

Heat and mass transfer in high-temperature particle-gas flows under high-flux irradiation

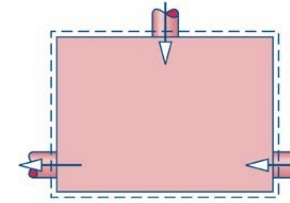
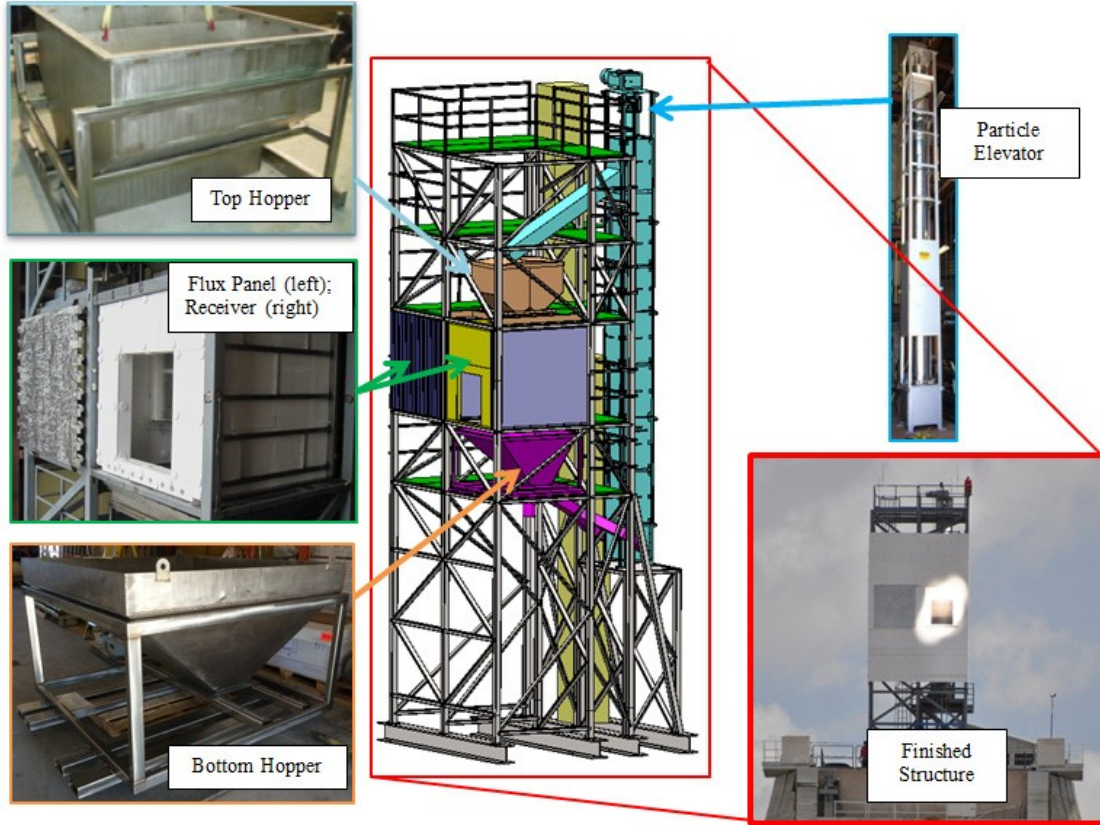
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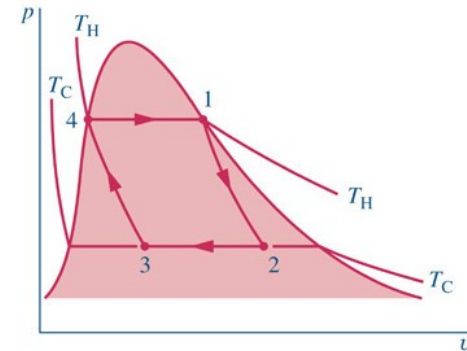
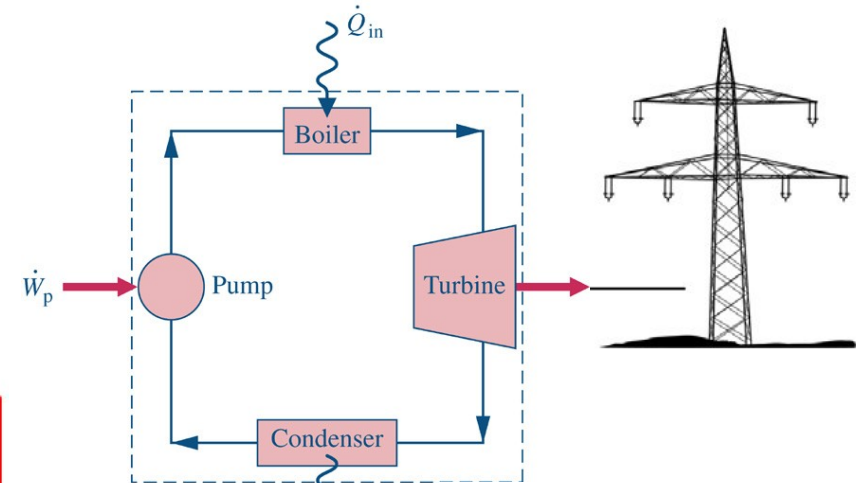
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Overview of solar power plant

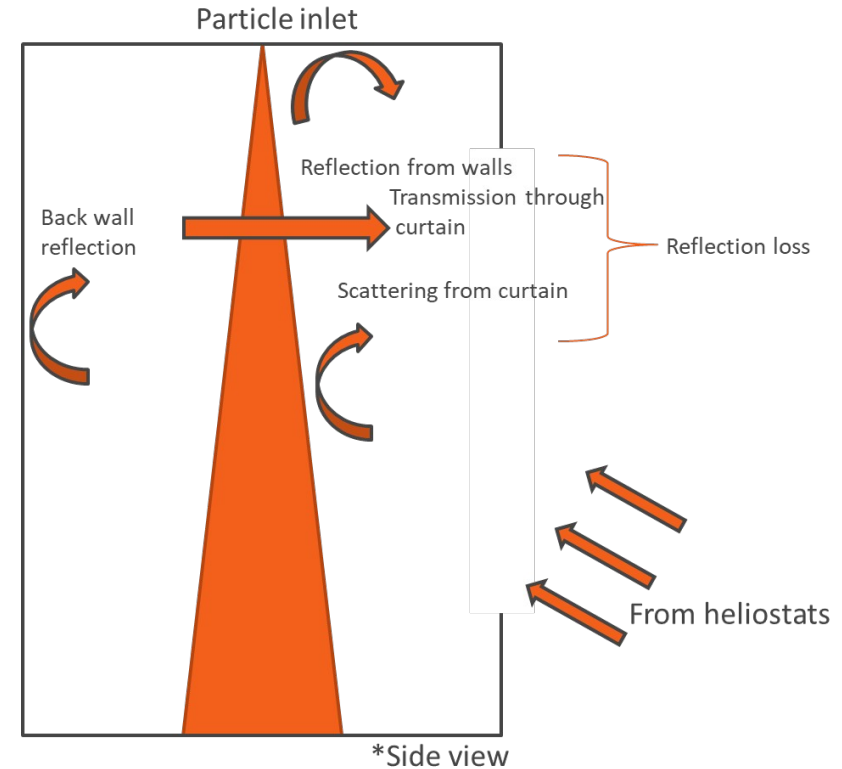


Heat exchanger



Falling particle receivers

- Falling particle receivers (FPRs) are a leading technology to couple with next generation CSP systems
- FPRs release a curtain of particles as the working fluid that are heated as they fall past the beam of concentrated solar radiation
- Advantages:
 - 1) Can achieve high particle temperatures
 - 2) High thermal efficiency
 - 3) Low cost transfer medium
 - 4) Efficient storage



J. Coventry, et al., AIP Conference Proceedings, 1850 (2017): 030011

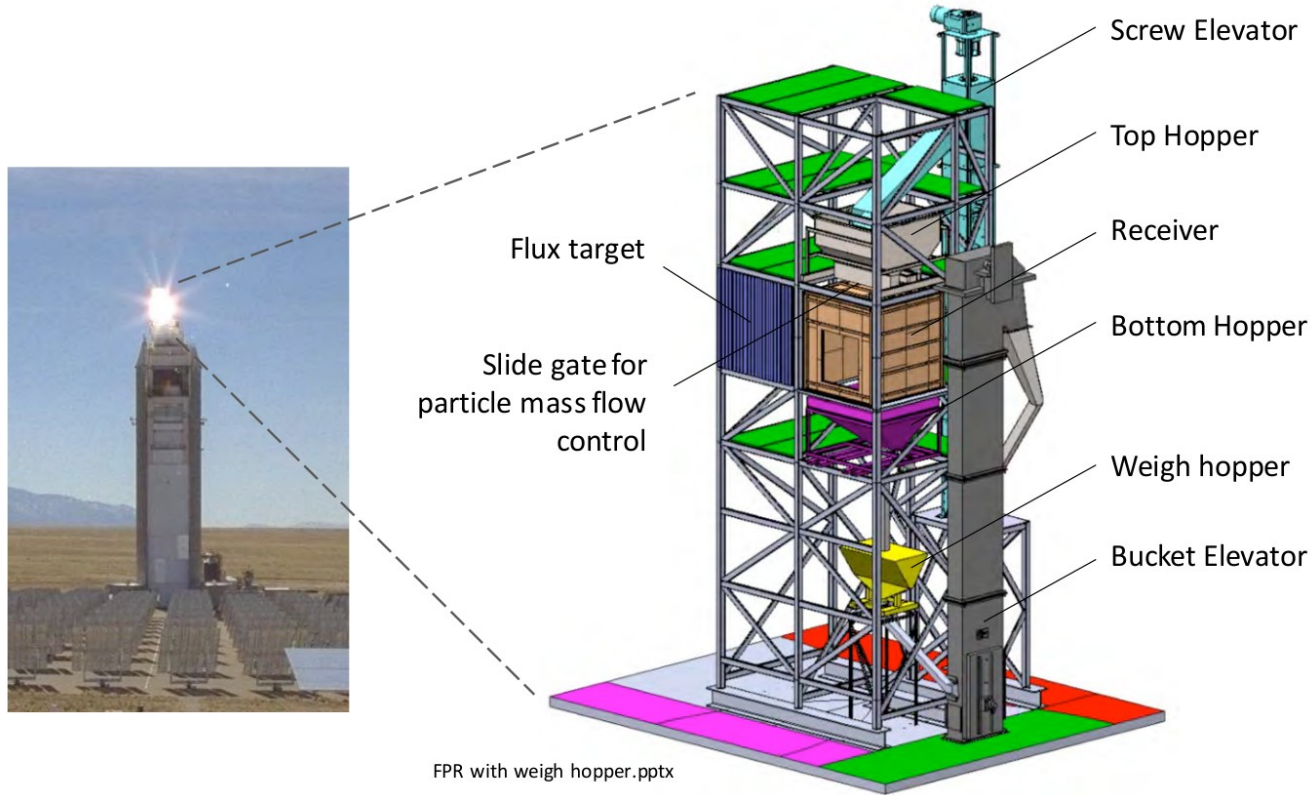
C.K. Ho, US Patent App. 16/700,134 (2020) C. Ho, Applied Thermal Engineering, 2016.

A. Kumar et al., ASME Journal of Solar Energy Engineering, 2018.

A. Kumar et al., International Journal of Heat and Mass Transfer, 2019.

Free-falling particle receiver (SNL)

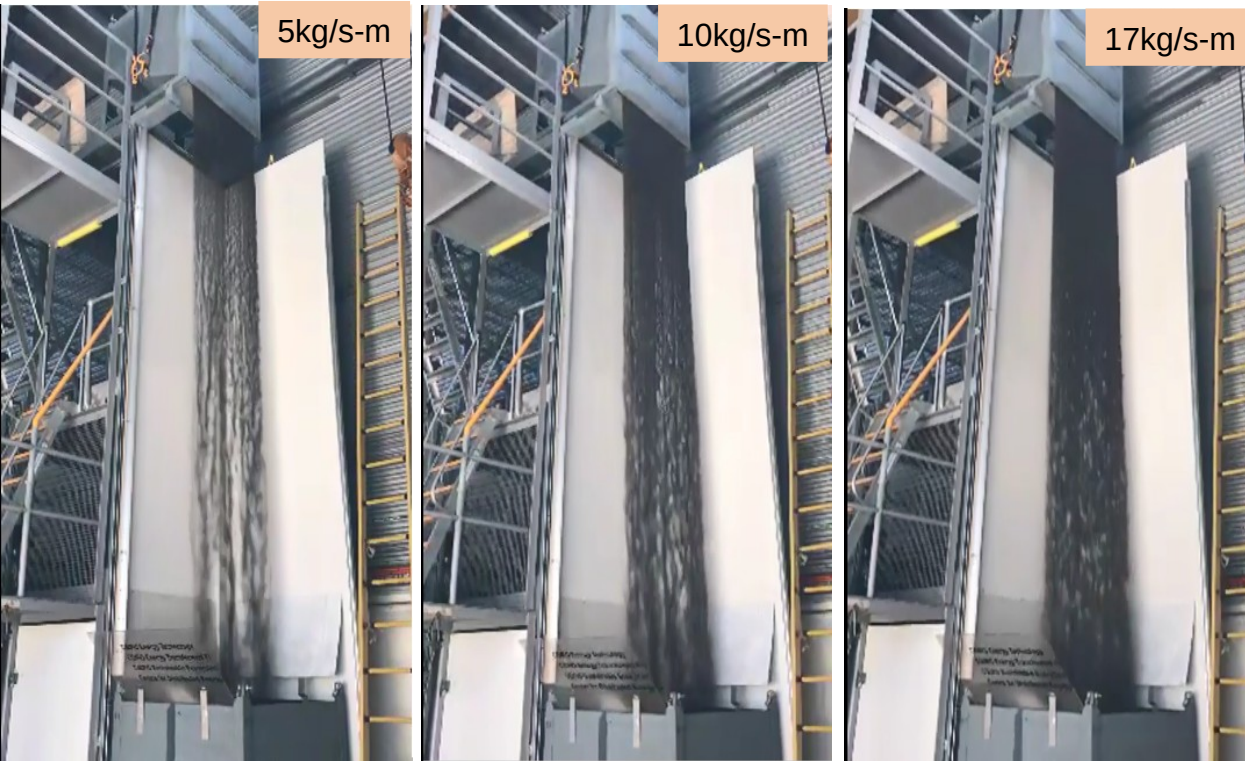
- Gen3 particle receiver & on-sun test



- CARBO HSP particles
- ~350 μ m diameter
 - ~0.9 solar absorptivity

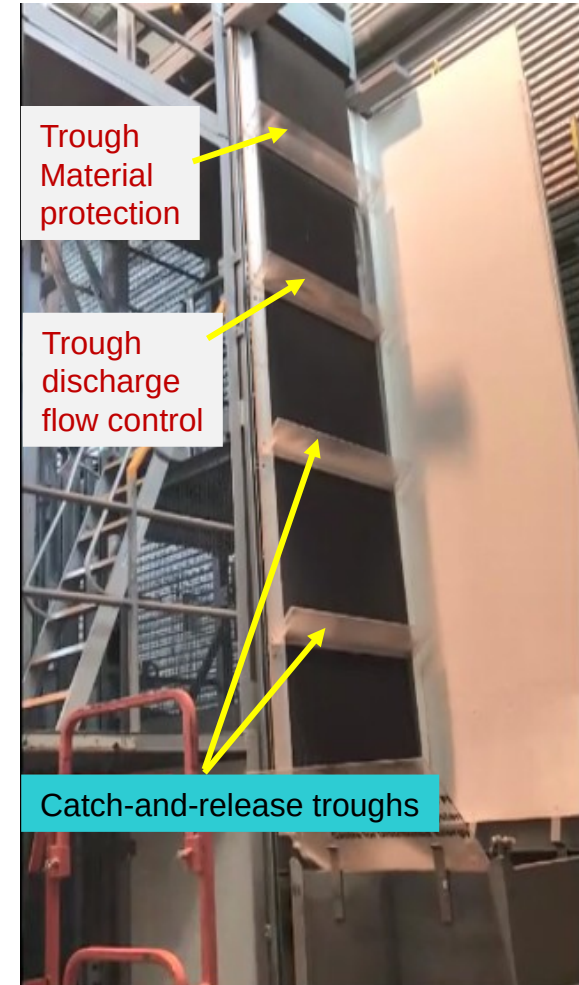
Multi-stage receiver (CSIRO)

Multi-stage falling



Free-falling particles:

- Decreased absorptance
- Flow instability
- Uneven heating
- Air entrainment



Multi-phase flow

- Gas phase

Euler

$$\frac{\partial}{\partial t}(\varepsilon_g \rho_g) + \frac{\partial}{\partial x_i}(\varepsilon_g \rho_g u_{gi}) = 0$$

$$\frac{\partial}{\partial t}(\varepsilon_g \rho_g u_{gi}) + \frac{\partial}{\partial x_j}(\varepsilon_g \rho_g u_{gj} u_{gi}) = -\varepsilon_g \frac{\partial p}{\partial x_i} + \frac{\partial \tau_{gij}}{\partial x_j} - F_i + \varepsilon_g \rho_g g_i$$

- Particle phase

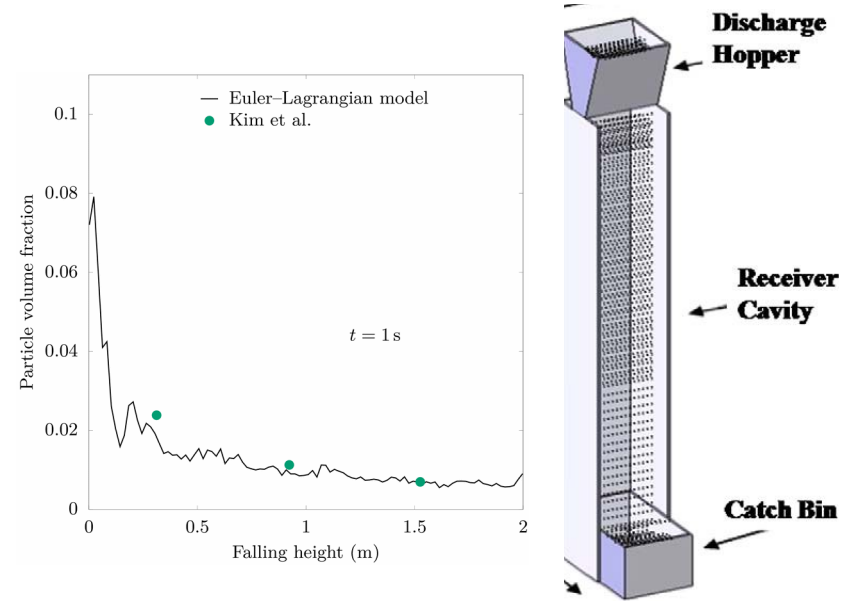
$$\frac{\partial f}{\partial t} + \sum_i \left[\frac{\partial (f u_{pi})}{\partial x_i} + \frac{\partial (f A_i)}{\partial u_{pi}} \right] = 0$$

$$\varepsilon_p = \int \int f \frac{m}{\rho_p} dm \Pi_j du_{pj}$$

$$\frac{\partial (\varepsilon_p \rho_p)}{\partial t} + \frac{\partial (\varepsilon_p \rho_p \bar{u}_{pi})}{\partial x_i} = 0$$

$$\frac{\partial (\varepsilon_p \rho_p \bar{u}_{pi})}{\partial t} + \frac{\partial (\varepsilon_p \rho_p \bar{u}_{pi} \bar{u}_{pi})}{\partial x_i} = -\varepsilon_p \frac{\partial p}{\partial x_i} - \frac{\partial \tau}{\partial x_i} + \varepsilon_p \rho_p g_i$$

$$+ \int \int f m D(u_{gi} - u_{pi}) dm du_{pj} - \frac{\partial \left[\int \int f m (u_{gi} - u_{pi})(u_{gi} - u_{pi}) dm du_{pj} \right]}{\partial x_i}$$



Multiphase particle-in-cell

M. Syamlal, W. Rogers, T. O'Brien, MFX documentation theory guide, 1993

M. Andrews, P. O'Rourke, Int. J. Multiphase Flow, 22 (1996): 379-402

D.M. Sniderr, J. Computational Physics, 170 (2001): 523-549

K. Kim, N. Siegel, et al., Solar Energy 83 (2009): 1784-1793

- Gas phase

$$\varepsilon_g \rho_g c_{p,g} \left(\frac{\partial T_g}{\partial t} + u_{gj} \frac{\partial T_g}{\partial x_j} \right) = - \frac{\partial q''_{gi}}{\partial x_i} - \frac{\partial q''_{ci}}{\partial x_i}$$

$$q''_{gi} = -\varepsilon_g k_g \frac{\partial T_g}{\partial x_i}$$

$$- \frac{\partial q''_{ci}}{\partial x_i} = 6\varepsilon_p \frac{\sum_{m=1}^{N_p} n_{p,m} d_{p,m}^2 h_{p,g} (T_{p,m} - T_g)}{\sum_{m=1}^{N_p} n_{p,m} d_{p,m}^3}$$

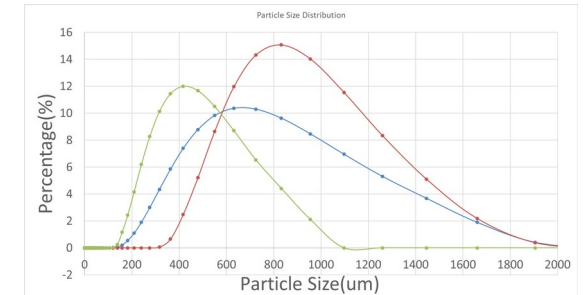
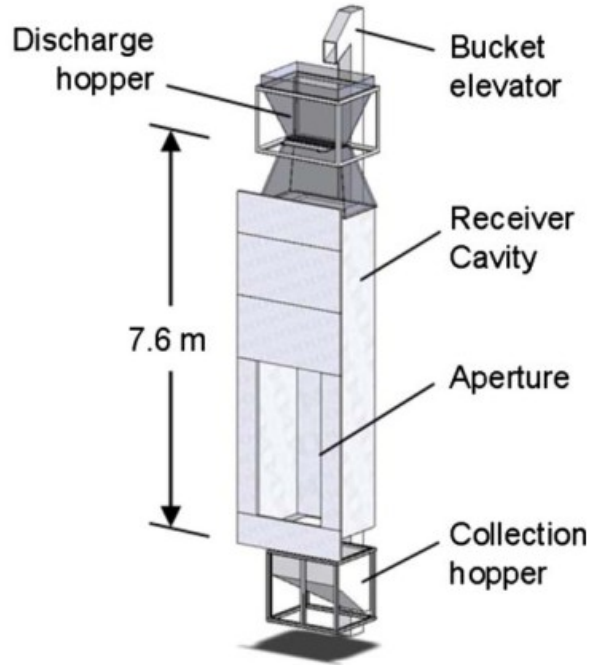
- Particle phase

$$n_{p,i} m c_{v,p} \frac{dT_{p,i}}{dt} = q_{c,i} + \underline{q_{r,i}},$$

$$q_{c,i} = n_{p,i} h_{p,g} \pi d_{p,i}^2 (T_g - T_{p,i})$$

$$\underline{q_{r,i}} = n_{p,i} \pi d_{p,i}^2 \underline{q''_{r,i}}$$

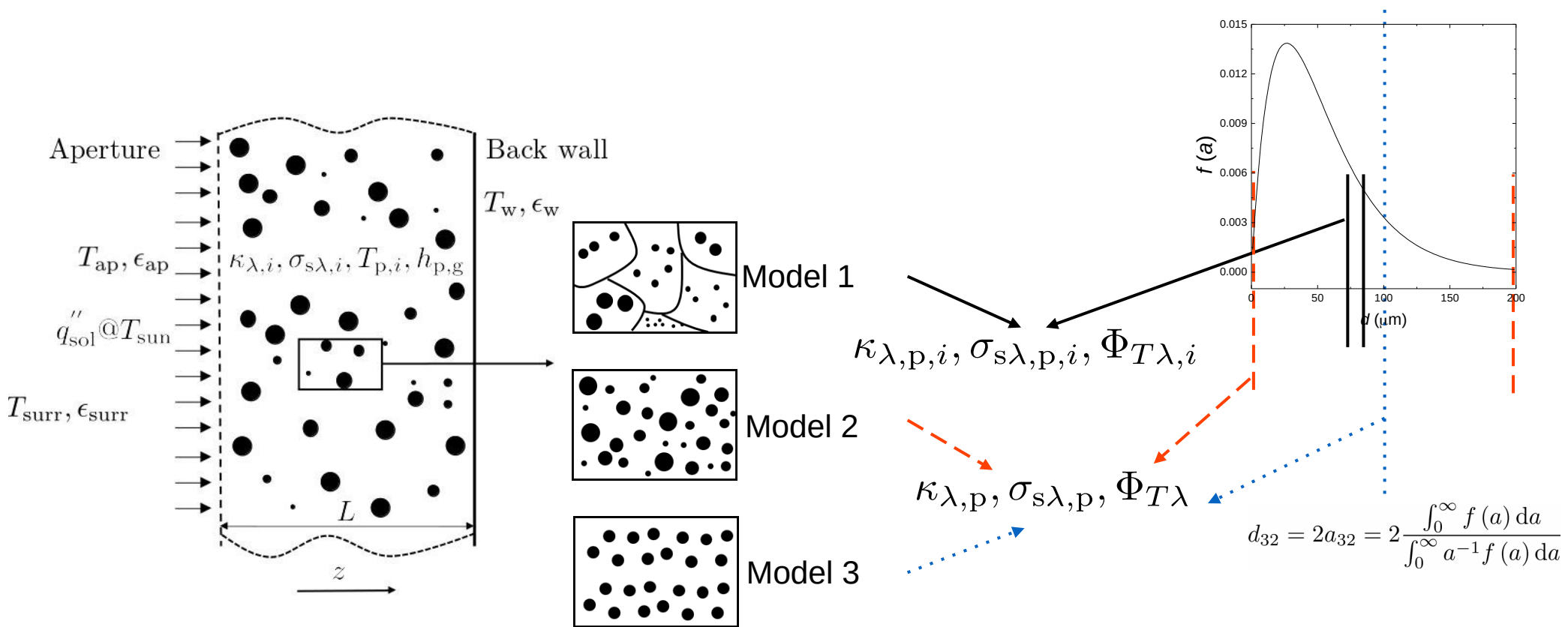
Radiative heat transfer



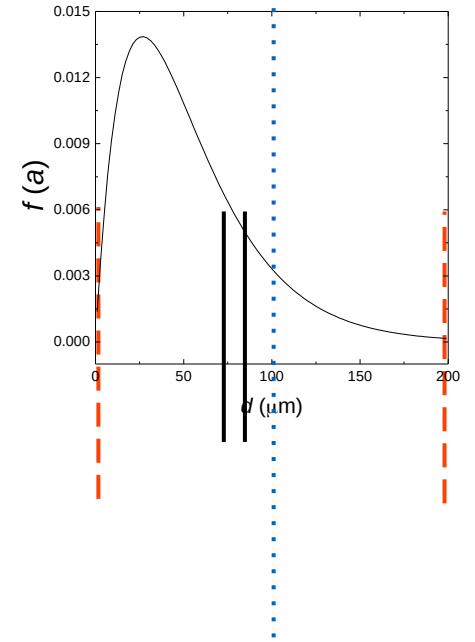
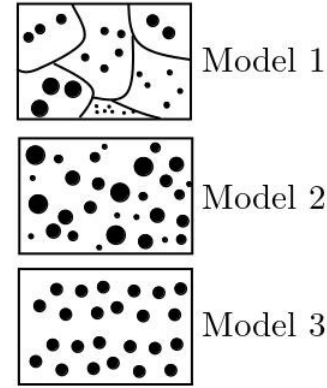
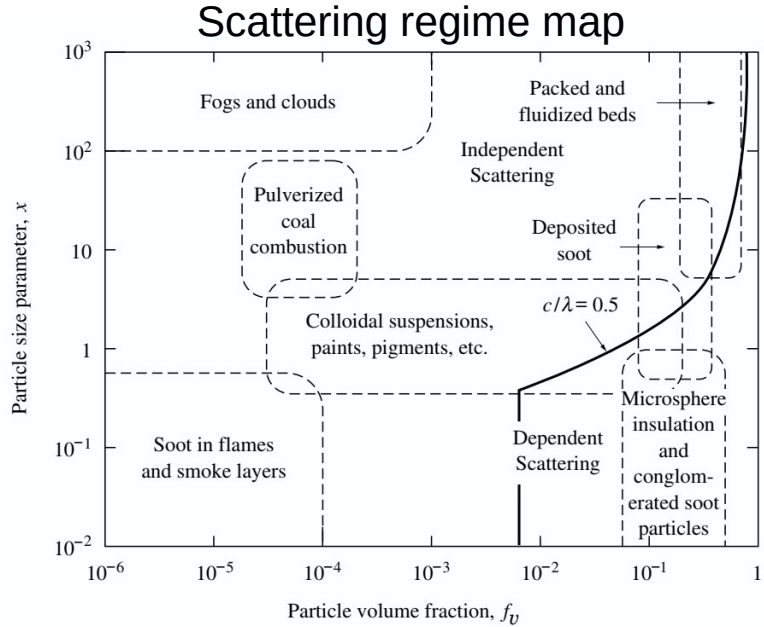
- J. Coventry, et al., AIP Conference Proceedings, 1850 (2017): 030011
C.K. Ho, US Patent App. 16/700,134 (2020)
N.P. Siegel, et al., Journal of Solar Energy Engineering, 132 (2010): 021008-1
W. Lipiński, et al., Heat and Mass Transfer, 41 (2005): 1021–1032
W. Lipiński, et al., Numerical Heat Transfer, Part B, 47 (2005): 443–457
A. Kumar, et al., International Journal of Heat and Mass Transfer, 146 (2020): 118821

Light–matter interactions in polydispersions

Radiative heat transfer



Radiative heat transfer



$$(a_{\min,i}, a_{\max,i}) \quad (0, a_{\max})$$

$$\frac{3}{4} \int_{a_{\min,i}}^{a_{\max,i}} \{Q_{\text{sca}}, Q_{\text{abs}}, Q_{\text{ext}}\} a^{-1} f(a) f_v da, \text{ App. 1 \& 2}$$

$$\{\sigma_s, \kappa, \beta\}_{\lambda,i} =$$

Mie theory

$$\frac{3f_v}{2d_{32}} \{Q_{\text{sca}}, Q_{\text{abs}}, Q_{\text{ext}}\}, \text{ App. 3}$$

C.L. Tien, et al., Annual Review of Numerical Fluid Mechanics and Heat Transfer, 1 (1987): 1–32

M.F. Modest, Radiative Heat Transfer, 2013

C. Bohren, et al., Absorption and Scattering of Light by Small Particles, 2008

Radiative heat transfer

- Radiative transfer equation

$$\frac{dI_\lambda}{ds} = \sum_{i=1}^M \kappa_{\lambda,i} I_{b\lambda,i}(T_{p,i}) - \left(\sum_{i=1}^M \beta_{\lambda,i} \right) I_\lambda + \frac{1}{4\pi} \int_{4\pi} \left(\sum_{i=1}^M \sigma_{s\lambda,i} \bar{\Phi}_{\lambda,i}(\hat{\mathbf{s}}_j, \hat{\mathbf{s}}) \right) I_\lambda(\hat{\mathbf{s}}_j) d\Omega_j$$

$$I_\lambda(z=0, \hat{\mathbf{s}}) = q''_\lambda \delta(\hat{\mathbf{s}} - \hat{\mathbf{s}}_0)$$

$$I_\lambda(z=L, \hat{\mathbf{s}}) = \epsilon_{\lambda,w} I_{b\lambda}(s) + \frac{\rho_{\lambda,w}}{\pi} \int_{\hat{\mathbf{n}} \cdot \hat{\mathbf{s}}' < 0} I_\lambda(s, \hat{\mathbf{s}}') |\hat{\mathbf{n}} \cdot \hat{\mathbf{s}}'| d\Omega'$$

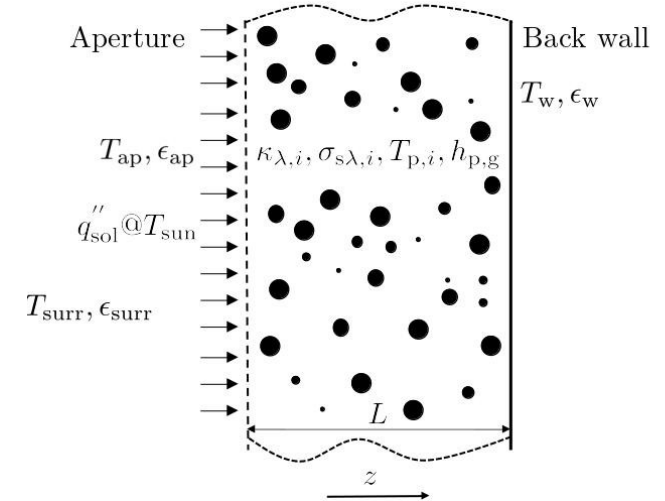
$$\nabla \cdot \mathbf{q}''_r = \int_0^\infty \int_{4\pi} \frac{dI_\lambda}{ds} d\Omega d\lambda = \int_0^\infty \kappa_{\lambda,p} (4\pi I_{b\lambda} - G_\lambda) d\lambda$$

- Numerical solution

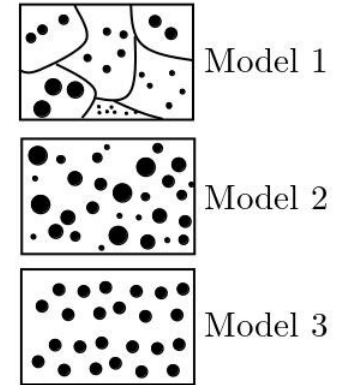
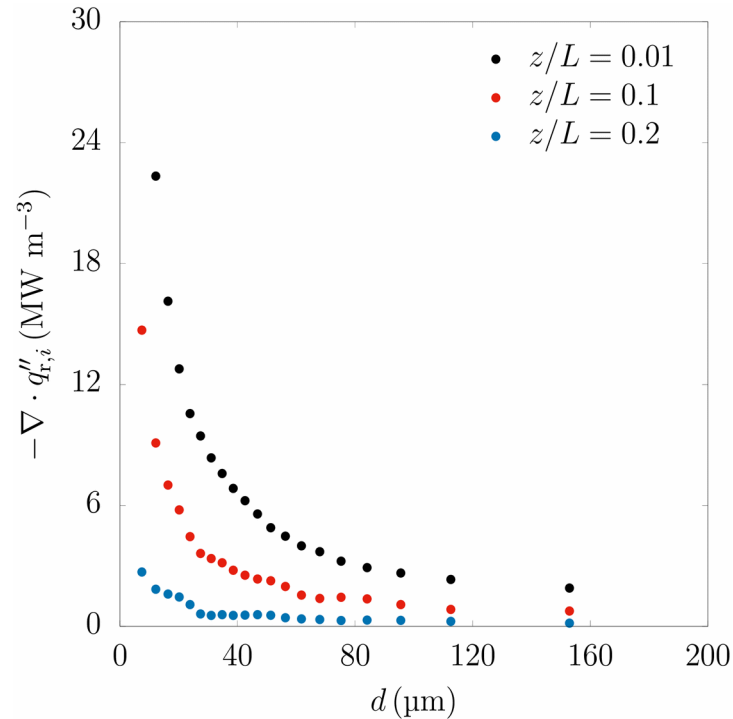
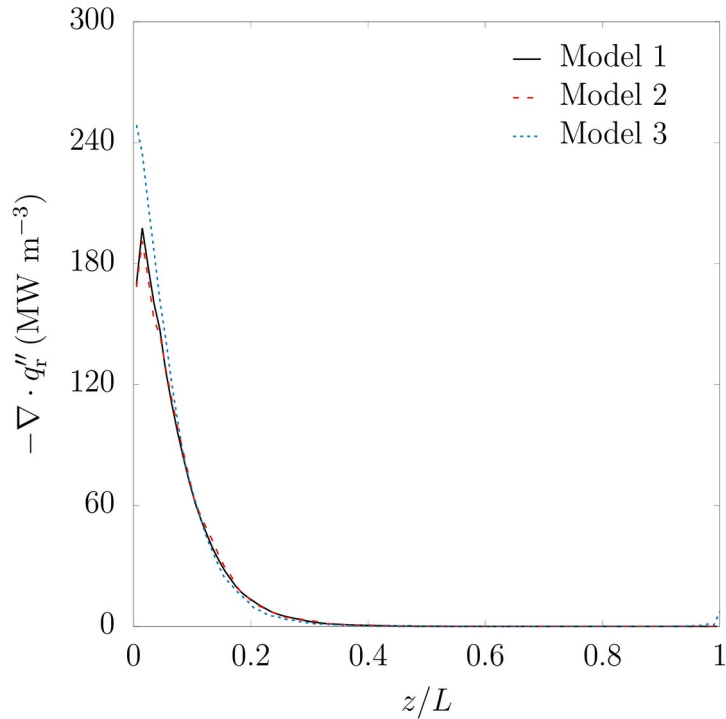
- Monte Carlo ray-tracing

$$q_{r,i} = - \int_{V_i} \nabla \cdot \mathbf{q}''_r dV = n_{a,i} q_{ray} - \int_{V_i} 4\kappa_P \sigma T^4 dV$$

$$q_{r,j} = - \int_{A_j} \mathbf{q}''_r \cdot \hat{\mathbf{n}} dA = n_{a,j} q_{ray} - \int_{A_j} \epsilon \sigma T^4 dA$$



Results: Radiative absorption



- Models 1 & 2 result in more intense radiation attenuation in the medium
- Radiation absorption in Model 3 is approximately 10% higher than in Models 1 & 2
- Strongly size-dependent radiation absorption is observed in Model 1

Summary and conclusions

- Multiphase particle-in-cell method is applied for particle–gas hydrodynamics
- Radiative transfer in polydispersed media is investigated by three alternative approaches
- Multi-component radiative transfer model (Model 1) gives insights into size-dependent transport phenomena and thermal response
- Multi-component radiative transfer model (Model 1) is coupled with particle–gas hydrodynamics models based on multiphase particle-in-cell method

Future work

- Experimental validation of the heat and mass transfer model
- Integration of the multi-component radiative transfer model (Model 1) with particle–gas flow in a full-scale particle receiver

Acknowledgements

ARENA



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