



## MPPIC model implementation in MFIx: frictional solid-stress model

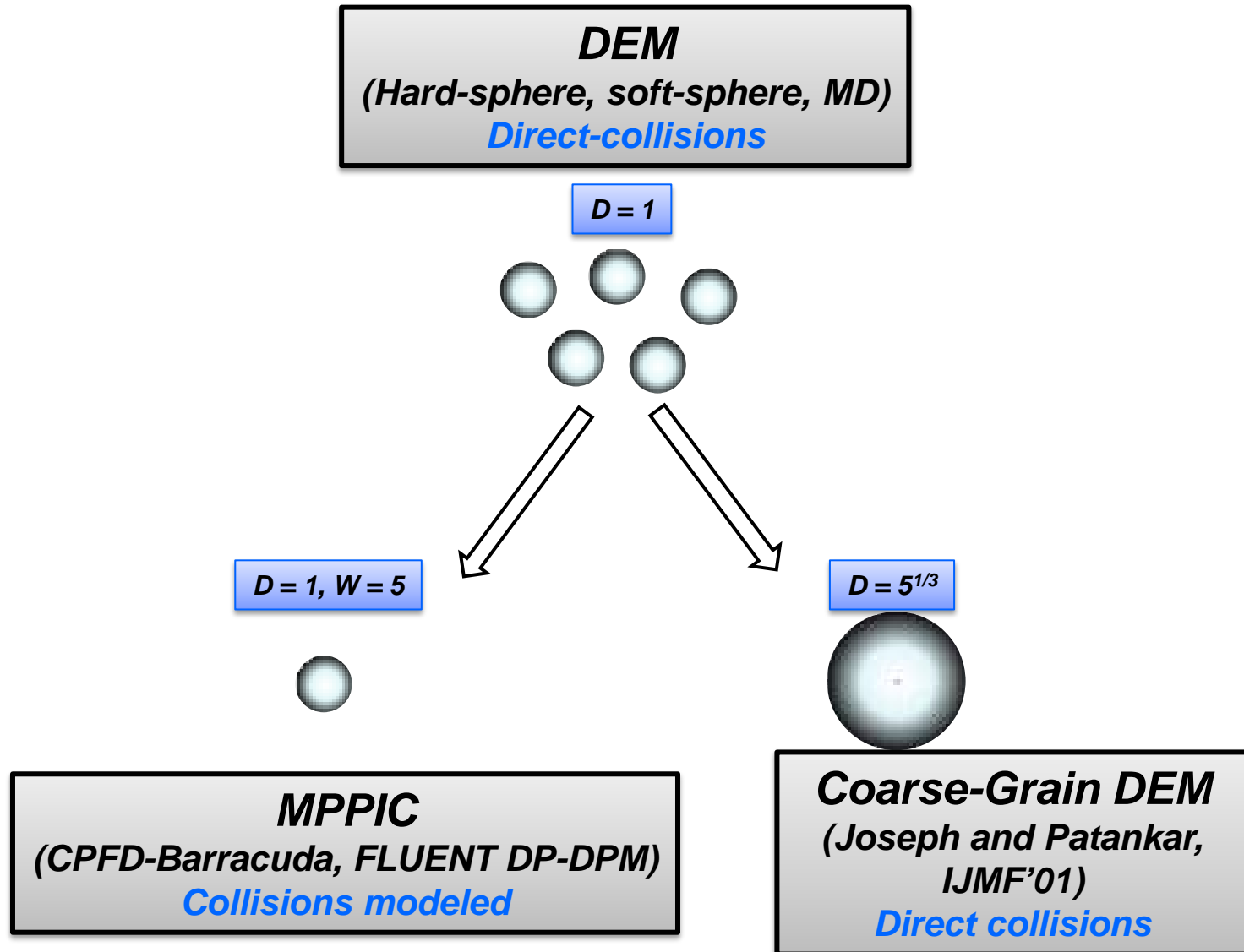
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1: National Energy Technology Laboratory

2: URS Corp.

3: WVURC

# Comparison b/w different discrete methods



# MPPIC: current state-of-the-art

- ✓ ***“IT WORKS!!!” “IT’S FAST”***
- ✓ Demonstrated to be a useful tool for quick turnaround simulations at pilot/device scales
- ✓ Several commercial implementations (Barracuda by CPFD, Dense-phase-DPM by ANSYS)
- ✓ Hard to ascertain and further develop sub-models (such as collision, friction, etc.)
  - ✓ Confusion among users regarding the exact form of models
- ***Objective of this study:*** understand, implement, and document MPPIC model in open-source MFI code to probe its accuracy and speed

# MPPIC model details

**Carrier Phase:** averaged Navier-Stokes equation

$$\frac{\partial(\varepsilon_g \rho_g)}{\partial t} + \nabla \cdot (\varepsilon_g \rho_g \mathbf{v}_g) = 0$$

$$\frac{D}{Dt}(\varepsilon_g \rho_g \mathbf{v}_g) = \nabla \cdot \bar{\bar{S}}_g + \varepsilon_g \rho_g \mathbf{g} - \mathbf{F}_{\text{drag}}$$

$\mathbf{A}_{\text{coll}}$  is the collision operator used to model collisions in the *kinetic* and *frictional* regimes.

**Dispersed Phase**

$$\frac{d\mathbf{X}_p}{dt} = \mathbf{V}_p$$

$$m \frac{d\mathbf{V}_p}{dt} = m\mathbf{g} + \mathbf{F}_{p,\text{drag}} + m\mathbf{A}_{\text{coll}}$$

Robust implementation of *frictional regime*  $\mathbf{A}_{\text{coll}}$  is critical to stability of MPPIC model

# Particle trajectory evolution

$$m \frac{d\mathbf{V}_p}{dt} = m\mathbf{g} + \mathbf{F}_{p,\text{drag}} + m\mathbf{A}_{\text{coll}}$$

$$\mathbf{X}_p^{n+1} = \mathbf{X}_p^n + \Delta t \mathbf{V}_p^{n+1}$$

$$\mathbf{V}_p^{n+1} = \widetilde{\mathbf{V}}_p + \mathbf{V}_{p\tau}$$

$$\widetilde{\mathbf{V}}_p = \mathbf{V}_p^n + \left( \mathbf{g} + \frac{\mathbf{F}_{p,\text{drag}}}{m} \right) \Delta t$$

Drag+body force

$$\widetilde{\mathbf{V}}_p \xrightarrow{A_{\text{coll}}} \mathbf{V}_{p\tau}$$

Impulse velocity

How is  $\mathbf{A}_{\text{coll}}$  applied ?

$$(\mathbf{X}_p^{n+1}, \mathbf{V}_p^{n+1}) \xrightarrow[\text{Specular}]{\text{Wall B.C.}} (\mathbf{X}_p^{*n+1}, \mathbf{V}_p^{*n+1})$$

# $A_{\text{coll}}$ implementation (frictional regime)

$$m \frac{d\mathbf{V}_p}{dt} = m\mathbf{g} + \mathbf{F}_{p,\text{drag}} + m\mathbf{A}_{\text{coll}}$$

$$\mathbf{X}_p^{n+1} = \mathbf{X}_p^n + \Delta t \mathbf{V}_p^{n+1}$$

$$\mathbf{V}_p^{n+1} = \widetilde{\mathbf{V}}_p + \mathbf{V}_{p\tau}$$

$$\widetilde{\mathbf{V}}_p = \mathbf{V}_p^n + \left( \mathbf{g} + \frac{\mathbf{F}_{p,\text{drag}}}{m} \right) \Delta t$$

$$\widetilde{\mathbf{V}}_p \xrightarrow{A_{\text{coll}}} \mathbf{V}_{p\tau}$$

$$(\mathbf{X}_p^{n+1}, \mathbf{V}_p^{n+1}) \xrightarrow[\text{Specular}]{\text{Wall B.C.}} (\mathbf{X}_p^{*n+1}, \mathbf{V}_p^{*n+1})$$

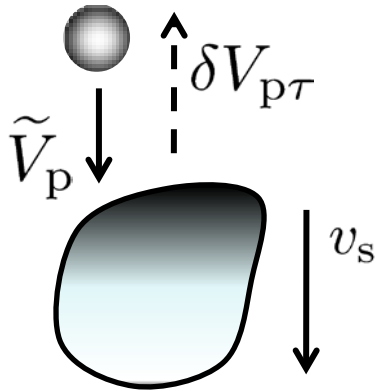
$$\begin{aligned} \chi &= \varepsilon_s & \varepsilon_s &\geq \varepsilon_{s_{cp}} \\ &= 0 & \text{otherwise} \end{aligned}$$

$$\delta \mathbf{V}_{p\tau} = -\nabla \chi$$

$\chi$  is like a coloring function used to indicate the close-packed regions.  $\delta \mathbf{u}_{p\tau}$  is non-zero inside *and* at the interfaces of close-packed regions. It only indicates the direction of the correction due to close-packing.

# $A_{\text{coll}}$ implementation

Case 1



if  $|\tilde{V}_p| > |v_s|$

**REBOUND**

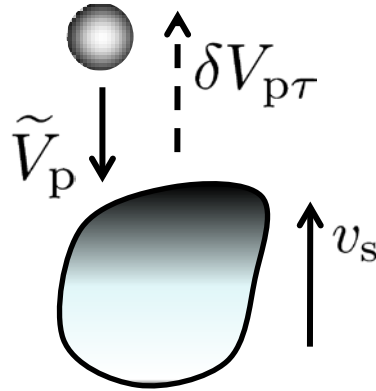
$$V_p^{n+1} = v_s - e_1^{\text{fric}}(\tilde{V}_p - v_s) \uparrow \downarrow$$

else

**SLOW DOWN**

$$V_p^{n+1} = e_2^{\text{fric}} \tilde{V}_p \downarrow$$

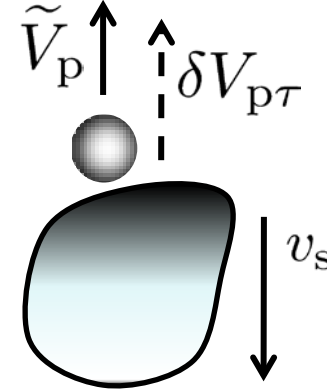
Case 2



**REBOUND**

$$V_p^{n+1} = v_s - e_1^{\text{fric}}(\tilde{V}_p - v_s) \uparrow$$

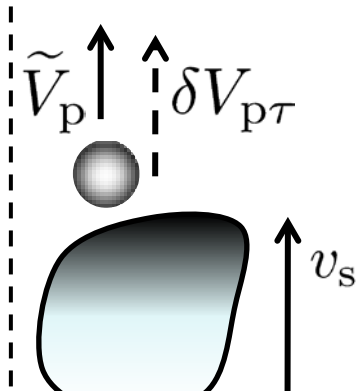
Case 3



**DO NOTHING**

$$V_p^{n+1} = v_s - e_1^{\text{fric}}(\tilde{V}_p - v_s) \uparrow$$

Case 4



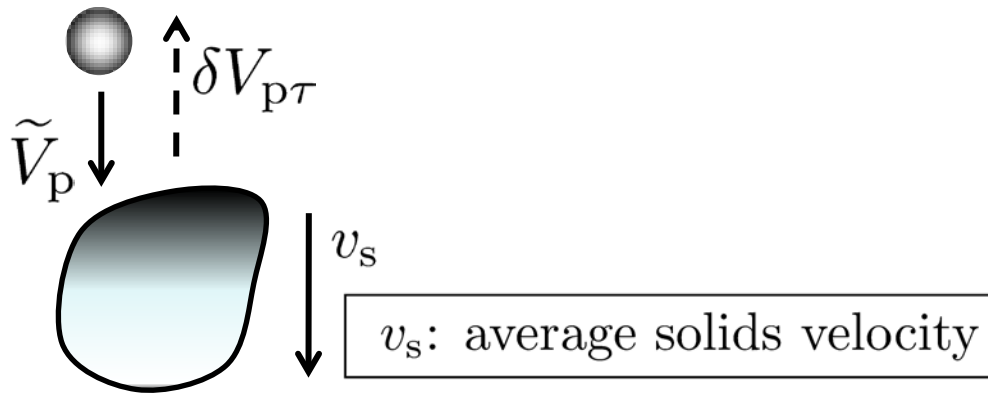
if  $\tilde{V}_p < v_s$

**BUMP**

else

**DO NOTHING**

# $A_{\text{coll}}$ implementation (Summary)



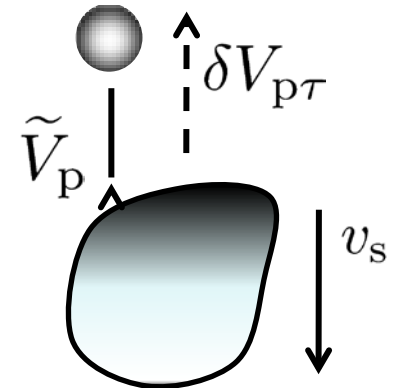
$$\mathbf{V}_{\text{rel}} = \tilde{\mathbf{V}}_p - \mathbf{v}_s$$

$V_{\text{rel}}$ : parcel's relative velocity wrt close-pack

$$\mathbf{V}_p^{n+1} = \mathbf{v}_s - e_1^{\text{fric}} \mathbf{V}_{\text{rel}}; \quad \text{if } \mathbf{V}_{\text{rel}} \cdot (\delta \mathbf{V}_{p\tau}) < 0$$



Case 1



if  $|\tilde{V}_p| > |v_s|$

REBOUND

$$V_p^{n+1} = v_s - e_1^{\text{fric}} (\tilde{V}_p - v_s) \updownarrow$$

else

SLOW DOWN

$$V_p^{n+1} = e_2^{\text{fric}} \tilde{V}_p \downarrow$$

Case 1b



# Comparison with existing literature

$$m \frac{d\mathbf{V}_p}{dt} = m\mathbf{g} + \mathbf{F}_{p,\text{drag}} + m\mathbf{A}_{\text{coll}}$$

$$\mathbf{V}_p^{n+1} = \widetilde{\mathbf{V}}_p + \mathbf{V}_{p\tau}$$
$$\widetilde{\mathbf{V}}_p = \mathbf{V}_p^n + \left( \mathbf{g} + \frac{\mathbf{F}_{p,\text{drag}}}{m} \right) \Delta t$$

No inter-particle collision term so far

Snider, D. M., An incompressible 3-D MP-PIC model for dense particle flows, JCP (2001)

# Comparison with existing literature

$$m \frac{d\mathbf{V}_p}{dt} = m\mathbf{g} + \mathbf{F}_{p,\text{drag}} + m\mathbf{A}_{\text{coll}}$$

$$\mathbf{V}_p^{n+1} = \widetilde{\mathbf{V}}_p + \mathbf{V}_{p\tau}$$

$$\tau = \frac{P_s \varepsilon_s^\beta}{\max [\varepsilon_{s\text{cp}} - \varepsilon_s, \epsilon (1 - \varepsilon_s)]}$$

Isotropic inter-particle stress (Harris and Crighton)

$$\delta \mathbf{V}_{p\tau} = -\frac{\Delta t \nabla \tau}{\rho_s \varepsilon_s}$$

Decides the direction of solid-stress correction velocity

$$(\nabla \tau) \cdot \mathbf{e}_k \leq 0$$

$$V'_{p\tau k} = \min \left( \mathbf{e}_k \cdot \delta \mathbf{V}_{p\tau}, (1 + \gamma)(\mathbf{v}_s - \widetilde{\mathbf{V}}_p) \cdot \mathbf{e}_k \right)$$

$$\mathbf{V}_{p\tau k} = \max \left( V'_{p\tau k}, 0 \right)$$

**Matters mostly near close-packing, otherwise statistical noise!**

# Comparison with existing literature

$$m \frac{d\mathbf{V}_p}{dt} = m\mathbf{g} + \mathbf{F}_{p,\text{drag}} + m\mathbf{A}_{\text{coll}}$$

$$\mathbf{V}_p^{n+1} = \widetilde{\mathbf{V}}_p + \mathbf{V}_{p\tau}$$

$$\tau = \frac{P_S \varepsilon_S^\beta}{\max [\varepsilon_{S_{cp}} - \varepsilon_S, \epsilon (1 - \varepsilon_S)]}$$

$$\delta \mathbf{V}_{p\tau} = -\frac{\Delta t \nabla \tau}{\rho_S \varepsilon_S}$$

**WHAT DO  
THESE  
LIMITERS  
IMPLY ?**

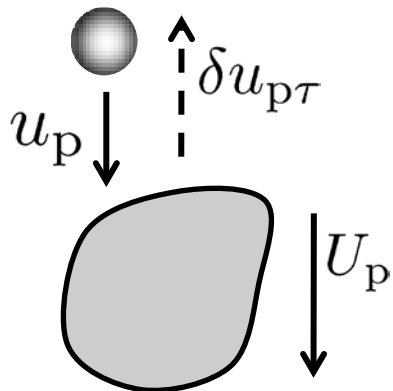
$$(\nabla \tau) \cdot \mathbf{e}_k \leq 0$$

$$V'_{p\tau k} = \min \left( \mathbf{e}_k \cdot \delta \mathbf{V}_{p\tau}, (1 + \gamma)(\mathbf{v}_s - \widetilde{\mathbf{V}}_p) \cdot \mathbf{e}_k \right)$$

$$\mathbf{V}_{p\tau k} = \max \left( V'_{p\tau k}, 0 \right)$$

# Explanation of limiters

Case 1



if  $|u_p| > |U_p|$

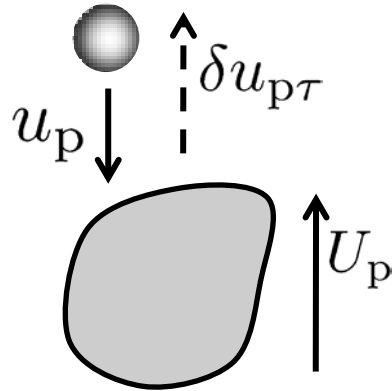
**REBOUND**

$$u_{p\tau} = (1 + \gamma)(U_p - u_p)$$

else

**DO NOTHING**

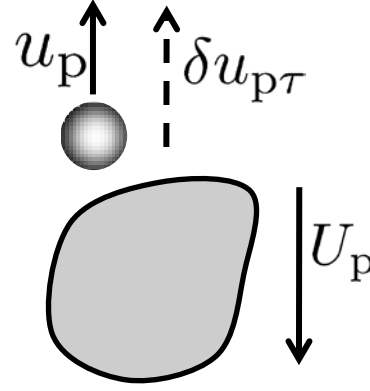
Case 2



**REBOUND**

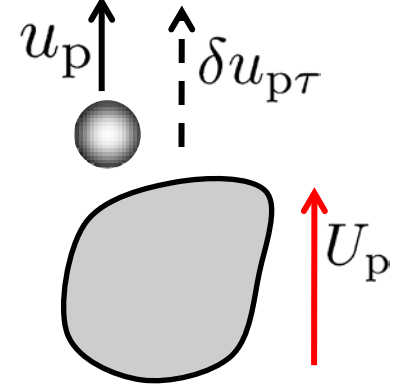
$$u_{p\tau} = (1 + \gamma)(U_p - u_p)$$

Case 3



**DO NOTHING**

Case 4



if  $u_p < U_p$

**BUMP**

$$u_{p\tau} = (1 + \gamma)(U_p - u_p)$$

else

**DO NOTHING**

$$\mathbf{u}_p^{n+1} = \tilde{\mathbf{u}}_p + \mathbf{u}_{p\tau}$$

$$\delta \mathbf{u}_{p\tau} = -\frac{\Delta t \nabla \tau}{\rho_s \varepsilon_s}$$

$$(\nabla \tau) \cdot \mathbf{e}_k \leq 0$$

$$u'_{p\tau_k} = \min(\mathbf{e}_k \cdot \delta \mathbf{u}_{p\tau}, (1 + \gamma)(U_p - u_p) \cdot \mathbf{e}_k)$$

$$u_{p\tau_k} = \max(u'_{p\tau_k}, 0)$$

# Snider's model vs. the new model

$$\mathbf{V}_p^{n+1} = \widetilde{\mathbf{V}}_p + \mathbf{V}_{p\tau}$$

$$\tau = \frac{P_s \varepsilon_s^\beta}{\max[\varepsilon_{scp} - \varepsilon_s, \epsilon(1 - \varepsilon_s)]}$$

$$\delta \mathbf{V}_{p\tau} = -\frac{\Delta t \nabla \tau}{\rho_s \varepsilon_s}$$

$$(\nabla \tau) \cdot \mathbf{e}_k \leq 0$$

$$V'_{p\tau k} = \min(\mathbf{e}_k \cdot \delta \mathbf{V}_{p\tau}, (1 + \gamma)(\mathbf{v}_s - \widetilde{\mathbf{V}}_p) \cdot \mathbf{e}_k)$$

$$\mathbf{V}_{p\tau k} = \max(V'_{p\tau k}, 0)$$

$$\mathbf{V}_{\text{rel}} = \widetilde{\mathbf{V}}_p - \mathbf{v}_s$$

$\mathbf{V}_{\text{rel}}$ : parcel's relative velocity wrt close-pack

$$\mathbf{V}_p^{n+1} = \mathbf{v}_s - \gamma \mathbf{V}_{\text{rel}}; \quad \text{if } \mathbf{V}_{\text{rel}} \cdot (\delta \mathbf{V}_{p\tau}) < 0$$

Two parameter model:  $P_s$  and  $\gamma$

$$\chi = \varepsilon_s \quad \varepsilon_s \geq \varepsilon_{scp}$$

$$= 0 \quad \text{otherwise}$$

$$\delta \mathbf{V}_{p\tau} = -\nabla \chi$$

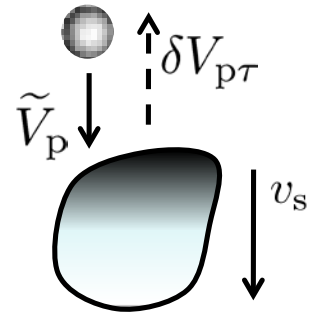
$$\mathbf{V}_{\text{rel}} = \widetilde{\mathbf{V}}_p - \mathbf{v}_s$$



$$\mathbf{V}_p^{n+1} = \mathbf{v}_s - \mathbf{e}_1^{\text{fric}} \mathbf{V}_{\text{rel}};$$

$$\text{if } \mathbf{V}_{\text{rel}} \cdot (\delta \mathbf{V}_{p\tau}) < 0$$

Case 1b



$$\text{if } |\widetilde{\mathbf{V}}_p| < |\mathbf{v}_s|$$

SLOW DOWN

$$\mathbf{V}_p^{n+1} = \mathbf{e}_2^{\text{fric}} \widetilde{\mathbf{V}}_p$$

Two parameter model:  $\mathbf{e}_1^{\text{fric}}$  and  $\mathbf{e}_2^{\text{fric}}$

# STILL DOESN'T WORK!

**A simple case of particles sedimenting in a vertical channel  
blows up due to the inability of the frictional model to sustain  
specified close-packing**

# Fix?

## Cases 1-4

$$\chi = \varepsilon_s \quad \varepsilon_s \geq \varepsilon_{s_{cp}}$$

$$= 0 \quad \text{otherwise}$$

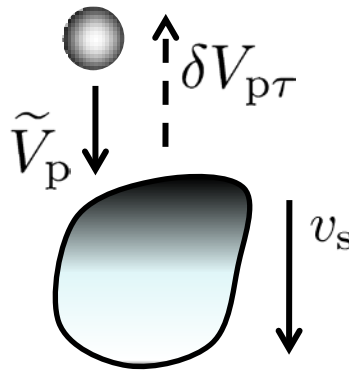
$$\delta V_{p\tau} = -\nabla \chi$$

$$\mathbf{V}_{rel} = \tilde{\mathbf{V}}_p - \mathbf{v}_s$$

$$\mathbf{V}_p^{n+1} = \mathbf{v}_s - \mathbf{e}_1^{fric} \mathbf{V}_{rel};$$

$$\text{if } \mathbf{V}_{rel} \cdot (\delta \mathbf{V}_{p\tau}) < 0$$

## Case 1b

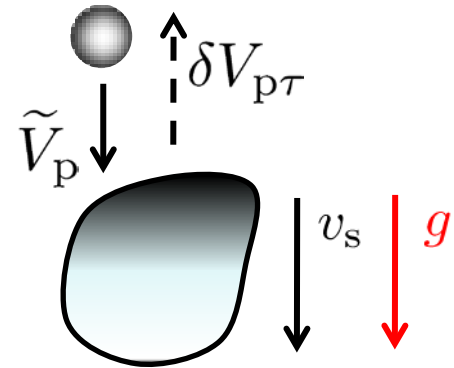


$$\text{if } |\tilde{V}_p| < |v_s|$$

SLOW DOWN

$$V_p^{n+1} = e_2^{fric} \tilde{V}_p$$

## Case 1a



$$|\tilde{V}_p| < > |v_s|$$

ALWAYS REBOUND

$$V_p^{n+1} = -e_1^{fric} \tilde{V}_p$$

**Results in unconditionally stable solver** (does not guarantee any results)

*Still a 2-parameter model*

# Other features/limitations/future development

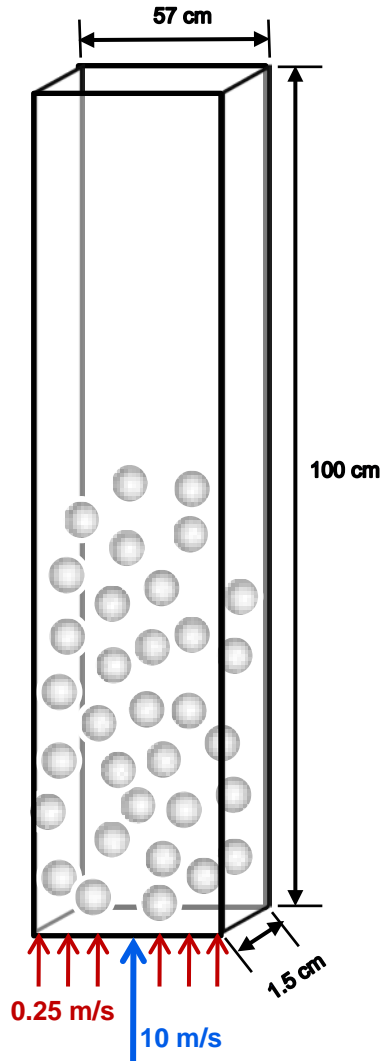
- ☐ Specular reflections at wall
- ☐ No friction at the walls
- ☐ No collisions in the viscous regime
- ☐ Robust extension to cut-cell



# Model development thought process

- ✓ **Three problems were chosen: sedimentation, spouted bed, and uniformly fluidized bed**
- ✓ **Any frictional model or a wild guess was tested by running all three problems**
  - Lot of times very encouraging results for one problem led to blow up of simulations for other problems
  - A stable model did not always imply a physically plausible model. The first model I tried was the most stable one but nothing really moved in that model either!
- ✓ **The final model is a trade off between numerical stability and physics. There are many other variants of this model possible.....**

# Sample Problem 1: Kuiper's jet



## Properties

**Solids:**  $D_p = 0.05 \text{ cm}$ ,  $\rho_p = 2.6 \text{ g/cm}^3$

Total number of particles (DEM) = 36 million

Total number of parcels (MPPIC) = 4,560 ~ **8000**  
particles per parcel

**Gas:** Air at standard conditions

**Bed Dimension**=  $(57 \times 100 \times 1.5) \text{ cm}^3 \equiv (31 \times 60 \times 1) \text{ cells}$

***No slip wall BC's for gas and free slip for solids  
phase mean velocity***

**Drag model:** Wen & Yu / Ergun

Pressure of bed weight = 7.1 kPa

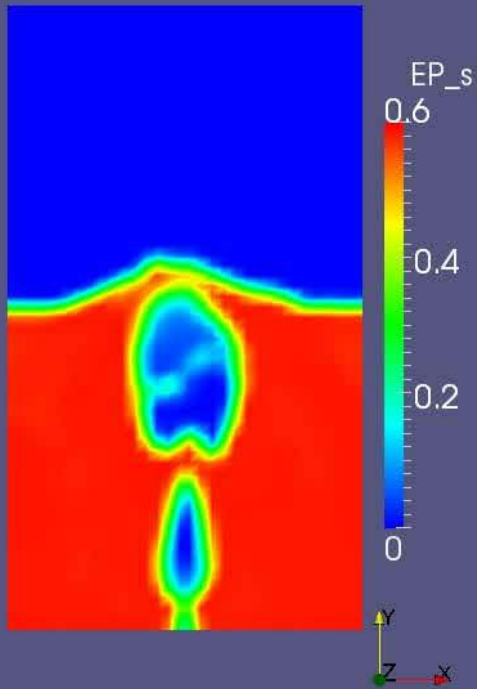
Easiest to bubble, hardest to simulate stably

# TFM vs MPPIC vs CPFD

TFM vs MPPIC vs CPFD

$$e_1^{\text{fric}} = 0.3, e_2^{\text{fric}} = 0.5$$

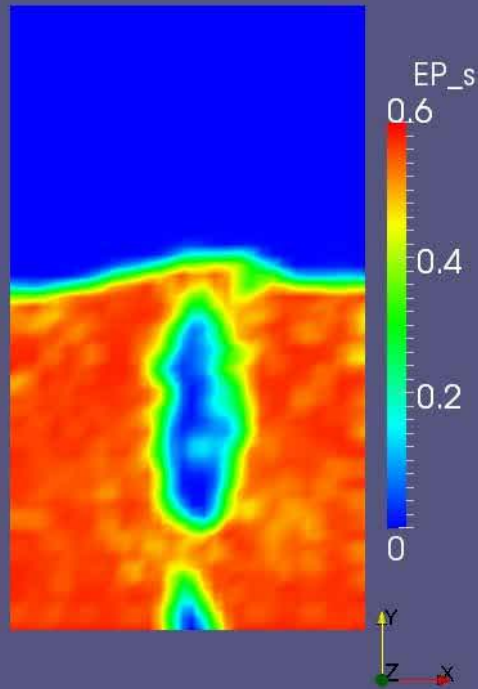
Time: 3.000192



TFM

TFM

Time: 3.000410



MPPIC

MFIX-PIC

3

Cells p-VolFra

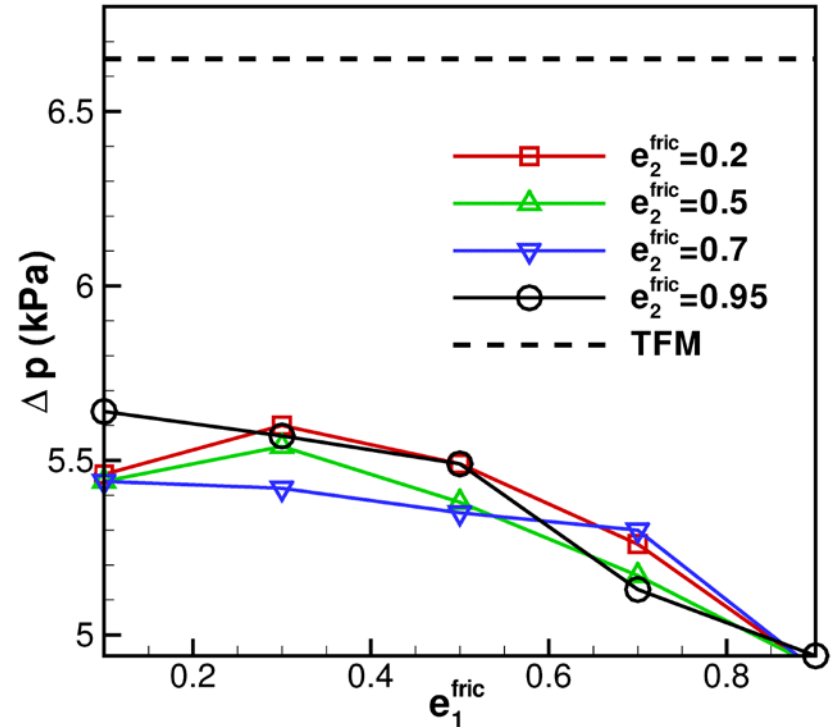
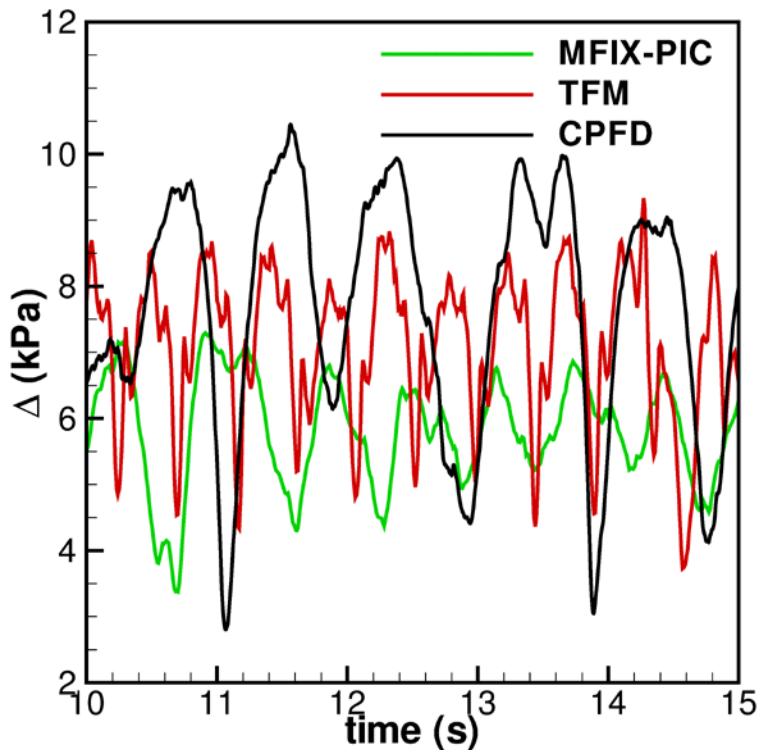


CPFD

CPFD

# Pressure Drop

$$e_1^{\text{fric}} = 0.3, e_2^{\text{fric}} = 0.5$$



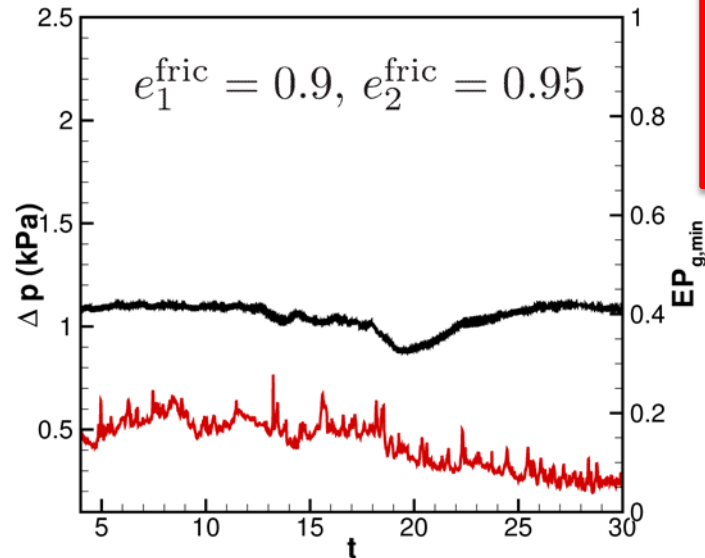
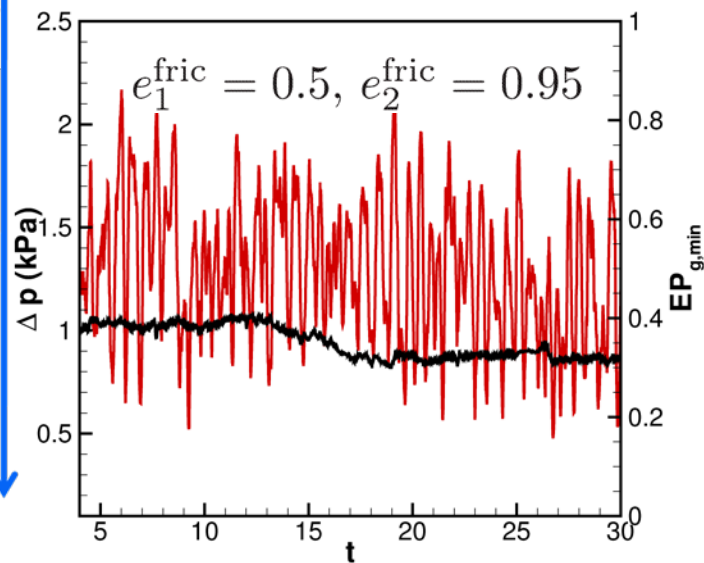
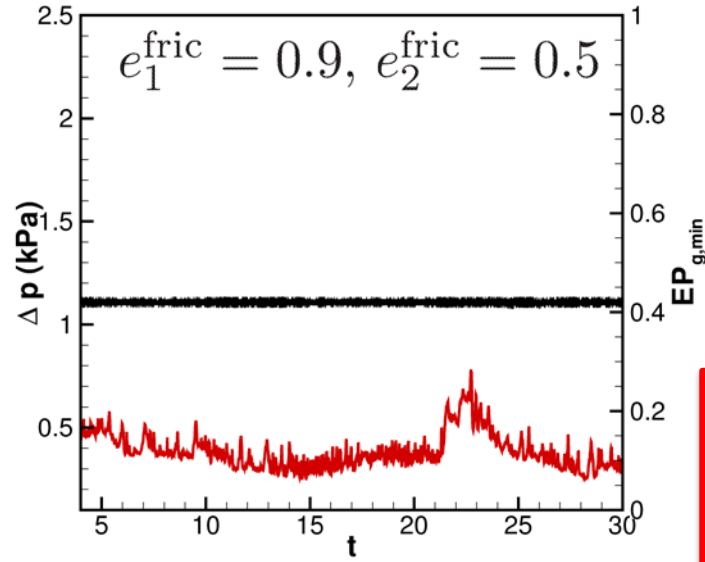
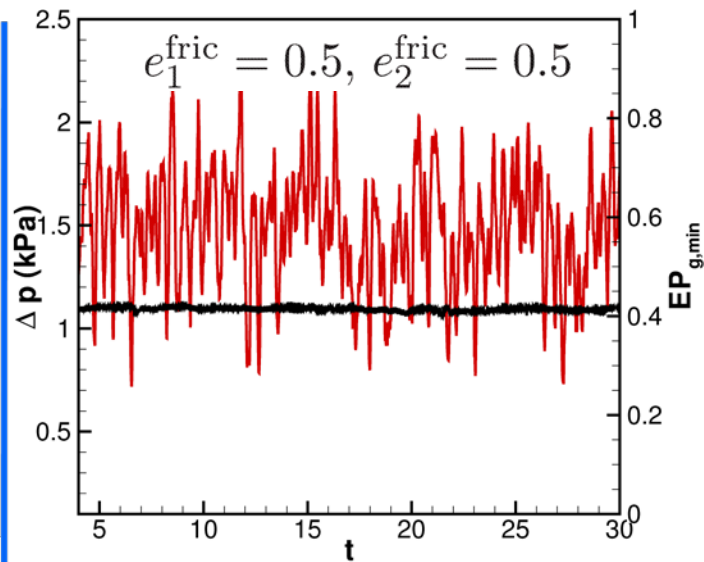
- Both MFIX-PIC and CPFD exhibit different bubble frequency with CPFD giving the lowest bubble frequency
- The amplitude of oscillations is higher in CPFD implying prediction of higher pressure fluctuations for design purposes

- Under-prediction of pressure drop by 15% for the best case.
- Pressure drop most sensitive to first frictional coefficient of restitution.
- Weak dependence on second frictional coefficient of restitution
- Recommended values of 0.3-0.6 for both parameters
- COMPUTATIONAL WALL TIMES:** TFM (400 mins), and MPPIC (80 mins) on a single core.

# Effect of frictional coefficient's of restitution

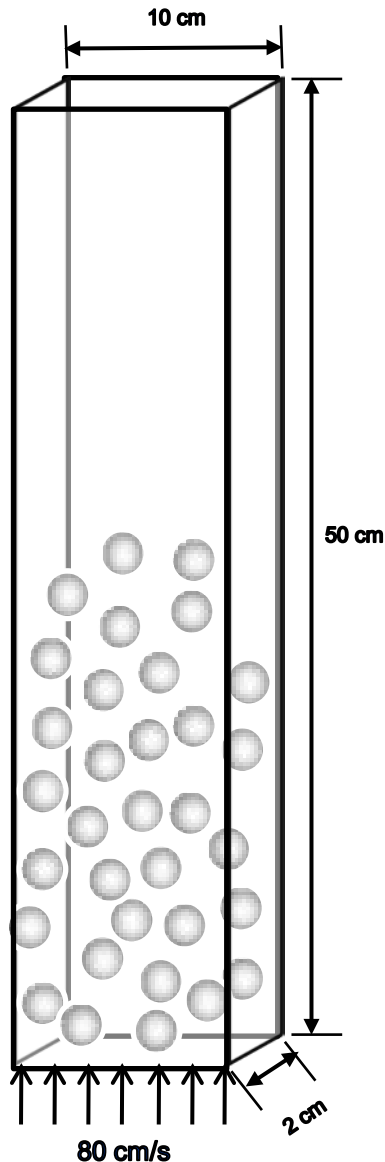
$$e_1^{\text{fric}}$$

$$e_2^{\text{fric}}$$



- The model's stability does not get affected by the first coefficient of restitution.
- Recommended values of 0.3-0.6 for both parameters

# Sample Problem 2: uniformly fluidized



## Properties

**Solids:**  $D_p = 0.1 \text{ cm}$ ,  $\rho_p = 2.5 \text{ g/cm}^3$

Total number of particles (DEM) = 305 K

Total number of parcels (MPPIC) = 16,000 ~ **20** particles per parcel

**Gas:** Air at standard conditions

Fluidization velocity = 80 cm/s

**box dimension** =  $(10 \times 50 \times 2) \text{ cm}^3 \equiv (20 \times 100 \times 4) \text{ cells}$

***FREE slip wall BC's for both gas and solids phase mean velocity***

**Drag model:** Wen & Yu / Ergun

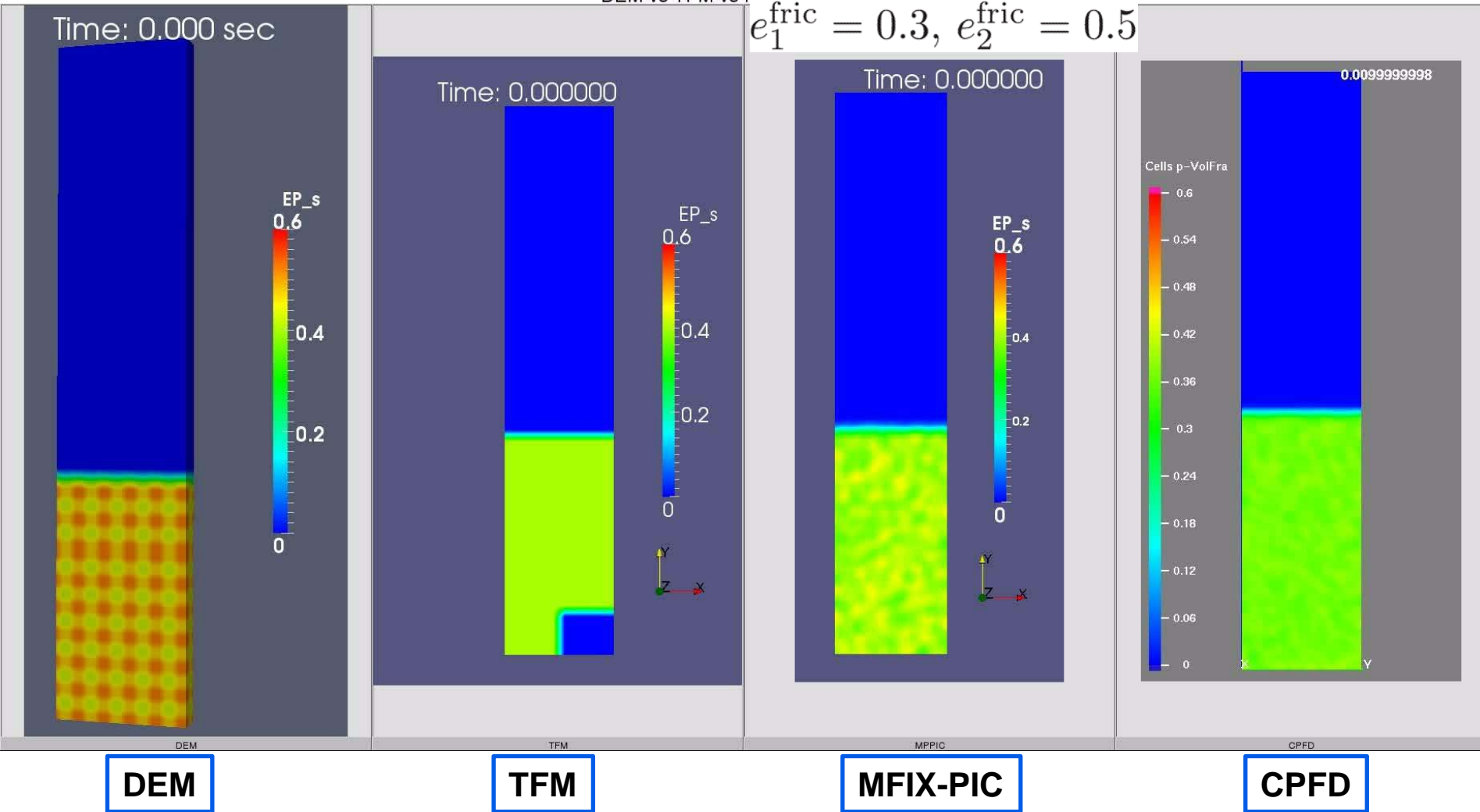
Pressure of bed weight = 1.96 kPa

Easiest to simulate, hardest to bubble!

# DEM vs TFM vs MPPIC vs CPFD

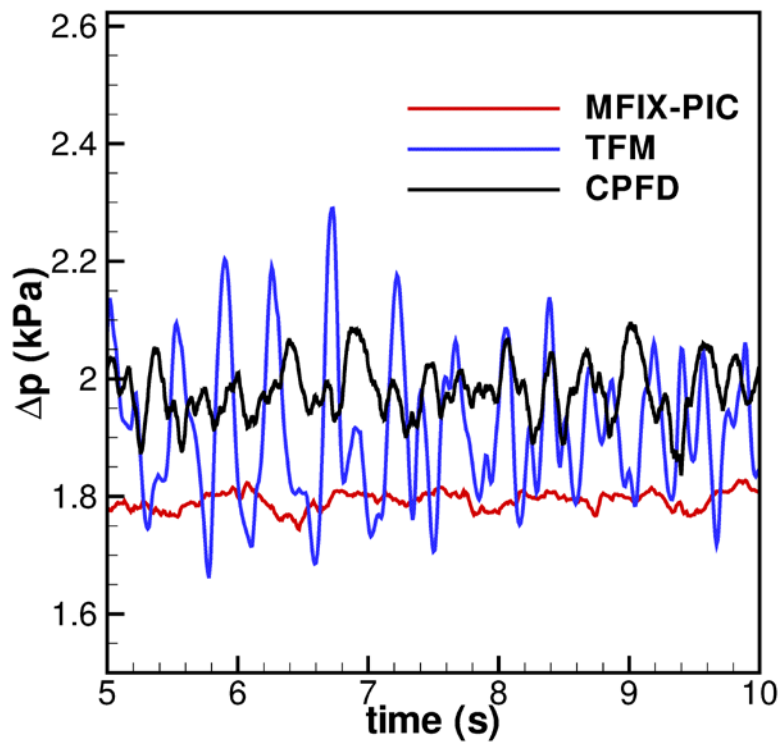
DEM vs TFM vs MPPIC vs CPFD

$$e_1^{\text{fric}} = 0.3, e_2^{\text{fric}} = 0.5$$



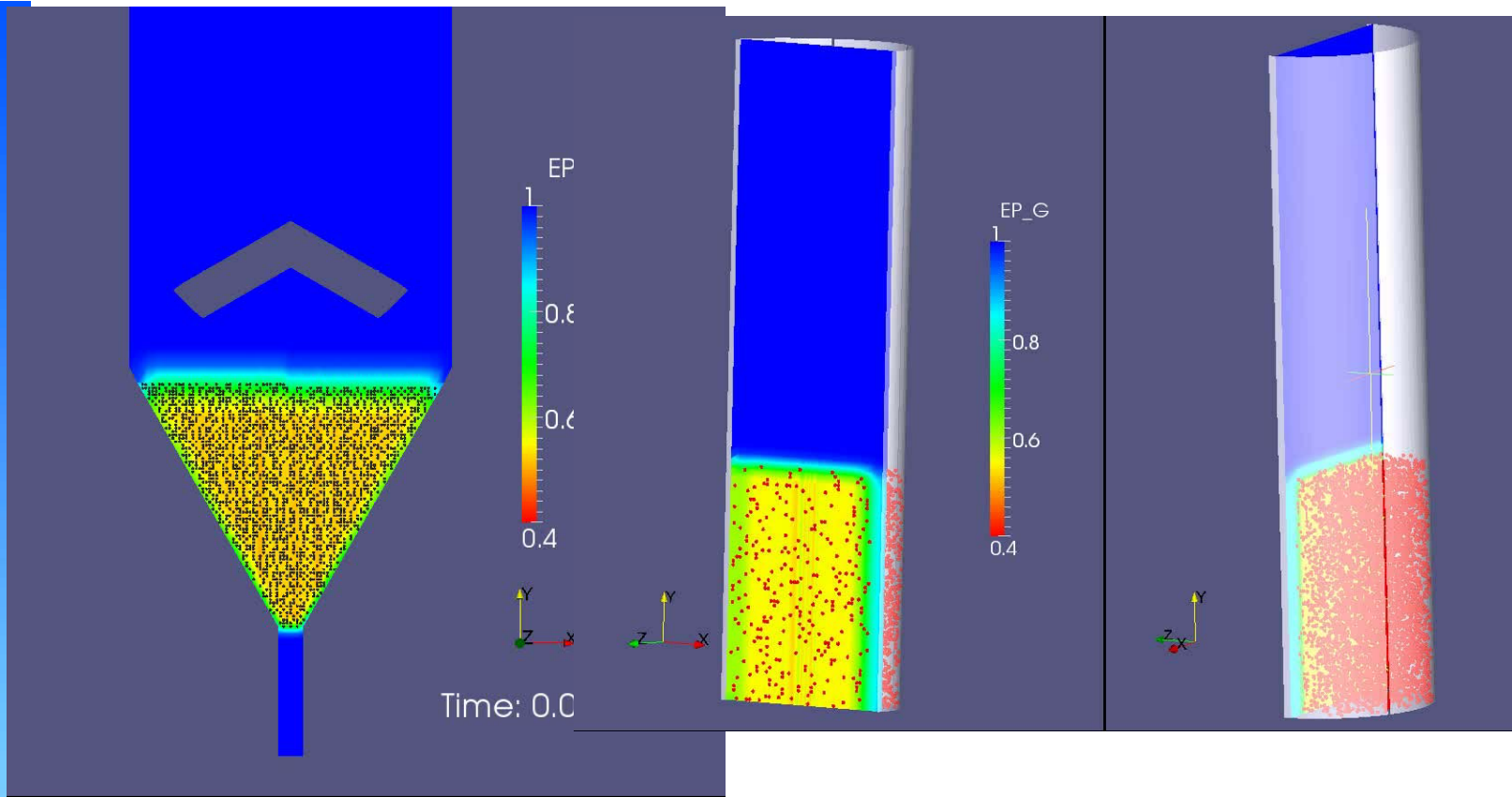
Both MFIX-PIC and CPFD do not bubble much and as a result predict low variations in pressure drop (see next slide)

# Pressure drop comparison





# Extension to Cartesian Grid



- **More work needed for robust extension of MPPIC model to cut-cell**
  - Forward interpolation of gas-phase velocity field
  - Calculation of solid phase frictional pressure on the Eulerian grid followed by its forward interpolation
  - Backward estimation of mean fields

# Conclusions/Observations

- **MPPIC model implemented in open-source MFIX code**
  - A new limiter based on physical arguments formulated for solid-stress model
- **MPPIC model compared against other CFD models and existing commercial MPPIC model**
- **MPPIC models found to be in qualitative and limited quantitative agreements with the more accurate DEM model**
- **Need to implement additional physical models for particle-particle and particle-wall interactions**

# Acknowledgments

This technical effort was performed in support of the National Energy Technology Laboratory's ongoing research in advanced numerical simulation of multiphase flow under the RES contract DE-FE0004000.