# Simulating Gas-Particle Flows Across All Flow Regimes in an Euler-Euler Framework

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#### Outline

- Motivation
- Operator-Splitting Algorithm
- Example Simulations
- Extension to Polydisperse Systems
- Summery and Future Work

## Motivation: Accurately Simulate Gas-Particle Flow

#### Two-Fluid Model (TFM)

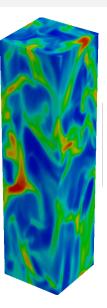
- Widely studied, developed and applied.
- Its hydrodynamic assumption has been proven invalid, especially when particles are dilute.

#### Quadrature-Based Moment Methods (QBMM)

- Direct numerical reconstruction, less modeling.
- Its explicit nature makes it inefficient when particles are dense.

#### Objective

 A solution algorithm that combines the best features of TFM and QBMM solvers, which can accurately simulate across all flow regimes.



## **Gas-Particle Flow Governing Equations**

Gas phase: Continuity and momentum transport equations

$$\begin{split} \frac{\partial \rho_g \alpha_g}{\partial t} + \nabla \cdot \rho_g \alpha_g \boldsymbol{U}_g &= 0 \\ \frac{\partial \rho_g \alpha_g \boldsymbol{U}_g}{\partial t} + \nabla \cdot (\rho_g \alpha_g \boldsymbol{U}_g \otimes \boldsymbol{U}_g + p_g \mathbf{I} - \rho_g \alpha_g \boldsymbol{\sigma}_g) &= \rho_g \alpha_g \boldsymbol{g} - \rho_p \alpha_p \boldsymbol{M}_{pg} \\ \boldsymbol{M}_{pg} &= \frac{1}{\tau_p} \left( \boldsymbol{U}_g - \boldsymbol{U}_p \right) - \frac{1}{\rho_p} \nabla p_g + \frac{\rho_g}{\rho_p} \nabla \cdot \alpha_g \boldsymbol{\sigma}_g \end{split}$$

Particle phase: Kinetic equation for velocity NDF  $f(\mathbf{v})$ 

$$\frac{\partial f(\mathbf{v})}{\partial t} + \mathbf{v} \cdot \frac{\partial f(\mathbf{v})}{\partial \mathbf{x}} + \frac{\partial}{\partial \mathbf{v}} \cdot f(\mathbf{v}) \mathbf{A} = \mathbb{S}$$

where A represents acceleration due to forces acting on each particle,  $\mathbb S$  represents other possible source terms, e.g. particle collisions

## Gas-Particle Flow Governing Equations: Velocity Moments

Moments Transport Equation:

$$\frac{\partial \mathbf{M}}{\partial t} + \nabla \cdot \mathbf{F} = \mathbf{S} \qquad M_{ijk}^{\gamma} = \int v_1^i v_2^j v_3^j f(\mathbf{v}) \, d\mathbf{v}$$

$$egin{aligned} M_{000}^0 = lpha_p, & egin{bmatrix} M_{100}^1 \ M_{010}^1 \ M_{001}^1 \end{bmatrix} = lpha_p oldsymbol{U}_p, & egin{bmatrix} M_{200}^2 & M_{110}^2 & M_{101}^2 \ M_{110}^2 & M_{021}^2 & M_{011}^2 \ M_{101}^2 & M_{002}^2 \end{bmatrix} = lpha_p oldsymbol{U}_p + lpha_p oldsymbol{ ext{P}}_p. \end{aligned}$$

Particle Continuity Equation:

$$\frac{\partial \rho_p \alpha_p}{\partial t} + \nabla \cdot \rho_p \alpha_p U_p = 0$$

Particle Momentum Equation:

$$\frac{\partial \rho_p \alpha_p \mathbf{U}_p}{\partial t} + \nabla \cdot \rho_p \alpha_p \left( \mathbf{U}_p \otimes \mathbf{U}_p + \mathbf{P}_p + \mathbf{G}_p + \mathbf{Z}_p \right) = \rho_p \alpha_p \mathbf{g} + \rho_p \alpha_p \mathbf{M}_{pg}$$

Particle Pressure-Tensor Equation:

$$\frac{\partial \rho_p \alpha_p \mathbf{P}_p}{\partial t} + \nabla \cdot \rho_p \alpha_p \left( \mathbf{U}_p \otimes \mathbf{P}_p + \mathbf{Q}_p + \mathbf{H}_p \right) + \rho_p \alpha_p \left[ \left( \mathbf{P}_p + \mathbf{G}_p \right) \cdot \nabla \mathbf{U}_p + \left( \nabla \mathbf{U}_p \right)^T \cdot \left( \mathbf{P}_p + \mathbf{G}_p \right) \right] \\
= \rho_p \alpha_p \mathbf{E}_{pg} + \rho_p \alpha_p \mathbf{C}_p$$

#### Particle Kinetic, Collisional and Frictional Flux

Kinetic Flux:

$$\mathbf{U}_{p} \otimes \mathbf{U}_{p} + \mathbf{P}_{p}$$

$$\mathbf{P}_{p} = \Theta_{p}\mathbf{I} - \mathbf{\sigma}_{p} = \Theta_{p}\mathbf{I} - 2\nu_{p,k}\mathbf{S}_{p}$$

$$\mathbf{S}_{p} = \frac{1}{2} \left[ \nabla \mathbf{U}_{p} + (\nabla \mathbf{U}_{p})^{T} - \frac{2}{3} (\nabla \cdot \mathbf{U}_{p}) \mathbf{I} \right]$$

Collisional Flux:

$$\mathbf{G}_p = \frac{p_{p,c}}{\rho_p \alpha_p} \mathbf{I} - 2\nu_{p,c} \mathbf{S}_p$$

Frictional Flux:

$$\mathbf{Z}_p = \frac{p_{p,f}}{\rho_p \alpha_p} \mathbf{I} - 2\nu_{p,f} \mathbf{S}_p$$

Heat Fluxes:

$$U_p \otimes \mathbf{P}_p + \mathbf{Q}_p + \mathbf{H}_p = U_p \otimes \mathbf{P}_p - \frac{2}{3} k_{\Theta} \nabla \otimes \mathbf{P}_p$$

## Flux-Splitting Scheme

$$\frac{\partial \mathbf{M}}{\partial t} + \nabla \cdot h_1 \mathbf{F} + \nabla \cdot (h_2 \mathbf{F} + \mathbf{G} + \mathbf{Z}) = \mathbf{S}$$

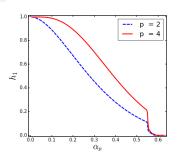
$$h_1 = 1 - h_2$$

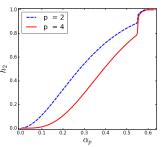
$$h_2 = \left(\frac{p_{p,c}^* + p_{p,f}}{p_{p,k} + p_{p,c}^* + p_{p,f} + \varepsilon}\right)^p$$

$$p_{p,c}^* = 2(1 + e)\rho_p \alpha_p^2 g_0 \Theta_p$$

$$\frac{\partial \mathbf{M}}{\partial t} + \nabla \cdot h_1 \mathbf{F} = \mathbf{0}$$

$$\frac{\partial \mathbf{M}}{\partial t} + \nabla \cdot (h_2 \mathbf{F} + \mathbf{G} + \mathbf{Z}) = \mathbf{S}$$





## Hydrodynamic Solver: $\partial \mathbf{M}/\partial t + \nabla \cdot (h_2 \mathbf{F} + \mathbf{G} + \mathbf{Z}) = \mathbf{S}$

Particle Volume Fraction:

$$\frac{\partial \alpha_p}{\partial t} + \nabla \cdot \mathbf{h_2} \alpha_p \mathbf{U}_p = 0,$$

Particle Velocity:

$$\frac{\partial \alpha_{p} \boldsymbol{U}_{p}}{\partial t} + \nabla \cdot \left( \mathbf{h}_{2} \alpha_{p} \boldsymbol{U}_{p} \otimes \boldsymbol{U}_{p} + \frac{p_{p}^{*}}{\rho_{p}} \boldsymbol{I} - 2\alpha_{p} \nu_{p}^{*} \boldsymbol{S}_{p} \right) = \alpha_{p} \boldsymbol{g} + \frac{\alpha_{p}}{\tau_{p}} \left( \boldsymbol{U}_{g} - \boldsymbol{U}_{p} \right) - \frac{\alpha_{p}}{\rho_{p}} \nabla p_{g} + \alpha_{p} \rho_{g} \nabla \cdot \alpha_{g} \boldsymbol{\sigma}_{g}$$

$$p_{p}^{*} = \mathbf{h}_{2} p_{p,k} + p_{p,c} + p_{p,f} \quad \nu_{p}^{*} = \left( 1 + \frac{8\eta \alpha_{p} g_{0}}{5} \right) \mathbf{h}_{2} \nu_{p,k} + \frac{3}{5} \nu_{p,b} + \nu_{p,f}$$

Particle Granular Temperature:

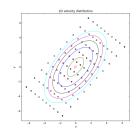
$$\frac{3}{2}\left(\frac{\partial\alpha_{p}\Theta_{p}}{\partial t}+\nabla\cdot\mathbf{\underline{h_{2}}}\alpha_{p}\Theta_{p}U_{p}\right)=\nabla\cdot(\alpha_{p}k_{\Theta}^{\dagger}\nabla\Theta_{p})-\left(\frac{p_{p}^{\dagger}}{\rho_{p}}\mathbf{I}-2\alpha_{p}\nu_{p}^{\dagger}\mathbf{S}_{p}\right):\nabla U_{p}-3\left(\frac{1-e^{2}}{2\tau_{c}}+\frac{1}{\tau_{p}}\right)\alpha_{p}\Theta_{p}$$

$$p_{p}^{\dagger} = \mathbf{h_{2}} p_{p,k} + p_{p,c} \quad \nu_{p}^{\dagger} = \left(1 + \frac{8\eta\alpha_{p}g_{0}}{5}\right) \mathbf{h_{2}} \nu_{p,k} + \frac{3}{5}\nu_{p,b} \quad k_{\Theta}^{\dagger} = \left(1 + \frac{12\eta\alpha_{p}g_{0}}{5}\right) \mathbf{h_{2}} k_{\Theta,k} + \frac{3}{2}\nu_{p,b}$$

## Free Transport Solver: $\partial \mathbf{M}/\partial t + \nabla \cdot h_1 \mathbf{F} = \mathbf{0}$

Anisotropic Gaussian Velocity Distribution:

$$g(\mathbf{v}) = \frac{\alpha_p}{(2\pi |\mathbf{P}_p|)^{3/2}} \exp\left[-\frac{1}{2}(\mathbf{v} - \mathbf{U}_p) \cdot \mathbf{P}_p^{-1} \cdot (\mathbf{v} - \mathbf{U}_p)\right]$$



**Granular Stress Tensor Transport** 

$$\begin{split} \frac{\partial \rho_p \alpha_p \boldsymbol{\sigma}_p}{\partial t} + \nabla \cdot \rho_p \alpha_p \left( \frac{\mathbf{h_2} \boldsymbol{U}_p \otimes \boldsymbol{\sigma}_p - \frac{2}{3} k_{\Theta}^{\dagger} \nabla \otimes \boldsymbol{\sigma}_p \right) &= \rho_p \alpha_p \left( \boldsymbol{S}_{2,\text{flux}} - \boldsymbol{S}_2 \right) \\ \boldsymbol{S}_{2,\text{flux}} &= \frac{2 p_p^{\dagger}}{\rho_p \alpha_p} \boldsymbol{S}_p - 2 \nu_p^{\dagger} \left[ \boldsymbol{S}_p \cdot \nabla \boldsymbol{U}_p + (\nabla \boldsymbol{U}_p)^T \cdot \boldsymbol{S}_p - \frac{2}{3} (\boldsymbol{S}_p : \nabla \boldsymbol{U}_p) \mathbf{I} \right] \\ \boldsymbol{S}_2 &= \left[ \frac{2}{\tau_p} + \frac{(3 - e)(1 + e)}{2\tau_c} \right] \boldsymbol{\sigma}_p \end{split}$$

#### Wall Boundary Conditions

Hydrodynamic solver:

$$\nu_{p}^{*} \frac{\partial \boldsymbol{U}_{p,t}}{\partial x_{w}} = -\mathbf{h}_{2,\mathbf{w}} \phi_{s} \mathcal{V}_{w} \boldsymbol{U}_{p,t} - \frac{p_{p,f} \tan \phi_{w}}{\rho_{p} \alpha_{p}} \frac{\boldsymbol{U}_{p,t}}{|\boldsymbol{U}_{p,t}|}$$
$$k_{\Theta}^{\dagger} \frac{\partial \Theta_{p}}{\partial \boldsymbol{x}_{w}} = \mathbf{h}_{2,\mathbf{w}} \left[ \phi_{s} \mathcal{V}_{w} |\boldsymbol{U}_{p,t}|^{2} - \frac{3}{2} \left( 1 - e_{w}^{2} \right) \mathcal{V}_{w} \Theta_{p} \right].$$
$$\mathcal{V}_{w} = (\pi/6) \sqrt{3\Theta_{p}}$$

Free transport solver:

$$\mathbf{F}_{w} = \mathbf{h}_{1,\mathbf{w}} \int_{\mathbf{v} \cdot \mathbf{n}_{w} > 0} \mathbf{G}_{r}(\mathbf{v}) (\mathbf{v} \cdot \mathbf{n}_{w}) d\mathcal{S}_{w}$$

$$f_{r}(\mathbf{v}) = \phi_{s} f_{r,d}(\mathbf{v}) + (1 - \phi_{s}) f_{r,s}(\mathbf{v})$$

$$f_{r,s}(\mathbf{v}) = f_{i} (\mathbf{v} - (1 + e_{w})(\mathbf{v} \cdot \mathbf{n}_{w}) \mathbf{n}_{w})$$

#### Solution Procedure

- Initialize all variables  $\mathbf{M}$ ,  $\{\alpha_p, \mathbf{U}_p, \Theta_p, \boldsymbol{\sigma}_p\}$ , and  $\{\alpha_g, \mathbf{U}_g, p_g\}$ .
- **2** Calculate  $h_1$  and  $h_2$ .
- **Solution** Explicit Free Transport Solver:

Compute kinetic-based moment fluxes to transport the moments Update  $\{\alpha_p, U_p, \Theta_p, \sigma_p\}$  using moments **M**.

- **1 Iterative** Hydrodynamic Solver:
  - Solve  $\{\alpha_p, U_p, \Theta_p\}$  hydrodynamic transport equations Solve gas phase velocity and pressure,  $\{U_g, p_g\}$ , equations.
- **Solve**  $\sigma_p$  transport equation.
- **6** Update moment set **M** using  $\{\alpha_p, U_p, \Theta_p, \sigma_p\}$ .
- Advance in time by repeating from Step 2 until simulation is complete.

# Example Simulations: Models in Hydrodynamic Solver

Drag

$$\tau_{p} = \frac{_{4\rho_{p}d_{p}^{2}}}{_{3\rho_{g}\nu_{g}C_{D}Re_{p}}}, \quad Re_{p} = \frac{_{\alpha_{g}d_{p}|U_{g}-U_{p}|}}{_{\nu_{g}}}, \quad C_{D} = \max\left[\frac{_{24}}{Re_{p}}\left(1 + Re_{p}^{0.687}\right), 0.44\right]\alpha_{g}^{-2.65}$$

Particle Collision:

$$\eta = \frac{1}{2}(1+e), \quad g_0 = \frac{1-\frac{1}{2}\alpha_p}{(1-\alpha_p)^3}, \quad au_c = \frac{d_p}{6\alpha_p g_0 \sqrt{\Theta_p/\pi}}, \quad \Delta^* = \eta^2 \Theta_p \mathbf{I} + (1-\eta)^2 \mathbf{P}_p$$

Particle Pressure:

$$p_{p,k} = \rho_p \alpha_p \Theta_p, \quad p_{p,c} = 4\rho_p \eta \alpha_p^2 g_0 \Theta_p - \rho_p \alpha_p \nu_{p,b} \nabla \cdot U_p, \quad p_{p,f} = Fr \frac{(\alpha_p - \alpha_{p,fr,min})^s}{(\alpha_{p,max} - \alpha_p)^s}$$

Particle Viscosity:

$$\begin{array}{l} \nu_{p,b} = \frac{8\eta\alpha_{p}g_{0}d_{p}\sqrt{\Theta_{p}}}{3\sqrt{\pi}}, \quad \nu_{p,k} = \frac{1}{2}\Theta_{p}\left[\frac{1}{\tau_{p}} + \frac{\eta(2-\eta)}{\tau_{c}}\right]^{-1}\left[1 + \frac{8}{5}\eta(3\eta-2)\alpha_{p}g_{0}\right] \\ \nu_{p,c} = \frac{8\eta\alpha_{p}g_{0}}{5}\nu_{p,k} + \frac{3}{5}\nu_{p,b}, \quad \nu_{p,f} = \frac{p_{p,f}}{\rho_{p}\alpha_{p}\|\mathbf{S}_{p}\|}\sin\phi \end{array}$$

Particle Conductivity:

$$k_{\Theta,k} = \frac{5}{2}\Theta_p \left[ \frac{3}{\tau_p} + \frac{4\eta(41 - 33\eta)}{\tau_c} \right]^{-1} \left[ 1 + \frac{12}{5}\eta^2 (4\eta - 3)\alpha_p g_0 \right] \quad k_{\Theta,c} = \frac{12\eta\alpha_p g_0}{5} k_{\Theta,k} + \frac{3}{2}\nu_{p,b}$$

# Example Simulations : 2D Fluidized Bed, p = 4

 $\alpha_p$ 

 $h_2$ 

 $U_{p,y}$ 

 $\Theta_p$ 

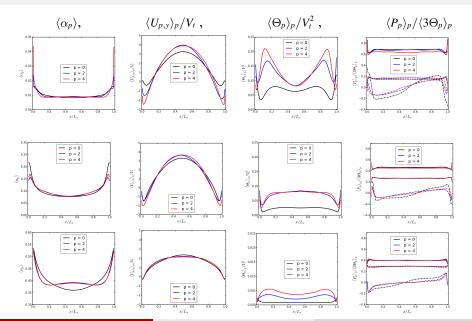
 $\sigma_{p,xy}$ 

#### 3D Wall-bound Vertical Channel: Instantaneous Fields

$$d_{p} = 100 \mu \text{m}, \rho_{p} = 1000 \text{ kg/m}^{3}, \rho_{g} = 1 \text{ kg/m}^{3}, \nu_{g} = 1.8 \times 10^{-5} \text{ m}^{2}/\text{s}, \\ e = 0.9, e_{w} = 0.9, \phi = 0.25, \phi_{s} = 0.1, \phi_{w} = 0.25, p = 4$$

$$\overline{\alpha}_{p} = 0.01 \qquad \overline{\alpha}_{p} = 0.4$$

#### Wall-bound Vertical Channel: Statistical results



#### Extension to Polydisperse Systems

Joint size-velocity NDF:

$$n(\xi, \mathbf{v}) = f(\xi) g(\mathbf{v}|\xi)$$

Free transport solver:

Size distribution  $f(\xi):\{M^0_{0000},M^0_{0001},M^0_{0002},M^0_{0003}\} \to \{w_1,w_2,\xi_1,\xi_2\}$ 

Size conditioned velocity distribution  $g(v|\xi)$ :  $U_n, \Theta_n, \sigma_n$ .

Hydrodynamic solver:

Direct QMOM, i.e. treat quadrature node as particle phase

$$\frac{\partial w_n}{\partial t} + \nabla \cdot (\mathbf{h_2} w_n \mathbf{U}_n) = 0$$

$$\frac{\partial \rho_n \alpha_n}{\partial t} + \nabla \cdot (\mathbf{h_2} \rho_n \alpha_n \mathbf{U}_n) = 0$$

$$\rho_n \alpha_n = w_n \xi_n = w_n (\rho_n \frac{1}{6} \pi d_n^3)$$

#### **Conclusions**

- A solution algorithm is proposed to accurately treat all fluid-particle regimes occurring simultaneously.
- This algorithm is based on splitting the free-transport flux solver dynamically and locally in the flow. Hydrodynamic solver is employed in close-packed to moderately dense regions, while in dilute to very dilute regions a kinetic-based finite-volume solver is used in conjunction with QBMM.
- To illustrate the accuracy and robustness of the proposed solution algorithm, it is implemented for particle velocity moments up to second order.
- By varying the average particle volume fraction in the flow domain, it is demonstrated that the flow solver can handle seamlessly all flow regimes present in fluid-particle flows.

#### Future Work

- Enable MFIX-QBMM to handle complex geometries by using Cutcell technique in MFIX.
- Implement Hyperbolic Quadrature Method of Moments (HQMOM) to better capture particle trajectory crossing (PTC).
- Implement and validate gas-particle turbulence model in MFIX.
- Consolidate previous QBMM implementations into current MFIX-QBMM module: DQMOM and QMOMK.

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Thank you for your attention !!!

Questions?