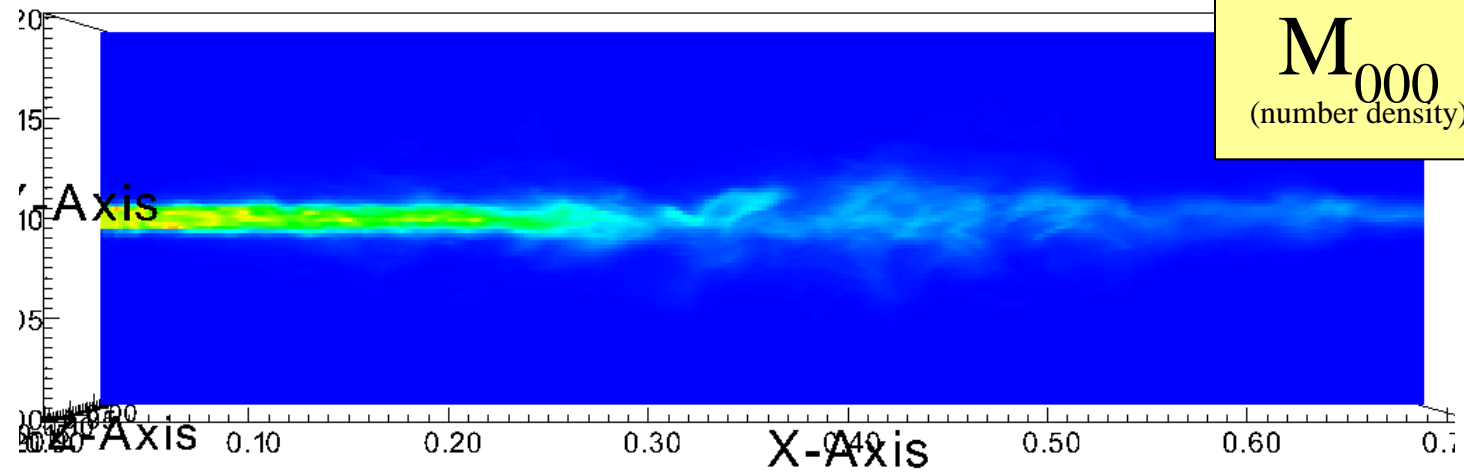


Particle Raw Coal Mass At x = 10 cm

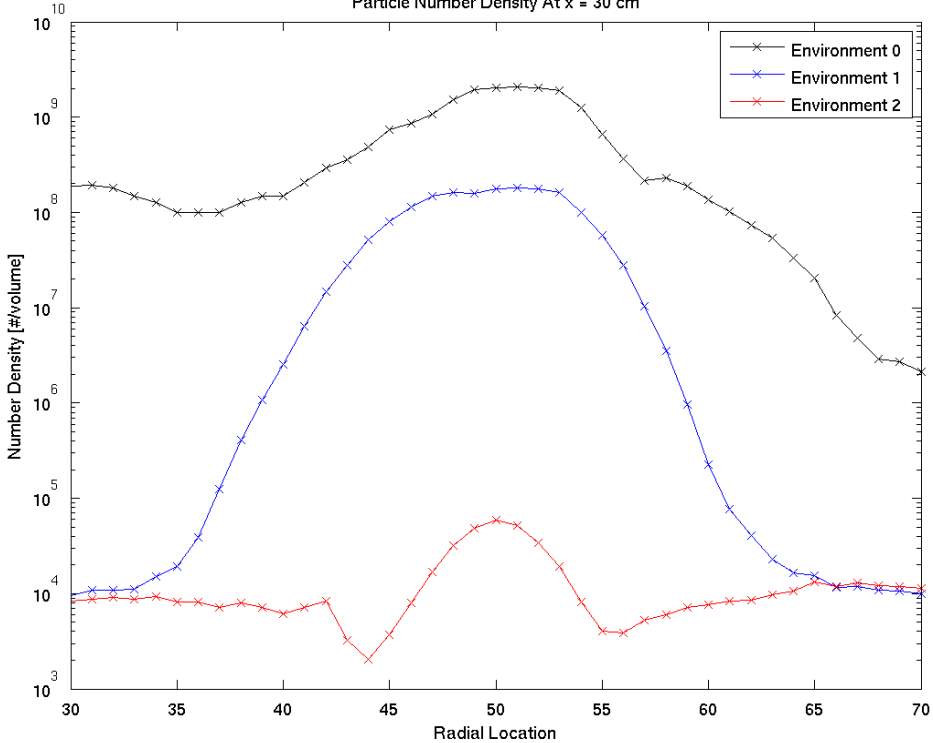




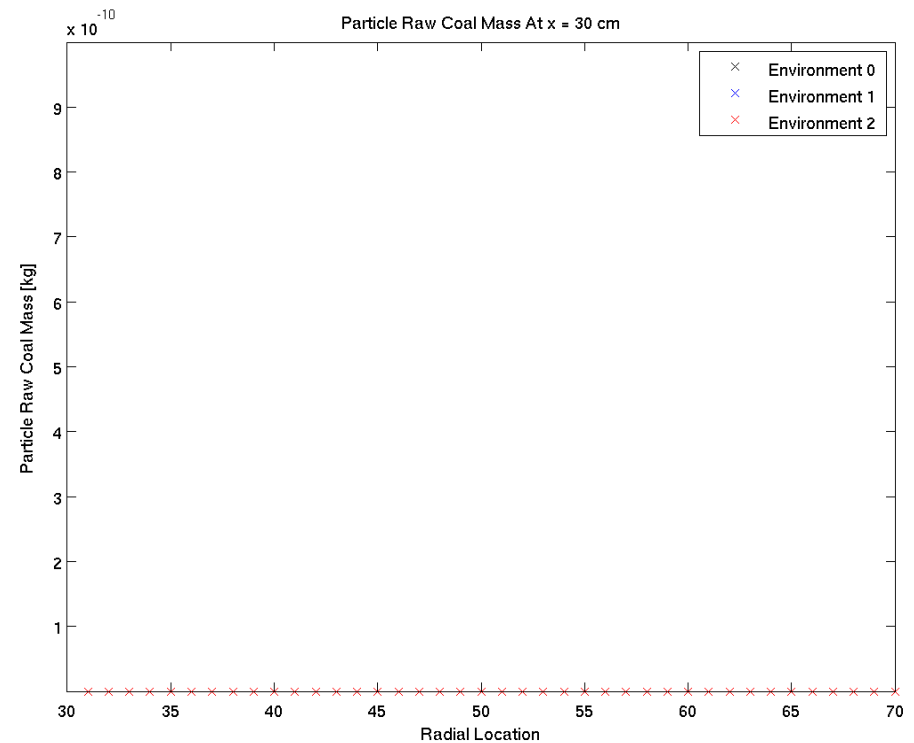
Max: 9.797e+09
Min: 1.525e+04



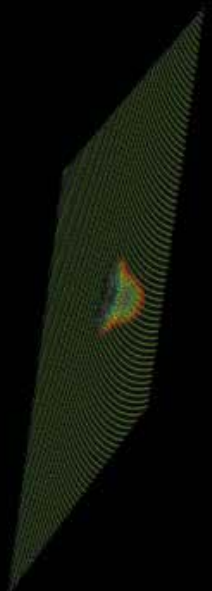
Particle Number Density At x = 30 cm



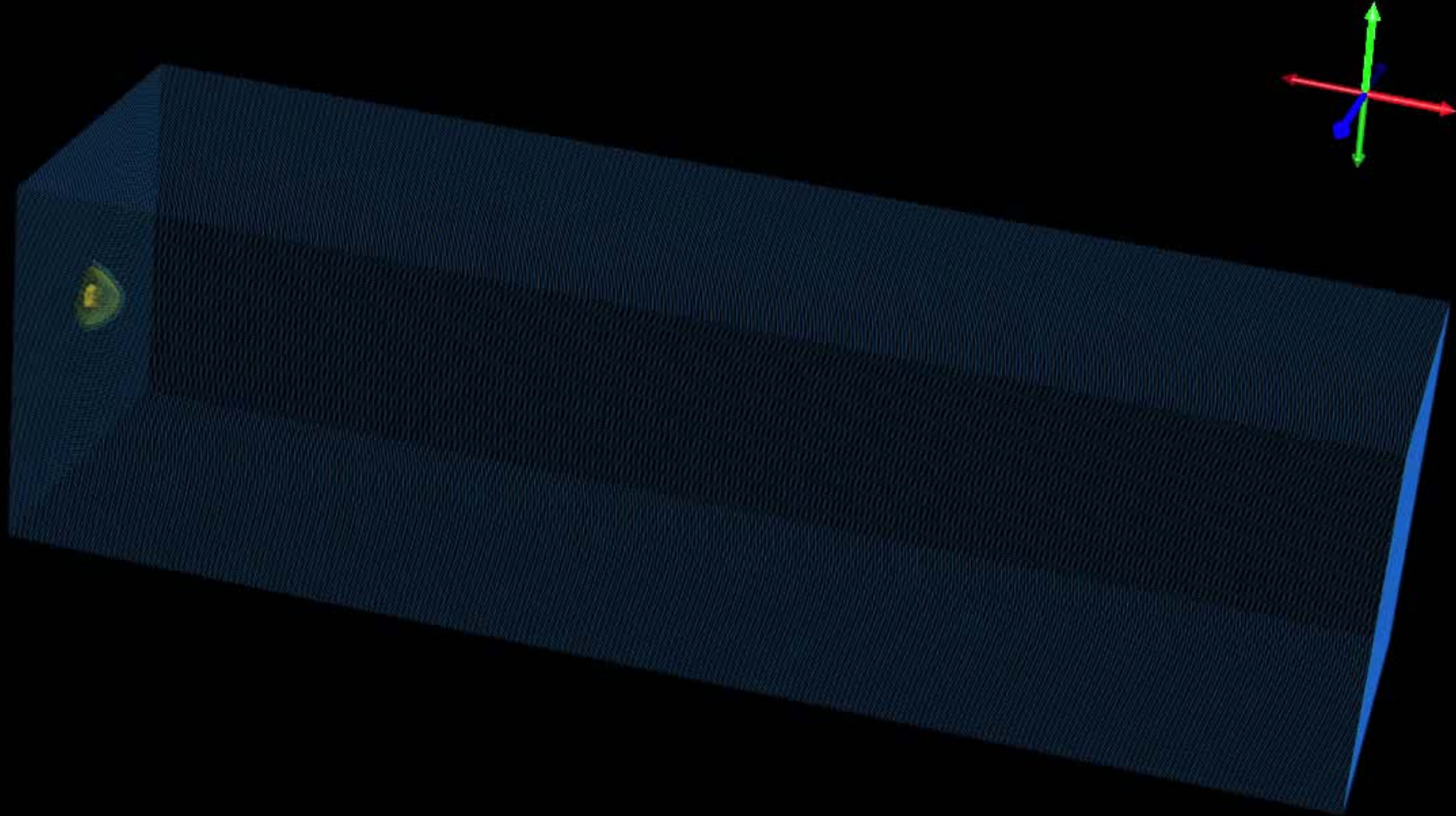
Particle Raw Coal Mass At x = 30 cm



Volume-Rendering: CO Concentration



Volume-Rendering: Mean Particle Size





Summary of Results

- Not focusing on how well the simulation reproduced the data
- Demonstrating a *procedure* for implementation of DQMOM in a massively parallel large-eddy simulation code
- What we've implemented, and why we're excited about it
- Gasification physics - lots of experience, existing numerical techniques
- 1DCOG, PCGC2/PCGC3, Glacier, Banff



Where To Go From Here?

- Improving coal gasification physics
- Improving particle physics
- Increase number of internal coordinates
- Begin formal validation procedure



Professor Philip Smith,
University of Utah

Professor Jeremy Thornock,
University of Utah

Professor Rodney Fox,
Iowa State University

This material is based upon work supported by
the Department of Energy under
Award Number FC26-08NT0005015

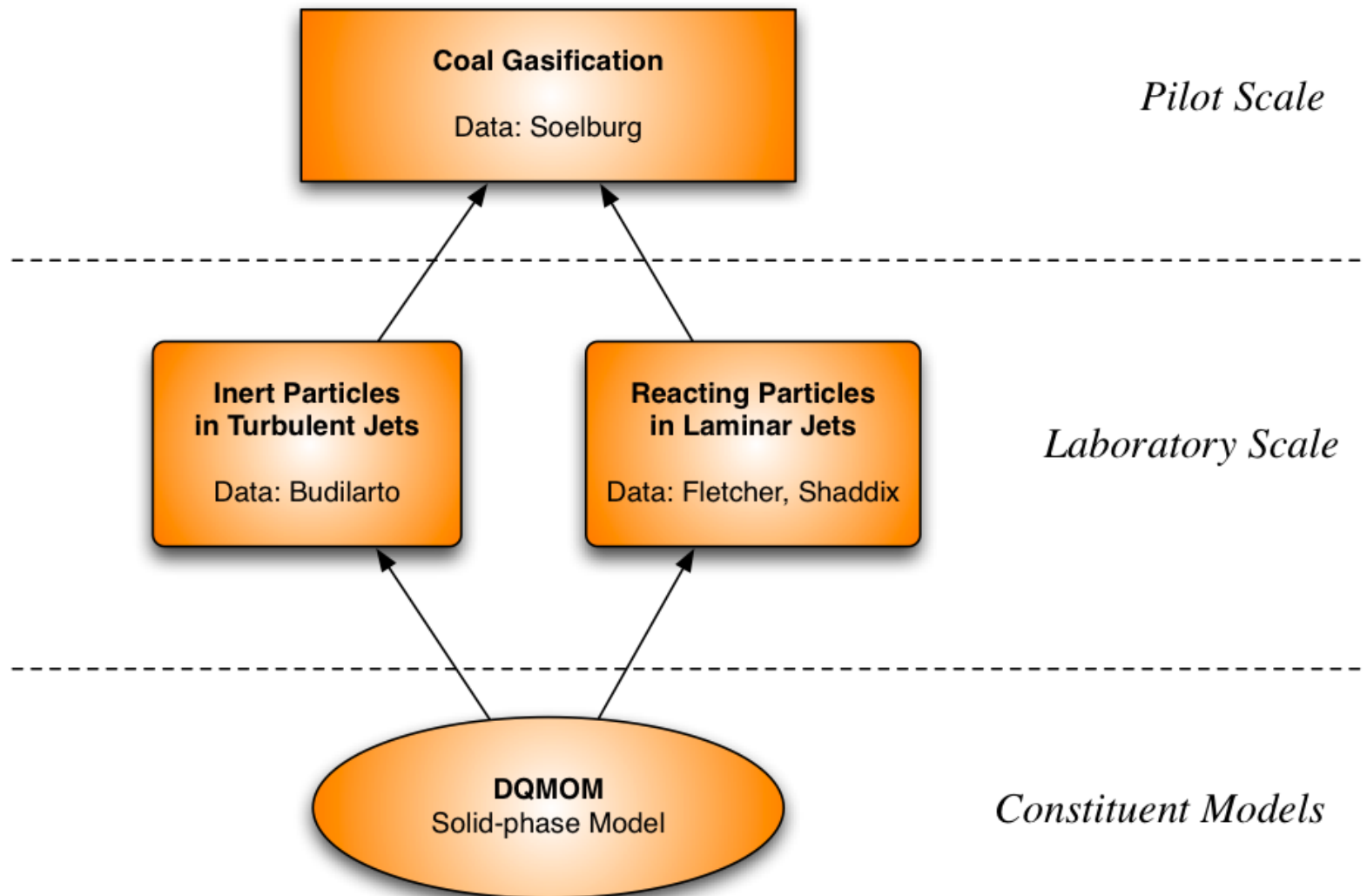


Questions?





Validation Roadmap:





Matrix Expressions

$$\mathbf{A}_1 = \left(1 - \sum_{m=1}^{N_\xi} k_m \right) \prod_{n=1}^{N_\xi} \langle \xi_n \rangle_\alpha^{k_n}$$

$$\mathbf{A}_{j+1} = (k_j) \left(\langle \xi_j \rangle_\alpha^{k_j - 1} \right) \left(\prod_{n \neq j, n=1}^{N_\xi} \langle \xi_n \rangle_\alpha^{k_n} \right)$$

$$\mathbf{S} = - \sum_{n=1}^{N_\xi} \left[\sum_{\alpha=1}^N w_\alpha \left(-k_n \langle \xi_n \rangle_\alpha^{k_n - 1} \right) \left(\prod_{m \neq n, m=1}^{N_\xi} \langle \xi_m \rangle_\alpha^{k_m} \right) (G_n (\langle \xi_n \rangle_\alpha)) \right]$$



Moment Definitions

$$m_k \approx \frac{\sum_{\alpha=1}^N w_{\alpha} \langle \xi \rangle_{\alpha}^k}{\sum_{\alpha=1}^N w_{\alpha}}$$

$$m_k \otimes \frac{\sum_{\alpha=1}^N \left\{ w_{\alpha} \left(\prod_{j=1}^{N_{\xi}} \langle \xi_j \rangle_{\alpha}^{k_j} \right) \right\}}{\sum_{\alpha=1}^N w_{\alpha}}$$