# **CFD Modeling of Multi-scale Air- and Oxy- coal Combustion Experiments**



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NETL Workshop on Multi-phase Flow Science

Pittsburgh, PA

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### **Program Overview**

- Objective: Characterize and predict performance and operational impacts of oxy-combustion retrofit designs on existing coal-fired boilers
- Approach: Utilize multi-scale testing and theoretical investigations to develop:
  - Fundamental data that describe combustion characteristics, corrosion rates, and ash properties during oxy-coal firing
  - Validated mechanisms that describe oxy-combustion processes
  - Firing system principles that guide oxy-burner design and fluegas recycle implementation
- Incorporate validated mechanisms into CFD software to evaluate full-scale oxy-combustion retrofit designs

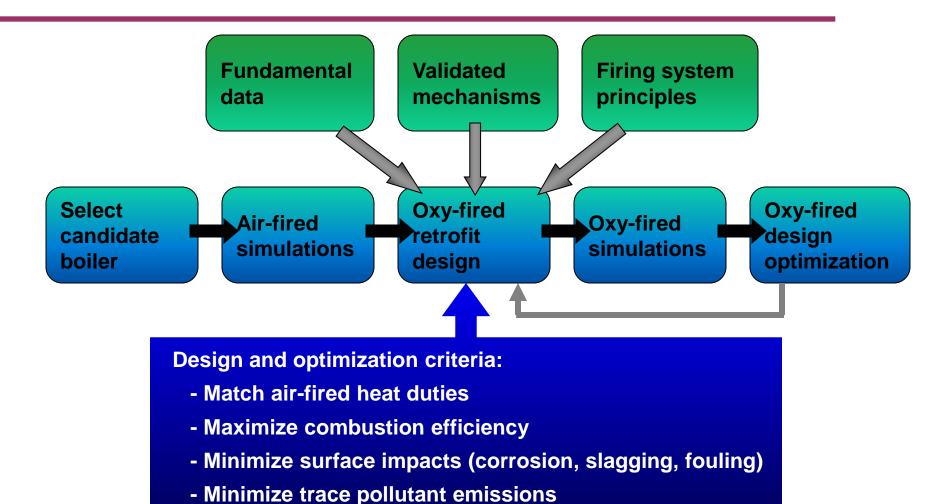


## **Program Overview**

Team Member	Project Role			
REI	program management, testing oversight, mechanism development, simulations			
University of Utah	laboratory and pilot-scale testing, mechanism development			
Siemens/ABT	burner technology			
Praxair	oxygen supply			
Brigham Young Univ.	soot measurements			
Corrosion Management	corrosion tests, mechanism development			
Sandia National Labs	bench-scale testing, mechanism development			
Vattenfall AB	mechanism development, validation data			
PacifiCorp, Praxair, Southern Company, Vattenfall, DTE Energy	Advisory Panel provides industrial perspective on R&D needs, retrofit requirements and constraints, suggested assessment studies			



### **Program Overview**





### Program Schedule

- Year 1 Key Tasks (ending 9/30/09)
  - Initiate char oxidation and OFC experiments
  - Design and fabricate pilot-scale oxy-burner
  - Complete initial slagging and fouling mechanism development
- Year 2 Key Tasks (ending 9/30/10)
  - Complete OFC ash characterization measurements without FGR
  - Continue char oxidation experiments and mechanism development
  - Complete pilot-scale burner, slagging, fouling, corrosion testing
- Year 3 Key Tasks (ending 3/31/12)
  - Finish char oxidation experiments and validate mechanism
  - Complete OFC ash characterization measurements with FGR
  - Validate slagging, fouling, corrosion, sooting mechanisms
  - Implement validated mechanisms into CFD code
  - Complete boiler retrofit assessment

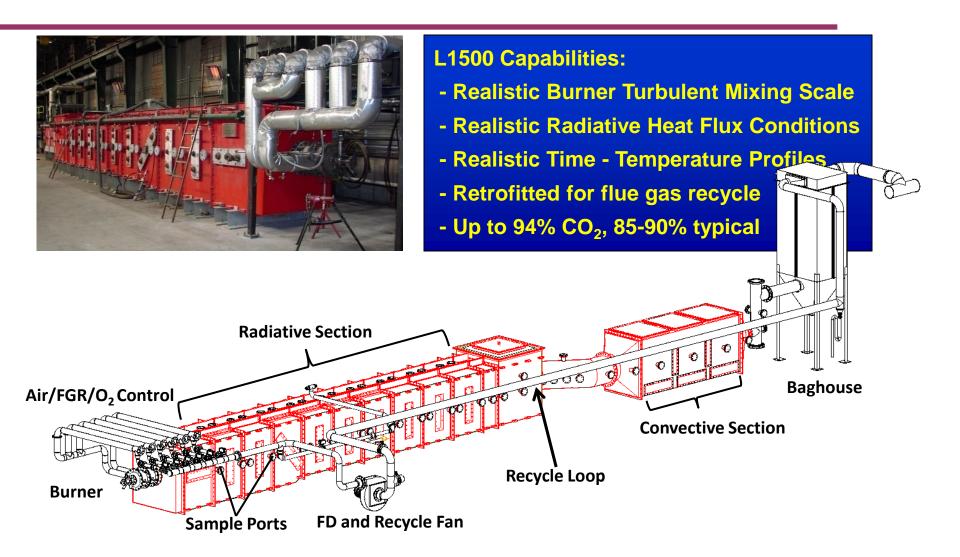


### Multi-scale Experiments

- Bench-Scale Optical Entrained Flow Reactor
  - Char Oxidation Kinetics
- 100 kW Oxy-Fuel Combustor (OFC) Tests
  - Ash Deposition and Characterization
  - Soot Evolution
- 1.2 MW Pilot-Scale Furnace (L1500) Tests
  - Impacts of Burner Configuration
  - Heat Flux, Corrosion and Particle Deposition
  - Flue Gas Chemistry, Sooting

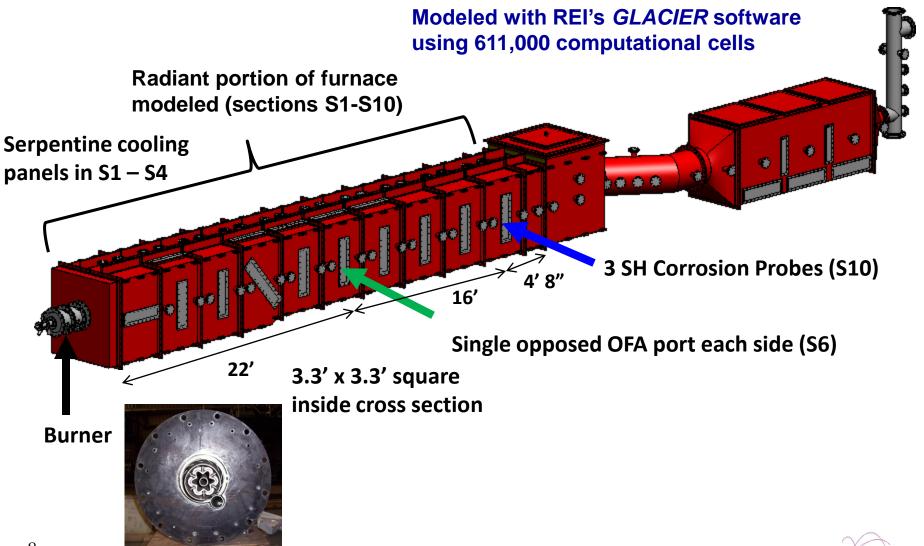


### 3.5 MBtu/hr Pilot-Scale Furnace (L1500)





### Furnace Model Geometry





## **Operating Conditions**

Coal Property	Utah Skyline		
Moisture (%)	3.18		
Ash (%)	8.83		
C (%)	70.60		
H (%)	5.06		
N (%)	1.42		
S (%)	0.53		
O (%)	10.38		
Volatile (%)	38.60		
Fixed C (%)	49.39		
HHV (Btu/lb)	12,606		

Parameter	Units	Air	Оху
Firing Rate	MBtu/hr	3.5	3.5
Excess O <sub>2</sub>	%, dry	3.14	3.07
BSR		0.9	0.9
Primary Gas/Fuel		1.8	1.8
Burner IS / OS		20/80	20/80
Overall O <sub>2</sub>	%, wet	21	27
Burner O <sub>2</sub>	%, wet	21	27
Primary O <sub>2</sub>	%, wet	21	21
IS O <sub>2</sub>	%, wet	21	28.7
OS O <sub>2</sub>	%, wet	21	28.7



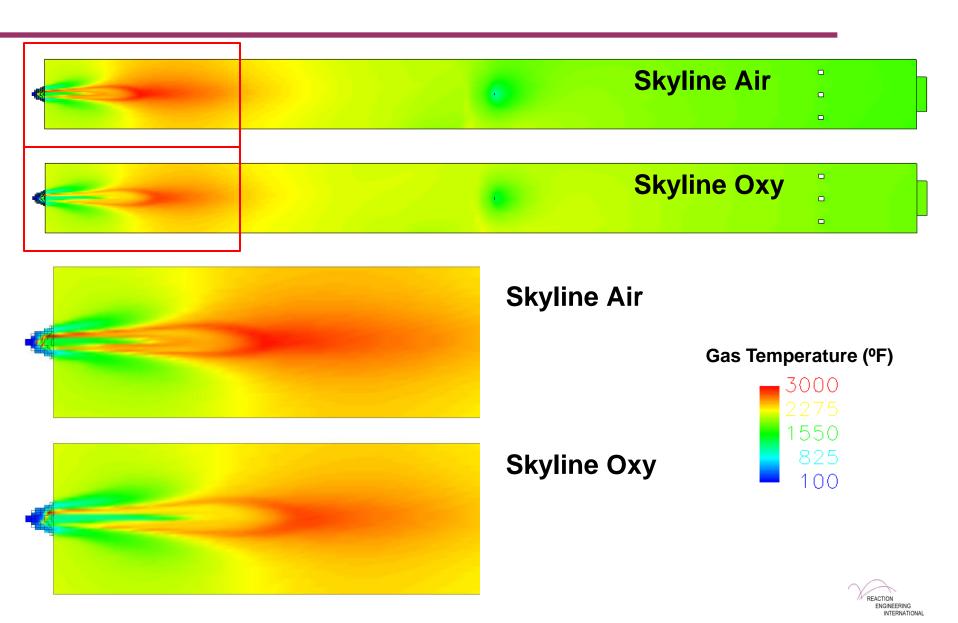
### **Baseline CFD Model Results**

(without newly developed sub-models)

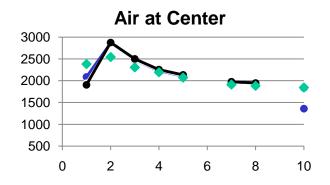
	Skyline Air Model	Skyline Air Ave Measured	Skyline Oxy Model	Skyline Oxy Ave Measured
Exit Temp (°F)	1743		1872	
Exit O <sub>2</sub> (%, dry)	3.14	3.18	3.03	3.07
Exit CO (ppmv, dry)	<1	16	126	90
Exit SO <sub>2</sub> (ppmv, dry)	444	425	1,788	1754
Exit CO <sub>2</sub> (%, dry)	15.9	15.9	89.9	89.9
Exit H <sub>2</sub> O (%)	6.7		25.6	
Gas Sensible Heat (%)	39.7		41.1	
Wall Heat Loss (%)	59.6		58.5	
Rad. / Conv. (%)	41.4 / 18.2		46.5 / 12.0	

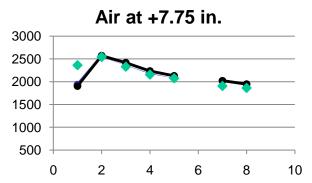


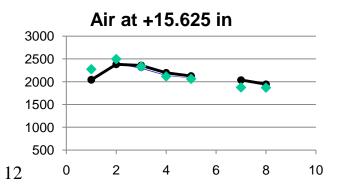
## Predicted Gas Temperature

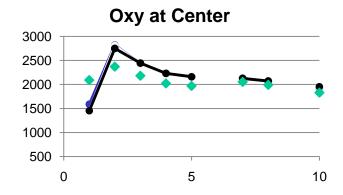


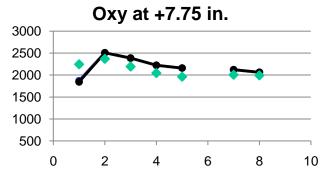
### Radial Gas Temperature Comparison

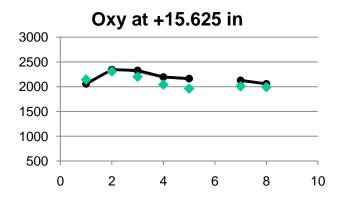






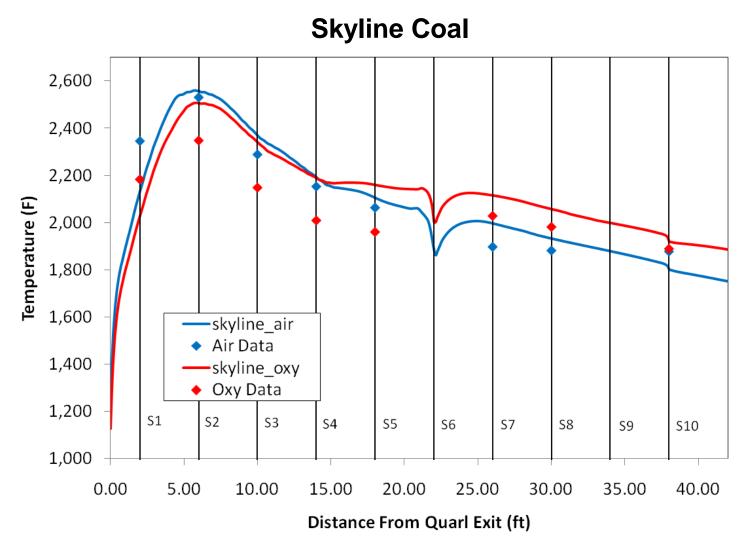






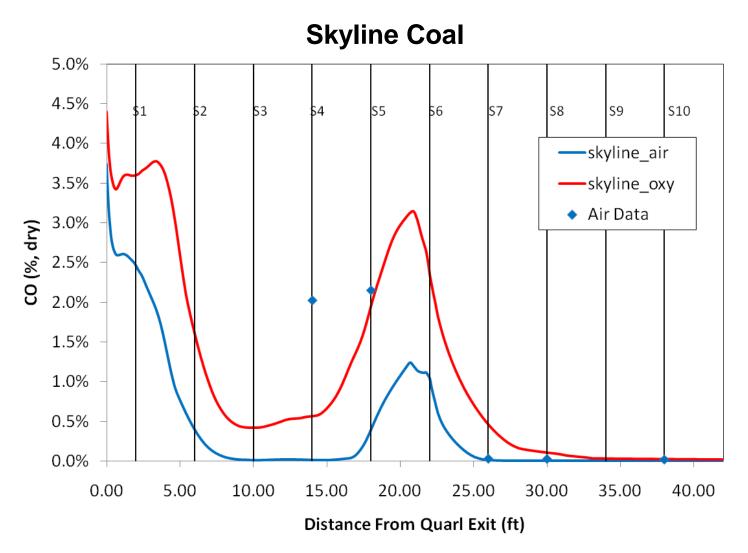


## Average Gas Temperature Comparison



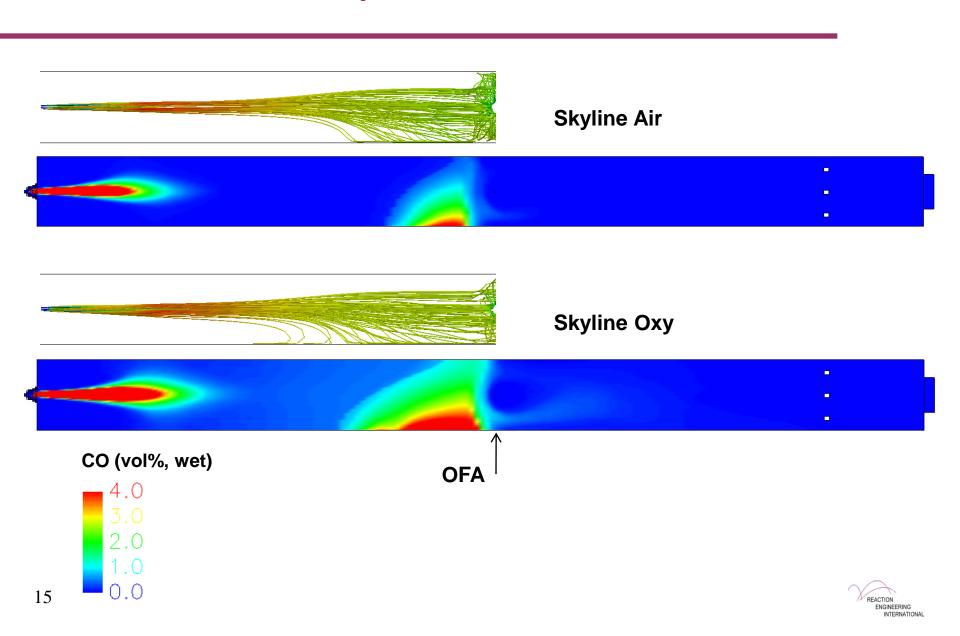


### Average CO Concentration Comparison





## Particle Trajectories and CO Profiles

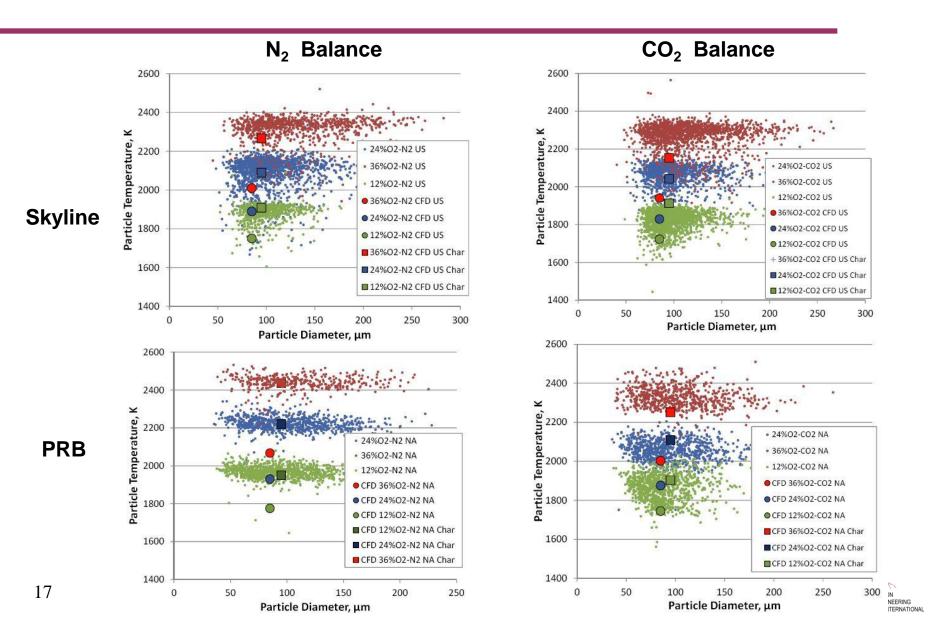


### **Extended Char Oxidation Model**

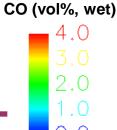
- Model development previously presented (Geier, Shaddix, Davis, Shim, "On the Use of Single-Film Models to Describe the Oxy-fuel Combustion of Pulverized Coal Char", 2011 Clearwater Clean Coal Conference)
- Based on work by Shaddix and Geier at Sandia using measurements in EFR and SKIPPY modeling
- Start with heterogeneous surface reactions
- Add Extended Single Film model including:
  - Steam gasification
  - CO<sub>2</sub> gasification



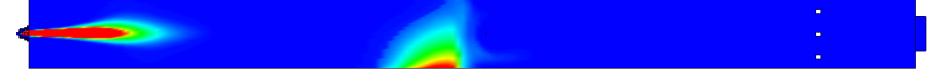
### Comparisons with Lab-scale Data



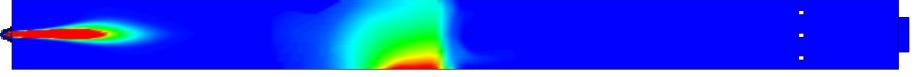
# CO Concentration Profiles Skyline Coal



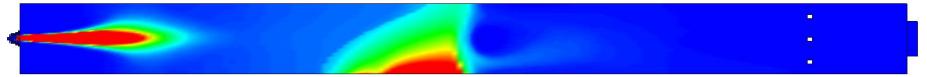
Air With Original Char Oxidation



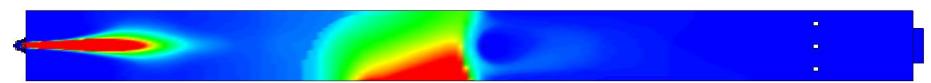
Air With Extended Char Oxidation



Oxy With Original Char Oxidation

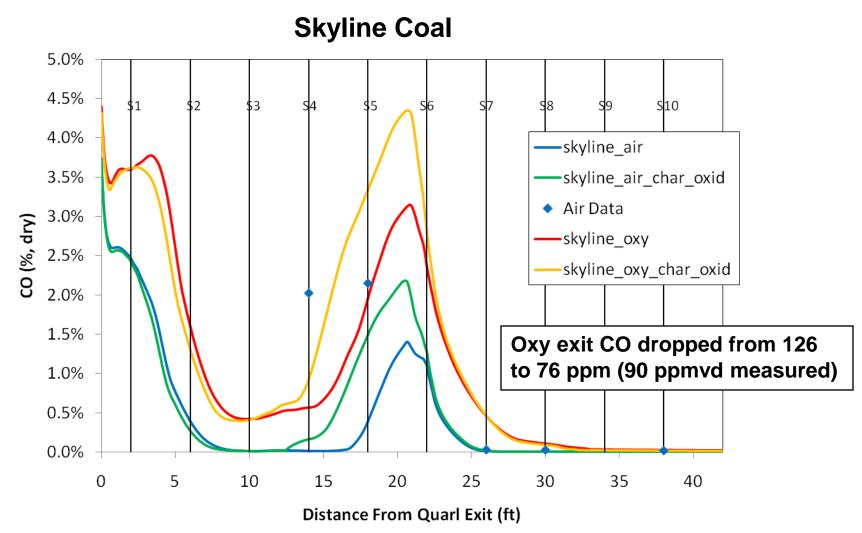


Oxy With Extended Char Oxidation





## CO Concentration Comparison





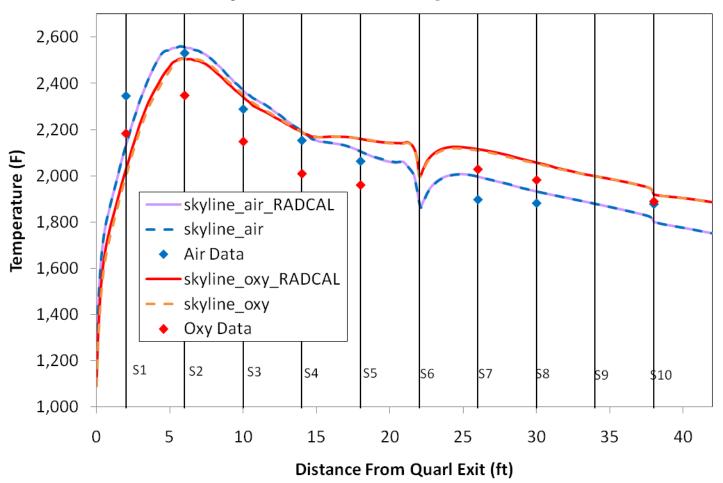
### Radiative Emissivity Model Impacts

- Evaluate impact of narrow band gas emissivity model
  - Original model is hybrid Hottel Chart weighted sum of gray gases model
  - Advanced model is narrow band model based on RADCAL code by NIST
  - Previous work has suggested:
    - Minimal emissivity impacts for short path lengths
    - Particle radiation dominates gas radiation in flame zone



## Radiative Emissivity Model Comparison

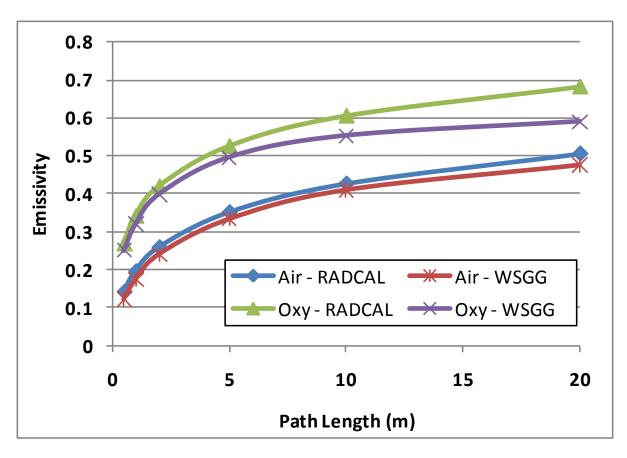
### **Skyline Coal - Temperature**





### **Emissivity Model Comparison**

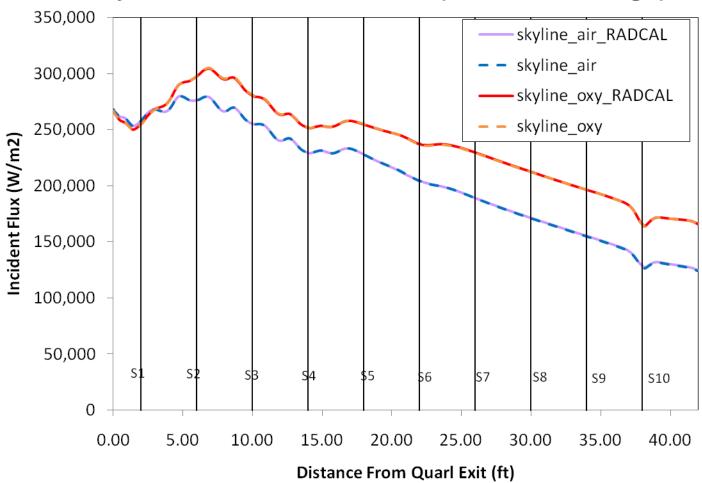
#### **Gas at 1500 K**





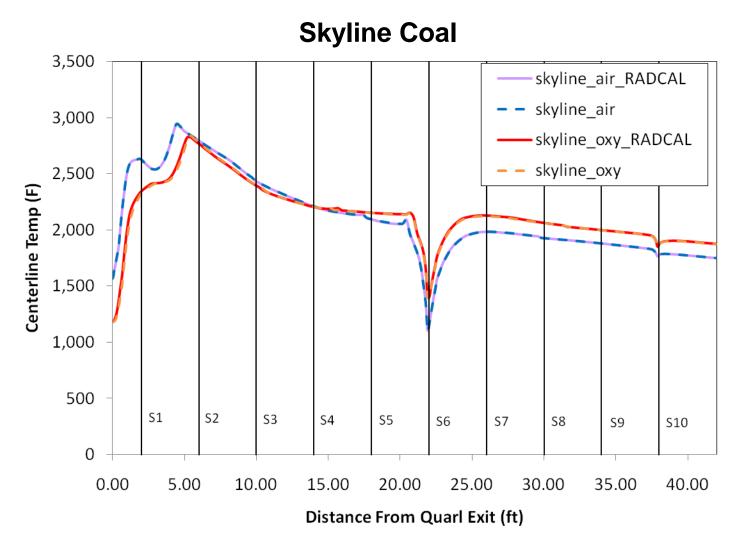
### Incident Radiative Heat Flux Comparison

### Skyline Coal - Incident Flux (one wall average)





### Furnace Centerline Temperature



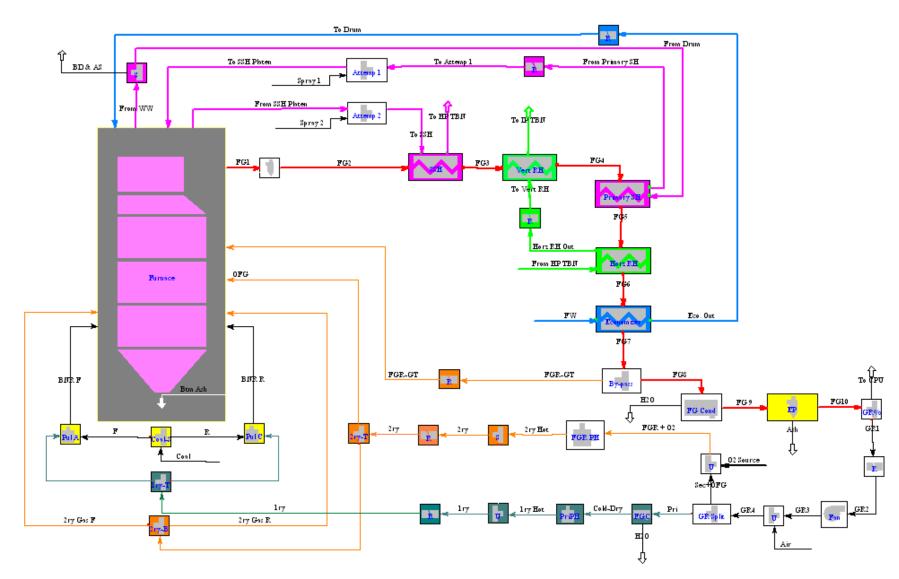


### Conclusions

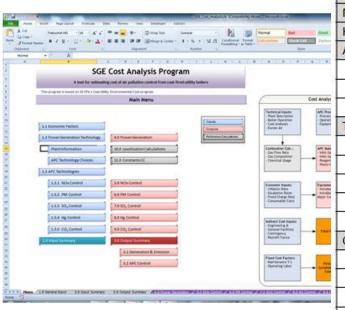
- Predicted gas temperature trends were correct, including temperature cross-over; oxy-fired predictions higher than measured data in staged zone
- Enhanced char oxidation model showed increased CO production in staged zone and better agreement with air data
- Refined gas emissivity model had negligible impact on results
- Model comparisons are on-going, and will also include soot and corrosion data
- Current activity includes oxy-combustion assessment in fullscale boilers (Hunter and River Rouge)



### Steam Gen Expert (SGE) Process Modeling



## Oxy-coal Retrofit Cost Analysis



	DOE/NETL*		CUECost	
	Ref	CO <sub>2</sub> Capture	Ref	CO <sub>2</sub> Capture
Gross MW	580	663	580	663
NetMW	550	550	547	555
Heat Rate (Btu/kWh)	8687	12002	8687	12002
Auxiliary power (MW)	30	113	33	108
Base plant load	26	42	26	42
FG Cleanup (SCR, baghouse, FGD, CO₂ capture)	4	26	7	12
CO <sub>2</sub> compression		45	-	54
Total plant capital cost (\$/kWe)	1647	2913	1729	2904
% increase		77%		68%
Base Plant (including SCR)	1413	1763	1476	1595
PM & SO <sub>x</sub> capture	234	297	253	303
CO <sub>2</sub> capture	82	766	S	882
CO <sub>2</sub> compression	(+	87		124
COE(\$/MWh) (levelized)	74.7	135.2	65.3	121.3
Capital	40.2	75.7	31.8	53.2
O&M	34.4	52.4	33.5	61.0
Fuel	18.0	24.9	18.9	29.4
Variable	6.3	11.0	6.4	16.9
Fixed	10.1	16.5	8.2	14.7
CO <sub>2</sub> TS&M	57	7.1	2	7.1
Increase in COE (%)		81		86
\$/tonne CO <sub>2</sub> avoided		69		79



### Acknowledgments

- This material is based upon work supported by the Department of Energy under Award Number DE-NT0005288, Timothy Fout Program Manager
- University of Utah Industrial Combustion and Gasification Research Facility technical staff
- CFD results displayed with Fieldview by Intelligent Light (www.ilight.com)



### Retrofit Assessment Capability

## Evaluate impact of oxy-firing design and flue gas recycle (FGR) ratio and composition on:

- Combustion Characteristics
  - Heat transfer (temperature, emissivity, sooting)
  - Particle ignition, char burnout
  - NOx, SOx, fine particulates
- Surface Characteristics
  - Heat flux profiles
  - Slagging
  - Fouling
  - Corrosion

