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Heat and Mass Transfer in Porous CO₂ Sorbent Particles

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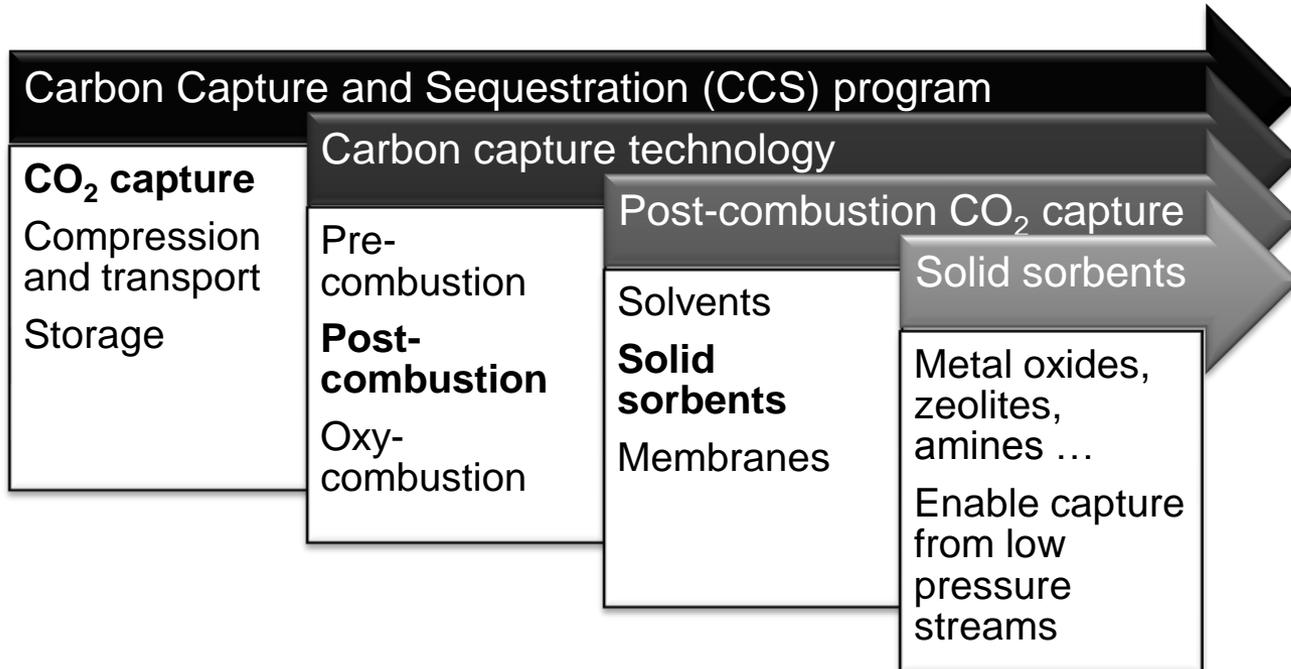
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Overview

- Introduction
- Approach
- Immersed Boundary Method
- Porous Medium Reconstruction
- Results
- Major Achievements
- Future work

Introduction

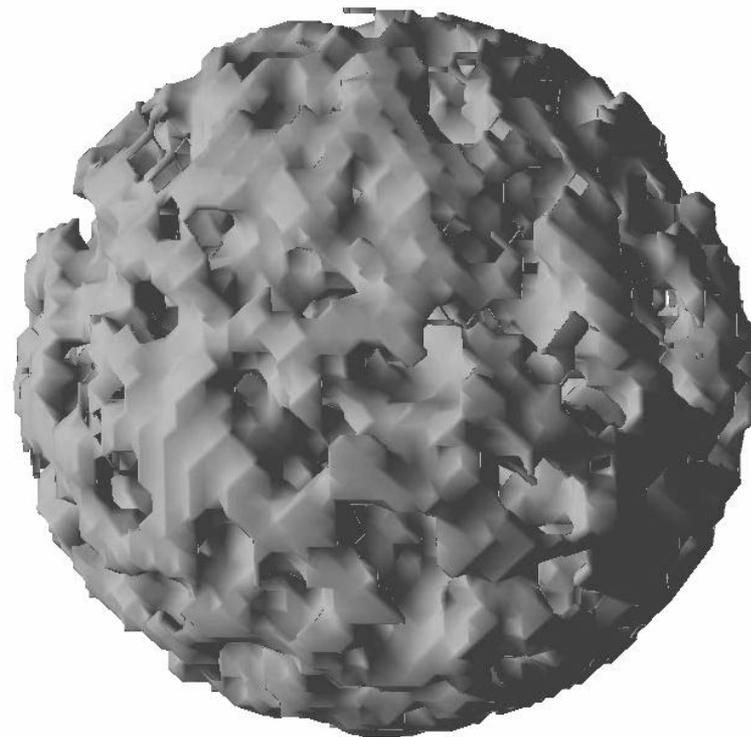


Achieve 90% CO₂ capture at less than a 30% increase levelized cost of electricity (COE) of post-combustion capture for new and existing coal-fired power plants ^[1]

Introduction

- Transfer of **heat and mass** in **porous particles** – a problem central to **solid sorbent CO₂ capture** processes
- Capture of CO₂ involves modeling of **species diffusion** and **reaction kinetics** through **complex porous microstructures**

Quantify the flow of heat and CO₂ with other gases into the porous particles with measured porosity and microstructure



A spherical particle generated with a porosity of 0.45

Approach

Immersed boundary method (IBM)

- Capability to resolve complex geometries
- Conjugate heat transfer and species transport modules

Porous reconstruction

- Use optimized stochastic reconstruction methods
- Perform X-ray CT imaging to obtain statistical descriptors

Understand involved process variables

- Perform DNS calculations to resolve the porous microstructure

Help improve CO₂ capture

- Could potentially lead to design of tailored microstructures to best achieve the adsorption process

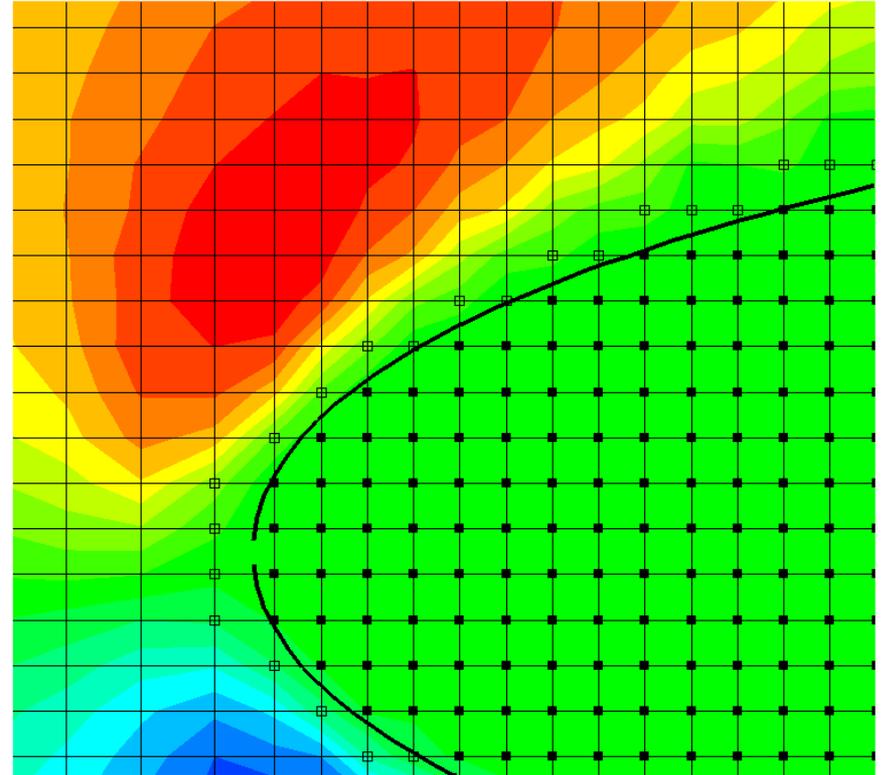
Approach

*Immersed boundary
method (IBM)*

- *Capability to resolve complex geometries*
- *Conjugate heat transfer and species transport modules*

IBM Implementation

- Adapted from Gilmonov et al. (2003)^[2]
- Steps
 - Identify the IB nodes – nodes closest to the boundary
 - Computations only on the fluid nodes (not on IB and solid nodes)
 - Change values at IB nodes – to satisfy the correct BC
- Implementation is within the framework of our in-house code – GenIDLEST



Calculation of flow over an airfoil performed on a background orthogonal mesh

IBM Implementation

GenIDLEST

- Turbulent flow on non-orthogonal meshes
- Optimized linear solvers
- Heat transfer and species transport
- Parallel framework

IBM implementation

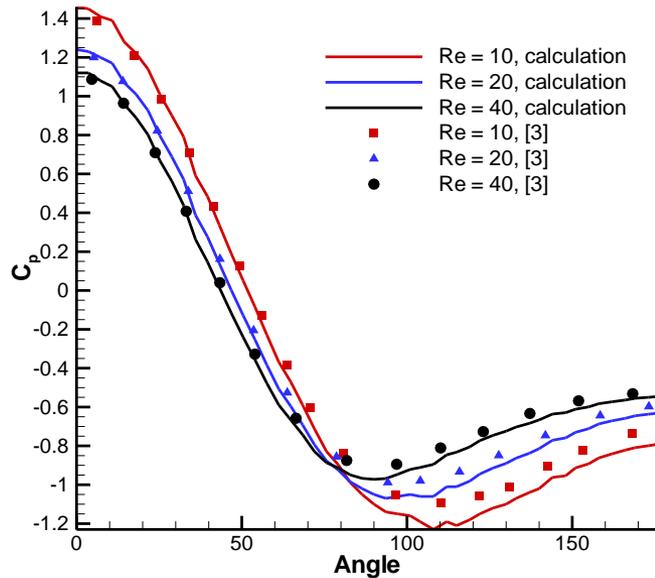
- Conjugate heat transfer
- Arbitrary solid shapes
- Movement/evolution of boundaries

GenIDLEST
+ IBM

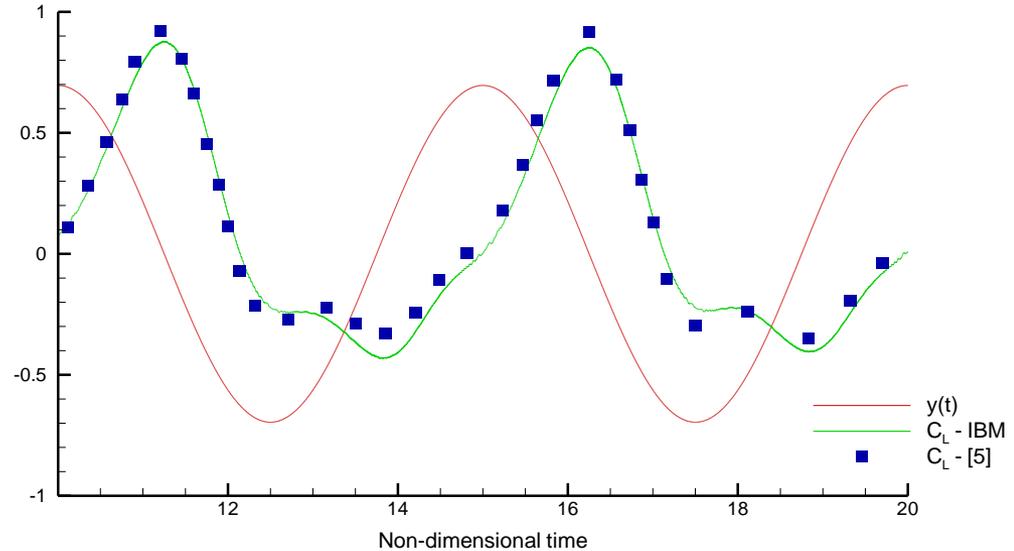
Simulation of main flow through complex geometries on non-orthogonal grids

Complex evolving porous microstructure simulation using IBM

Fluid Flow with IBM



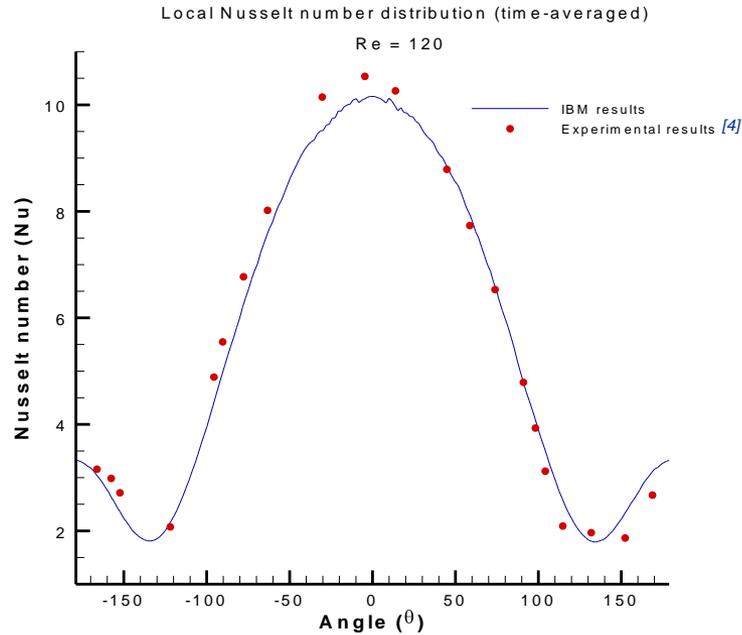
Pressure coefficients obtained for steady flow over a stationary cylinder



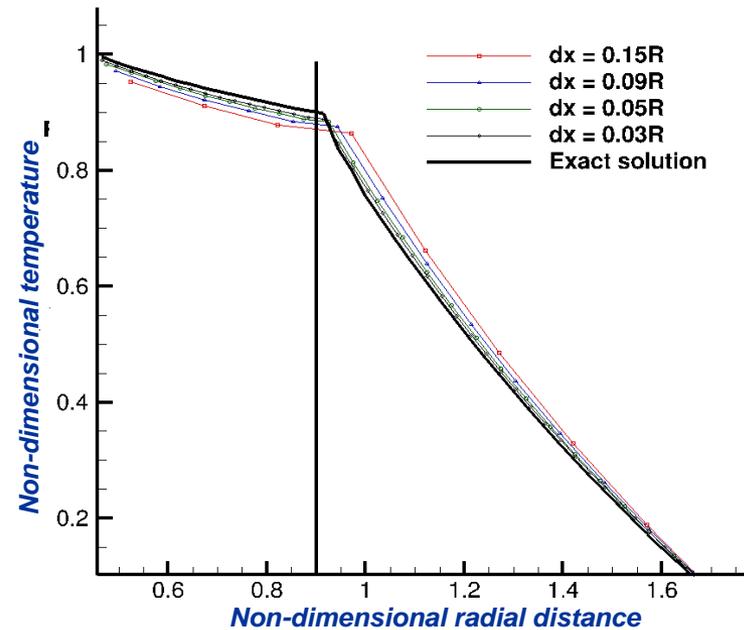
Lift coefficient comparison with experiments obtained for an oscillating cylinder at $Re = 200$

Validations performed for stationary and moving boundary cases for a variety of 2D and 3D problems

Heat Transfer with IBM



Time-averaged local Nusselt number distribution on a stationary cylinder at $Re = 120$ for isothermal case



Comparison of temperature fields obtained in a conjugate heat transfer setup between coannular cylinders at various grid levels

Validations and comparisons with boundary conforming code results performed check different heat transfer BCs

Approach

Immersed boundary method (IBM)

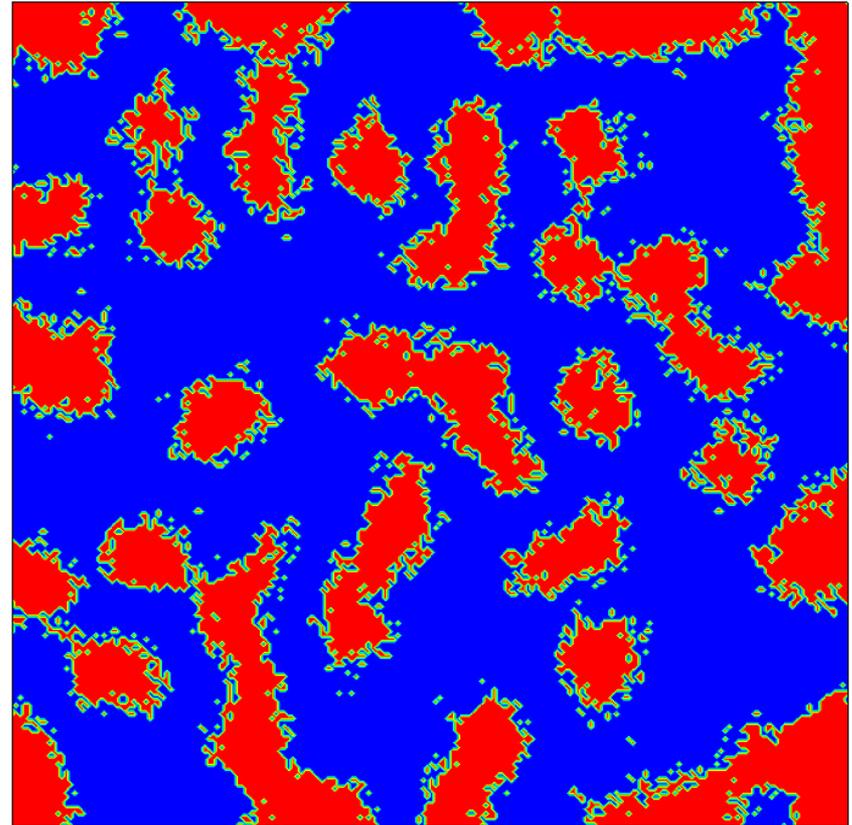
- *Capability to resolve complex geometries*
- *Conjugate heat transfer and species transport modules*

Porous reconstruction

- *Use optimized stochastic reconstruction methods*
- *Perform X-ray CT imaging to obtain statistical descriptors*

Porous Medium Reconstruction

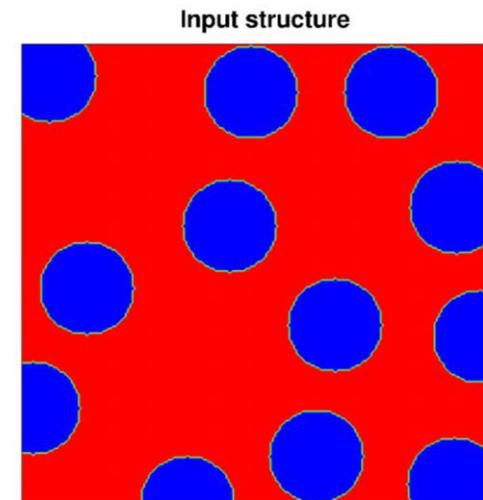
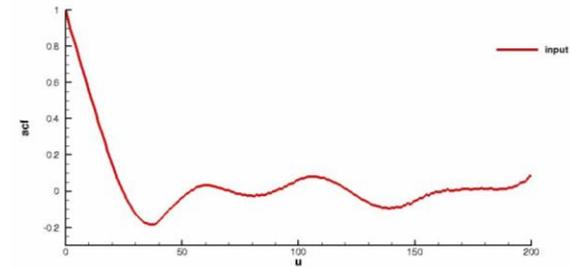
- Use of stochastic reconstruction method – **simulated annealing** [6]
- Input – experimentally determined **auto-correlation function (ACF)**
- Initial – **random field** with desired porosity
- Final – porous structure with **desired porosity and auto-correlation**



A 2D porous medium generated with a porosity of $\epsilon = 0.60$

Porous Medium Reconstruction

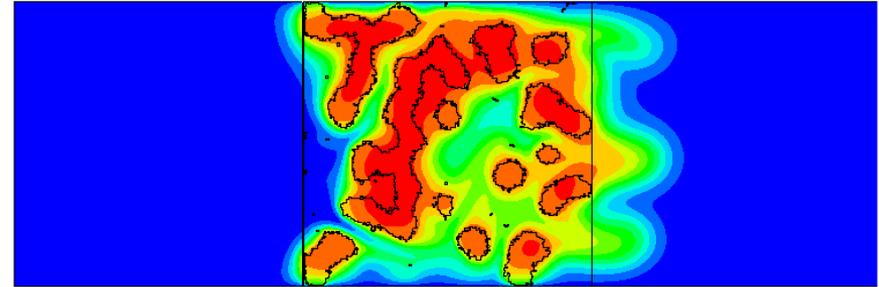
- Simulated annealing algorithm [6]
 - Obtain input ACF
 - Define a random initial distribution
 - Compute energy of the system
 - Interchange two arbitrarily chosen solid and pore nodes
 - Compute energy of the new system
 - Accept the new system based on Metropolis rule:
$$P(\Delta E) = \begin{cases} 1 & \text{if } \Delta E \leq 0 \\ \exp\left(\frac{-\Delta E}{T}\right) & \text{if } \Delta E > 0 \end{cases}$$
- Currently, arrangement of packed spheres (circles in 2D) are used for generating auto-correlation functions (2-point ACFs)



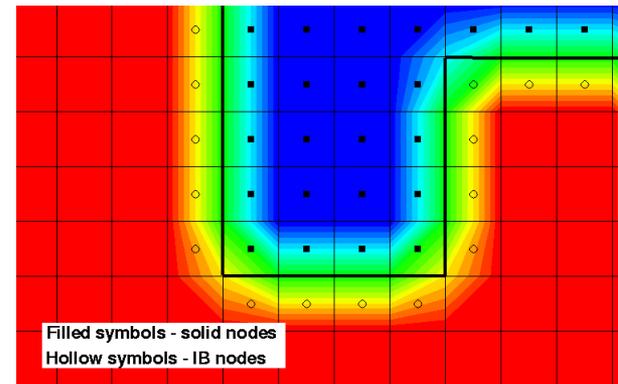
Stochastic reconstruction of a 2D porous medium with porosity of 0.75

Porous Flows with IBM

- Modified **surface element detection** for porous structures
- Input porous structure: **Binary information** (fluid – 1, solid – 0)
- Test cases
 - Comparison of pressure drops with analytical solutions
 - Species diffusion through porous particles



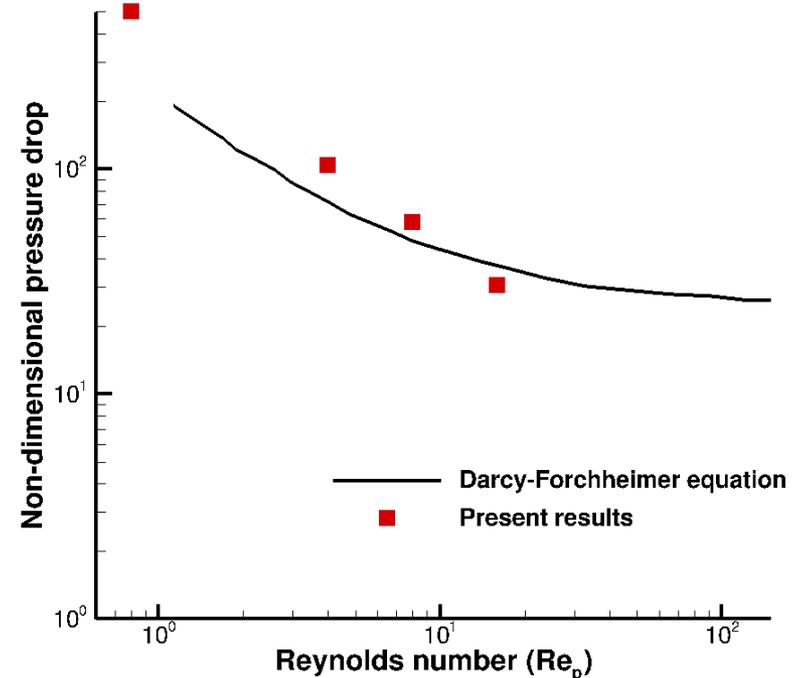
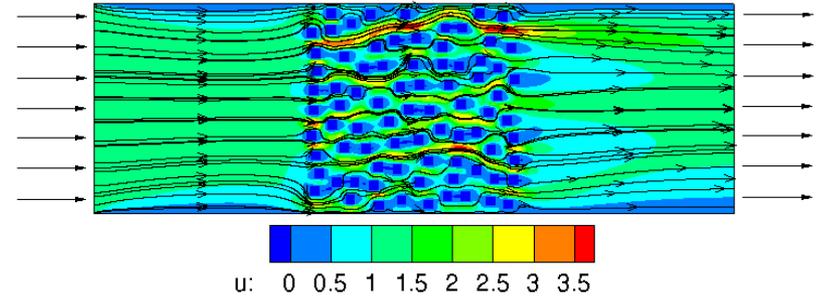
Temperature contours in a porous channel flow with conjugate heat transfer



Zoomed view of the velocity field around the porous structure and the corresponding nodal identifications

Porous Flows with IBM

- Porous media used
 - Square blocks randomly placed in a channel flow
 - “Porous channel” is squeezed between the two non-porous channels
 - 2D random porous structures generated using simulated annealing
- Pressure drops obtained using Darcy-Forchheimer equation [7]



Approach

Immersed boundary method (IBM)

- *Capability to resolve complex geometries*
- *Conjugate heat transfer and species transport modules*

Porous reconstruction

- *Use optimized stochastic reconstruction methods*
- *Perform X-ray CT imaging to obtain statistical descriptors*

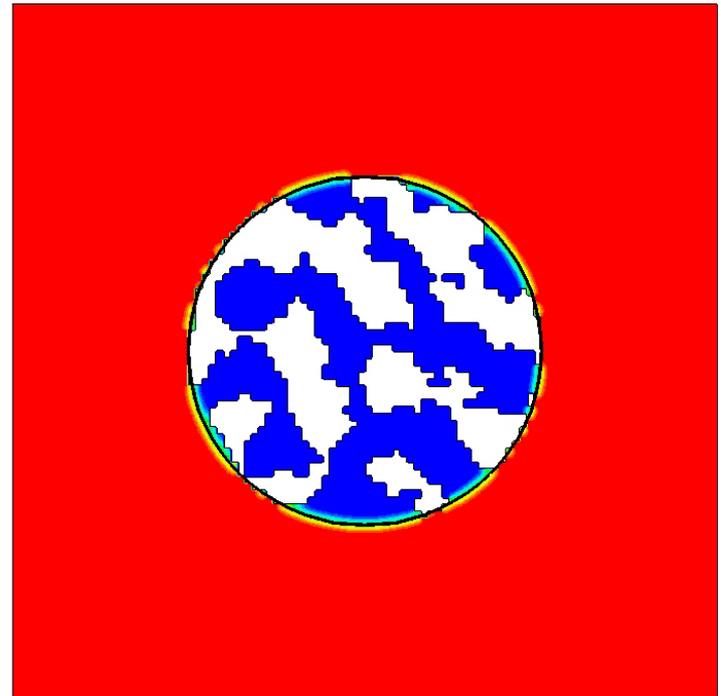
Understand involved process variables

- *Perform DNS calculations to resolve the porous microstructure*

Species Diffusion

- Transport of species into porous particles (2D)
 - Square cavity with 15% CO₂ concentration at the walls
 - Zero gradient BC at the porous medium walls
 - Initial - 15% CO₂ in air outside
 - Particle diameter – 500 microns

spcs1: 0.01 0.02 0.03 0.04 0.05 0.06 0.07 0.08 0.09 0.1 0.11 0.12 0.13 0.14

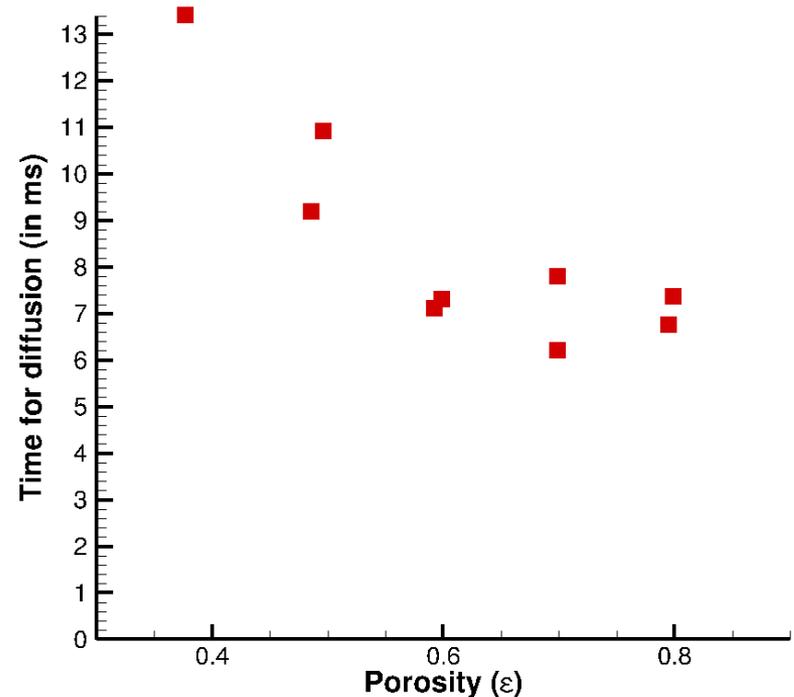


Time = 0.00 ms

Diffusion of CO₂ into a porous 2D particle

Species Diffusion

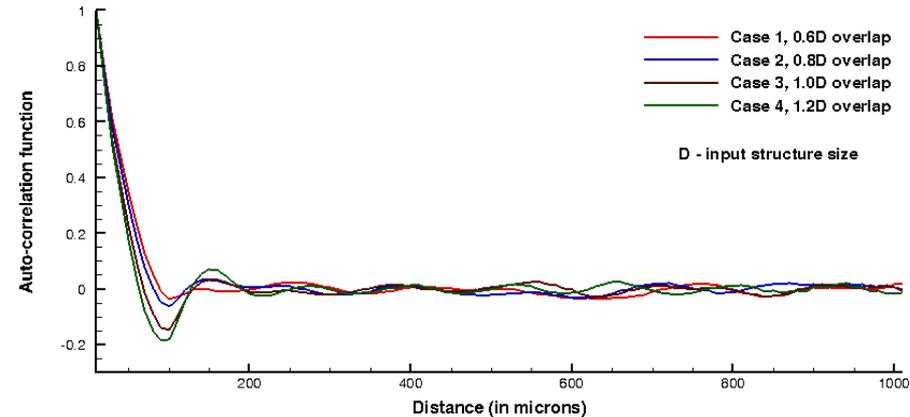
- Particle diameter (2D) - 500 microns
- Time taken for CO₂ diffusion – 95% of the ambient value
- Varying particle porosities
- Is the time affected by the structural characteristics – the auto-correlation function?



Diffusion times observed for a 500 micron 2D porous particle with varying porosities

Species Diffusion

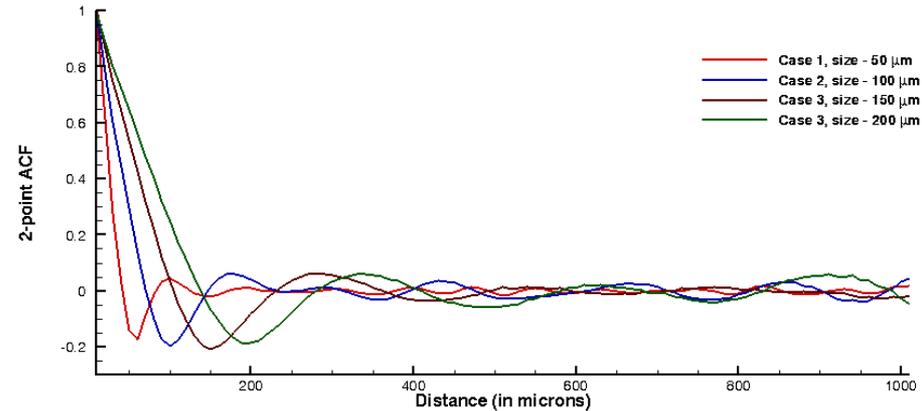
- Variation with change in the ACF
 - Overlap distance between the input structures ($\epsilon = 0.60$)



Overlap	Time for diffusion (ms)
0.6 D	7.995
0.8 D	7.246
1.0 D	6.01
1.2 D	7.709

Species Diffusion

- Variation with change in the ACF
 - Overlap distance between the input structures ($\varepsilon = 0.60$)
 - Size of the input structures ($\varepsilon = 0.75$)



Size (μm)	Time for diffusion (ms)
50	6.85
100	6.66
150	6.911
200	7.29

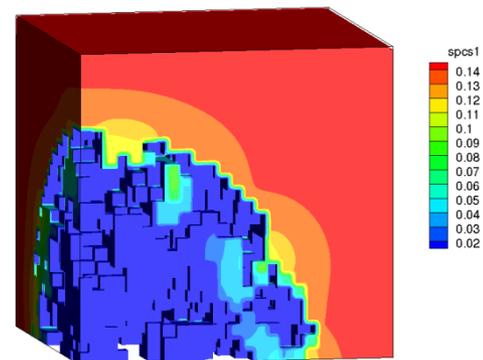
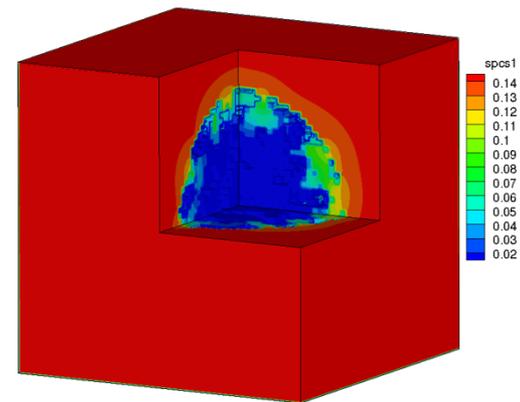
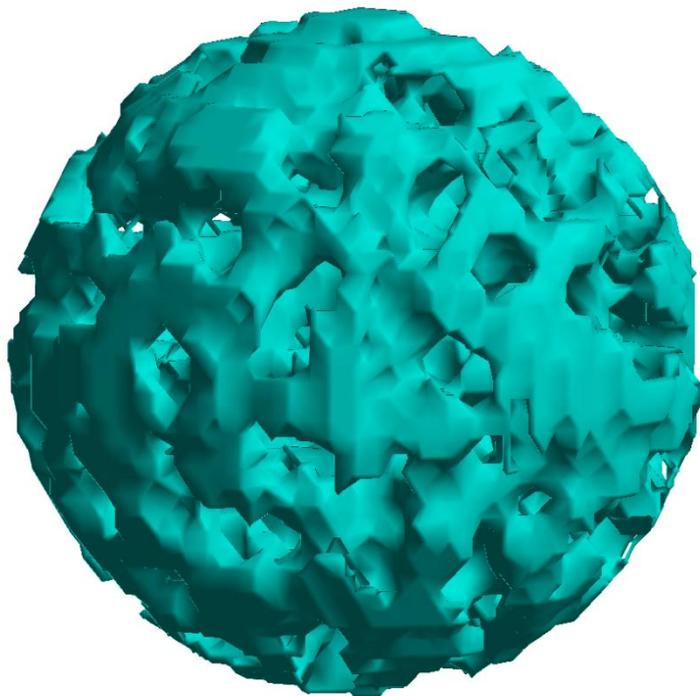
Species Diffusion

- Variation with change in the ACF
 - Overlap distance between the input structures ($\varepsilon = 0.60$)
 - Size of the input structures ($\varepsilon = 0.75$)
- No definite pattern observed so far
 - Simulations performed for $\varepsilon > 0.60$, for which diffusion time is in the **asymptotic range**

Overlap	Time for diffusion (ms)
0.6 D	7.995
0.8 D	7.246
1.0 D	6.01
1.2 D	7.709

Case	Time for diffusion (ms)
1	6.85
2	6.66
3	6.911
4	7.29

Species Diffusion



*Contour plots obtained from a 3D diffusion simulation
through a porous particle ($\epsilon = 0.45$)*

Major Achievements

- Capability to handle arbitrary 2-D and 3-D surface contours
 - Validation for stationary and moving boundary problems
- Temperature BC for heat transfer studies into IBM framework
 - Validation for uniform flow over a stationary cylinder
 - Includes implementation of conjugate heat transfer
- Porous flow simulation
 - Stochastic reconstruction of arbitrary porous structures
 - Simulation and comparison with analytical results
 - Species diffusion through 2D and 3D porous particles

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Help improve CO₂ capture

- *Could potentially lead to design of tailored microstructures to best achieve the adsorption process*

Future work

- **Parallelization** of IBM framework to enable faster computations (a major bottle-neck currently)
- **Digital reconstruction** of porous microstructure of typical sorbent particles through X-ray CT (or TEM/SEM) imaging
- Use of **physical CO₂ adsorption rates** in simulations depending on the local surface conditions
- **Spatio-temporal evolution** of the porous microstructure with adsorption

Acknowledgements

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- Multiphase Flow Research Group (MFRG) at NETL

References

1. DOE/NETL Advanced carbon dioxide capture R&D program: Technology update, September 2010
2. A general reconstruction algorithm for simulating flows with complex 3D immersed boundaries on Cartesian grids, Gilmonov, A., Sotiropoulos, F. and Balaras E., J. Comp. Phy., Vol. 191, pp. 660-669, 2003.
3. Numerical solutions of flow past a circular cylinder at Reynolds numbers up to 160, Park, J., Kwon, K. and Choi, H., KSME Int. J., Vol. 12, No. 6, pp. 1200-1205, 1998.
4. An immersed boundary finite-volume method for simulation of heat transfer in complex geometries, J. Kim and H. Choi, KSME Int. J., Vol. 18, No. 6, pp 1026-1035, 2004.
5. Vortex wake and energy transitions of an oscillating cylinder at low Reynolds number, Stewart, B., Leontini, J., Hourigan, K. and Thompson, M.C., ANZIAM J., Vol. 46(E), pp. C181-C195, 2005.
6. A hybrid process-based and stochastic reconstruction method of porous media, Politis, M.G., Kikkinides, E.S., Kainourgiakis, M.E. and Stubos, A.K., Microporous Mesoporous Mat., Vol. 110, pp. 92-99, 2008.
7. Direct simulation of forced convection flow in a parallel plate channel filled with porous media, Rahimian, M.H. and Pourshaghagy, Int. Comm. Heat Mass Transfer, Vol 29, No. 6, pp. 867-878, 2002.



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Thank you!

Stochastic Reconstruction

- Porous medium represented by

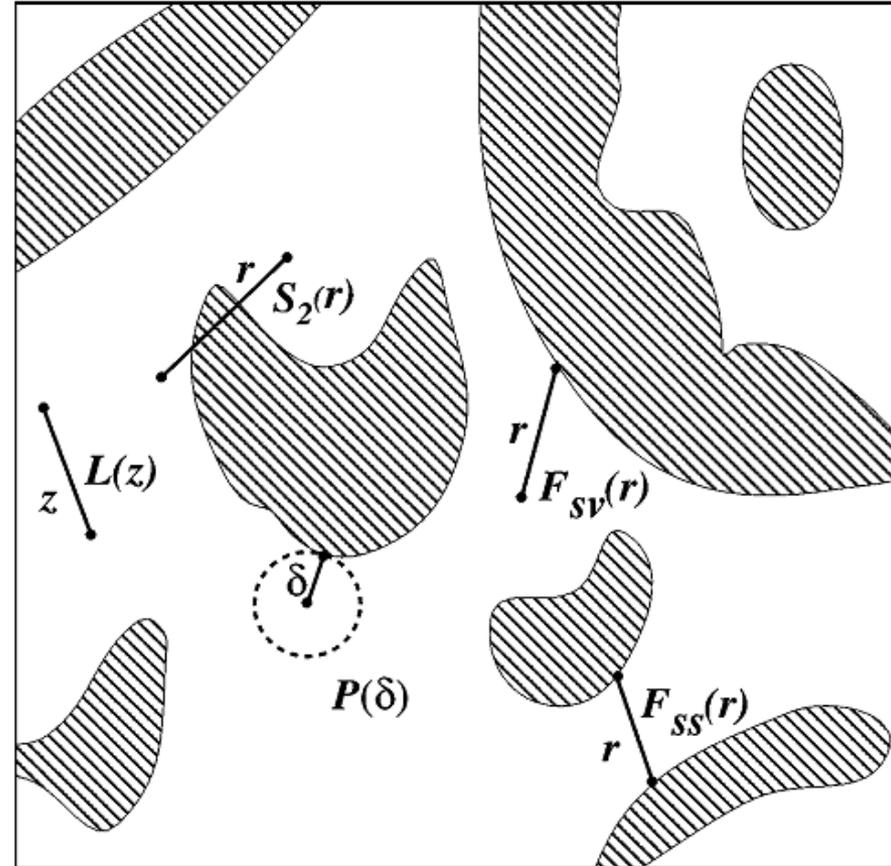
$$y(\mathbf{x}) = \{1 \text{ for pore} | 0 \text{ for solid}\}$$

- Porosity

$$\varepsilon = \langle y(\mathbf{x}) \rangle$$

- Two point correlation

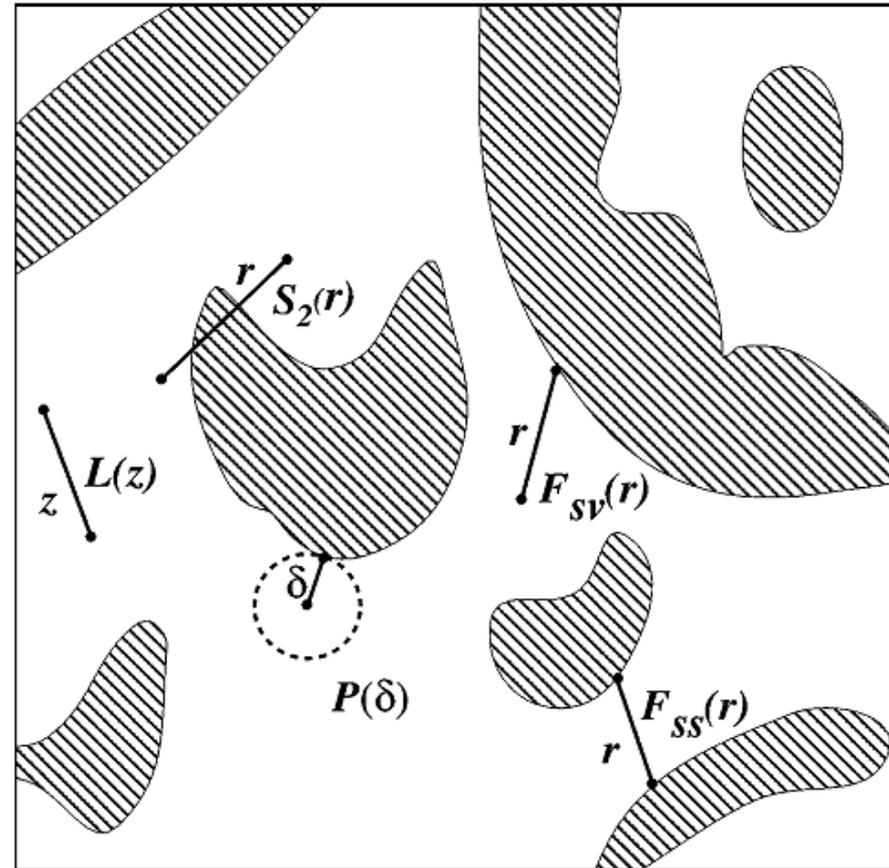
$$s_2(\mathbf{r}) = \langle y(\vec{\mathbf{x}})y(\vec{\mathbf{x}} + \mathbf{r}) \rangle$$



Taken from Ref2

Stochastic Reconstruction

- **Pore size distribution $P(\delta)$ - is the probability of finding pore space which lies from solid surface at a distance between δ and $d\delta$.**



Taken from Ref2

Simulated annealing

Steps:

$$E = \sum (f(x) - f_{ref}(x))^2 \quad (1)$$

Where f is any statistic function. In case of multiple statistic function total energy is obtained by summation with weight factor α_i

$$E = \sum \alpha_i E_i \quad (2)$$

1. Define initial distribution and find Energy (eq.1)
2. Interchange two arbitrarily chosen pore and solid
3. Compute the energy for modified system and find change in energy ($\Delta E = E_{new} - E_{old}$).
4. Accept the new configuration based on Metropolis rule(Eq.3)
5. Repeat from 2 to 4 after certain number of iteration

$$P(\Delta E) = \begin{cases} 1 & \text{if } \Delta E \leq 0 \\ \exp\left(\frac{-\Delta E}{T}\right) & \text{if } \Delta E > 0 \end{cases} \quad (3)$$

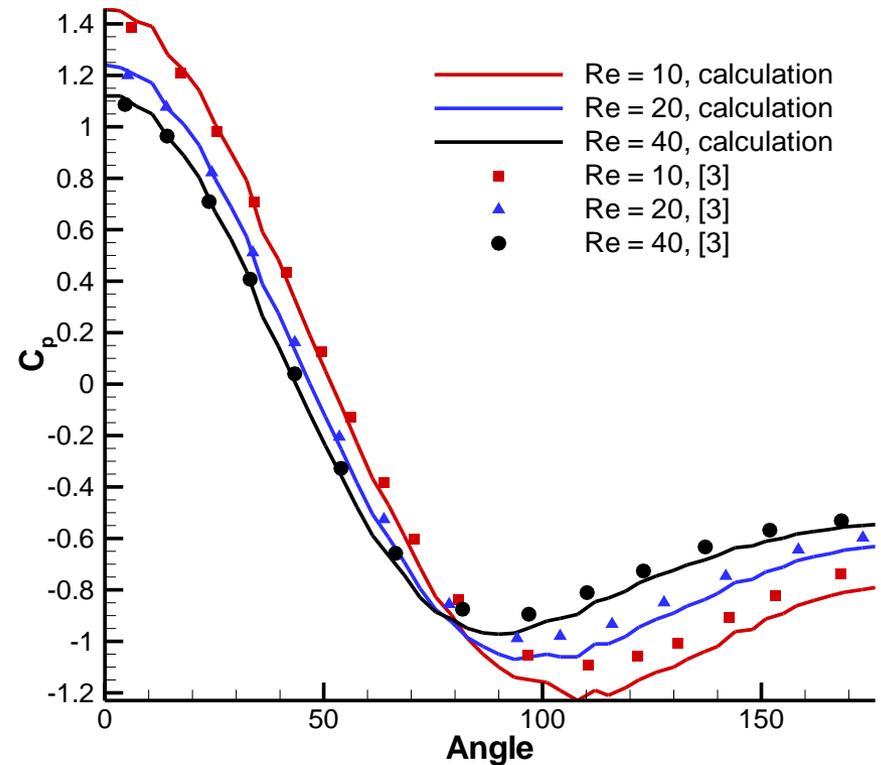
Where T is temperature and by reducing the value as iteration progress configuration with minimum deviation(low values of E) will be generated.

Stationary cylinder results

- **Steady case**

- $Re = 10, 20$ and 40
- Point of reattachment (L_w)
- Coefficient of drag (C_D)
- Comparison with Park et al. (1998)^[2]

Re	C_D	C_D [3]	L_w	L_w [2]
10	2.74	2.78	0.26	0.25
20	2.02	2.01	0.94	0.95
40	1.58	1.51	2.23	2.30



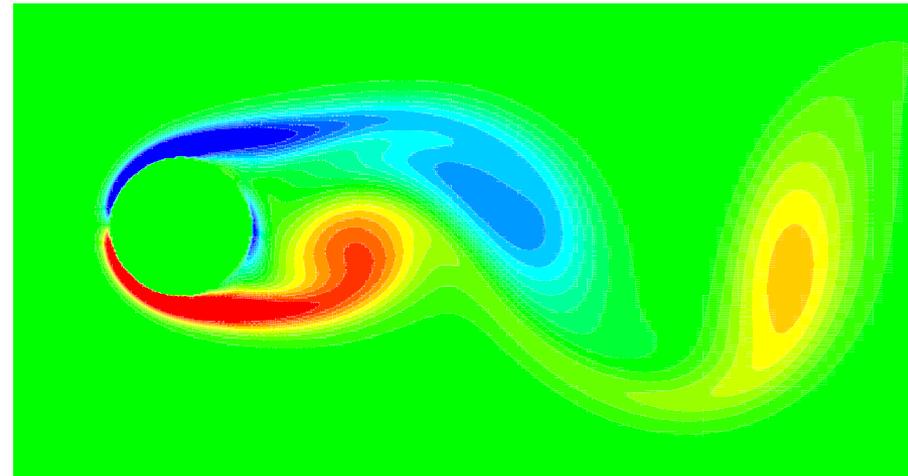
Stationary cylinder results

- **Unsteady case**

- Karman vortex street
- $Re = 100, 150$ and 200
- Strouhal number comparison

Re	St	St [3]
100	0.166	0.16
150	0.185	0.18
200	0.198	0.20

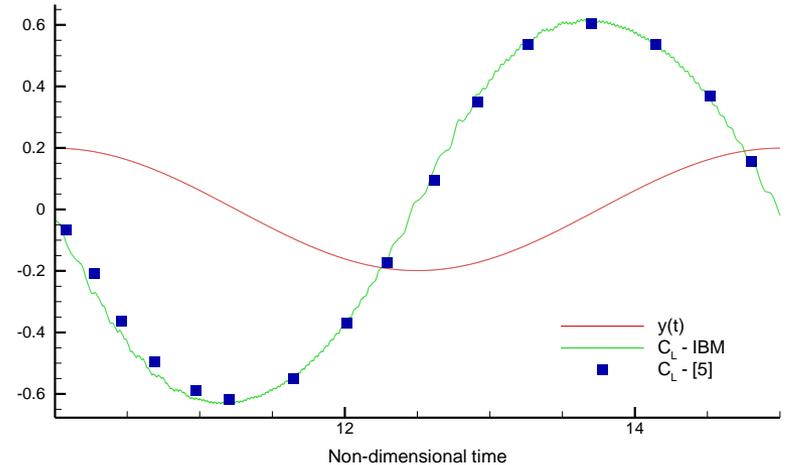
$Re = 150$



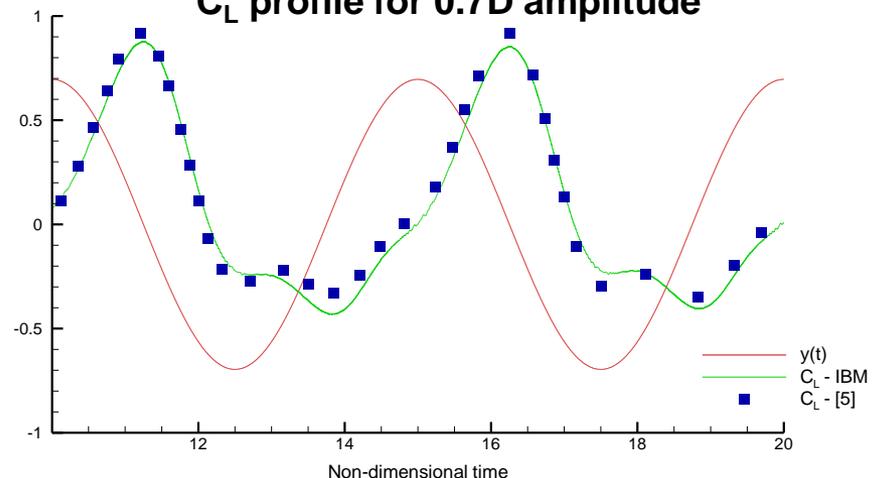
Oscillating Cylinder

- $Re = 200$
- Frequency – 0.2
- Amplitudes – 0.2D and 0.7D
- Grid size of 0.00625D
- C_L profile
 - Correct values predicted
 - Compared with numerical results of Stewart et al.^[5]
- Correct prediction of changed vortex shedding pattern for 0.7D amplitude

C_L profile for 0.2D amplitude

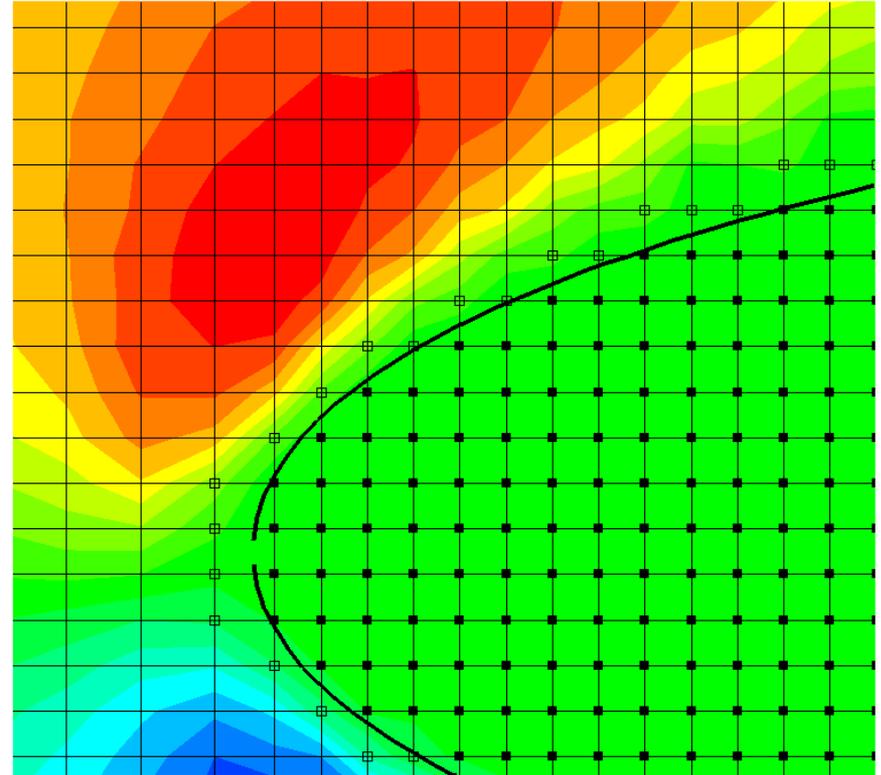


C_L profile for 0.7D amplitude



Arbitrary surface contours

- Implementation of IBM to simulate flow around solid bodies of **arbitrary shapes**
- Applicable to both **2-D** and **3-D problems**



Flow over an airfoil

Heat transfer with IBM

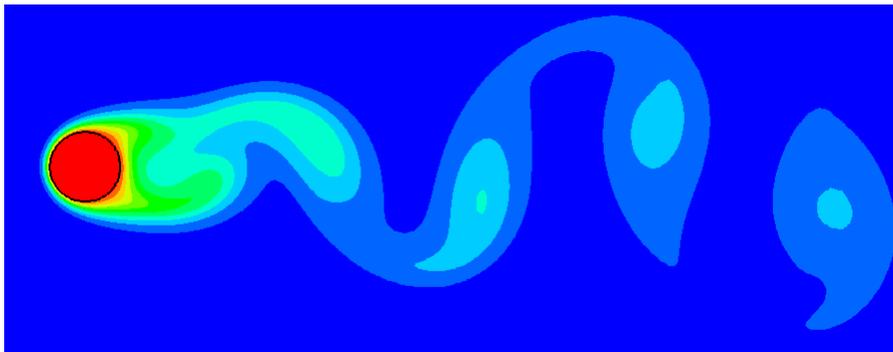
- **Temperature BC** for energy equation implemented in IBM
- **Validation** completed for uniform flow over a stationary cylinder
- Constant **heat flux** and constant **temperature** conditions implemented

- **Implementation** of conjugate heat transfer
- Results compared with exact solution
 - Rotational flow between concentric cylinders
 - Good comparison!

Heat transfer results

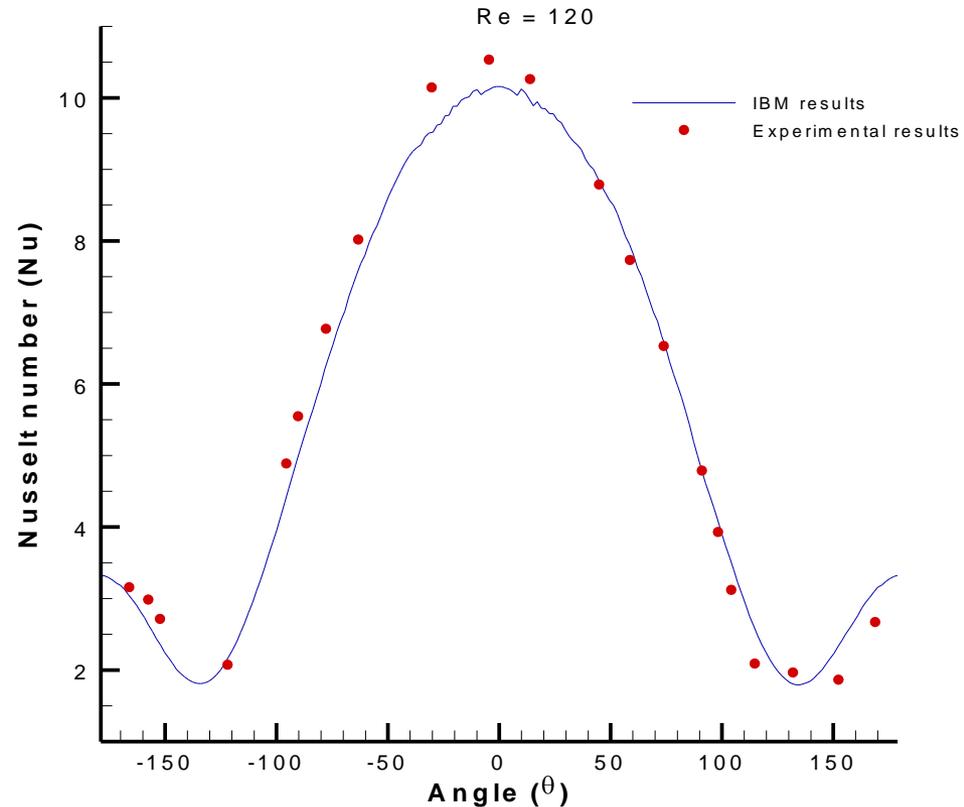
Nusselt number comparisons (iso-thermal)

Re	Experimental results [5]	Present
10	1.80	1.83
40	3.28	3.18
120	5.69	5.56

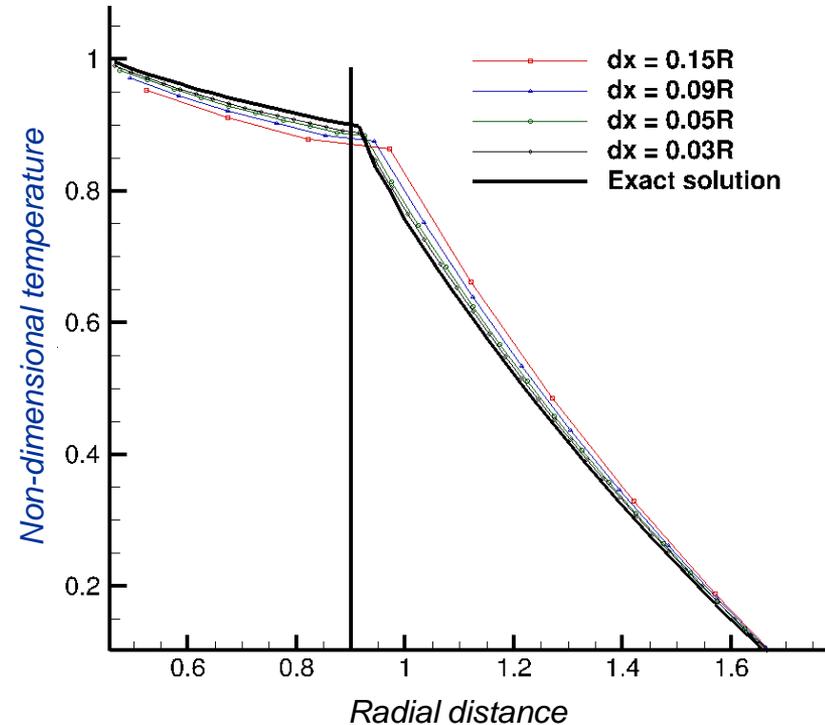
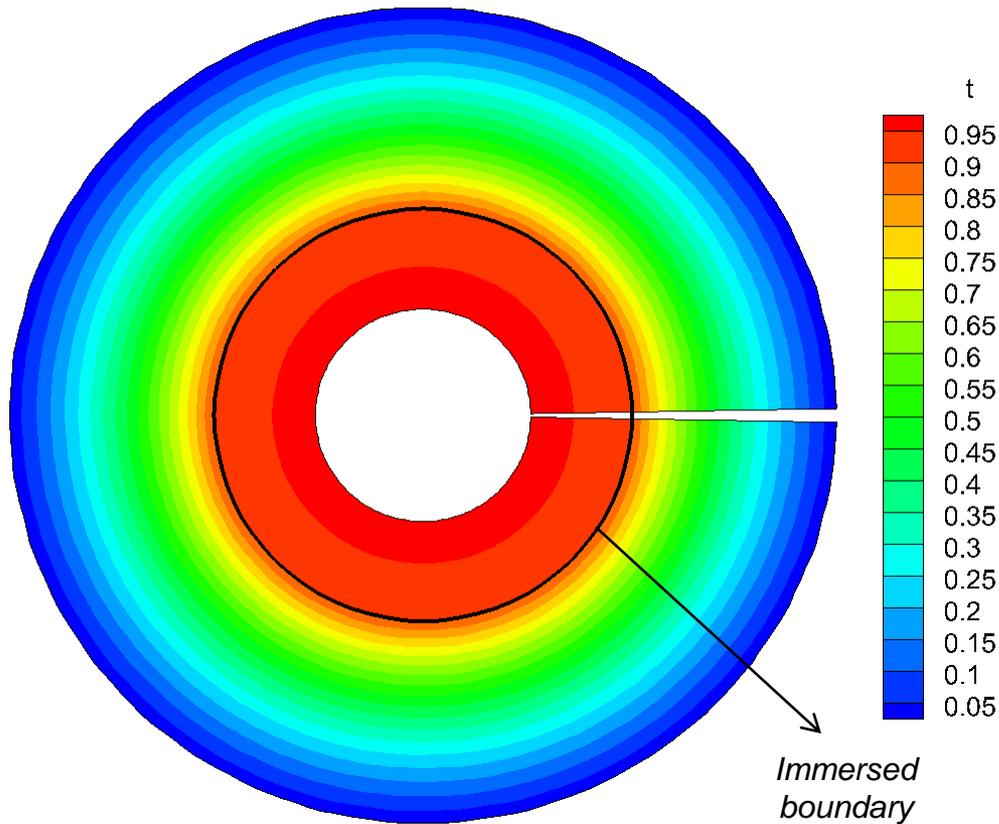


t: 0.05 0.15 0.25 0.35 0.45 0.55 0.65 0.75 0.85 0.95

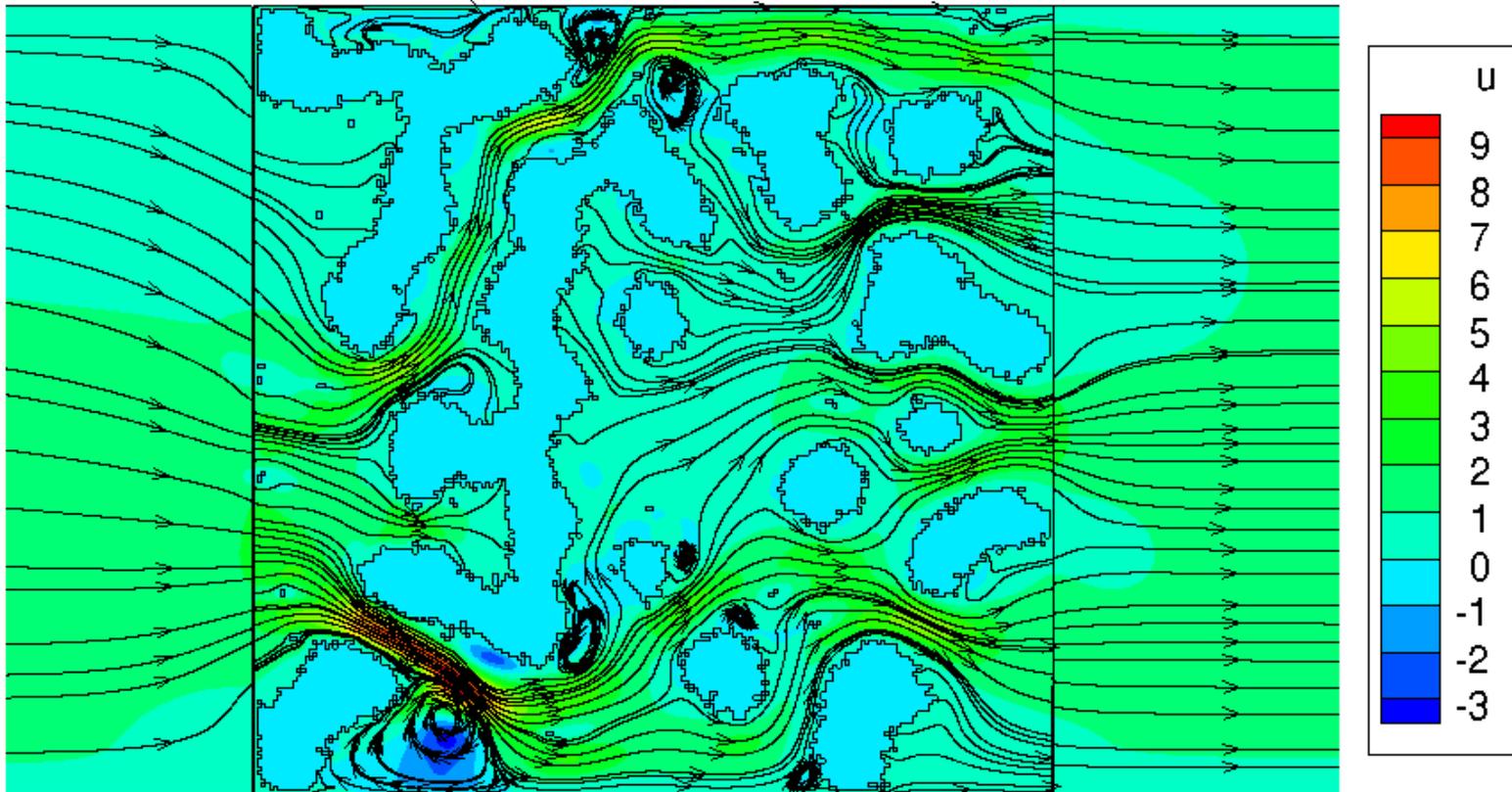
Local Nusselt number distribution (time-averaged)



Conjugate heat transfer results



Porous flows with IBM



Porous flows with IBM

