

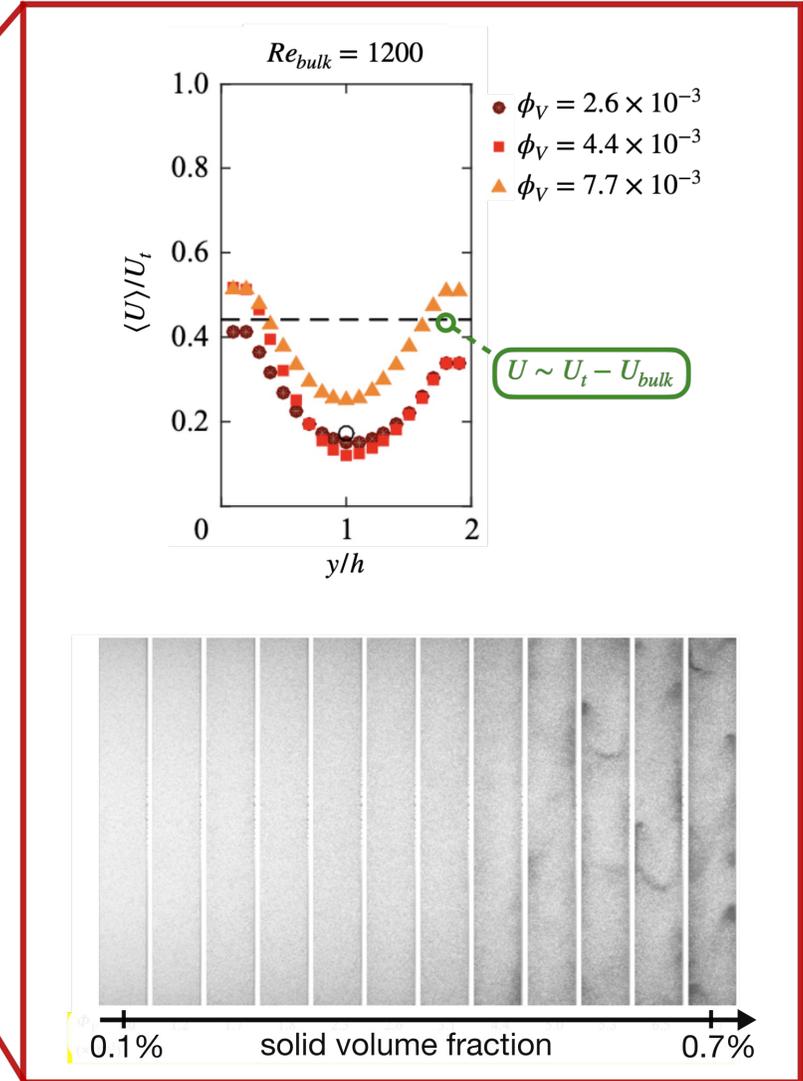
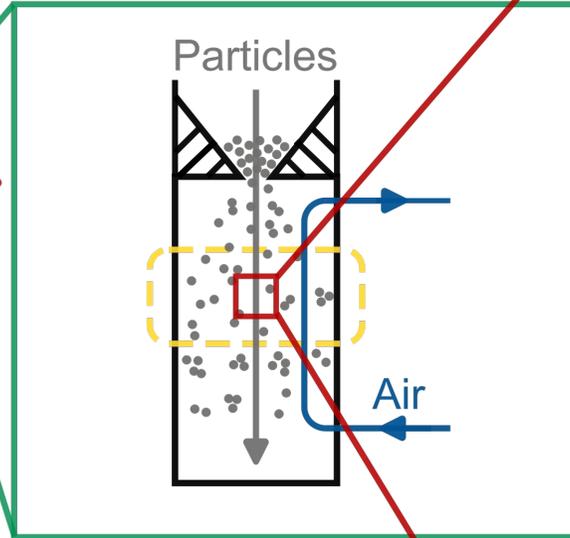
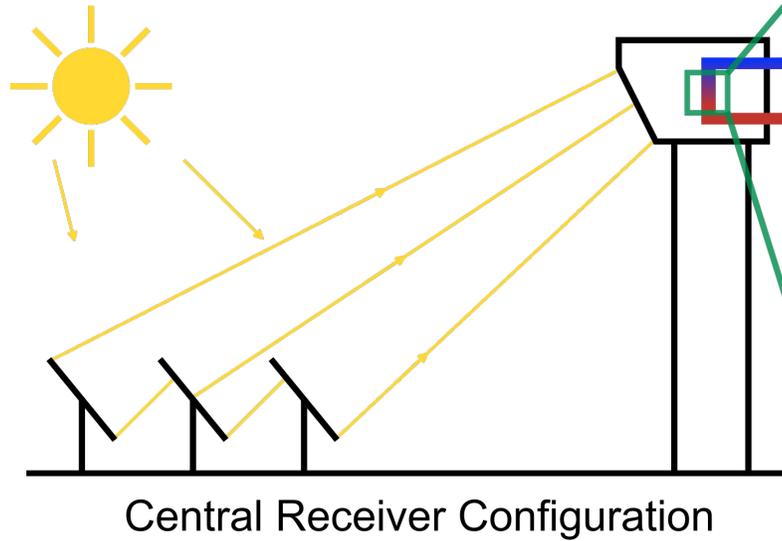


# Development of a High-Temperature Counter-Flow Solar Particle Receiver

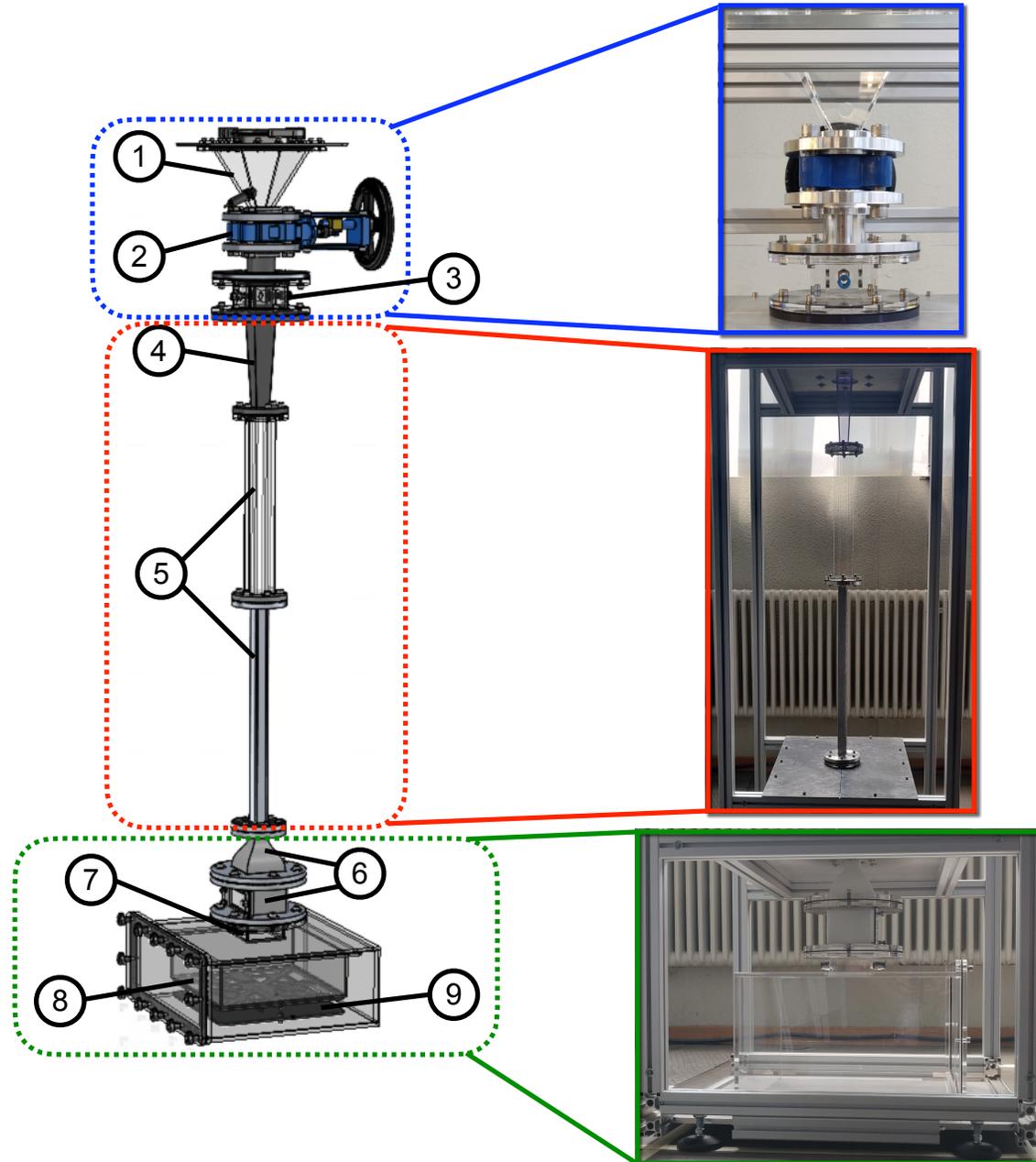
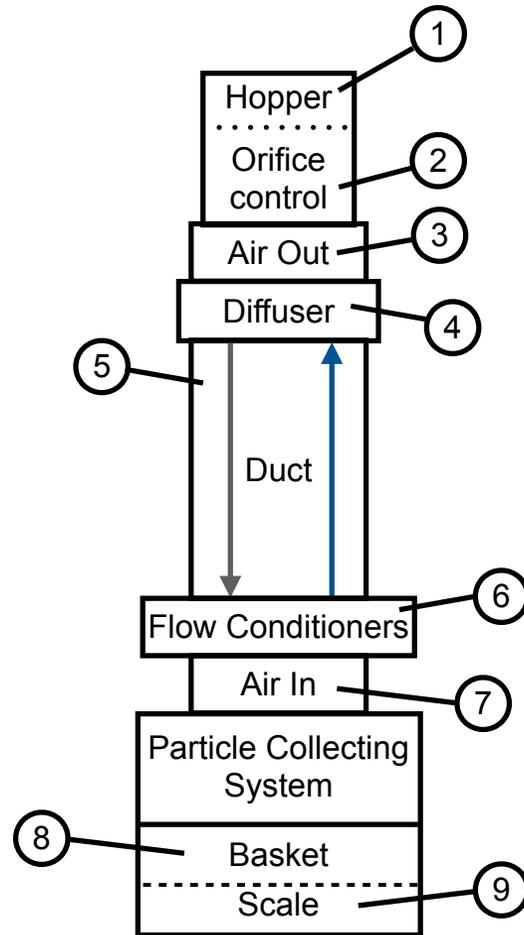
Anton Hartner, Filippo Coletti & Aldo Steinfeld

01. August 2023, Zurich

# Introduction



# Experimental Set-Up



# 1D Heat Transfer Model – General

General Assumptions:

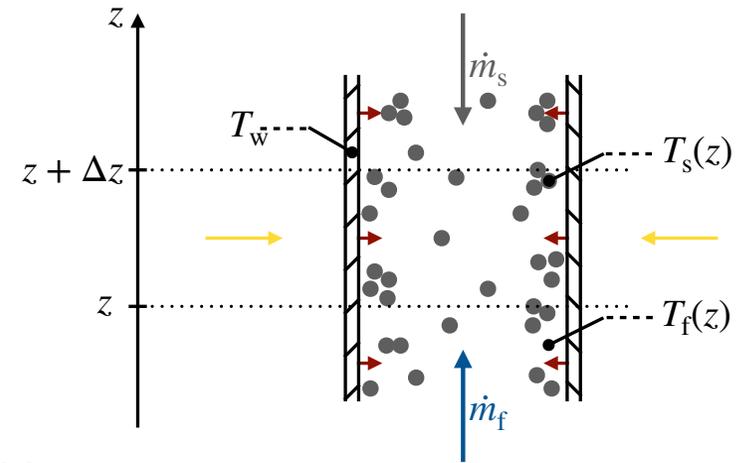
- 1D problem along the z-direction
- Steady state, no accumulation of heat
- No pressure drop

Fluid Phase:

- Non-participating medium
- Conduction neglected
- Convection: Fluid-Particles, Fluid-Wall

Solid Phase:

- Participating medium
- Inter-/ Intra-particle conduction neglected
- Convection: Fluid-Particles



Energy Balances:

$$\begin{array}{l}
 \text{Fluid Phase: } \boxed{\dot{m}_f c_{p,f} \frac{dT_f}{dz}} = \boxed{\frac{6 \phi_{v,s}^2}{d_p} A_{cs,duct} h_{s-f} [T_s - T_f]} + \boxed{h_{w-f} [T_w - T_f]} \\
 \text{Solid Phase: } \boxed{-\dot{m}_s c_{p,s} \frac{dT_s}{dz}} = \boxed{-\frac{6 \phi_{v,s}^2}{d_p} A_{cs,duct} h_{s-f} [T_f - T_s]} - \boxed{\frac{\dot{Q}_{rad}}{\Delta z}} \quad \forall \dot{m}_s < 0
 \end{array}$$

convection      heat exchange fluid - solid      heat exchange fluid - wall

convection      heat exchange fluid - solid      radiative source term

# 1D Heat Transfer Model – Radiative Source Term

The radiative source term can be expressed by

$$\dot{Q}_{\text{rad}} = \underline{\nabla}q_r A_{\text{cs,duct}} \Delta z \quad \text{with} \quad \underline{\nabla}q_r = 4\pi \int_0^\infty a_\lambda [i'_{\lambda b}(S) - \bar{i}'_\lambda(S)]$$

with  $\underline{\nabla}q_r$  being the divergence of the radiative flux. An expression for  $\underline{\nabla}q_r$  can be found with the help of the radiative transfer equation

$$\frac{di'_\lambda}{dS} = -\text{Loss by absorption} + \text{Gain by emission} - \text{Loss by scattering} + \text{Gain by scattering}$$

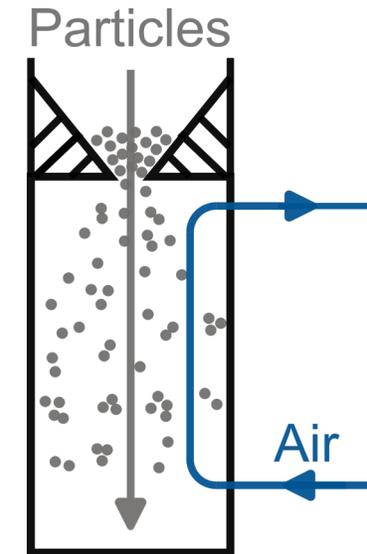
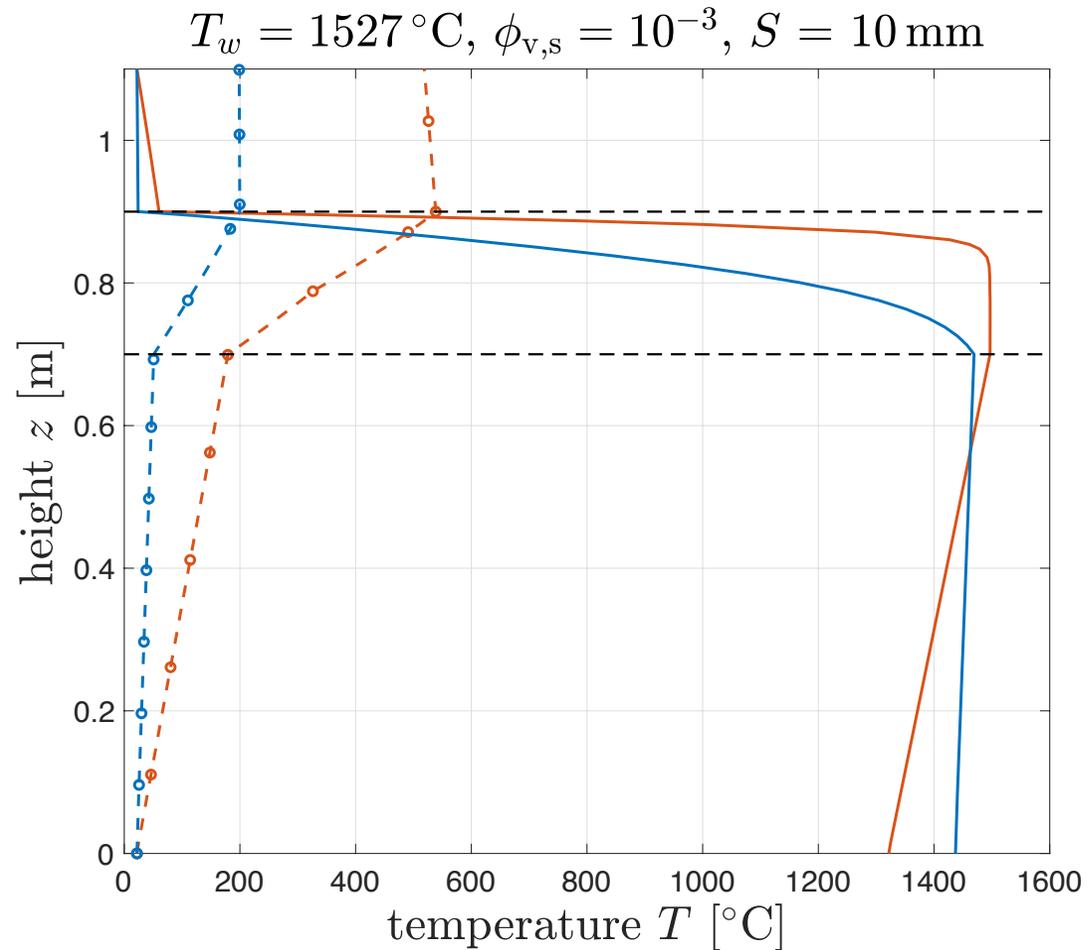
Assumptions:

- No augmentation by incoming scattering
- The temperature of the particle is constant along the width/ depth of the duct
- Each wall acts as a gray emitter
- Constant absorption & scattering coefficient
- Only collimated rays emitted by the inner walls
- Absorption/ scattering coefficient computed for large diffusely reflecting spheres

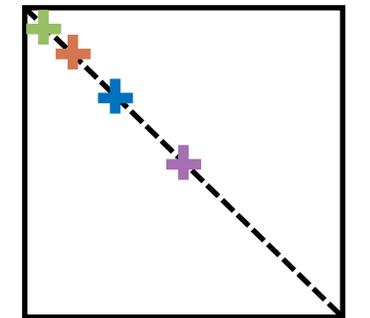
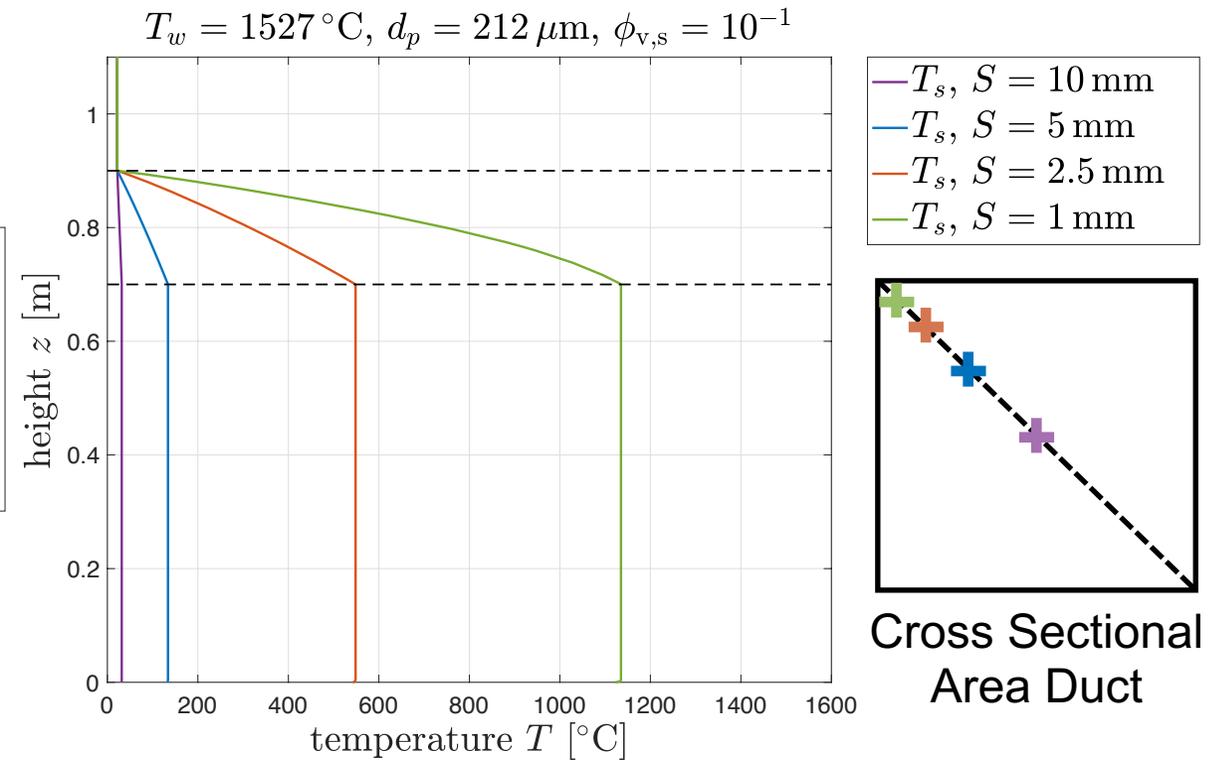
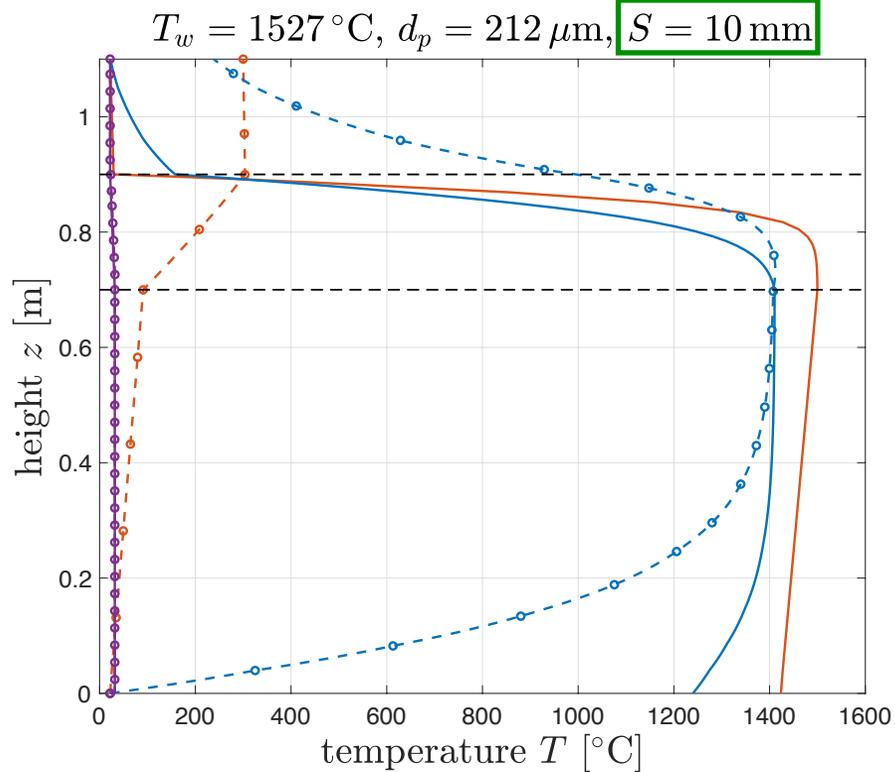
Then, the divergence of the radiative flux of one wall is given by

$$\underline{\nabla}q_{r,\text{one wall}} = 4a \left[ \sigma \varepsilon_s T_s(S)^4 - \sigma \varepsilon_w T_w^4 \exp(-KS) - \frac{a\sigma \varepsilon_s T_s(S)^4}{K} \{1 - \exp(-KS)\} \right]$$

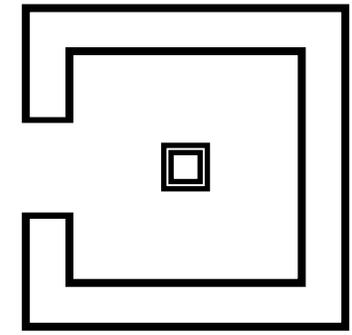
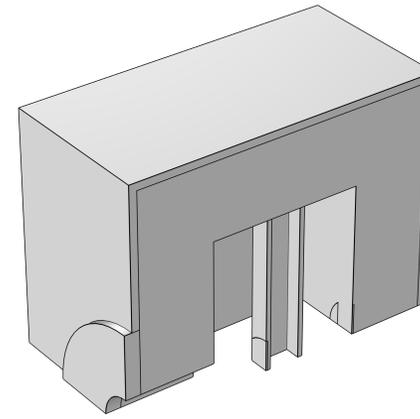
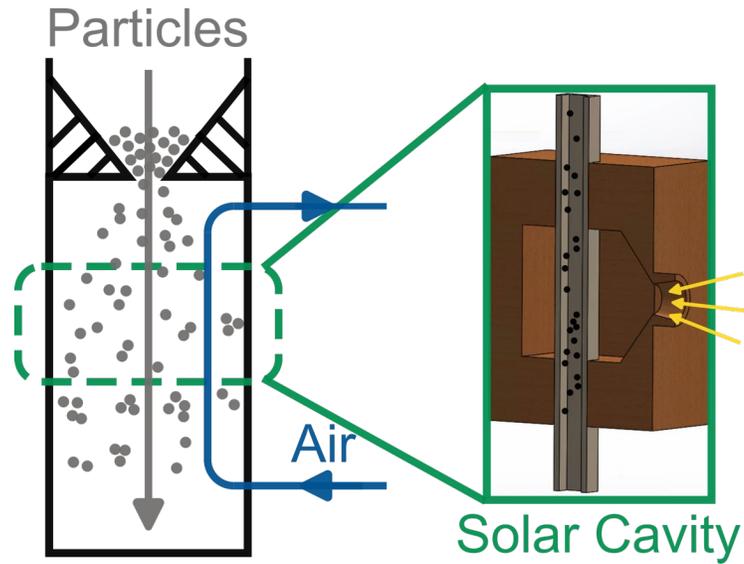
# 1D Heat Transfer Model – Results: Influence of Particle Diameter



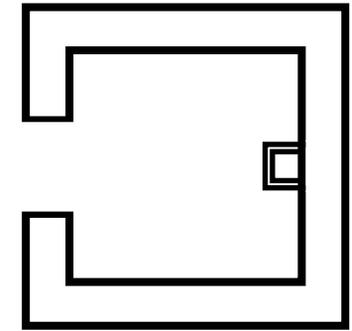
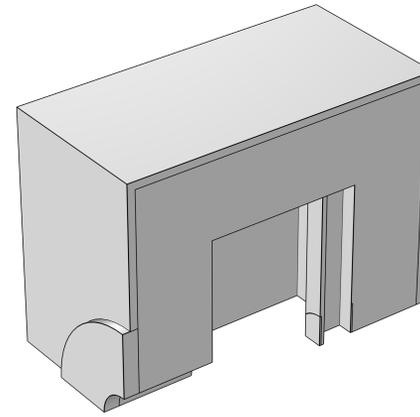
# 1D Heat Transfer Model – Results: Influence of Solid Volume Fraction



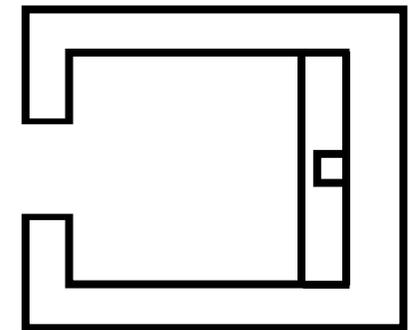
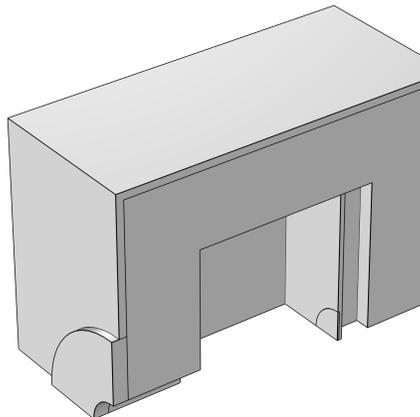
# Design of Solar Cavity



Configuration A



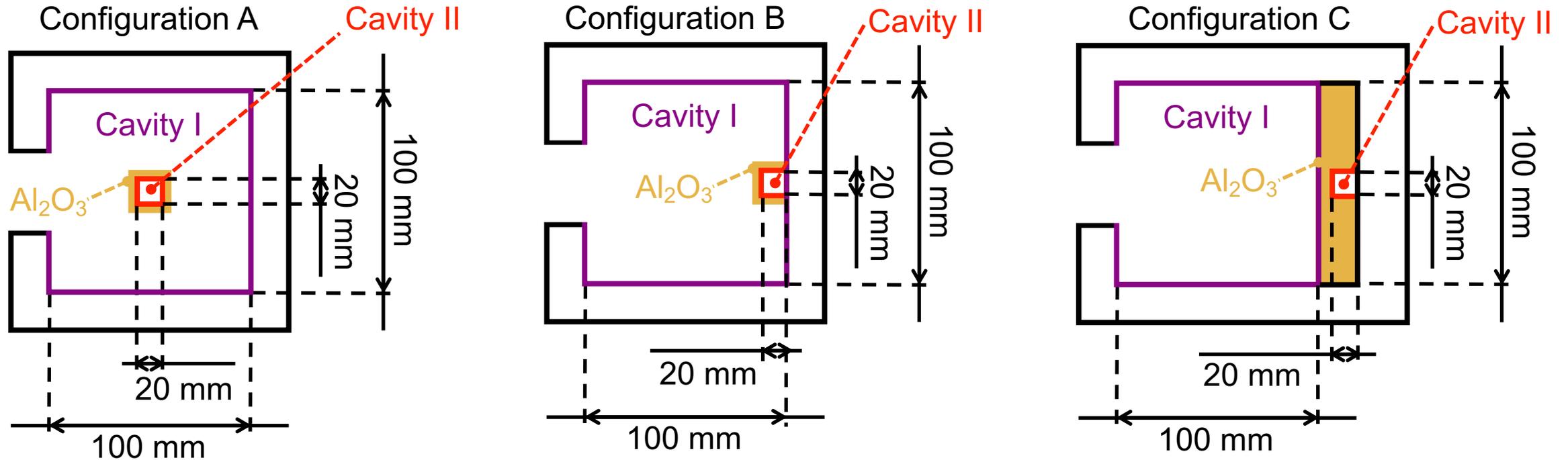
Configuration B



Configuration C

Welte et al. *Ind. Eng. Chem. Res.*, 2016, **55** (40), doi: 10.1021/acs.iecr.6b02853

# Design of Solar Cavity – Dimensions of Configurations



Further, for all configurations:

- Diameter of Aperture: 40 mm
- Thickness of Insulation: 50 mm
- Wall Thickness of Alumina: 3mm  
(except for configuration C – here the thinnest part has a wall thickness of 3 mm)

# Simulation Conditions

Radiation Source:

- Collimated Rays
- Direction
- Source heat flux

$$\underline{r} = [x, y, z]^T = [1, 0, 0]^T$$

$$\dot{q}_{\text{solar}} = 1 \cdot 10^6 \text{ Wm}^{-2}$$

It follows:

$$\dot{Q}_{\text{solar}}^{\text{theoretical}} = \dot{q}_{\text{solar}} A_{\text{aperture}} \cong 1256.6 \text{ W}$$

→ This is equivalent to a concentration ratio of  $C = 1000$  suns

Further:

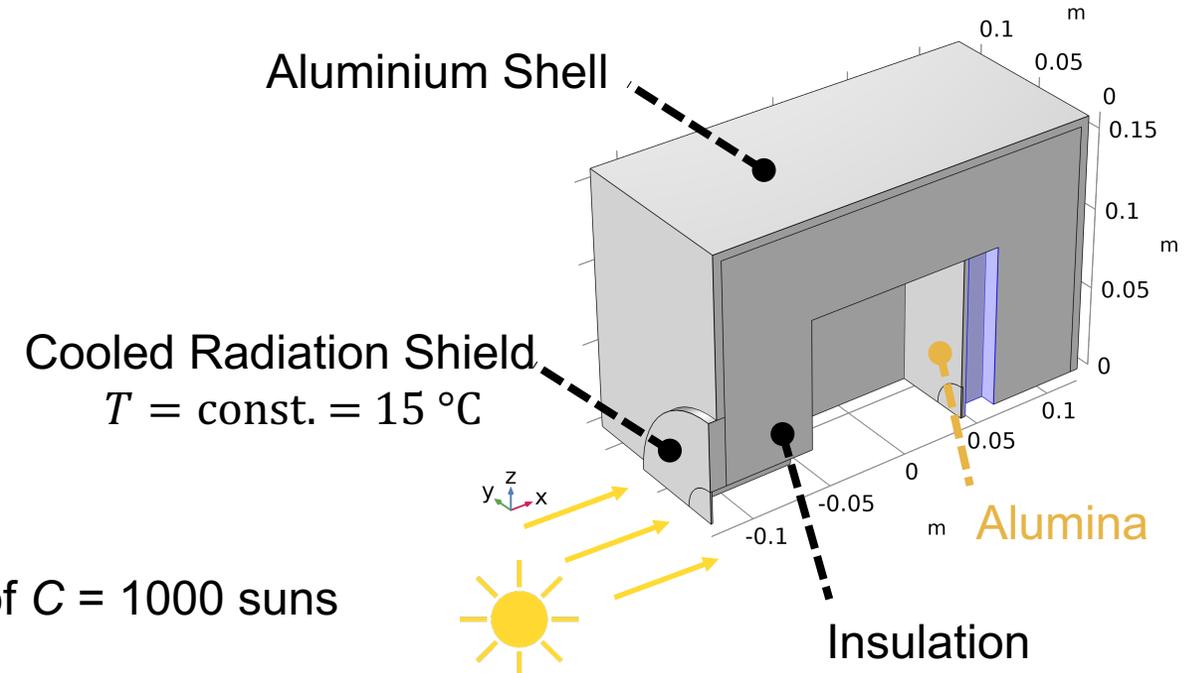
- Surfaces of aluminium shell radiate heat to the ambient
- Inside the second cavity a convective heat flux is imposed on the surfaces (surfaces highlighted blue)

$$\dot{q}_{\text{sink}} = h_{\text{conv}} [T_{\text{ext}} - T_w] \quad \text{with} \quad T_{\text{ext}} = \text{const.} = 20 \text{ }^\circ\text{C} \quad \& \quad h_{\text{conv}} = 450 \text{ Wm}^{-2}\text{K}^{-1}$$

- Thermal conductivities of alumina and insulation are assumed to be constant and measured for  $1000 \text{ }^\circ\text{C}$

$$k_{\text{insulation}} = 0.25 \text{ Wm}^{-1}\text{K}^{-1}$$

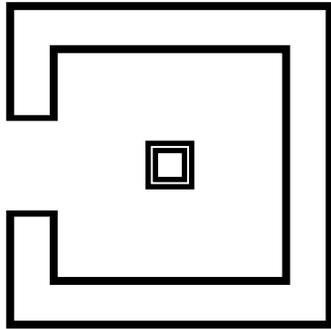
$$k_{\text{Al}_2\text{O}_3} = 6.77 \text{ Wm}^{-1}\text{K}^{-1}$$



# Estimated Conversion Efficiencies

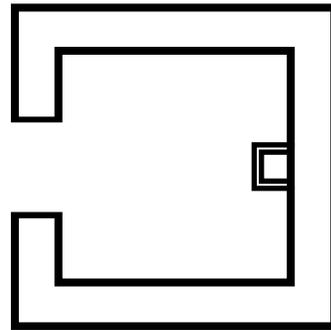
The three configurations are compared based on the conversion efficiency

$$\eta_{\text{conversion}} = \frac{|\dot{Q}_{\text{sink}}|}{\dot{Q}_{\text{solar}}}$$



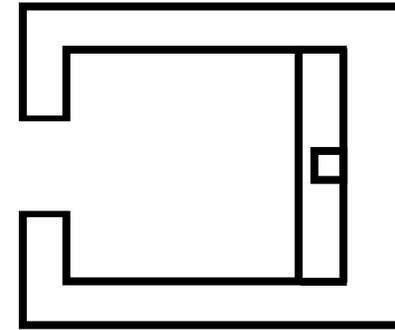
Configuration A

$$\eta_{\text{conversion}}^{\text{A}} \cong 49.7 \%$$



Configuration B

$$\eta_{\text{conversion}}^{\text{B}} \cong 55.0 \%$$



Configuration C

$$\eta_{\text{conversion}}^{\text{C}} \cong 78.3 \%$$

# Conclusion

- The 1D heat transfer model captures the most important heat transfer modes, convection and radiation, and estimates temperature profiles which agree with the literature:
  - i. Increasing the particle diameter leads to a decrease of the particle temperature
  - ii. Increasing the solid volume fraction decreases the particle temperature
- The conversion efficiency is predicted to be highest for configuration C  
→ Building the solar cavity similar to this geometry.

# Outlook

- Investigating the hydrodynamics of the counter-current solar particle receiver under room temperature conditions using back lighting and high speed imaging.
- Finalizing the CAD of an experimental facility that will allow to study the thermal performance of the solar particle receiver:
  1. What is the outlet temperature of the particle phase as a function of the particle loading and the velocity of the counter-current air flow?
  2. What is the overall heat transfer coefficient?
- Assessing if the cluster formation has an effect on the heat transfer performance of the receiver.