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Uncertainty Quantification Analysis in Multiphase Flow CFD Simulations With Application to Coal Gasifiers

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Presentation Outline

- Gasification
- Overview of Uncertainty Quantification Framework
- Preliminary Results for Demonstration of Non-intrusive UQ Analysis :
 - Gasification simulations
 - C3M PCCL simulations
- Summary & Conclusions
- Future Direction



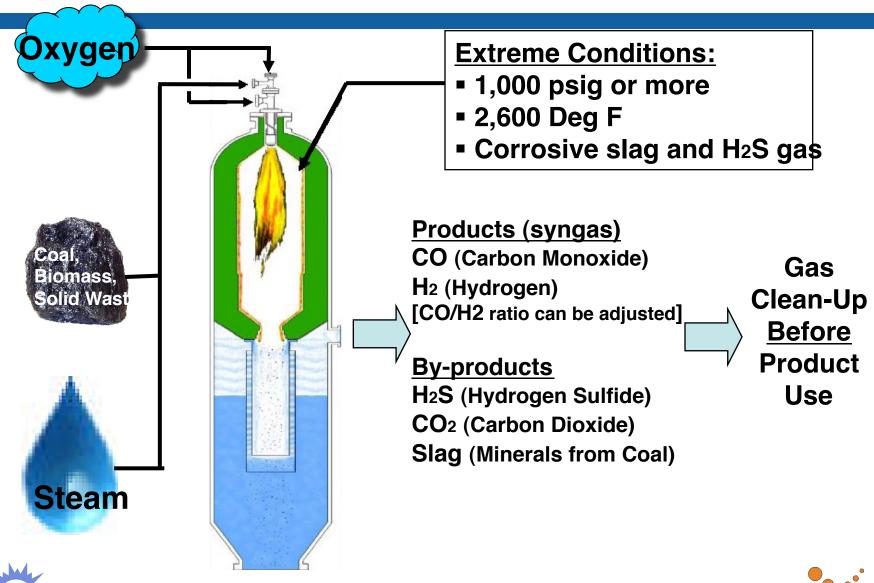
Gasification

- Over 40% of electricity worldwide is generated through the use of coal
- New environmental regulations, mandating reduction on green house gases and other pollutants will impact coal-based power plants
- Coal gasification technology promises to generate power with reduced environmental impact



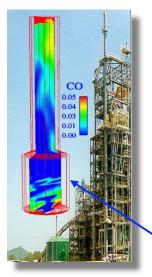


What is Gasification?



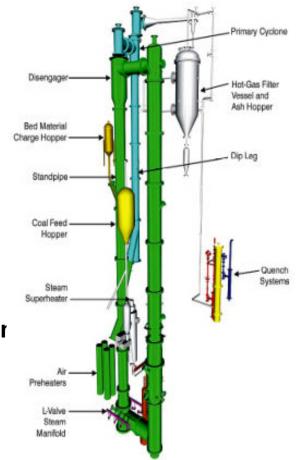
Challenge: How can we design commercial scale gasifiers for optimized operation?

Use validated computer models for answering scale up questions



Parametric Study

- Length/Diameter
- Coal feed rate
- Solids circulation rate
- Recycled syngas
- Coal jet penetration



MFIX simulation of pilot scale 13 MW
transport gasifier at Wilsonville, AL.
Validation of the computer model with
prototype system
C. Guenther et al (2003)

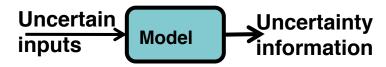
Simulation Based Engineering by employing computational models with Computational Fluid Dynamics (CFD)

Commercial Scale Gasifier



Quick Overview of Uncertainty Quantification (UQ) Methods

Intrusive UQ



Stochastic simulation (UQ embedded in the model)

Several Available Methods:

- Polynomial Chaos Expansions (PCE)
- Stochastic Expansion

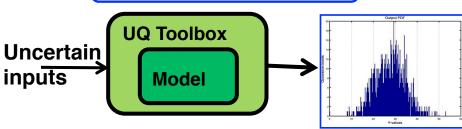
Pros:

Quick prediction

Cons:

Surgery in the code and long

Non-Intrusive UQ



Many deterministic simulations

Several Available Methods:

- **Bayesian Techniques**
- PCE
- Surrogate Model + Monte Carlo

Pros:

Short development time

Cons:

Sampling error



Several Questions To Be Addressed By Using Non-intrusive Uncertainty Quantification and Propagation In Our Simulations?

- What parameters have uncertainty and how to represent these uncertainties adequately?
- What impact do parameter uncertainties have on model outputs? Establish confidence levels & quantitative quality assessment in simulation results.
- Which parameters cause the most output uncertainties?
 [Sensitivity Analysis]
- How do output uncertainties affect input uncertainties?
 [Inverse UQ]
- How to use observed data to calibrate system parameters? [Data Fusion and Calibration]
- In view of uncertainty, how to quantify risk? E.g. given input uncertainties what is the probability of achieving carbon conversion below certain level? [Risk analysis]

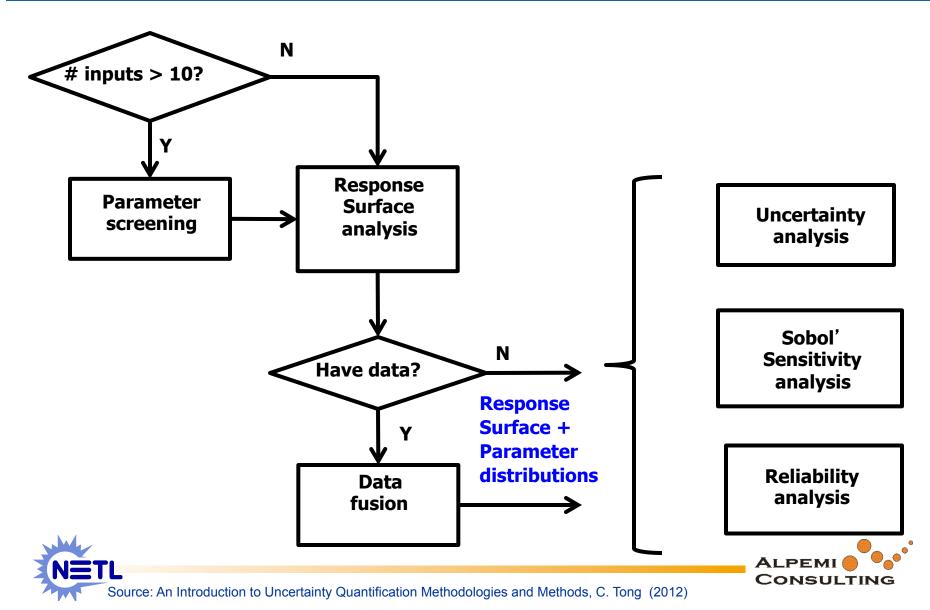
Survey To Identify Various Parametric Sources of Uncertainties and Their Mathematical Characterization

Columns:	Δ	<u>B</u>	<u>C</u>	<u>D</u>	<u>E</u>	<u>E</u>	<u>G</u>	<u>H</u>	1	<u>J</u>	<u>K</u>	<u>L</u>	<u>M</u>	<u>N</u>
	Enter either Nominal value AND (Min/Max values OR Min/Max %)													
Importance Rank (Select)	Sources of Uncertainty in Model Input or Uncertain Input Parameters	Symbol or Variable Name	Units	The most likely value (n) or the Nominal value	Minimum value: (a) { (a) < (n) }	Maximum value: (b) { (n) < (b) }	Minimum value (% of n)	Maximum value (% of n)	Justification for the provided "most likely value" and lower/upper bounds (Please provide reference citations)	Uncertainty	Characterize Uncertainty (Select from list)	if Aleatory, set Probability distribution & parameters	Is it correlated with any other source of uncertainty?	If correlated then specify input parameter & why
1	Mean solids circulation rate	Gs	kg/s	14			90	110.00%	Experimental data [1,2]	Aleatory (A)	PDF	N(13.97,0.34)	Υ	FsI
2	Mean superficial gas velocity at bottom	Ug	m/s	7.58			95	105.00%	Experimental data [1,3]	Aleatory (A)	PDF	N(7.57,0.04)	Υ	FsI
5	Gas flow rate from standpipe and L-valve	FsI	SCMs	0.029			99.955	100.05%	Experimental data [1,3]	Aleatory (A)			N	i
11	Temperature	Т	K	293	287	299			Experimental data [1,3]	Aleatory (A)			N	i
10	Pressure at top exit	Р	kPa	105			99.996	100.00%	Experimental data [1,3]	Aleatory (A)			N	
6	Particle diameter	dp	um	802	784	820			Experimental data [1]	Aleatory (A)			N	i
7	Particle density	rho	kg/m3	863			99.99	100.01%	Experimental data [1]	Aleatory (A)			N	i
8	restitution coefficient	е	-	0.8					Literature [4]	Epistemic (E)			N	
9	sphericity (*)	phi	-	0.95					Experimental data [1]	Aleatory (A)			N	i
3	wall boundary for solids phase (\$)	BC	-	partial-slip					Expert opinion [5]	Epistemic (E)			N	i
4	interphase drag (&)	beta	-							Epistemic (E)				ĺ

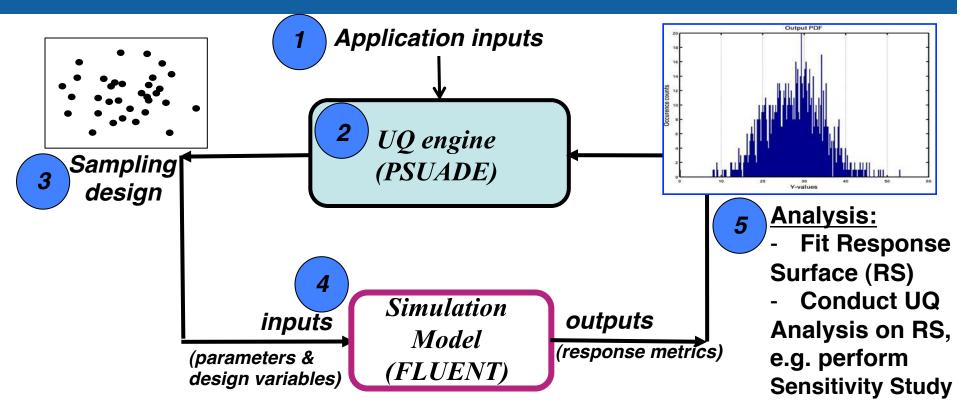




A Simple Workflow for Non-intrusive Parametric Uncertainty Quantification and Propagation:



Input Uncertainty Propagation and Quantification – Non-intrusive method



- No need to modify simulation models: "black boxes"
- No need for analysis of the mathematical structures in the model
- May require large sample size for sufficient accuracy
- Model form uncertainty and numerical approximation uncertainty are disregarded.



Preliminary Results for Demonstration of Non-intrusive Parametric Uncertainty Quantification Study with MFIX Simulations:

- Sample Problem # 1: 2D Gasification (Aleatory) *
- Sample Problem # 2: 2D Gasification (Mixed)
- Sample Problem # 3: C3M PC Coal Lab (Aleatory)

* This work was presented at the 2012 ASME V&V Symposium in Las Vegas, Nevada, May 3rd, 2012.





Sample Problem # 1 for Parametric Non-Intrusive UQ Study: 2D Gasification (Aleatory Uncertainty only)

Objective: Determine the effect of uncertainty in mass flow rate and O2 mass fraction on the species composition at the outlet of the gasifier.

Gasifier Model

Solids: PRB coal with $d_p = 0.015$ cm, $\rho_p = 2.93$ g/cm³

Geometric dimensions = 52 cm x 1300 cm

Grid Resolution = 4,579 cells

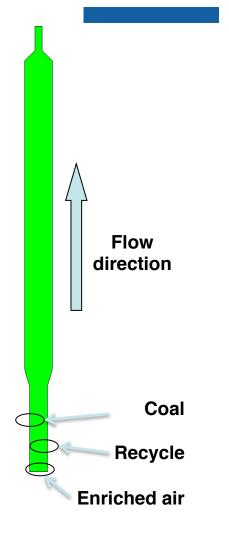
Governing Physics & Models: Multiphase flow (TFM)

hydrodynamics, heat transfer, chemical reactions.

Spatial discretization: Second Order Upwind

Temporal discretization: 1st order

Computational time per simulation: ~ 2 weeks, 16 cores





Sample Problem # 1 for Parametric Non-Intrusive UQ Study: 2D Gasification (Aleatory Uncertainty only - cont'd)

Uncertainty Quantification Study Properties:

Input parameters with Uncertainty (min-max range):

(1) Inlet mass flow rate (kg/s)

[1.575 - 2.424]

(2) O₂ species mass fraction [0.259 - 0.4]

System Response Variables:

Time averaged mole fraction at the exit plane for species

(1) CH4 (2) CO (3) H2

Sampling Method: CCD, SparseGrid

Sample Size = 17 (CCD), 13 (SparseGrid)

^{*} This work was presented at the 2012 ASME V&V Symposium, Las Vegas, Nevada, May 3rd, 2012.



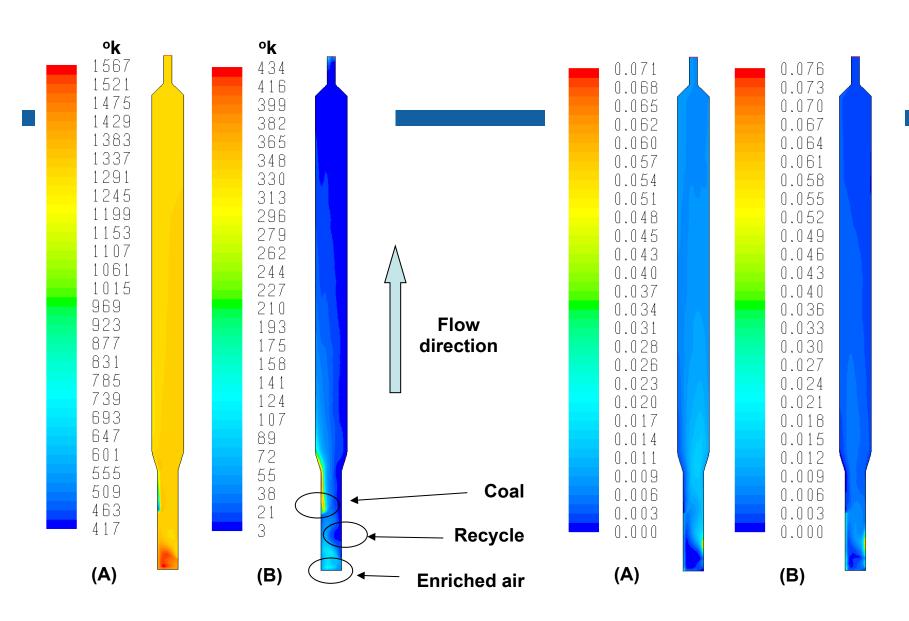


Flow direction

Coal

Recycle

Enriched air



Time averaged temperature (A) and its RMS value (B)

Time averaged CO mass fraction (A) and its RMS value (B)



Challenges in Multiphase Flow Simulation

- Typical 3D CFD simulation of a gasifier can take up to 6 to 8 weeks to reach a pseudo-steady state
- To expedite the process, a 2D transport gasifier is modeled using the Two-Fluid Multiphase model in ANSYS FLUENT version 14.0
- Coal pyrolysis, combustion, gasification along with H₂,
 CO and CH₄ and soot combustion are modeled using 16 chemical reactions
- Total of 33 transport equations are solved



Surrogate Model Construction

- Non-intrusive UQ requires many samples, i.e.,
 - many simulations with the CFD code
- Computational cost per sample may prohibit UQ
 - On the average 30 days on 16 cores were employed to achieve converged solutions for the gasifier.
 - Other constraints such as license cost could be factor
- Need to construct a surrogate model
- Various surrogate models available:
 - Data-fitted surrogate models (Parametric polynomial response surfaces, Nonparametric MARS, GPM)
 - Reduced-order Models (ROM)
 - Stochastic collocation Models with Sparse Grid



Surrogate Model Construction (cont'd)

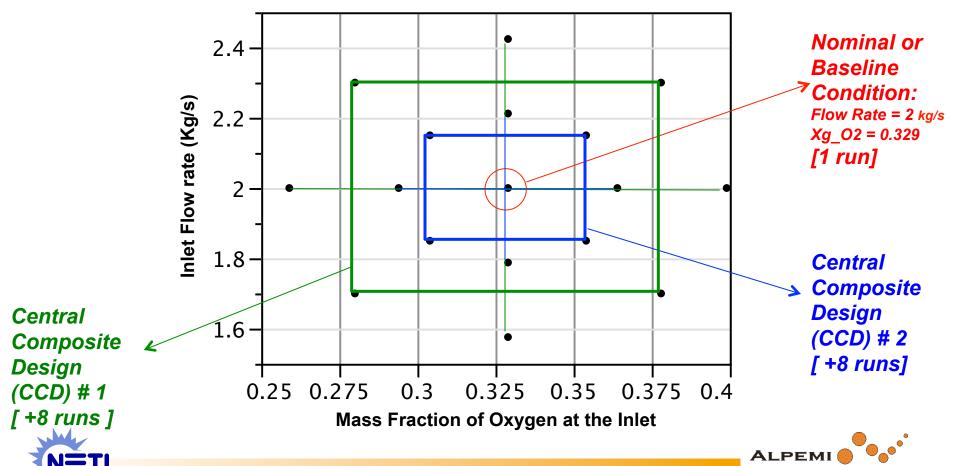
- Employed statistical design of experiments to sample
 - Computational cost constrained the sampling method choice.
 - Initially 9 simulations based on Central Composite Design (CCD) was employed. This analysis necessitated additional runs.
 - Initial run matrix was augmented with another 8-run CCD

	Input	Factors	Response Variables or Quantities of Interest									
Run	#1	#2	#1	#2	#3	#4	#5	#6	#7			
No	Inlet Flow Rate	Xg_O2	CH4	CO2	CO	H2	H2O	Soot	wgs			
1	1.700	0.280	0.0798	0.0145	0.0040	0.0828	0.5732	0.0804	0.5131			
2	2.300	0.280	0.0752	0.0208	0.0051	0.0764	0.5434	0.0748	0.5568			
3	1.700	0.378	0.0781	0.0199	0.0050	0.0798	0.5765	0.0775	0.5288			
4	2.300	0.378	0.0743	0.0286	0.0065	0.0740	0.5489	0.0737	0.5789			
5	1.576	0.329	0.0799	0.0160	0.0042	0.0827	0.5750	0.0803	0.5354			
6	2.424	0.329	0.0779	0.0228	0.0055	0.0793	0.5597	0.0784	0.5742			
7	2.000	0.259	0.0787	0.0155	0.0041	0.0814	0.5640	0.0796	0.5266			
8	2.000	0.399	0.0791	0.0237	0.0058	0.0802	0.5705	0.0798	0.5651			
9	2.000	0.329	0.0776	0.0198	0.0049	0.0793	0.5661	0.0775	0.5493			
10	1.850	0.304	0.0783	0.0162	0.0042	0.0811	0.5658	0.0786	0.5445			
11	2.150	0.304	0.0776	0.0180	0.0045	0.0796	0.5652	0.0778	0.5557			
12	1.850	0.354	0.0789	0.0188	0.0046	0.0812	0.5716	0.0792	0.5632			
13	2.150	0.354	0.0780	0.0215	0.0052	0.0797	0.5645	0.0785	0.5733			
14	1.788	0.329	0.0781	0.0175	0.0045	0.0807	0.5679	0.0783	0.5376			
15	2.212	0.329	0.0774	0.0206	0.0050	0.0794	0.5611	0.0778	0.5769			
16	2.000	0.294	0.0781	0.0165	0.0042	0.0809	0.5645	0.0783	0.5538			
17	2.000	0.364	0.0783	0.0199	0.0049	0.0803	0.5665	0.0787	0.5659			



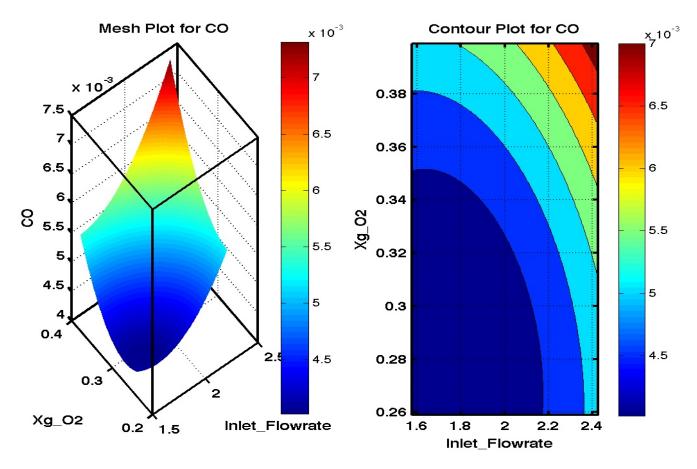
Surrogate Model Construction (cont'd)

 Visual illustration of the sampling locations in the parameter space for two input parameters:



Surrogate Model Construction (cont'd) Response # 3 mole fraction CO

Quadratic polynomial regression based surrogate model



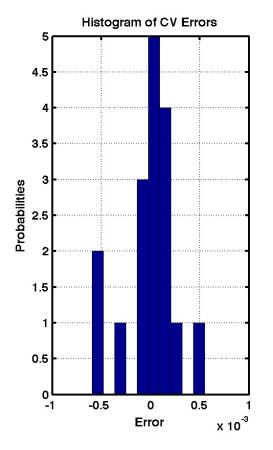


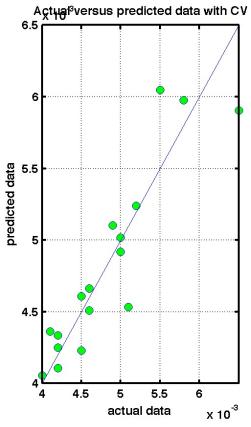
Surrogate Model Adequacy Check Response # 3 mole fraction CO

Polynomial regression metrics:

Adj
$$R^2 = 95.5\%$$

- Cross-validation errors:
 - No systematic bias error as mean CV error0
 - •Standard deviation of errors ~ 2.8e-04

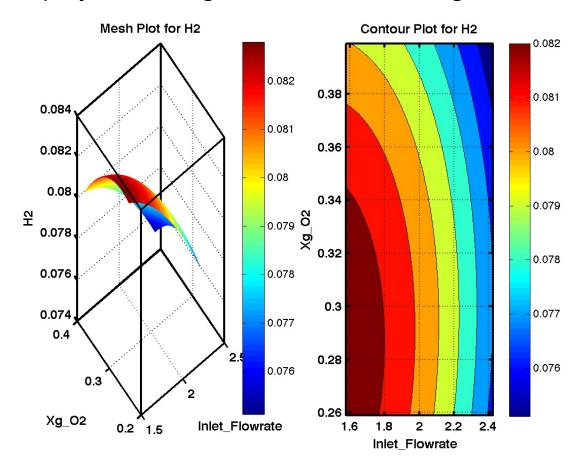






Surrogate Model Construction (cont'd) Response # 4 mole fraction H2 (iteration 1)

Quadratic polynomial regression based surrogate model





Surrogate Model Adequacy Check

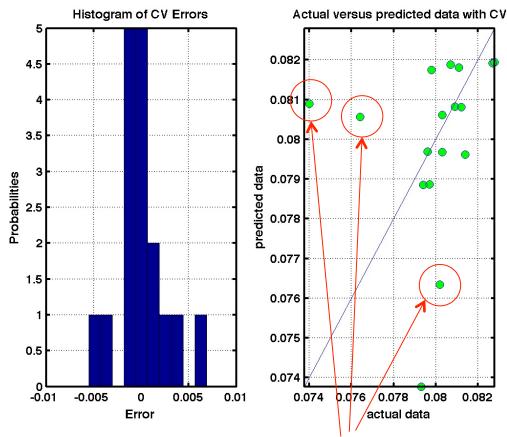
Response # 4 mole fraction H2 (iteration 1)

Polynomial regression metrics:

Adj.
$$R^2 = 64.3\%$$

- Cross-validation errors:
 - •No systematic bias error as mean CV error
 - ~ 0
 - •Standard deviation of errors ~ 2.8e-03

Adjusted R² implies only 64 % of the variability observed in H2 mass fraction can be explained with the quadratic regression based surrogate model constructed!



Several outliers causing the degradation in the surrogate model



Surrogate Model Adequacy Check

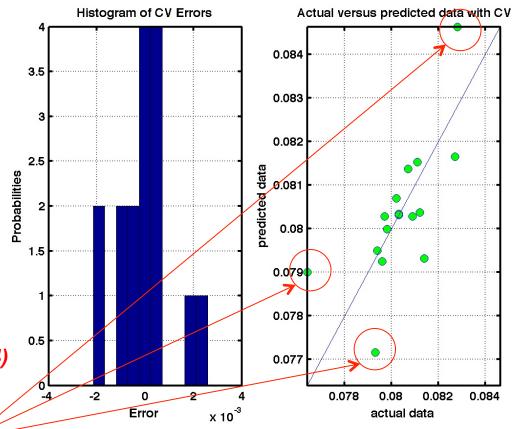
Response # 4 mole fraction H2 (iteration 2)

Polynomial regression metrics:

Adj
$$R^2 = 86.3\%$$

- Cross-validation errors:
 - No systematic biaserror as mean CV error0
 - Standard deviation of errors ~ 1.2e-03

Adjusted R² improved by removing one outlier (Run # 4)

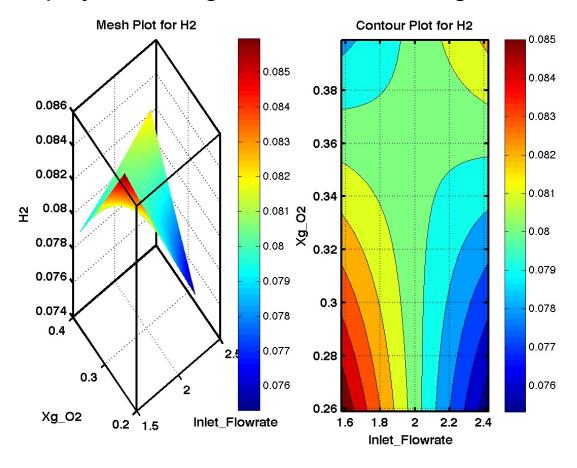


Still several outliers causing problems but we have limited number of samples so assumed the surrogate model to be adequate for the purposes of this study.



Surrogate Model Construction (cont'd) Response # 4 mole fraction H2 (iteration 2)

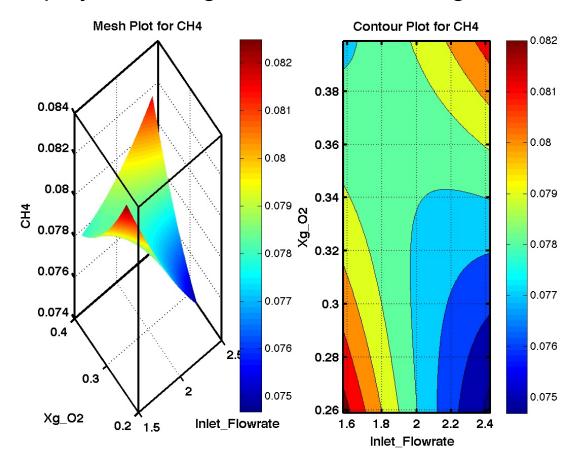
Quadratic polynomial regression based surrogate model





Surrogate Model Construction (cont'd) Response # 1 mole fraction CH4 (iteration 2)

Quadratic polynomial regression based surrogate model





Surrogate Model Adequacy Check

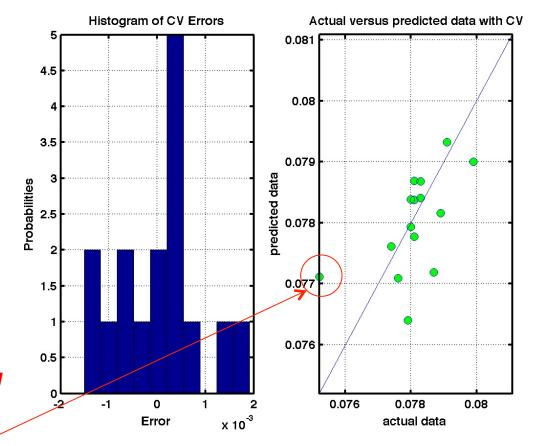
Response # 1 mole fraction CH4 (iteration 2)

Polynomial regression metrics:

Adj
$$R^2 = 84\%$$

- •Cross-validation errors:
 - No systematic biaserror as mean CV error0
 - •Standard deviation of errors ~ 9.1e-04

Adjusted R² improved from 51% (iteration 1) by removing one outlier (Run # 4)



Still several outliers causing problems but we have limited number of samples so assumed the surrogate model to be adequate for the purposes of this study.

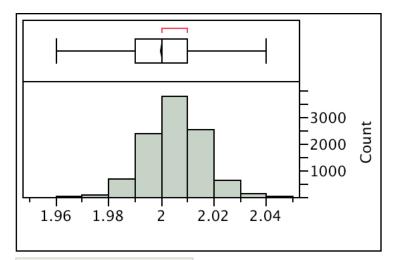


Input Uncertainty Propagation and Quantification – Non-intrusive method

- Both input parameters were assumed to be aleatory uncertainty
- Probability density functions were assigned and Monte Carlo simulation was performed by random drawings for both variables and evaluating surrogate.

(1) Inlet Flow Rate

Normal (2 kg/s , 0.01 kg/s) truncated [1.575,2.424]

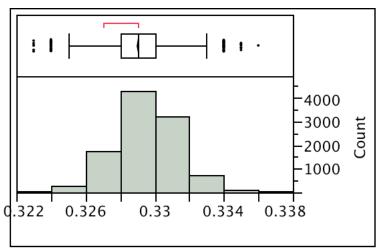


Summary Statistics

Mean2.000115Std Dev0.0105938Std Err Mean0.0001059Upper 95% Mean2.0003227Lower 95% Mean1.9999073N10000

(2) O2 mass fraction

Normal (0.329, 0.0017) truncated [0.259,0.4]



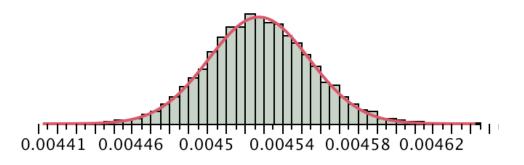
Summary Statistics

Mean	0.3290139
Std Dev	0.0017313
Std Err Mean	1.7313e-5
Upper 95% Mean	0.3290478
Lower 95% Mean	0.32898
N	10000



Input Uncertainty Forward Propagation with 10000 sample Monte Carlo Simulation using the Surrogate:

Response # 3 CO



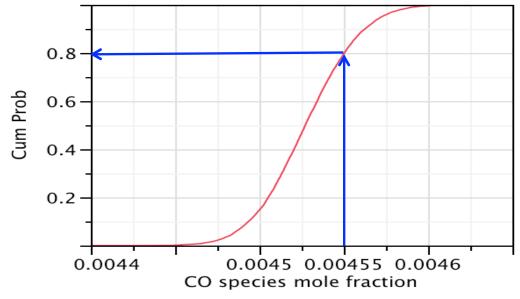
Summary Statistics

Mean0.0045277Std Dev2.678e-5Std Err Mean2.678e-7Upper 95% Mean0.0045282Lower 95% Mean0.0045272N10000

CO species mole fraction

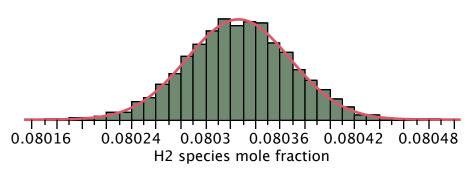
Quantiles								
100.0%	maximum	0.00464						
99.5%		0.0046						
97.5%		0.00458						
90.0%		0.00456						
75.0%	quartile	0.00455						
50.0%	median	0.00453						
25.0%	quartile	0.00451						
10.0%		0.00449						
2.5%		0.00448						
0.5%		0.00446						
0.0%	minimum	0.00442						

Empirical Cumulative Distribution Function





Input Uncertainty Forward Propagation with 10000 sample Monte Carlo Simulation using the Surrogate: Response # 4 H2

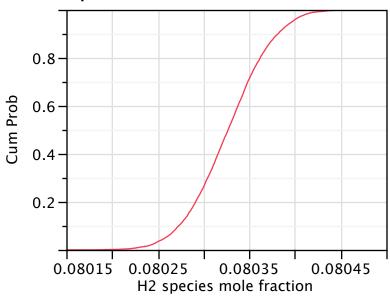


Summary	Statistics
----------------	-------------------

Mean	0.0803268
Std Dev	0.0000418
Std Err Mean	4.1805e-7
Upper 95% Mean	0.0803276
Lower 95% Mean	0.080326
N	10000

Empirical Cumulative Distribution Function

Quantiles								
100.0%	maximum	0.08048						
99.5%		0.08043						
97.5%		0.08041						
90.0%		0.08038						
75.0%	quartile	0.08035						
50.0%	median	0.08033						
25.0%	quartile	0.0803						
10.0%		0.08027						
2.5%		0.08025						
0.5%		0.08022						
0.0%	minimum	0.08018						







Sample Problem # 2 for Parametric Non-Intrusive UQ Study: 2D Gasification (Mixed Epistemic & Aleatory Uncertainty)

Epistemic

Uncertainty

Uncertainty Quantification Study Properties:

Input parameters with Uncertainty (min-max range):

(1) Inlet mass flow rate (kg/s)

[1.575 - 2.424]

(2) O_2 species mass fraction [0.259 – 0.4]

System Response Variables:

Time averaged mole fraction at the exit plane for species

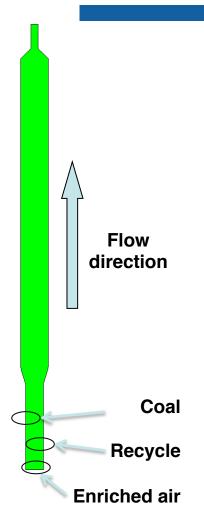
(1) CH4

(2) CO

(3) H2

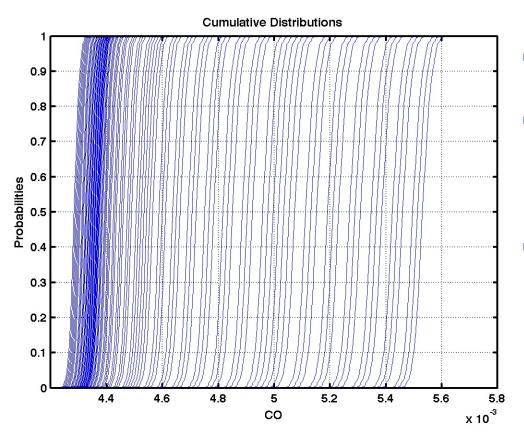
Sampling Method: CCD, SparseGrid

Sample Size = 17 (CCD), 13 (SparseGrid)





Input Uncertainty Forward Propagation for Mixed Epistemic & Aleatory Uncertainty using the Surrogate: Response # 3 CO



- Gaussian Process Model based surrogate model employed.
- There are many CDFs
 - Each corresponds to aleatoric parameters with the epistemic fixed.
- Epistemic uncertainties are dominating.



(in collaboration with K. Chaudhari and Prof. R. Turton of WVU, P. Nicoletti of URS Corp.)

Objective: Determine the effect of uncertainty in heating rate, temperature and pressure on species mass fractions

Uncertainty Quantification Study Properties:

Input parameters with Uncertainty [min-max range]:

(1) Heating rate ($^{\circ}$ C/s) [200 – 9727]

(2) Temperature (°C) [500 – 1010]

(3) Pressure (kPa) [861 – 3447]

System Response Variables:

Species mass fractions computed by C3M - PCCL

(1) CO (2) CO2 (3) tar (4) H2 (5) H2O (6) CH4

Sampling Method: LPTAU, Direct Monte Carlo,

SparseGrid

Sample Size = 250 (LPTAU), 10,000 (Direct Monte Carlo)



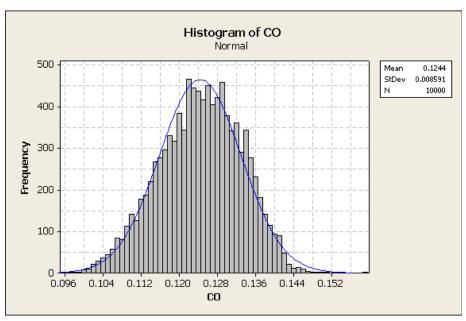
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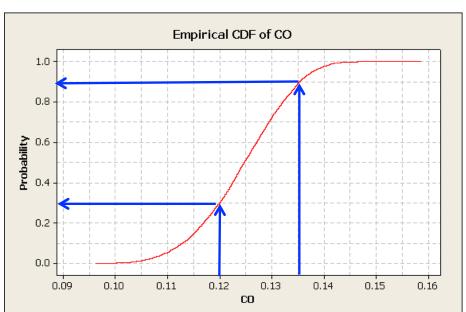
- The input parameters were <u>assumed as aleatory uncertainty</u> and assigned with the following PDFs for Monte Carlo simulations:
 - Heating Rate: Normal (μ =3000, σ =1000)
 - Temperature: Normal (μ =800, σ =100)
 - Pressure: Normal (μ =2000, σ =500)
- PSUADE UQ toolbox was used to generate truncated PDFs from the above prescribed distributions for random drawings to be used in the Monte Carlo simulations.
- Two approaches employed:
 - 1. Monte Carlo(MC) Simulation through a surrogate model
 - C3M-PCCL runs at 250 sample points performed to create MARS based nonparametric response surface to act as surrogate model.
 - 2. Direct Monte Carlo Simulation without a surrogate model
 - Instead of employing a surrogate model, C3M-PCCL was directly executed for the 10,000 sample conditions.



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Empirical CDF Plots Response 1: CO species mass fraction





Direct Monte Carlo Simulation Results for Species Mass Fraction CO

Above plot shows Empirical Cumulative Density Function plot from Direct Monte Carlo simulations.



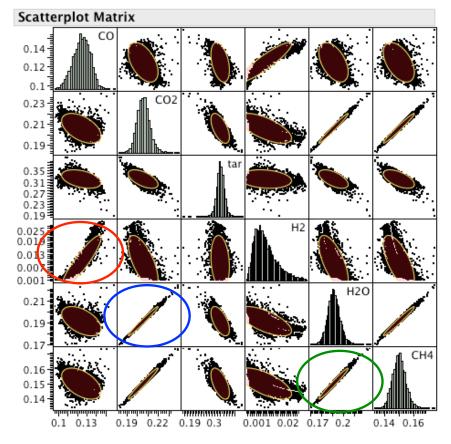
Given prescribed input uncertainties the probability of CO mass fraction being between 0.12 and 0.135 is about 60%.



cont'd

Correlation Matrix and Scatterplot for Species Mass Fractions (Response Variables 1 to 6)

1ultiva	ultivariate											
Correlations												
	CO	CO2	tar	H2	H2O	CH4						
CO	1.0000	-0.4990	-0.3964	0.9087	-0.4965	-0.5003						
CO2	-0.4990	1.0000	-0.5844	-0.6626	0.9836	0.9802						
tar	-0.3964	-0.5844	1.0000	-0.1835	-0.5870	-0.5804						
H2	0.9087	-0.6626	-0.1835	1.0000	-0.6586	-0.6615						
H2O	-0.4965	0.9836	-0.5870	-0.6586	1.0000	0.9802						
CH4	-0.5003	0.9802	-0.5804	-0.6615	0.9802	1.0000						

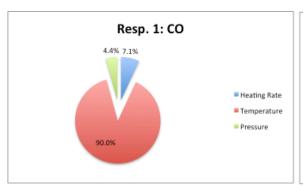


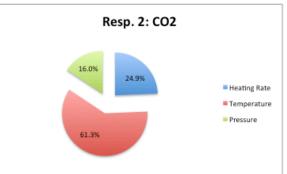


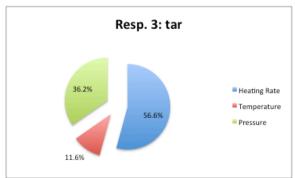


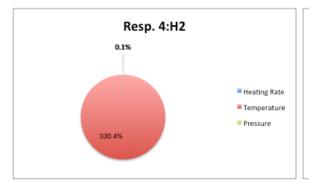
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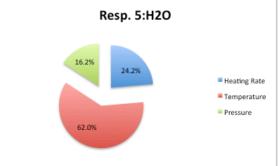
Sensitivity Analysis with Sobol Total Indices Method (Response Variables 1 to 6 with MARS based surrogate model from 250 runs)

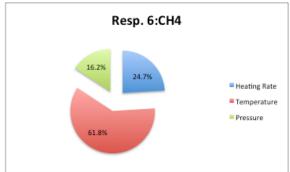












Summary and Conclusions

- Identification and characterization of uncertainties are as important as propagation/analysis of uncertainties
- Effective and efficient UQ requires cross fertilization between various disciplines.
- Non-intrusive UQ enables black box treatment of the application code but requires many samples to achieve the necessary accuracy by reducing sampling error.
- Typically 80% of effort spent goes into constructing an adequate surrogate model.
- The surrogate model adequacy check points out to the need for better convergence criteria in CFD
- The surrogate model is able to capture when pyrolysis
 is dominant and when gasification is dominant

Survey To Identify Various Parametric Sources of Uncertainties and Their Mathematical Characterization

Columns:	Δ	<u>B</u>	<u>C</u>	<u>D</u> Enter eithe	<u>E</u> r Nominal value	<u>F</u> ∍ <u>AND</u> (Min/Ma	<u>G</u> x values <u>OR</u> M	H in/Max %)		<u>J</u>	<u>K</u>	Ŀ	<u>M</u>	N
Importance Rank (Select)	Sources of Uncertainty in Model Input or Uncertain Input Parameters	Symbol or Variable Name	Units	The most likely value (n) or the Nominal value	Minimum value: (a) { (a) < (n) }	Maximum value: (b) { (n) < (b) }	Minimum value (% of n)	Maximum value (% of n)	Justification for the provided "most ikely value" and lower/upper bounds (Please provide reference citations)		Uncertainty	if Aleatory, set Probability distribution & parameters	Is it correlated with any other source of uncertainty?	If correlated then specify input parameter & why
1	Mean solids circulation rate	Gs	kg/s	14			90	110.00%	Experimental data [1,2]		PDF	N(13.97,0.34)		FsI
	Mean superficial gas velocity at bottom	Ug	m/s	7.58			95		Experimental data [1,3]		PDF	N(7.57,0.04)	Υ	Fsl
	Gas flow rate from standpipe and L-valve	Fsl	SCMs	0.029			99.955	100.05%	Experimental data [1,3]	Aleatory (A)			N	
11	Temperature	T	K	293	287	299			Experimental data [1,3]	Aleatory (A)			N	
10	Pressure at top exit	P	kPa	105			99.996	100.00%	Experimental data [1,3]	Aleatory (A)			N	
6	Particle diameter	dp	um	802	784	820			Experimental data [1]	Aleatory (A)			N	
7	Particle density	rho	kg/m3	863			99.99	100.01%	Experimental data [1]	Aleatory (A)			N	
8	restitution coefficient	е		0.8					Literature [4]	Epistemic (E)			N	
	sphericity (*)	phi	-	0.95					Experimental data [1]	Aleatory (A)			N	
3	wall boundary for solids phase (\$)	BC	-	partial-slip					Expert opinion [5]	Epistemic (E)			7	
4	interphase drag (&)	beta	-							Epistemic (E)				
	<u> </u>													

Justification for the provided "most likely value" and lower/upper bounds (Please provide reference citations)		Characterize Uncertainty (Select from list)	if Aleatory, set Probability distribution & parameters	Is it correlated with any other source of uncertainty?	If correlated then specify input parameter & why
Experimental data [1,2]	Aleatory (A)	PDF	N(13.97,0.34)	Υ	Fsl
Experimental data [1,3]	Aleatory (A)	PDF	N(7.57,0.04)	Υ	FsI
Experimental data [1,3]	Aleatory (A)			N	
Experimental data [1,3]	Aleatory (A)			N	
Experimental data [1,3]	Aleatory (A)			N	
Experimental data [1]	Aleatory (A)			N	
Experimental data [1]	Aleatory (A)			N	
Literature [4]	Epistemic (E)			N	
Experimental data [1]	Aleatory (A)			N	
Expert opinion [5]	Epistemic (E)			N	
	Epistemic (E)				

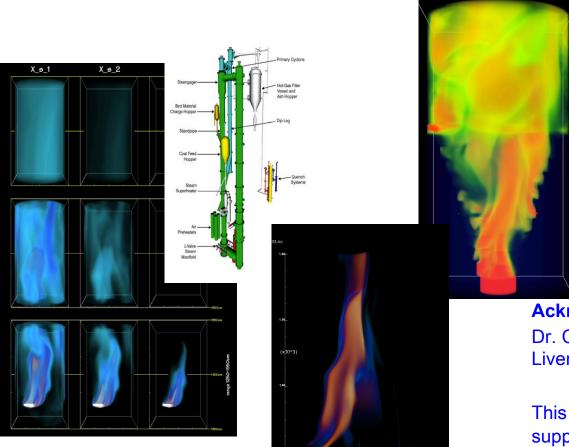


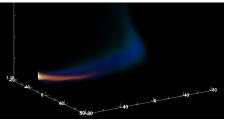
Future Work

- Improve identification and characterization of uncertainties for application domain.
- Expand the work on mixed aleatory and epistemic uncertainty cases.
- Explore Bayesian techniques
 - GPM/SA toolbox from Los Alamos Lab.
- Better quantification of sampling error and surrogate model errors
- Extend stochastic collocation and polynomial chaos based surrogate model using sparse grids.



Questions?





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