



NATIONAL ENERGY TECHNOLOGY LABORATORY

Solid Sorbent Modeling for the Carbon Capture Simulation Initiative

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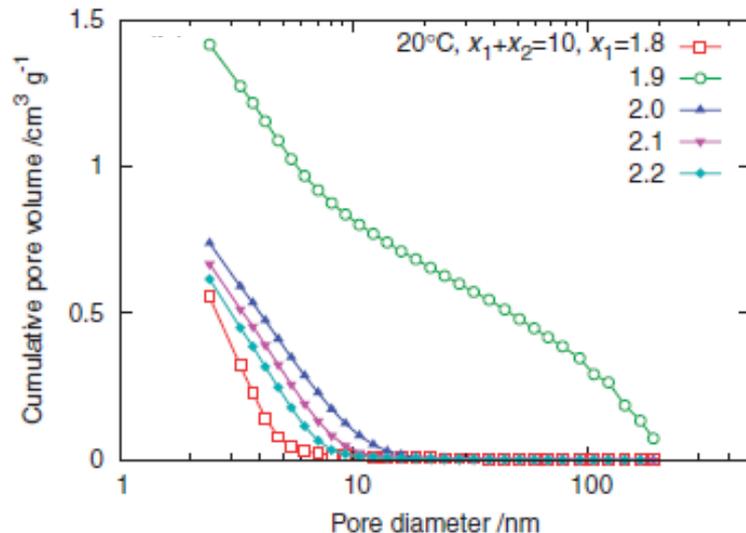
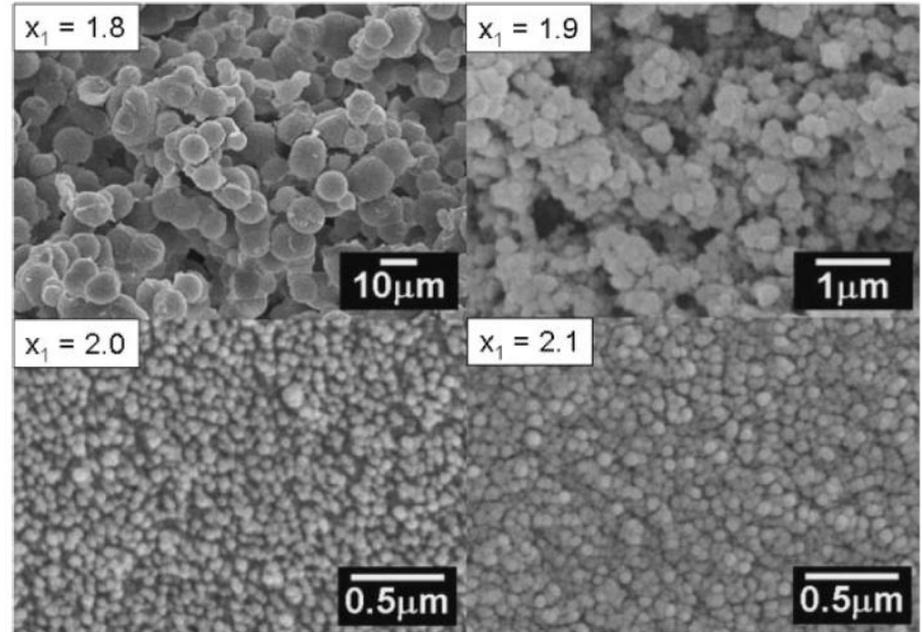


outline

- **intro to silica-supported amine sorbents**
- **first-generation model**
- **high-fidelity approach**
- **outlook**
 - statistical methods in model calibration
 - reduced-order modeling

the sorbent: silica support

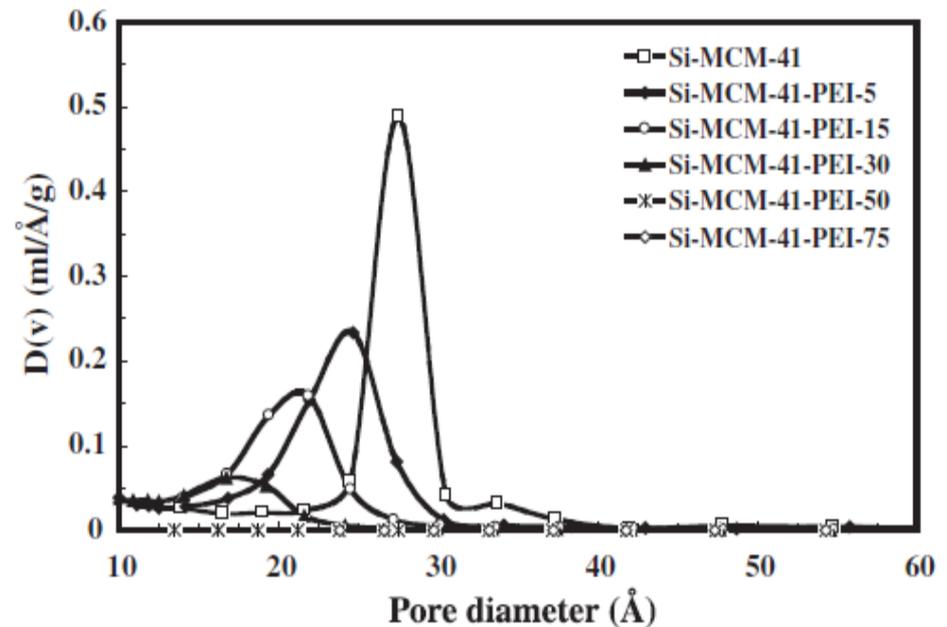
- mesoporous silica forms the substrate
- silica xerogels (sol-gel process) most economical
- substrate particles agglomerates of micron-sized mesoporous particles



K. Kajihara, et al., Bull. Chem. Soc. Jpn. **82** (2009) 1470.

the sorbent: PEI loading

- substrate impregnated with poly(ethyleneimine), or PEI
- PEI tends to fill the mesopores, reducing porosity and internal surface area



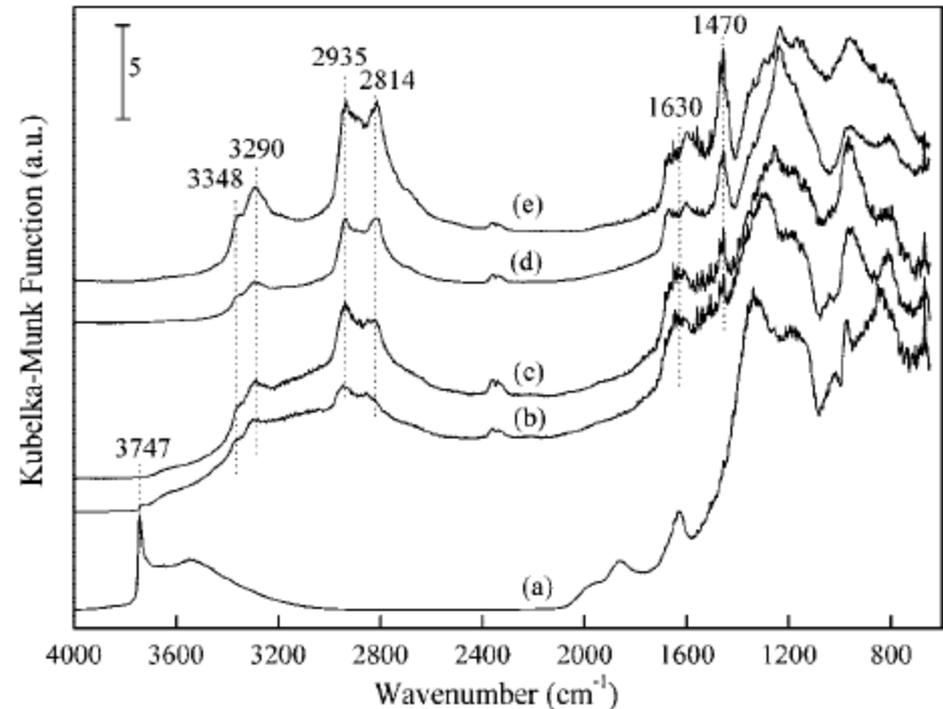
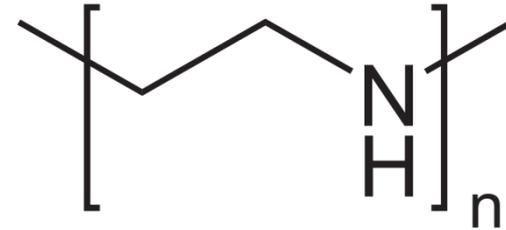
X. Xu, et al., *Micropor. Mesopor. Mat.* **62** (2003) 29.

the sorbent: PEI loading

- substrate impregnated with poly(ethyleneimine), or PEI
- PEI tends to fill the mesopores, reducing porosity and internal surface area
- some amines bind with silanol sites that cover the surface of the substrate

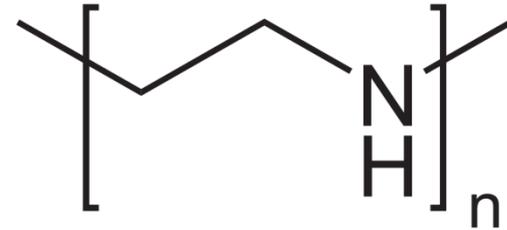
An IR peak associated with silanol (3747 cm^{-1}) disappears when PEI is loaded onto the substrate.

X. Wang, et al., *J. Phys. Chem. C* **113** (2009) 7260.



the sorbent: PEI loading

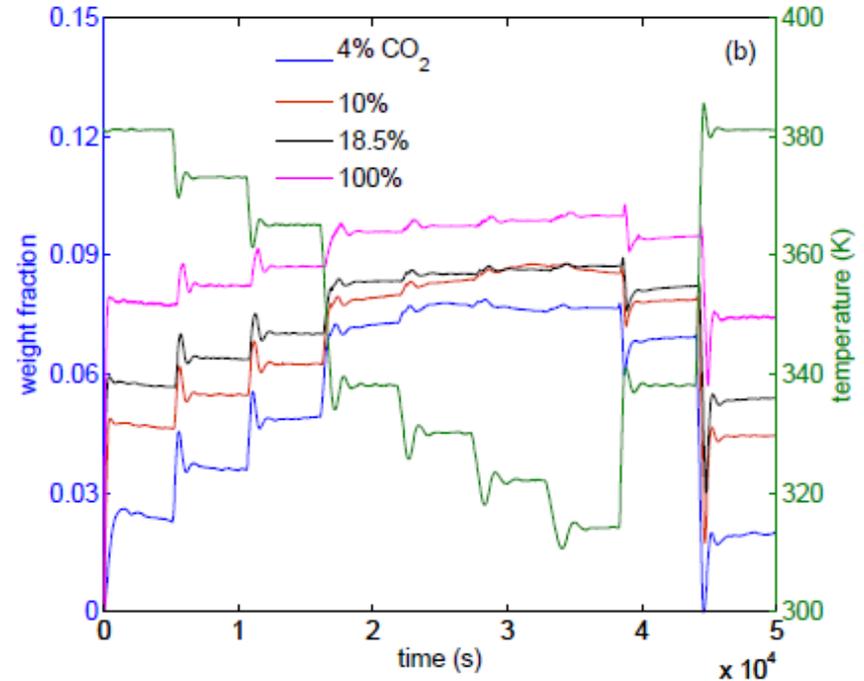
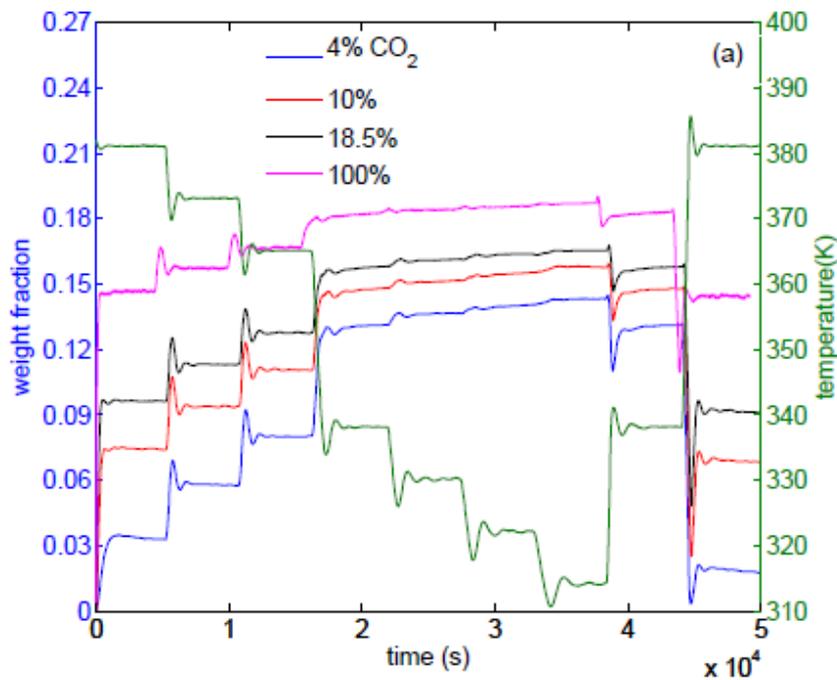
- substrate impregnated with poly(ethyleneimine), or PEI
- PEI tends to fill the mesopores, reducing porosity and internal surface area
- some amines bind with silanol sites that cover the surface of the substrate
- capacity scales with internal surface area



sample	BET surface area (m ² g ⁻¹)	pore volume (cm ³ g ⁻¹)	pore diameter (nm)	CO ₂ cap. ^a mg/g of sorb
MCM-41	1229	1.15	2.7	6.3
PEI(50)/MCM-41 (MBS-1)	11	0.03	0	89.2
SBA-15	950	1.31	6.6	5.0
PEI(50)/SBA-15 (MBS-2)	80	0.20	6.1	140

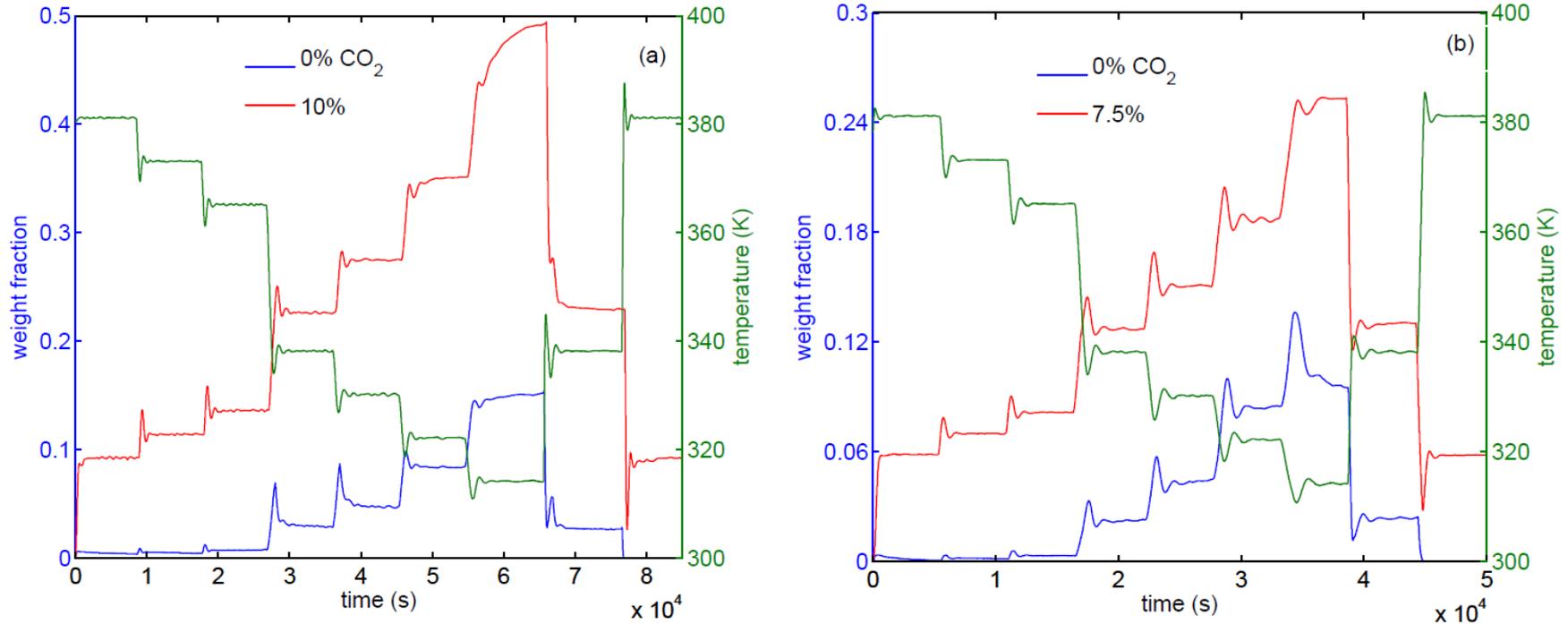
X. Ma, et al., J. Am. Chem. Soc. **131**
(2009) 5777.

the sorbent: dry TGA behavior



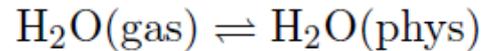
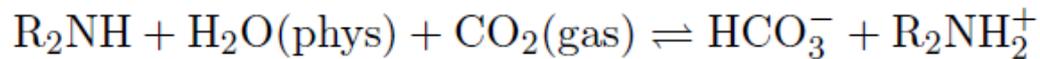
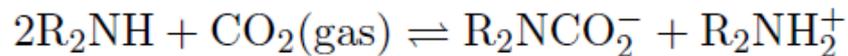
(a) Sorbent NETL-196C, ~44.1 wt-% PEI (b) NETL-32D, ~22.5 wt-% PEI. Dry atmosphere. Sorbent synthesis: McMahan Gray, NETL; Sorbent characterization: Daniel Fauth, NETL.

the sorbent: wet TGA behavior



(a) Sorbent NETL-196C, ~44.1 wt-% PEI (b) NETL-32D, ~22.5 wt-% PEI. Humid atmosphere: ~9.1 mol-% H_2O . Sorbent synthesis: McMahan Gray, NETL; Sorbent characterization: Daniel Fauth, NETL.

first-generation model



$$\frac{\partial x}{\partial t} = k_c (s^2 p_c^m - xw/\kappa_c)$$

$$\frac{\partial b}{\partial t} = k_b (sap_c - bw/\kappa_b)$$

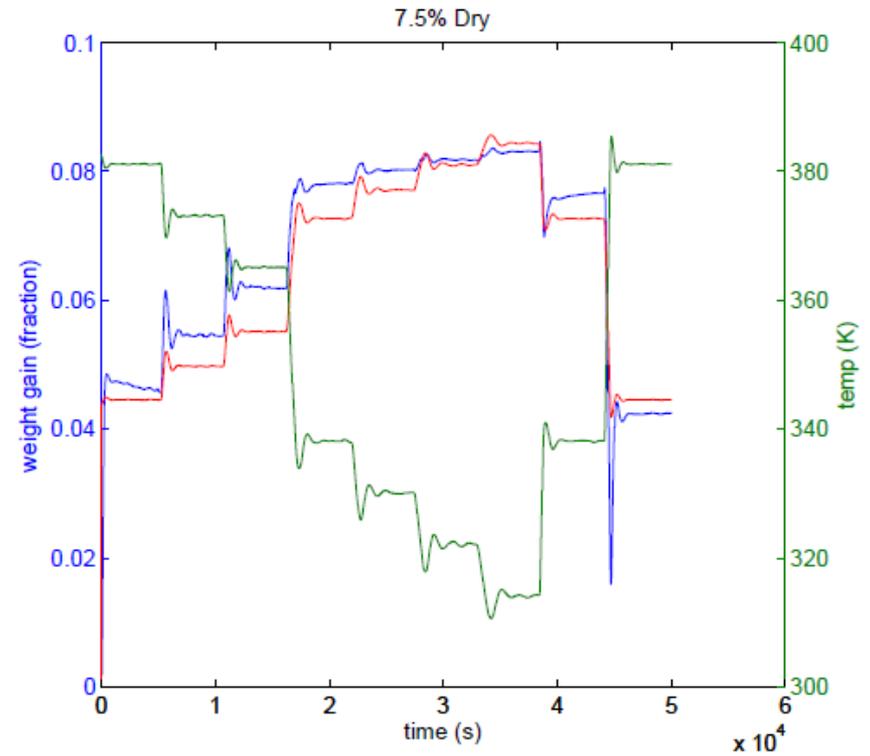
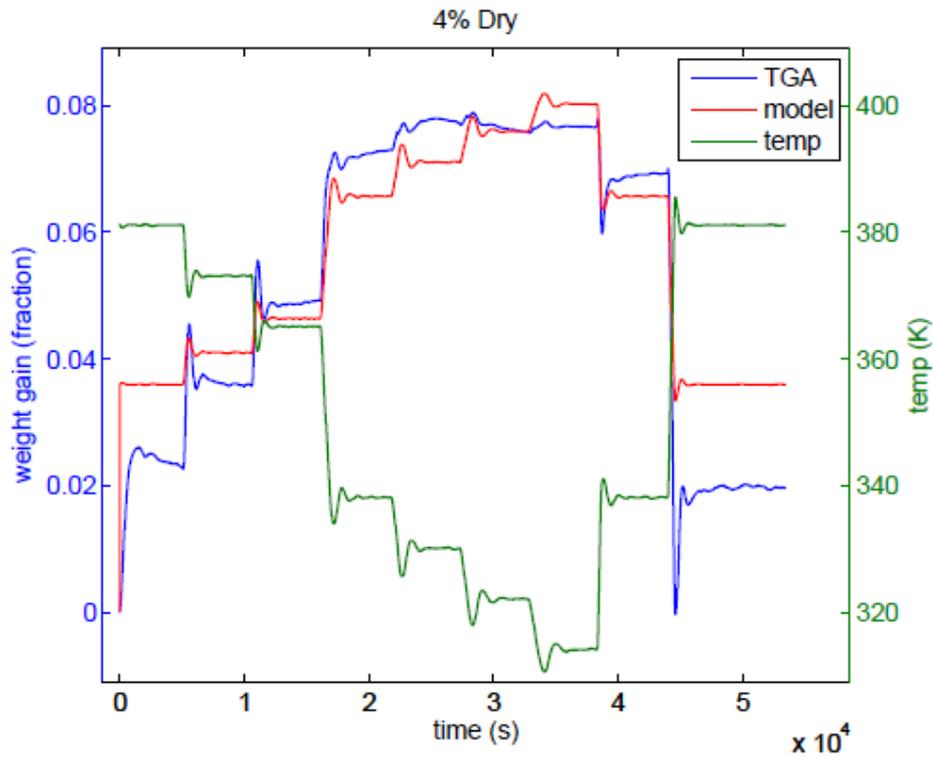
$$\frac{\partial a}{\partial t} = k_h (p_h - a/\kappa_h)$$

$$1 = s + w + x$$

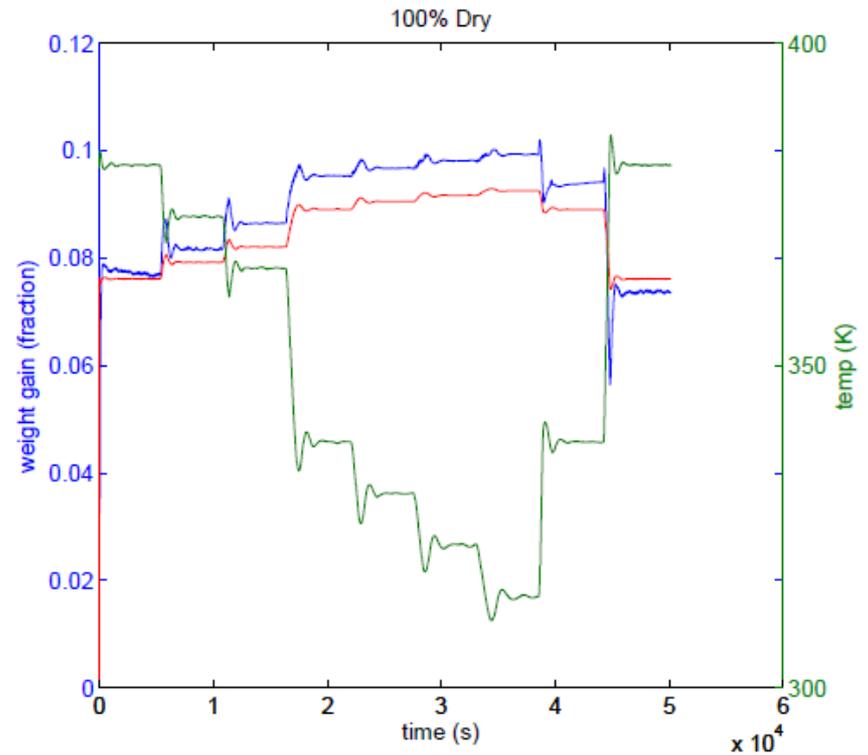
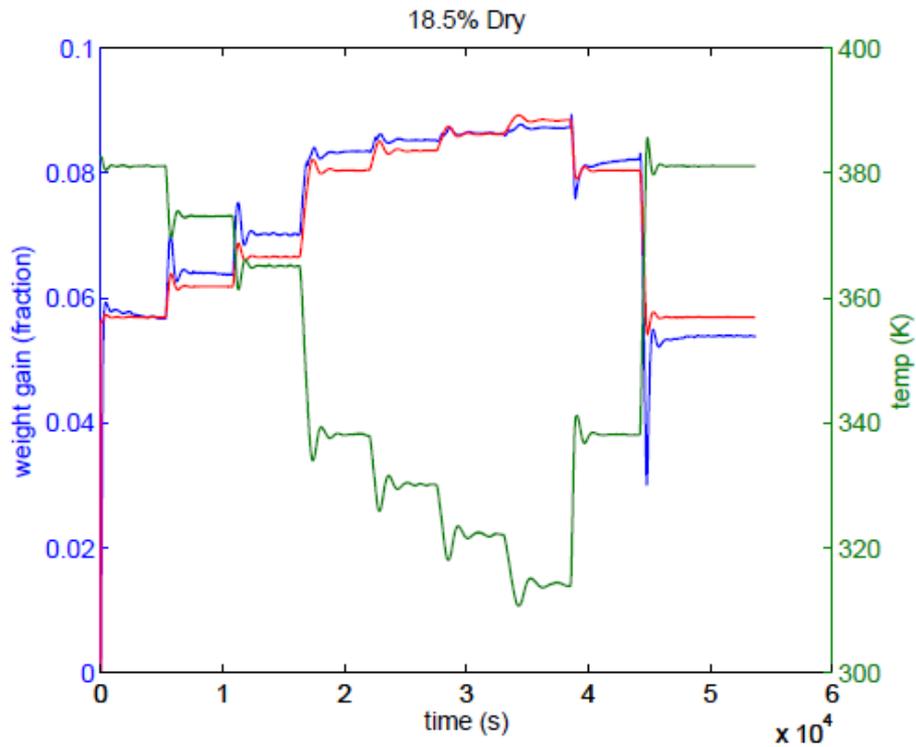
$$w = x + b/n_v$$

- **13 parameters fit to data sequentially**
 - dry (carbamate) kinetic and equilibrium (5)
 - water uptake kinetic and equilibrium (4)
 - bicarbonate kinetic and equilibrium (4)

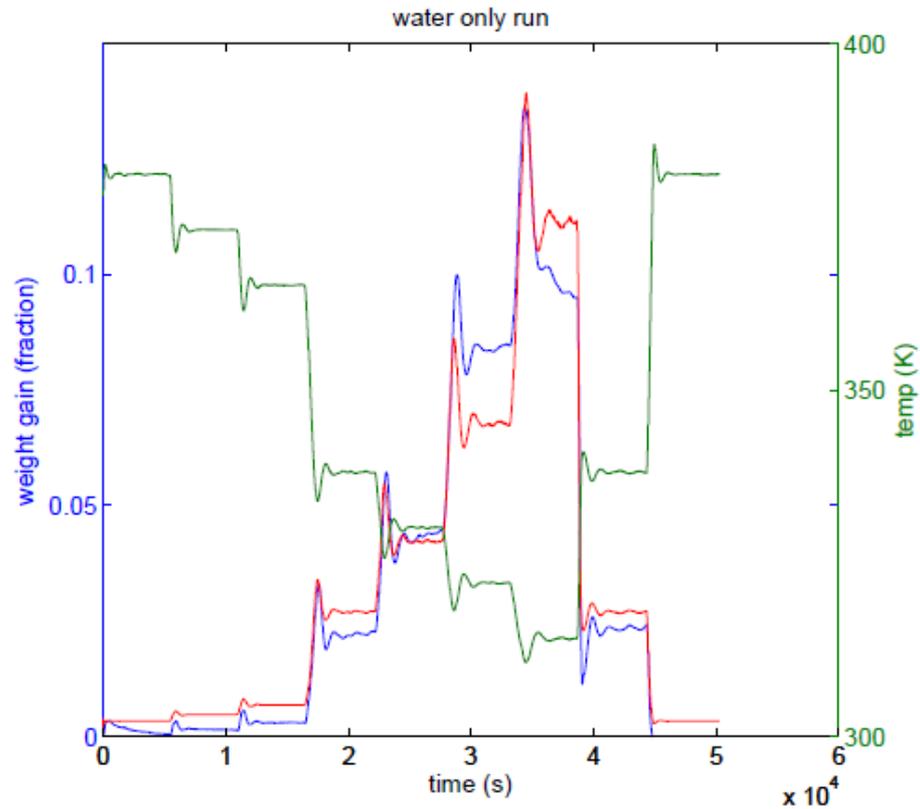
first-generation model: fit for NETL-32D



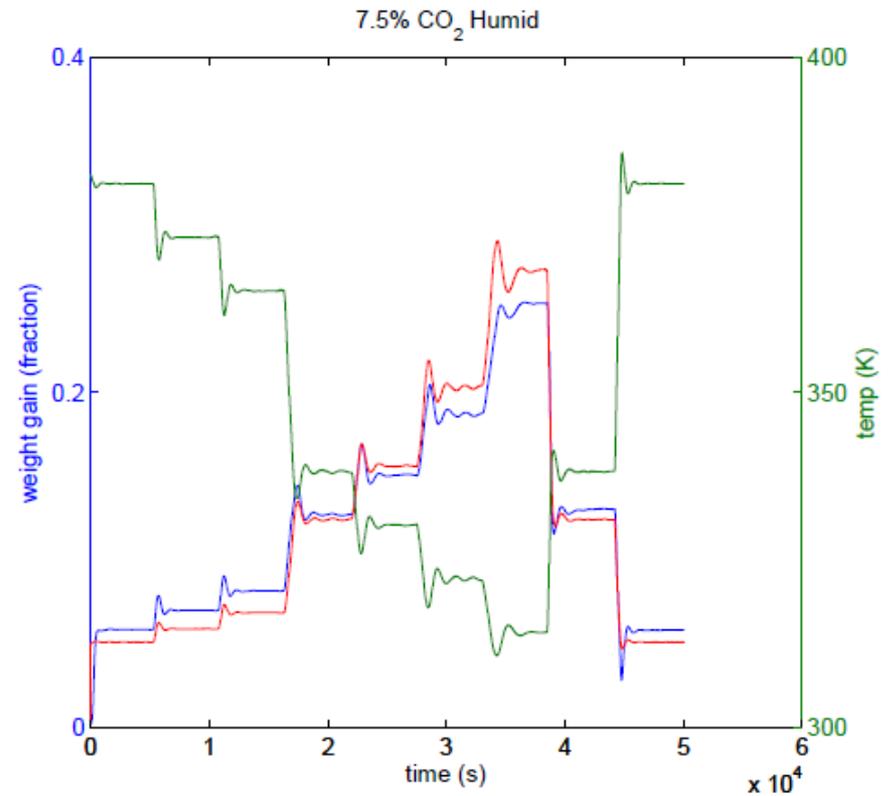
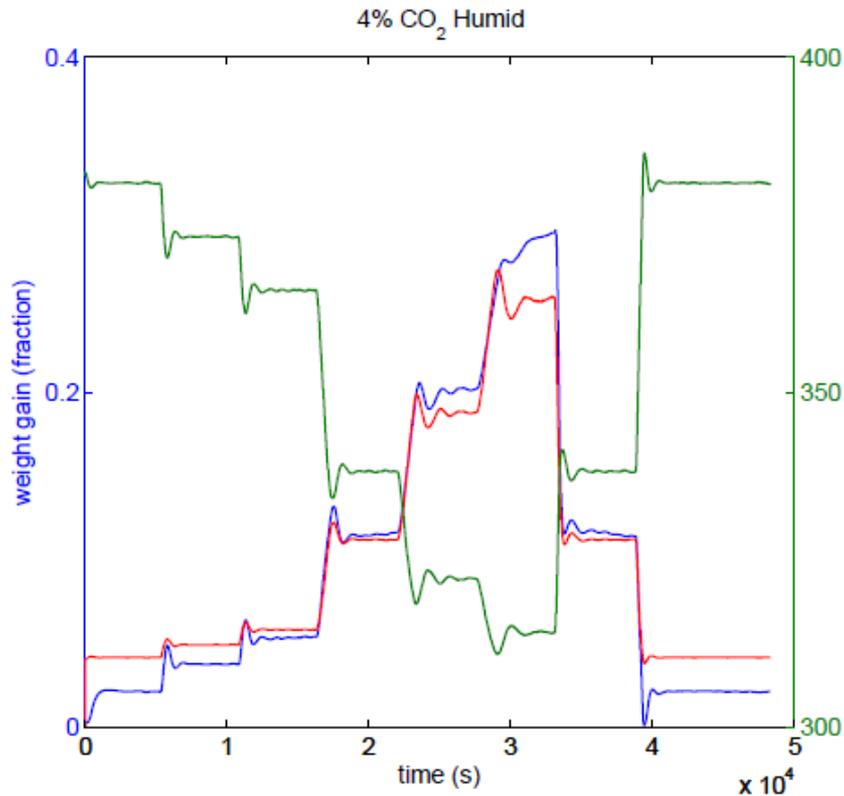
first-generation model: fit for NETL-32D



first-generation model: fit for NETL-32D



first-generation model: fit for NETL-32D



- **heat of reaction in dry conditions: 65 kJ/mol calculated, vs. 67 kJ/mol measured by calorimetry¹**

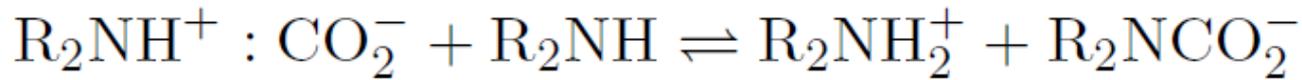
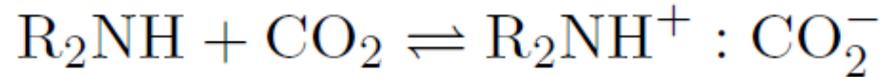
¹R. Serna-Guerrero and A. Sayari, Chem. Eng. J. 161 (2010) 182.

first-generation model

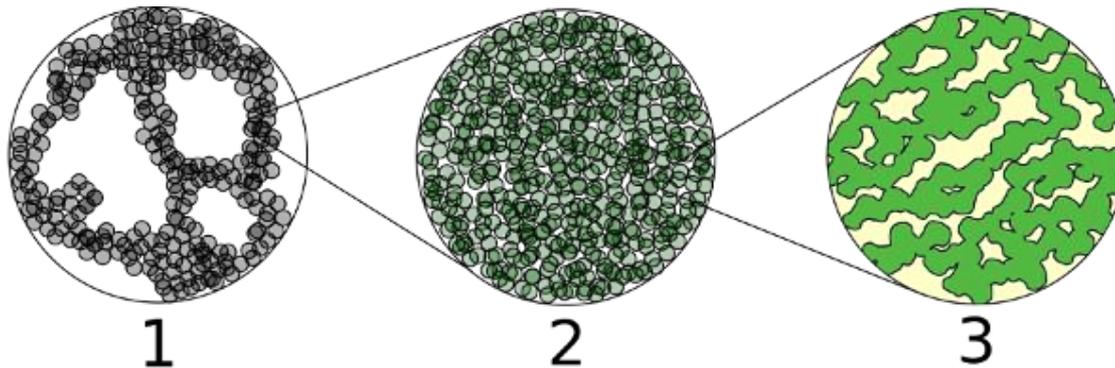
- **advantages**
 - quickly prepared
 - easy to implement at larger modeling scales
 - flexible
- **disadvantages**
 - accuracy
 - weak identification with actual physical processes

high-fidelity approach

- **carbamate formation is actually two-step:**



- **three modes of mass transport:**
 - gas phase bulk
 - gas phase Knudsen
 - solid state (zwitterion-mediated hopping)



high-fidelity approach

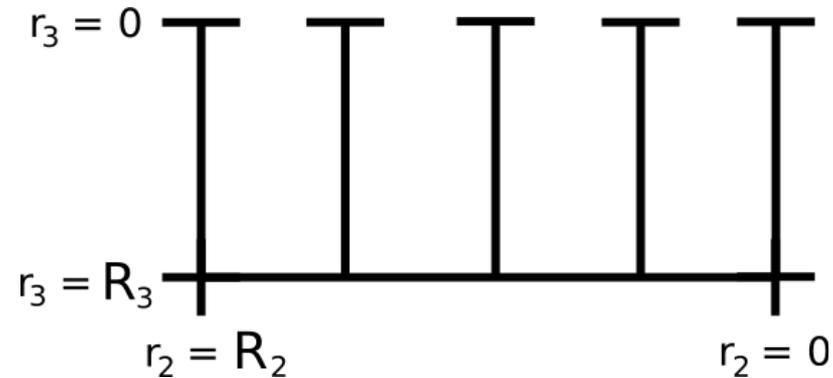
$$\left[\epsilon_2 + RTn_s a_2 \frac{\kappa_z(1 - 2x_s)}{(1 + \kappa_z p)^2} \right] \frac{\partial p}{\partial t} = \frac{4\epsilon_2}{3\tau_2} K_o \left(\frac{8RT}{\pi M} \right)^{1/2} \nabla_2^2 p - RTa_2 n_s \left(\frac{1 - \kappa_z p}{1 + \kappa_z p} \right) \frac{\partial x_s}{\partial t} + RTq_{2,t}$$

$$q_{2,t} = -RTu_b n_s a_2 (n_v N_a)^{2/3} \left[z_s(1 - 2x_1 - z_1) - z_1(1 - 2x_s - z_s) \right]$$

$$\epsilon_3 \frac{\partial z}{\partial t} = \frac{\epsilon_3}{\tau_3} RTu_b \nabla_3 \cdot \left[(1 - 2x) \nabla_3 z + 2z \nabla_3 x \right] - \frac{\partial x}{\partial t}$$

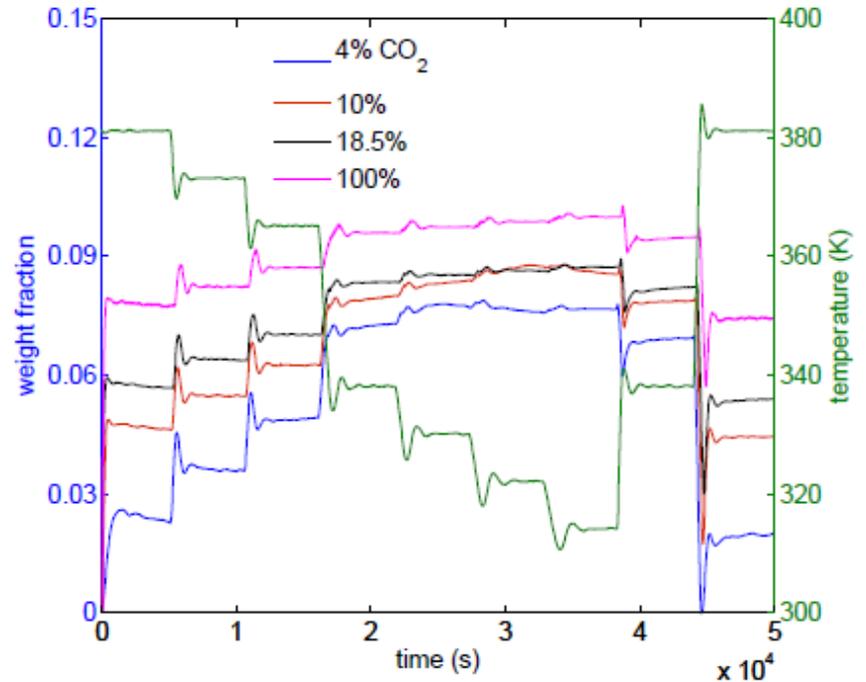
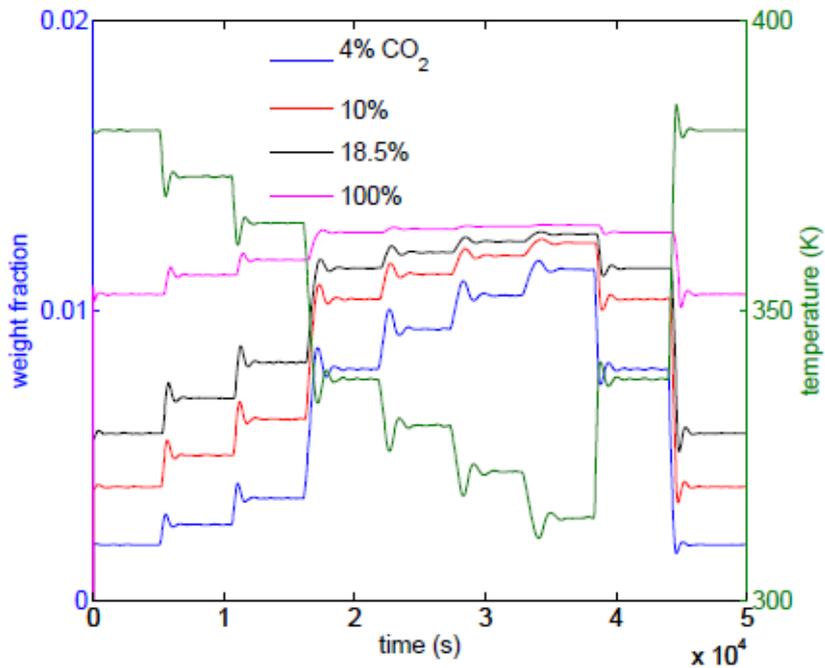
$$\frac{\partial x}{\partial t} = k_x \left[(1 - 2x - z)z - x^2 / \kappa_x \right]$$

high-fidelity approach



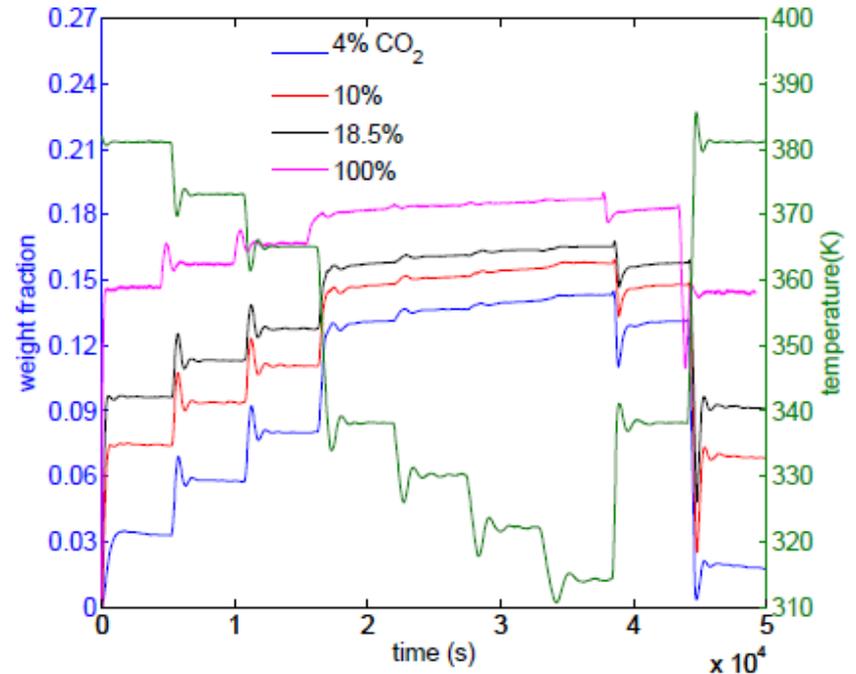
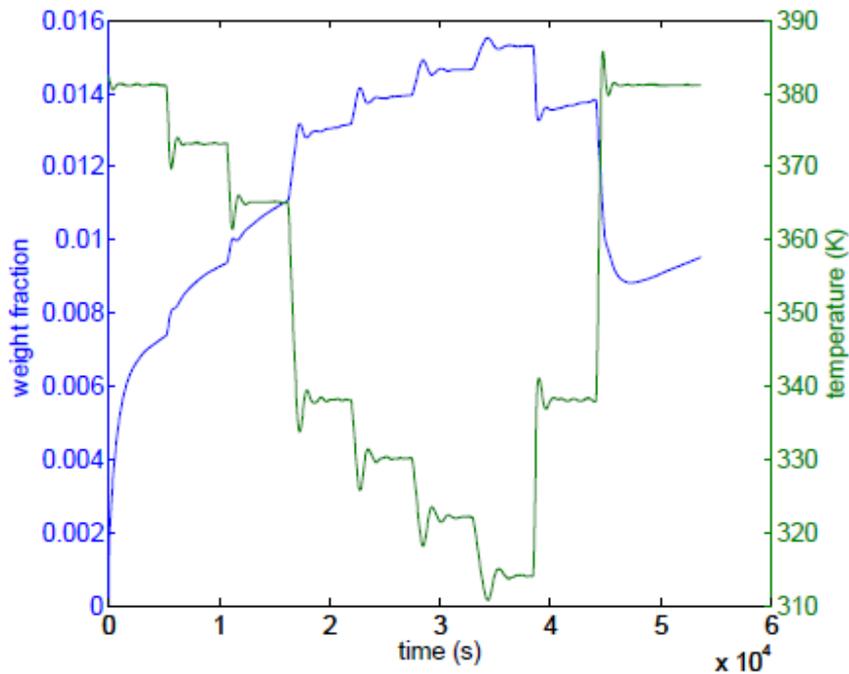
- **line-by-line iterative method**
- **set of 12 unknown parameters**

high-fidelity approach



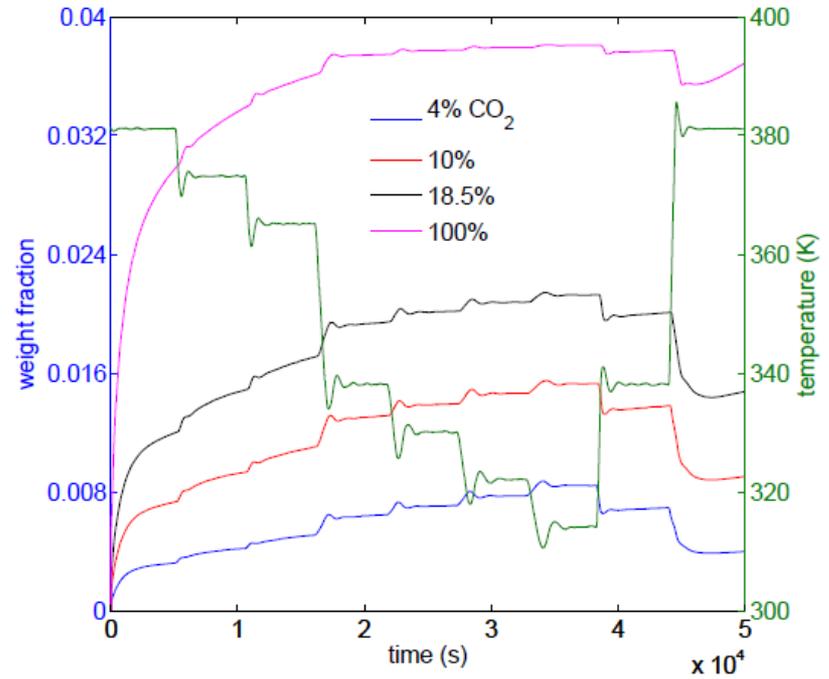
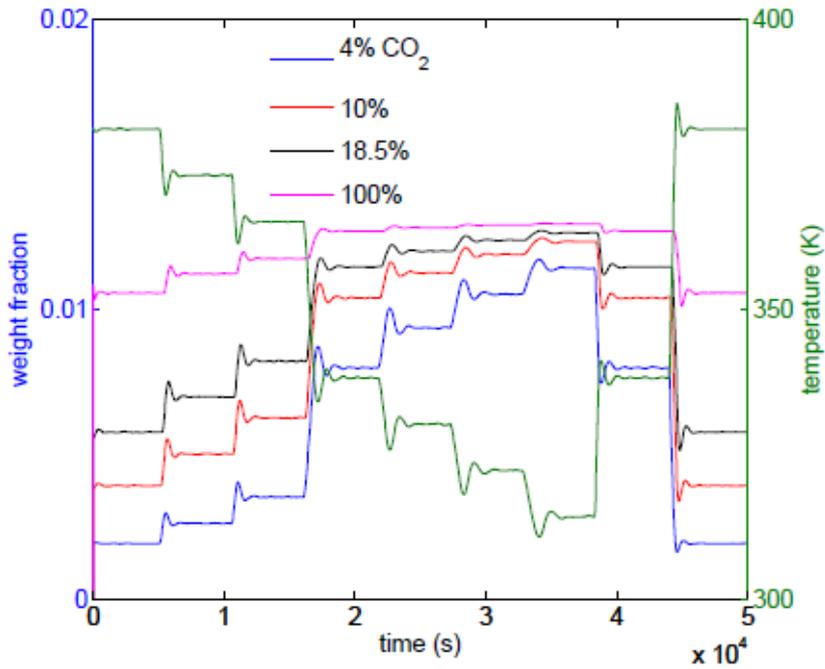
(left) calculated output of the high-fidelity sorbent model (right) experimental TGA for NETL-32D

high-fidelity approach



(left) calculated output of the high-fidelity sorbent model (right) experimental TGA for NETL-196C

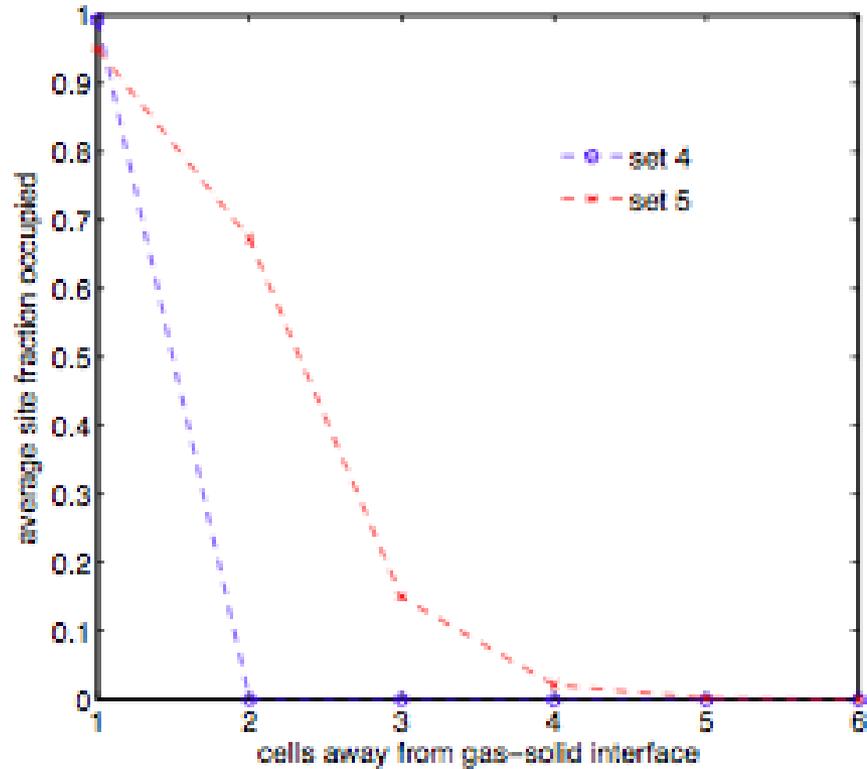
high-fidelity approach



set	K_o/τ_2	τ_3	f	n_v	ΔH_{tot}	ΔS_{tot}	ΔH_5	ΔS_5	ΔH_6^\ddagger	ζ'_6	ΔH_b^\ddagger	ζ'_b
4	$10^{-8.57}$	3.98	3.26	2.31×10^4	-0.61	-35.0	-0.57	-16.0	0.39	$10^{3.87}$	1.20	$10^{-10.1}$
5	$10^{-9.40}$	2.35	1.78	2.44×10^4	-0.51	-38.9	-0.40	-11.5	0.35	$10^{4.20}$	1.25	$10^{-4.7}$

high-fidelity approach

average cross-sectional site fraction of adsorbed CO₂ in the PEI bulk

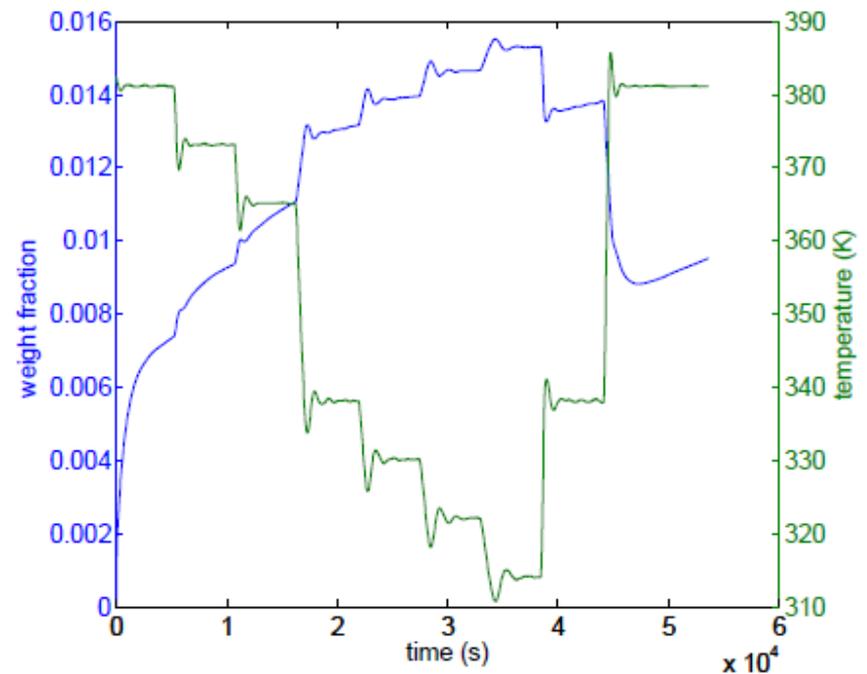
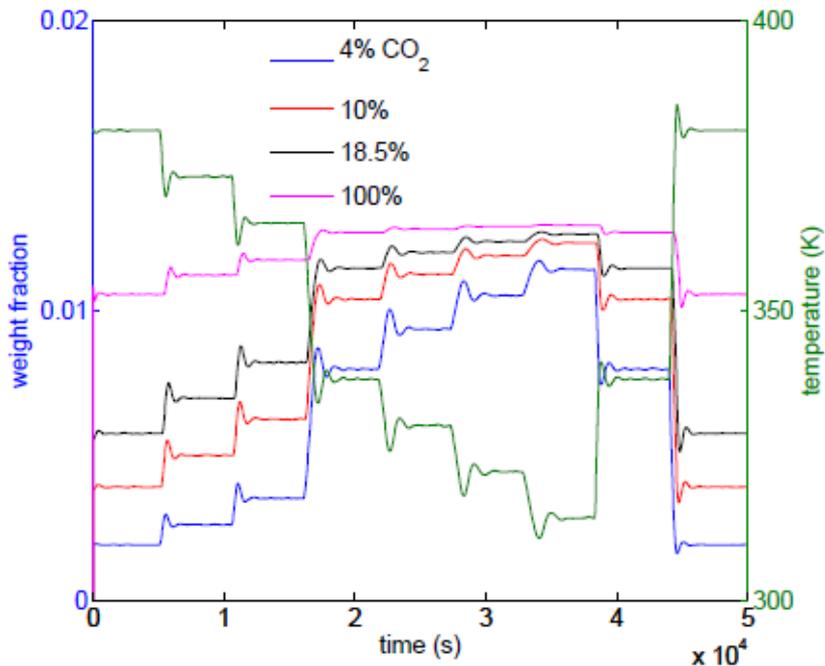


outlook: parameter estimation

- **Bayesian statistical methodology for parameter estimation**
 - parameter set not a single, ‘true’ set of values, but a joint probability distribution
 - prior probability distributions arise from similar chemistries (*e.g.*, aqueous amines), advanced microscopic measurements or *ab initio* calculations
- **model replaced by a Gaussian process emulator**
 - reduced order model for the process itself
 - normally distributed error includes inadequacy of the ROM and of the high-fidelity model itself, along with experimental error
- **Monte Carlo simulation for optimization**
 - analogous to genetic algorithm
 - leads to posterior probability distribution for parameters

outlook: reduced-order model

- proper orthogonal decomposition is homologous to a singular value decomposition



summary

- **first-generation model for silica-supported amine sorbents**
 - set of three nonlinear, ordinary differential equations
 - model parameters fit to data for two NETL sorbents
- **high-fidelity model for silica-supported amine sorbents**
 - hierarchical, microstructurally homogenized grain model
 - captures principal qualitative aspects of sorbent behavior
 - efficient vehicle for multi-scale modeling
- **Bayesian approach to multi-scale modeling**
 - microscopic data incorporated in statistically rigorous way
 - proper orthogonal decomposition looks promising

acknowledgements

- **Dan Fauth, NETL**
- **Mac Gray, NETL**
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- **Brian Kail, URS**
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- **Sankaran Sundaresan, Princeton**
- **David Miller, NETL**
- **Chris Guenther, NETL**
- **Madhava Syamlal, NETL**