

# CCSI<sup>TM</sup>

## Carbon Capture Simulation Initiative

### Uncertainty quantification in chemistry sub-models

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Daniel J. Fauth,<sup>\*</sup> McMahan L. Gray<sup>\*</sup>

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U.S. DEPARTMENT OF  
**ENERGY**

# Carbon Capture Simulation Initiative



Identify  
promising  
concepts



Reduce the time  
for design &  
troubleshooting



Quantify the technical  
risk, to enable reaching  
larger scales, earlier



Stabilize the cost during  
commercial deployment

## National Labs



## Academia

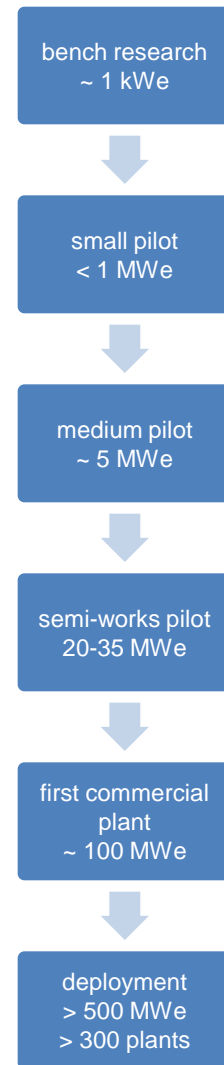


## Industry



# Carbon Capture Challenge

- The traditional pathway from discovery to commercialization of energy technologies can be quite long, i.e., ~ **2-3 decades**
- President's plan requires that barriers to the widespread, safe, and cost-effective deployment of CCUS be overcome **within 10 years**
- To help realize the President's objectives, new approaches are needed for taking carbon capture concepts **from lab to power plant, quickly, and at low cost and risk**
- CCSI will accelerate the development of carbon capture technology, from discovery through deployment, with the help of **science-based simulations**

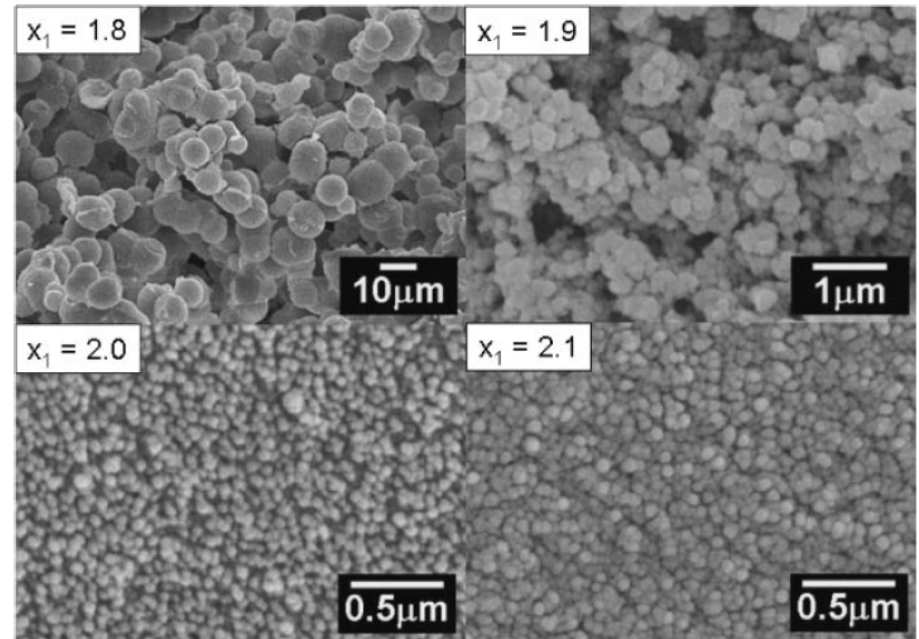


# outline

- overview of high-fidelity sorbent modeling
- Bayesian calibration applied to sorbent equilibrium models

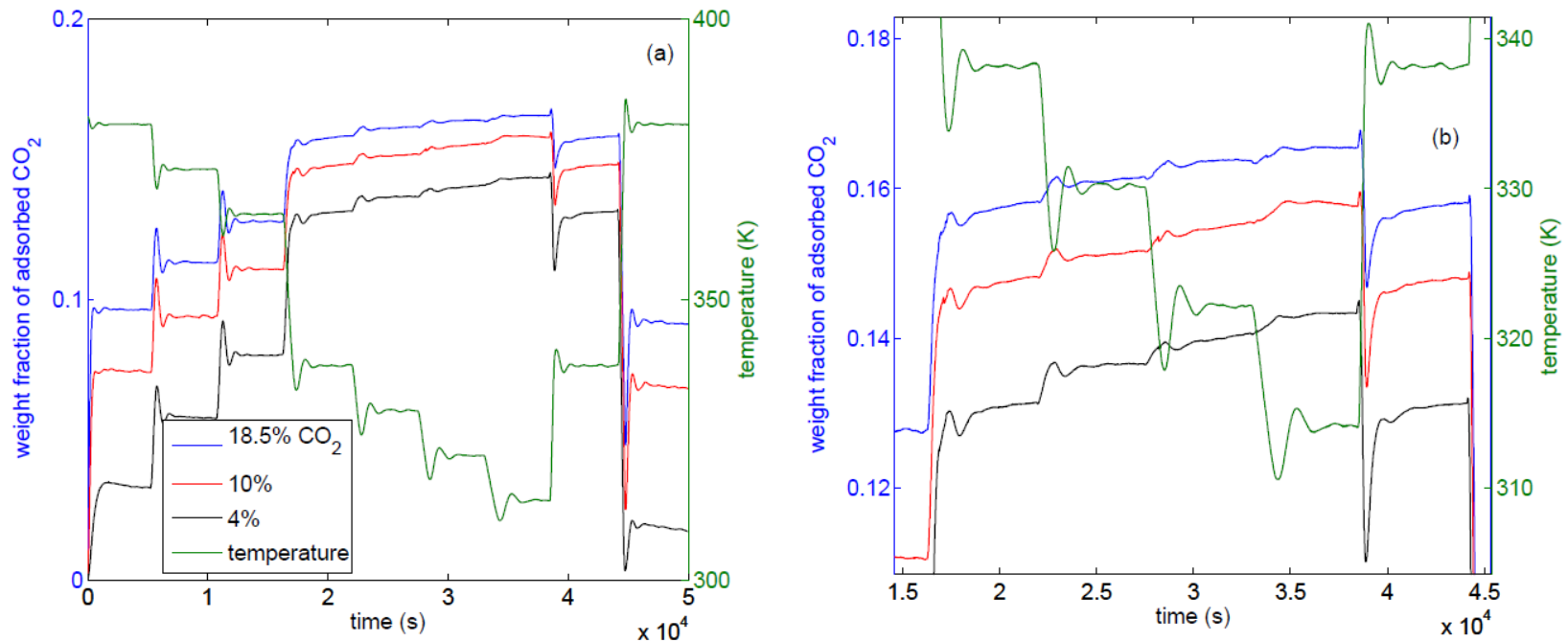
# the sorbent

- mesoporous silica forms the substrate
- substrate particles agglomerates of micron-sized mesoporous particles
- mesopores impregnated with an active material, such as polyethyleneimine (PEI)



K Kajihara, et al., Bull Chem Soc Jpn, 82 (2009) 1470.

# the sorbent: dry TGA behavior

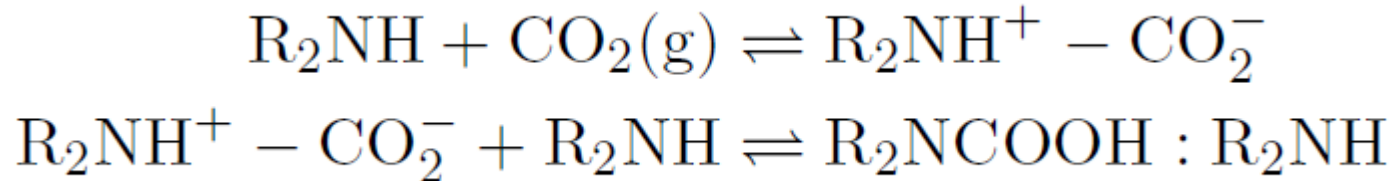


(a)-(b) Sorbent NETL-196C, ~44.1 wt-% PEI, Dry atmosphere. Sorbent synthesis: McMahan Gray, NETL; Sorbent characterization: Daniel Fauth, NETL.

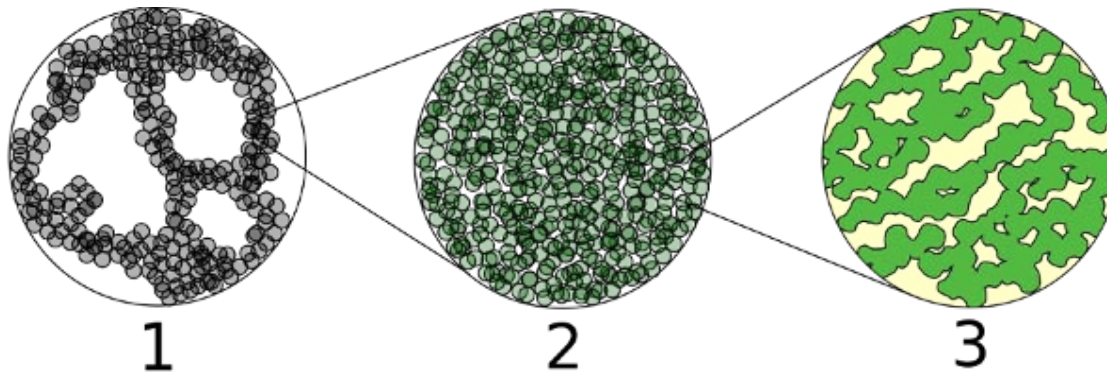


# anhydrous model

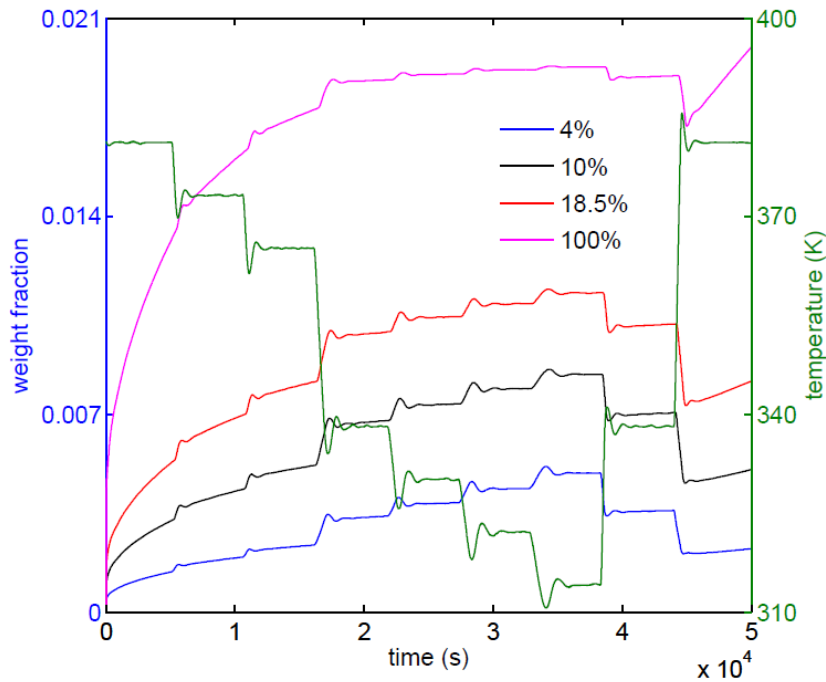
- two-step formation of carbamic acid:



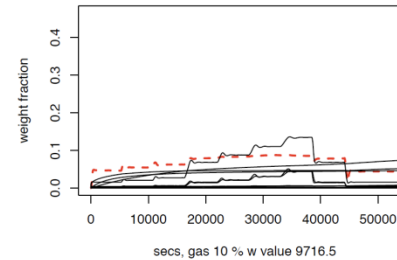
- three modes of mass transport:
  - gas phase bulk
  - gas phase Knudsen
  - solid state (zwitterion-mediated hopping)



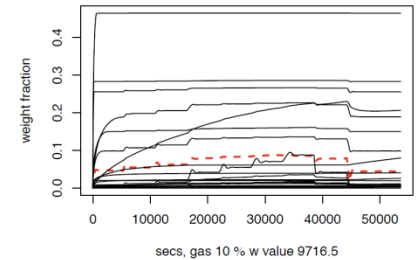
# anhydrous model



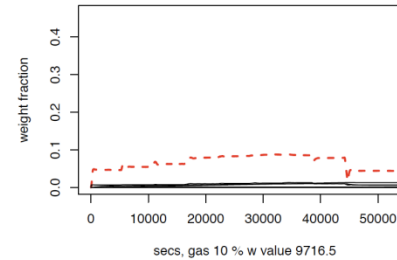
average value delta-S kap5 : low -198.276  
average value delta-H kap5 : low -43749.442



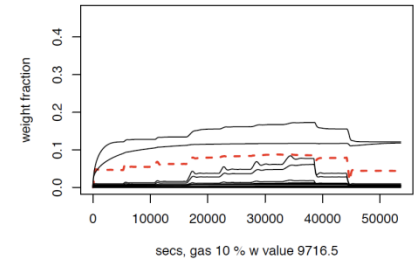
average value delta-S kap5 : high -91.691  
average value delta-H kap5 : low -45708.107



average value delta-S kap5 : low -197.458  
average value delta-H kap5 : high -17490.28



average value delta-S kap5 : high -94.555  
average value delta-H kap5 : high -18482.67

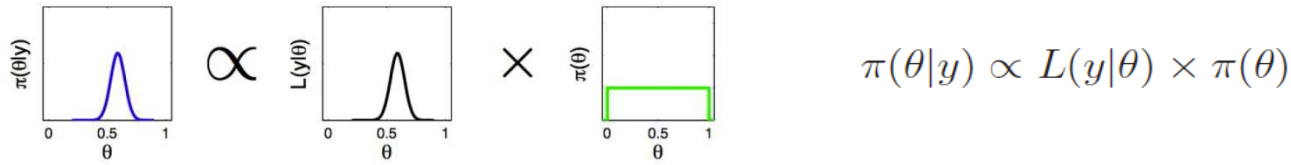


(left) sample calculated output of the sorbent model showing diffusion effects (right) sensitivity analysis highlighting the importance of zwitterion stability to sorbent working capacity



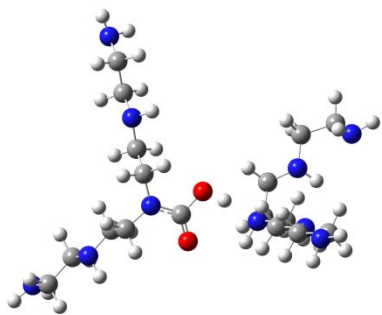
# Bayesian methods in parameter estimation

- Bayes' theorem enables the incorporation of prior information in model-based parameter estimates.

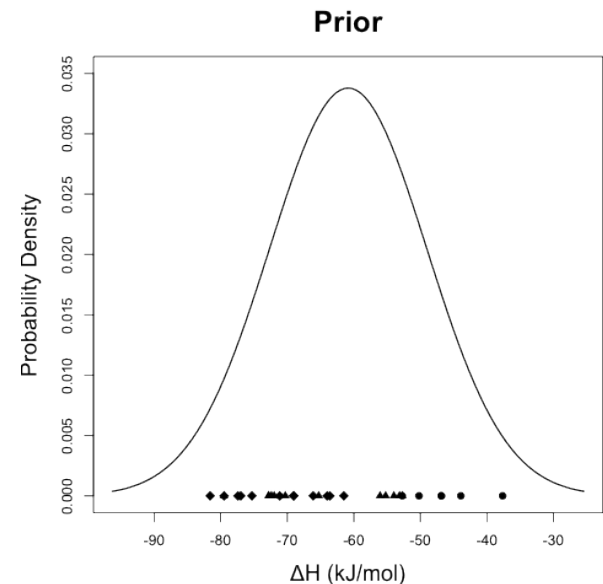


$$\pi(\theta|y) \propto L(y|\theta) \times \pi(\theta)$$

- If model parameters relate to physical quantities, prior information is available through *ab initio* calculations.



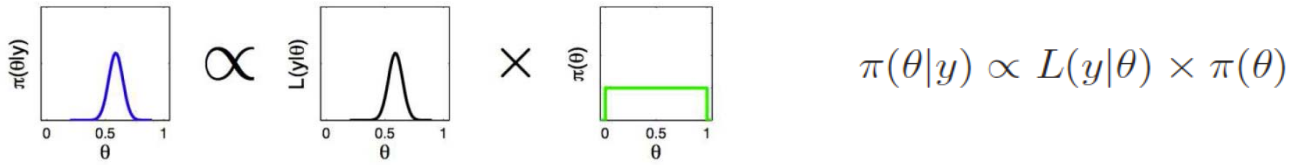
rxn	B3LYP	PBE	MP
1	-52.72	-76.36	-62.76
2	-46.86	-70.29	-62.97
3	-50.21	-72.8	-62.76
4	-46.86	-70.71	-64.43
5	-37.66	-69.04	-62.76
6	-43.93	-68.41	-72.38



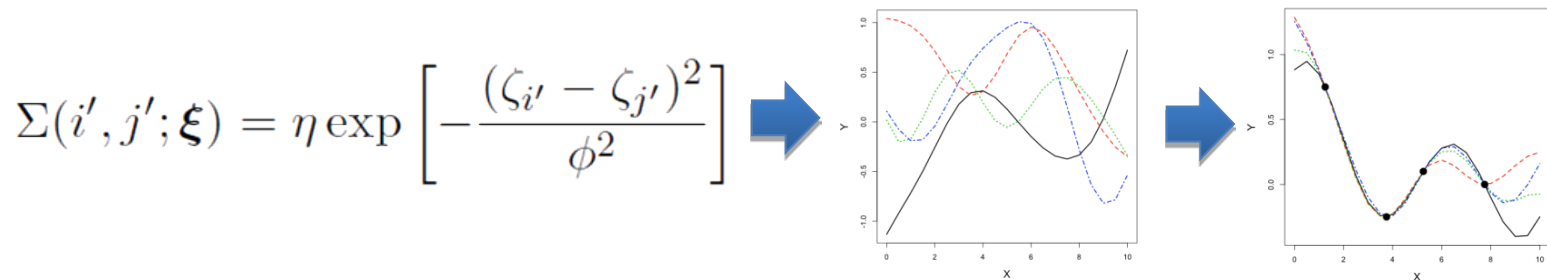
DS Mebane, KS Bhat, JD Kress, et al., in prep.

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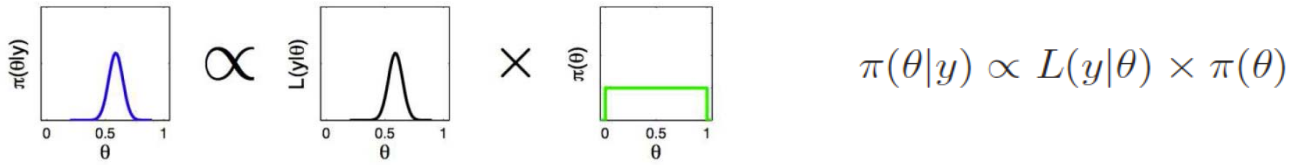


- The error in the form of the model must also be accounted for.
- A Gaussian process generates a stochastic set of curves adhering to certain general properties.



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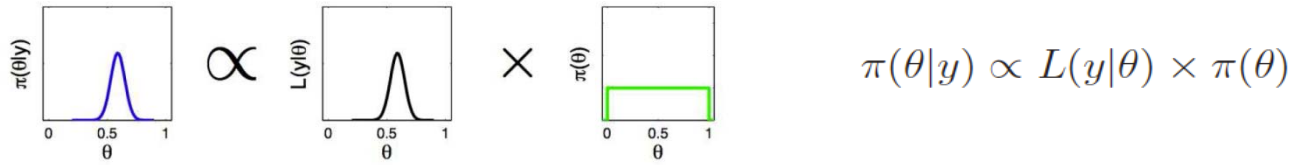
- The error in the form of the model must also be accounted for.
- A Gaussian process generates a stochastic set of curves adhering to certain general properties.

$$\mathbf{Y} = \mathbf{Z}(\boldsymbol{\theta}, \boldsymbol{\zeta}) + \boldsymbol{\delta}(\boldsymbol{\xi}, \boldsymbol{\zeta}) + \boldsymbol{\epsilon}(\boldsymbol{\psi})$$

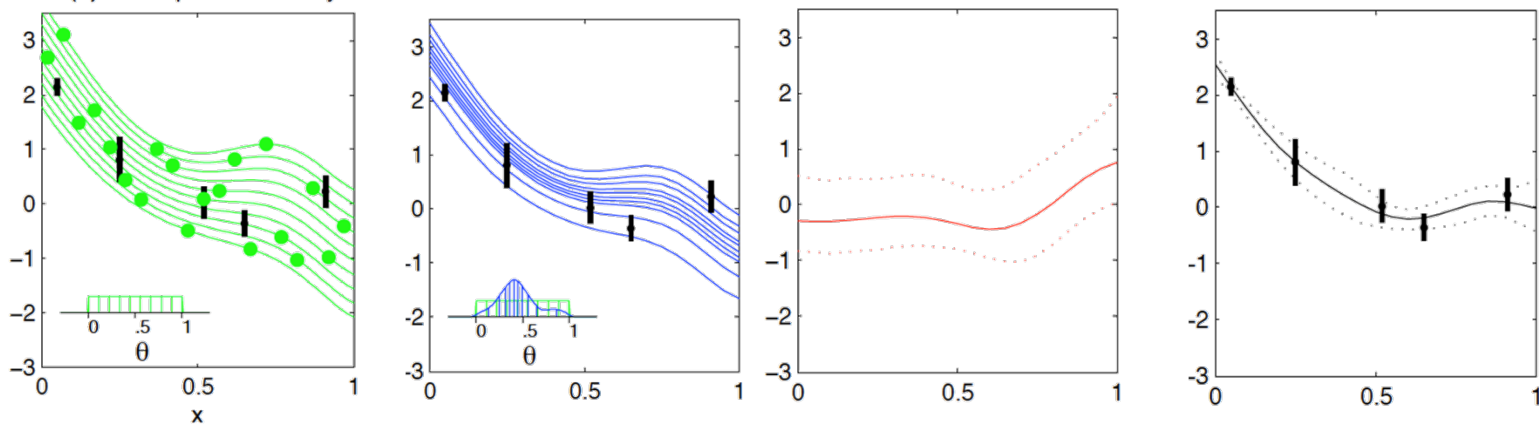
$$\mathbf{Y} \sim N[\mathbf{Z}(\boldsymbol{\theta}, \boldsymbol{\zeta}), \Sigma(\boldsymbol{\xi}) + \boldsymbol{\psi}\mathbf{I}] = \mathcal{L}(\mathbf{Y}|\boldsymbol{\theta}, \boldsymbol{\xi}, \boldsymbol{\psi})$$

# Bayesian methods in parameter estimation

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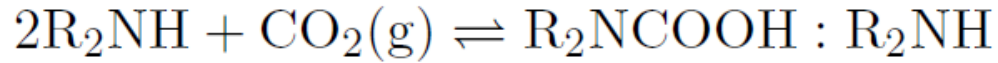


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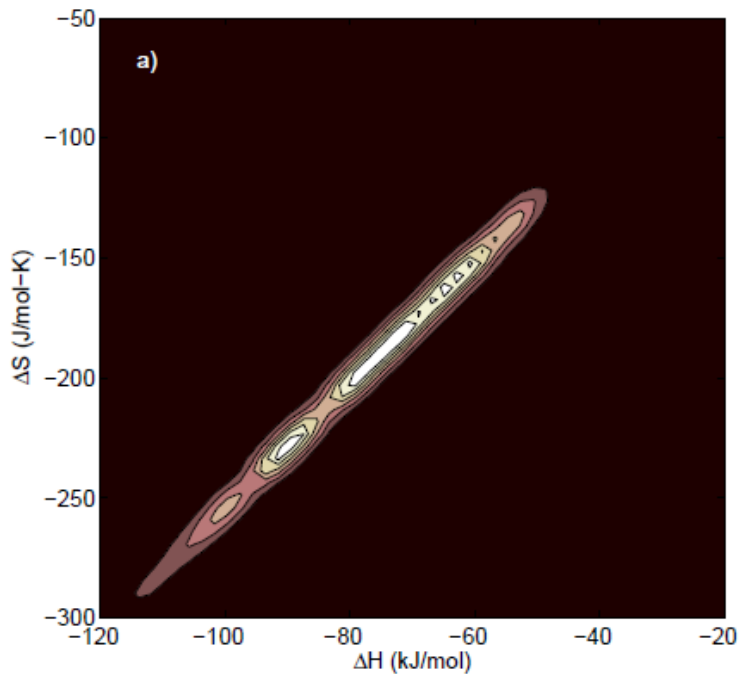


MC Kennedy and A O'Hagan, J Royal Stat Soc B, 63 (2001) 425.

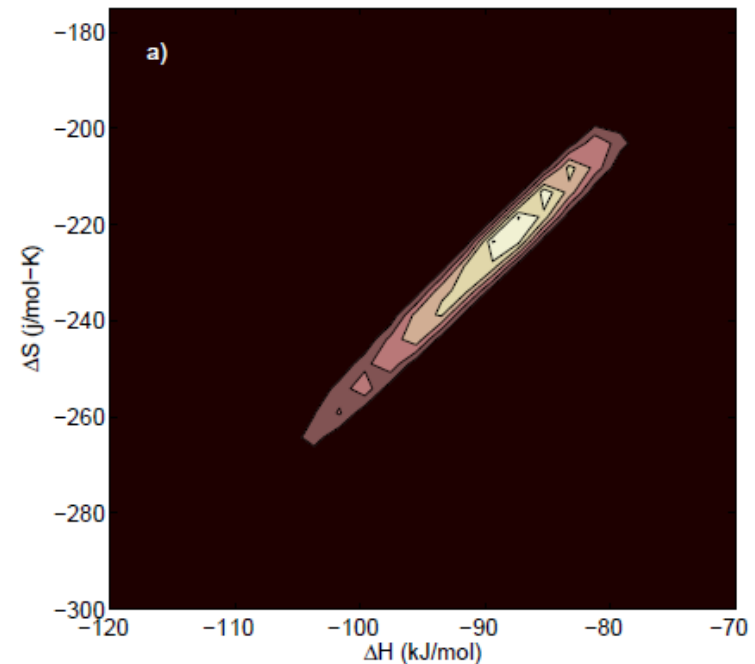
# Bayesian methods in parameter estimation



$$\kappa = \frac{x^2}{(1 - 2x)^2 p} = \exp\left(\frac{\Delta S}{R}\right) \exp\left(\frac{-\Delta H}{RT}\right) / P \quad w = Mn_v x / \rho$$

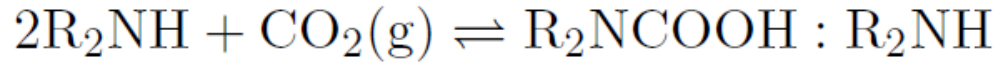


posterior  
distributions (left)  
without and (right)  
with informative  
priors

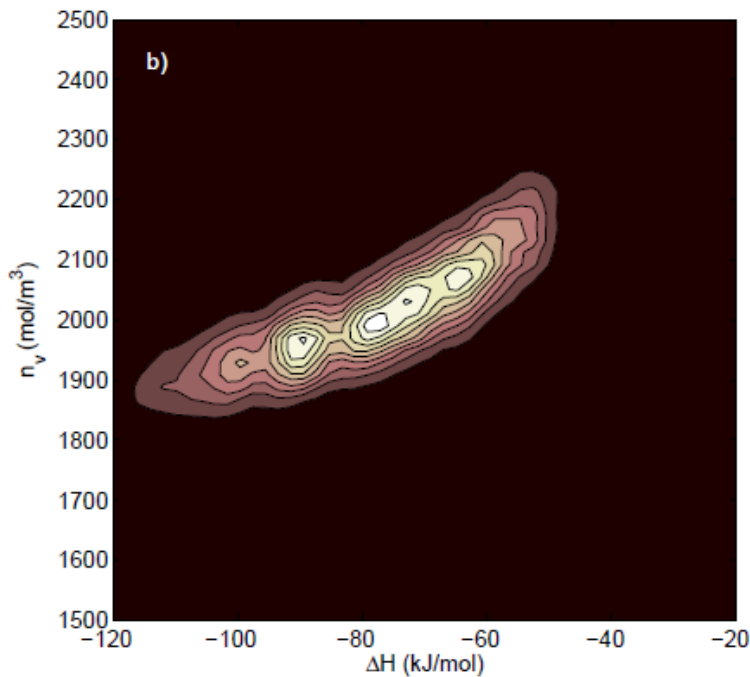


DS Mebane, KS Bhat, JD Kress, et al., in prep.

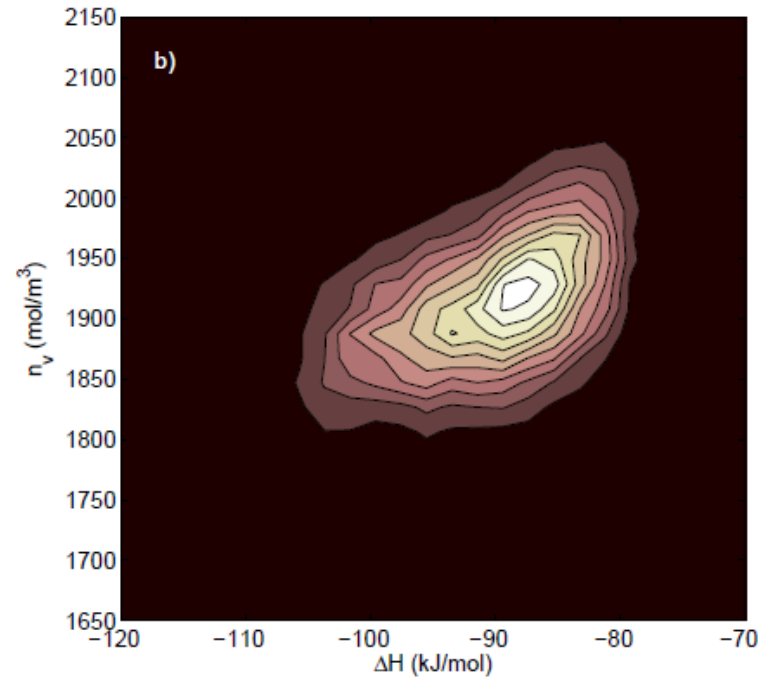
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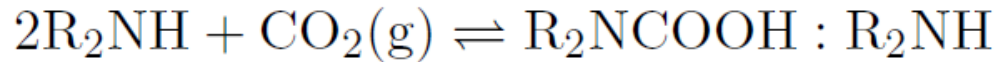
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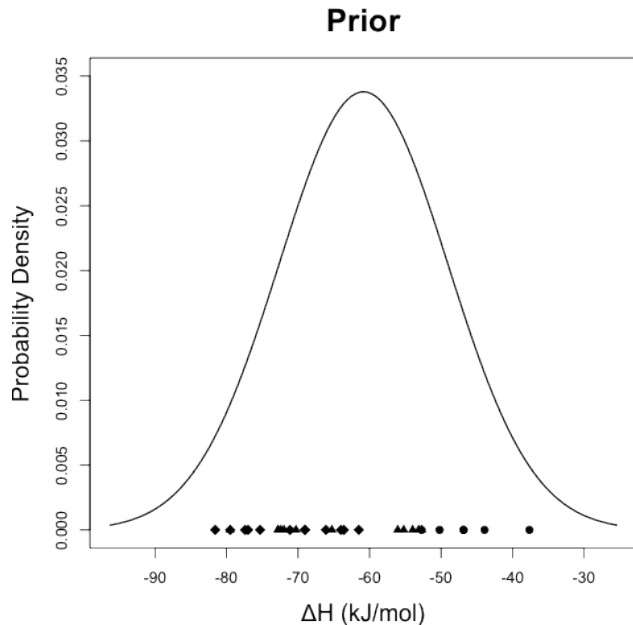
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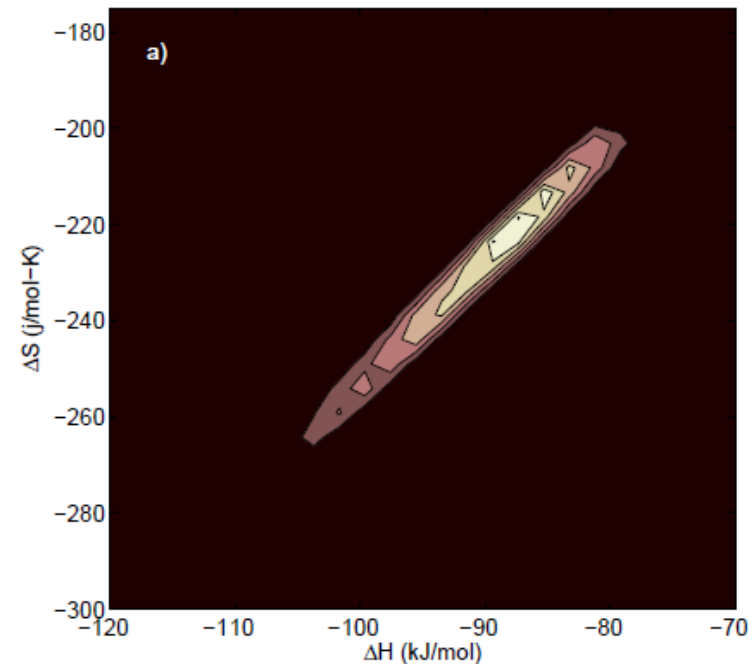
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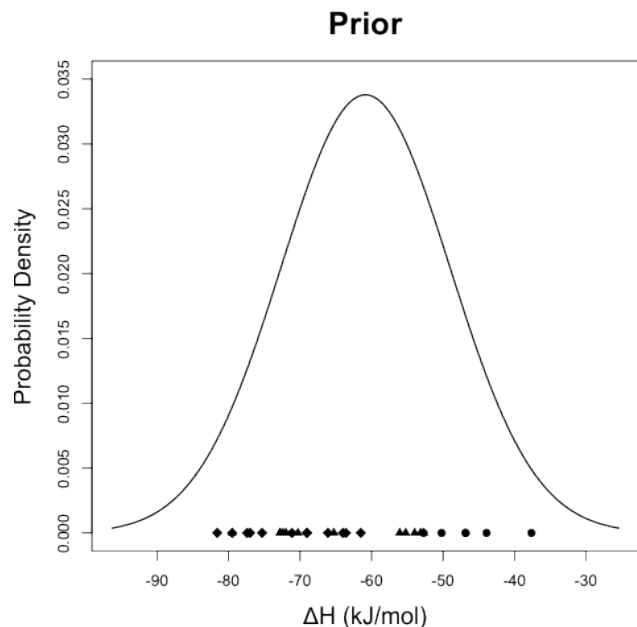
(left) prior  
distribution for  
adsorption  
enthalpy, and  
(right) posterior  
distribution



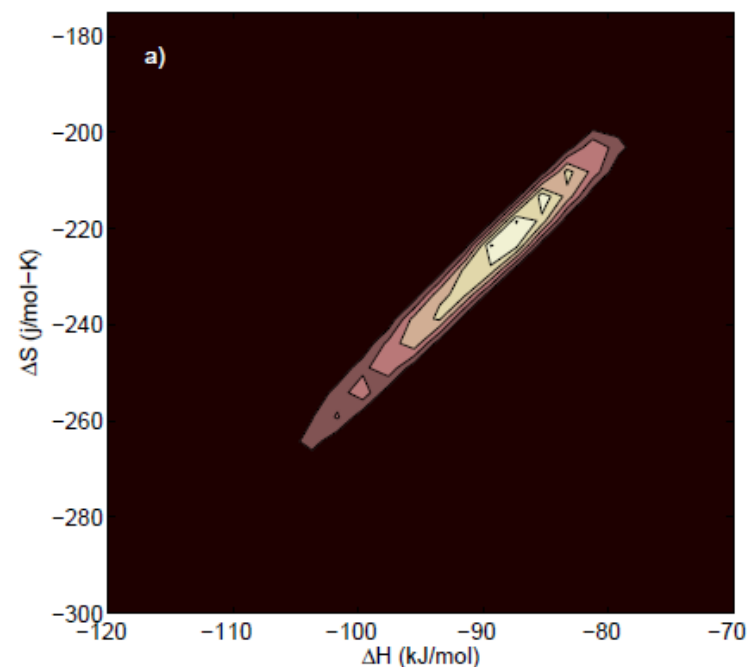
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# Bayesian methods in parameter estimation

reaction	B3LYP	PBE	PBE0	MP2	MP3
$\text{CO}_2 + 2\text{MMA} \rightarrow \text{P-COOH:P}$	-52.72	-71.13	-81.59	-52.72	-72.8
$\text{CO}_2 + \text{MMA} + \text{DMA} \rightarrow \text{S-COOH:P}$	-46.86	-63.60	-76.99	-53.97	-71.96
$\text{CO}_2 + \text{MMA} + \text{DMA} \rightarrow \text{P-COOH:S}$	-50.21	-66.11	-79.50	-53.14	-72.38
$\text{CO}_2 + 2\text{DMA} \rightarrow \text{S-COOH:S}$	-46.86	-64.02	-77.40	-56.07	-72.80
$\text{CO}_2 + \text{DETA} + \text{EDA} \rightarrow \text{P-COOH:S}$	-37.66	-69.04	-69.04	-55.23	-70.29
$\text{CO}_2 + \text{DETA} + \text{EDA} \rightarrow \text{S-COOH:P}$	-43.93	-61.50	-75.31	-65.27	-79.50

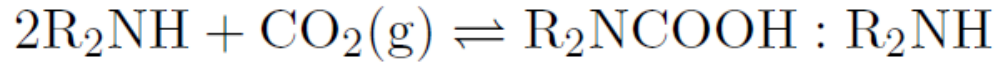


(left) prior distribution for adsorption enthalpy, and (right) posterior distribution

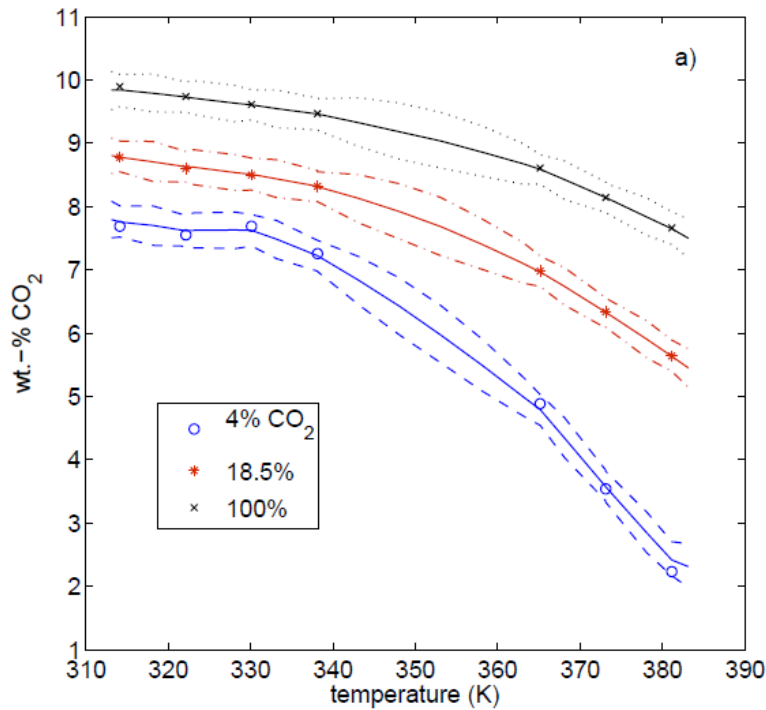


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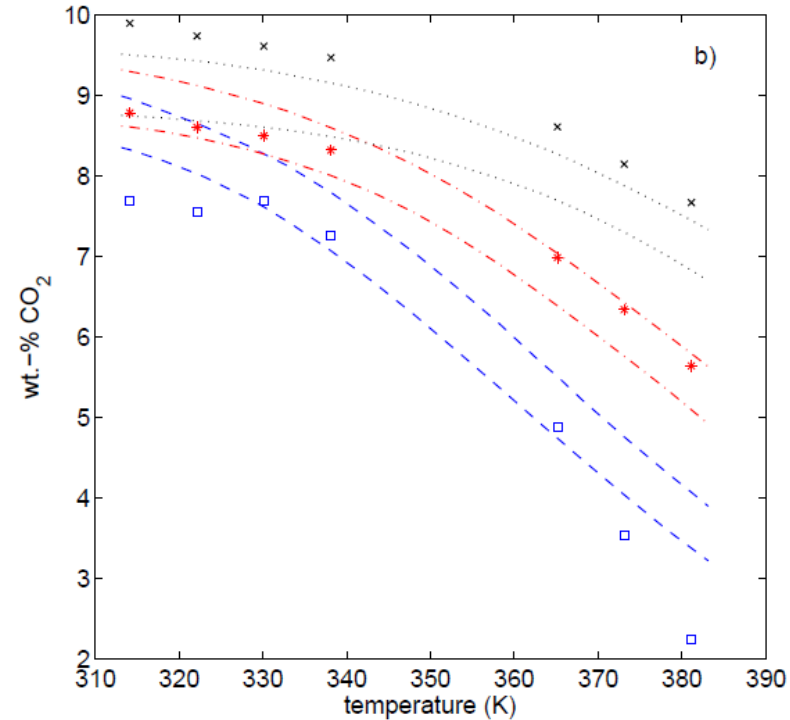
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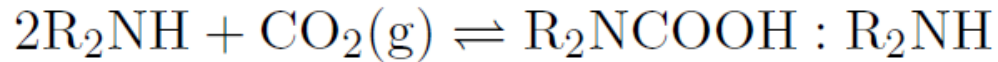


(left) conditioned model + discrepancy predictions, and (right) model predictions, with 95% confidence bounds

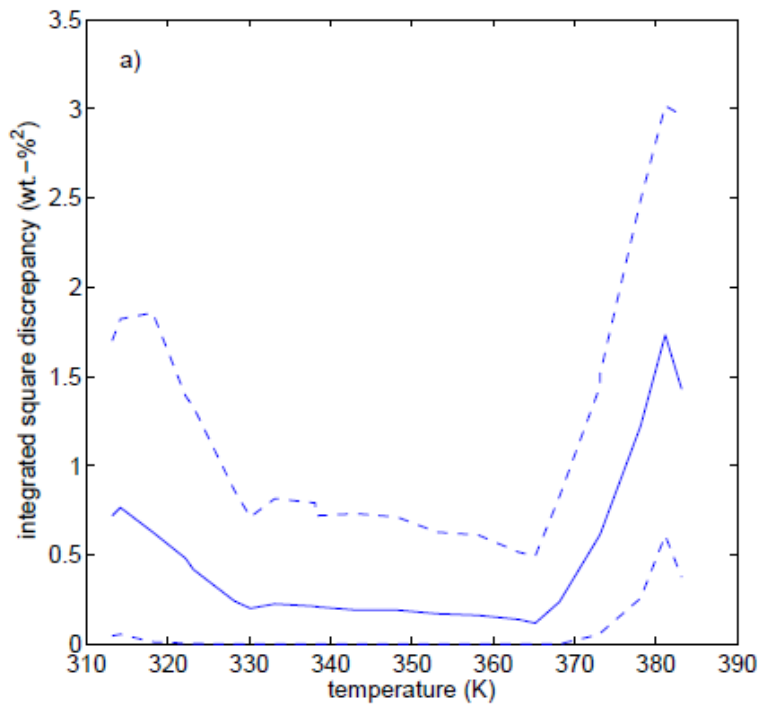


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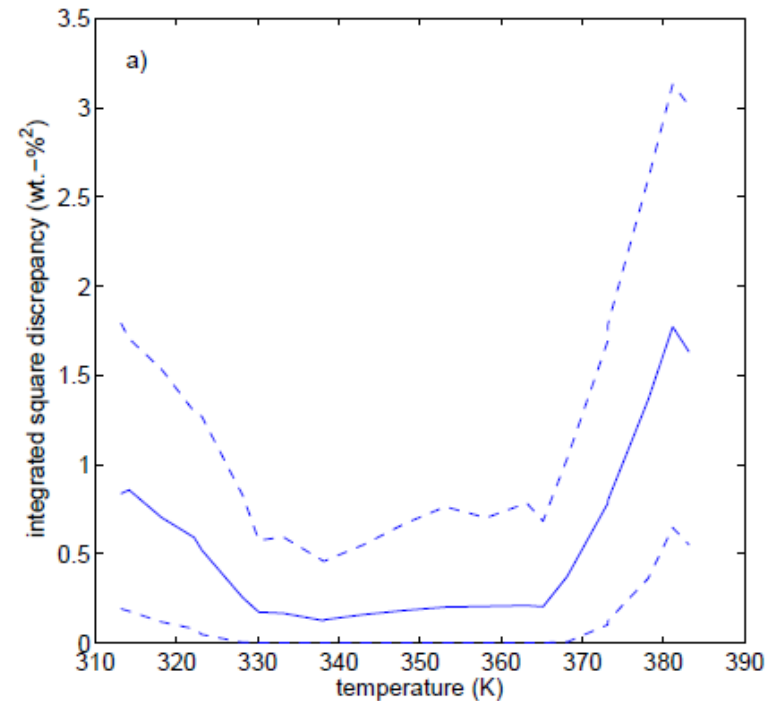
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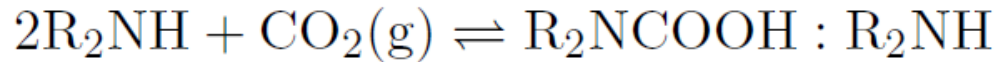


(left) normalized discrepancy for uniform priors with 95% bounds, and (right) normalized discrepancy for informative priors, 4% CO<sub>2</sub>

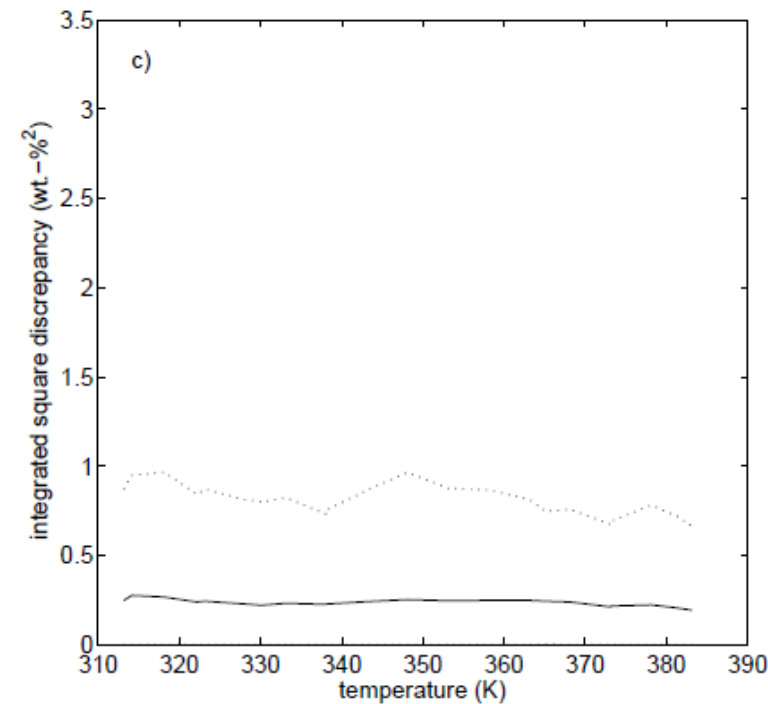


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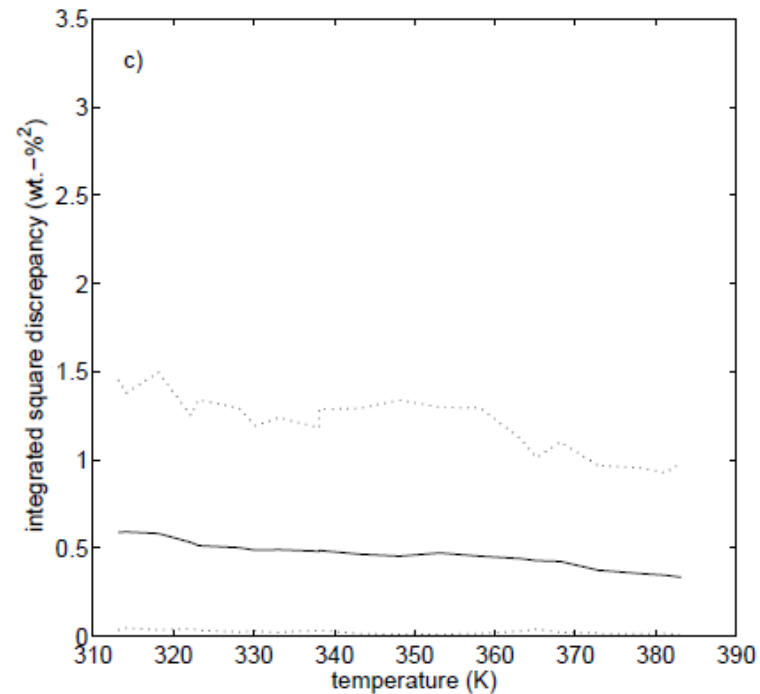
# Bayesian methods in parameter estimation



$$\kappa = \frac{x^2}{(1 - 2x)^2 p} = \exp\left(\frac{\Delta S}{R}\right) \exp\left(\frac{-\Delta H}{RT}\right) / P \quad w = Mn_v x / \rho$$



(left) normalized discrepancy for uniform priors with 95% bounds, and (right) normalized discrepancy for informative priors, 100% CO<sub>2</sub>



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# conclusions / future work

- *Ab initio* calculations can be used in along with a valid model form discrepancy in a Bayesian framework to influence the experimental calibration of engineering-useful models of complex chemical systems.
- A conditioned model form discrepancy enables the direct use of experimental information in scale-up through a model-plus-discrepancy approach, providing penalties for interpolation and extrapolation that become smaller as models improve.
- Work is underway to demonstrate the effects of model form discrepancy in upscaling of a simple kinetic model for CO<sub>2</sub> capture through to the process scale.



# acknowledgements

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