

Enhancing Accuracy of Large Eddy Simulation for Particle-Laden Wall-Bounded Flows Through Stochastic Subgrid Scale Fluctuations Modeling

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- **Introduction**

- Motivation and objective
- Solver and computational domain

- **Results**

- FDNS results
- Particles dispersion and deposition:
FDNS vs DNS
- Stochastic SGS fluctuations modeling

- **Conclusions and future study**

Turbulent particle-laden flow

Aerosol in exhaled breath or sneeze



Sediment transport in rivers



blood flow (plasma (liquid), red blood cells(solid))



Air pollution



Volcanic eruptions



Rain formation in clouds



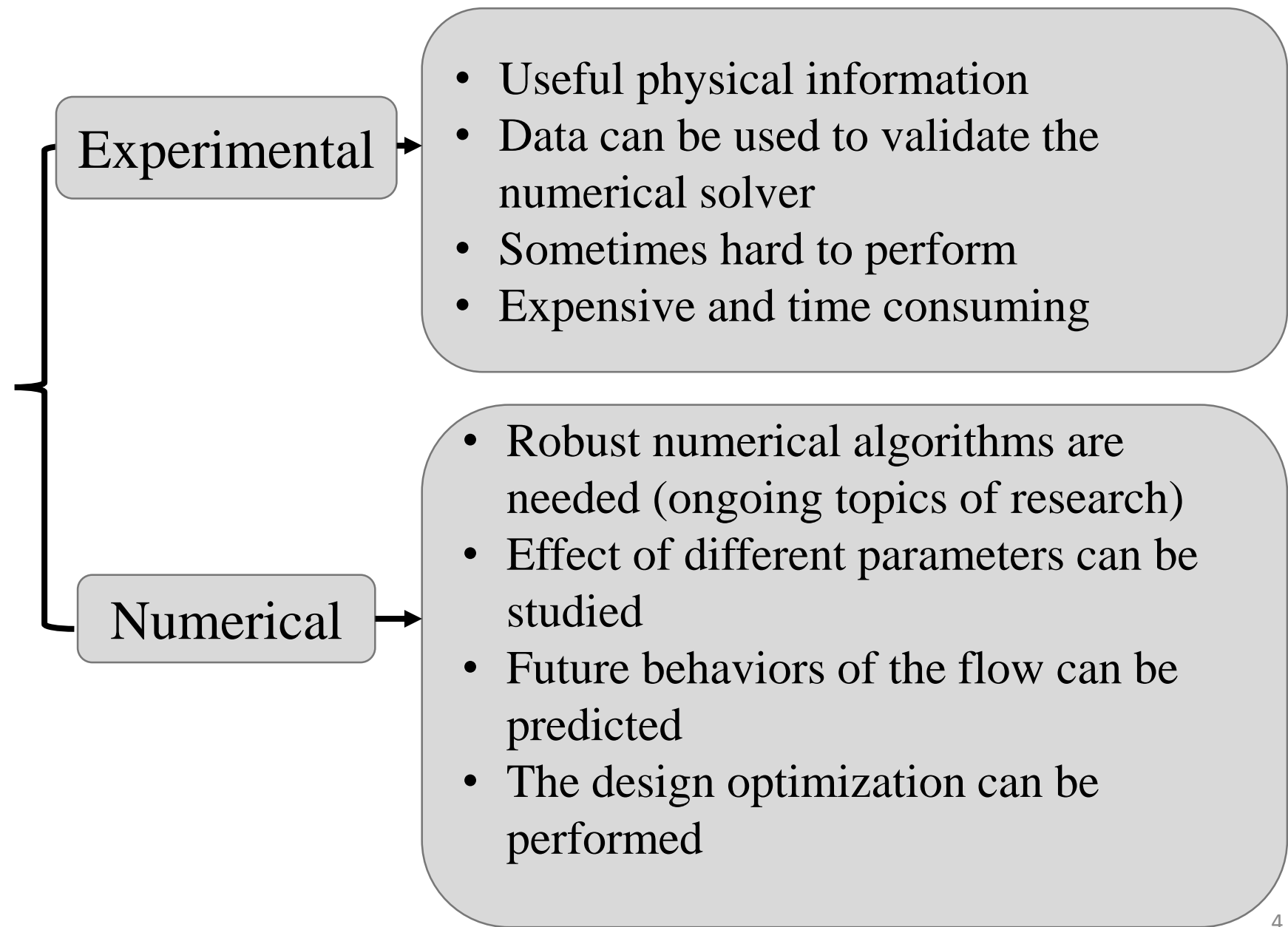
Sand and dust storms



Turbulent particle-laden flow

Study of turbulent particle-laden flows

Due to inherent complexity of turbulent flow, analyzing its interaction with dispersed phase, particle deposition and heat transfer is challenging.

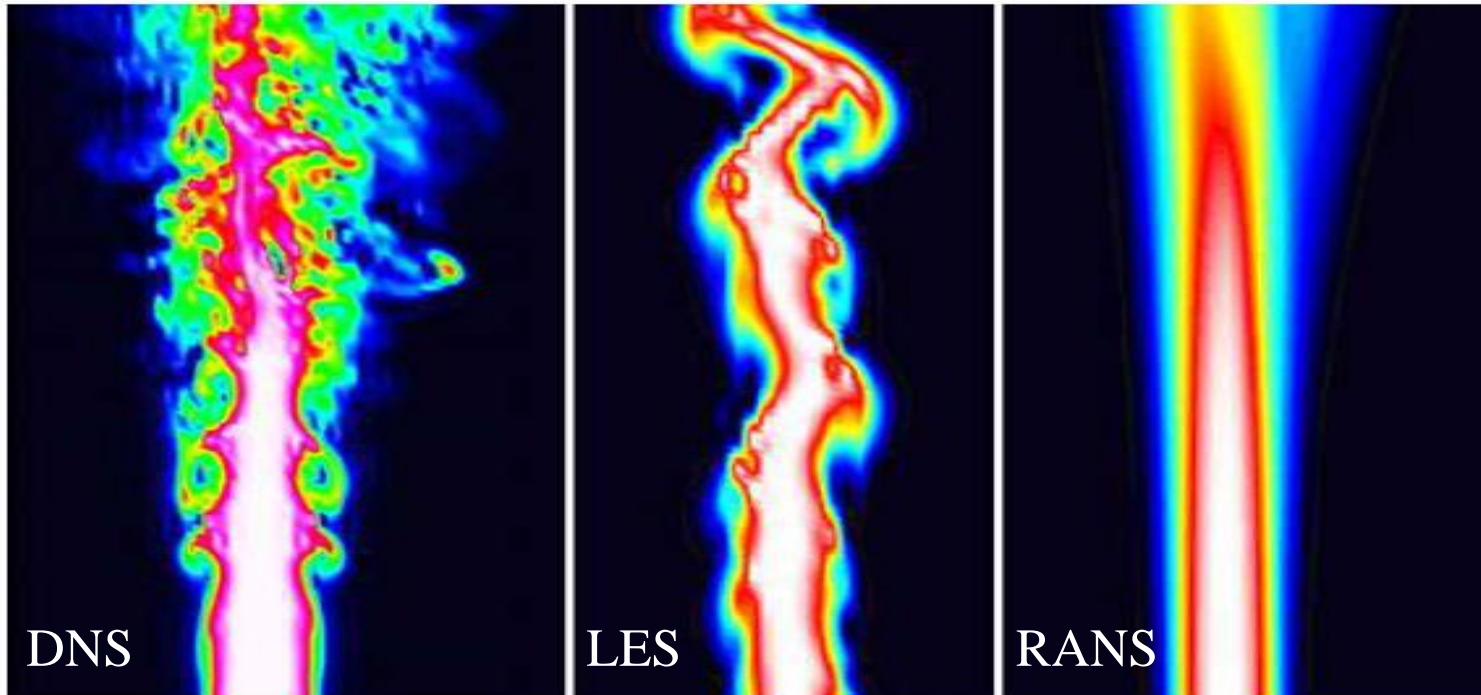


Numerical
simulation

Eulerian-Lagrangian
method
With point-particle
assumption

- **High accuracy**
To resolve the dispersed phase at lower mass fractions.
- **Simplicity of modeling**
The interaction between the phases.

Carrier phase, Eulerian



DNS

LES

RANS

- Resolving all of the turbulence scales
- No modeling
- Computationally expensive

- Resolving large scales
- Sub-grid Scale stresses are model
- Trade-off between accuracy and computational cost

- Mean quantities of fluid flows
- Reynolds stress terms are model
- Lowest computational cost

Maries, Adrian, et al. "Interactive exploration of stress tensors used in computational turbulent combustion." *New Developments in the Visualization and Processing of Tensor Fields*. Springer, Berlin, Heidelberg, 2012. 137-156.

Motivation

- Enhancing LES accuracy in particle-laden wall-bounded flows through subgrid-scale fluctuations modeling for particles.

Objective

- Develop an appropriate Langevin equation for simulating sub-grid scale velocity fluctuations seen by particles so that particle fluctuation and concentration are correctly predicted.

Solver and Computational domain

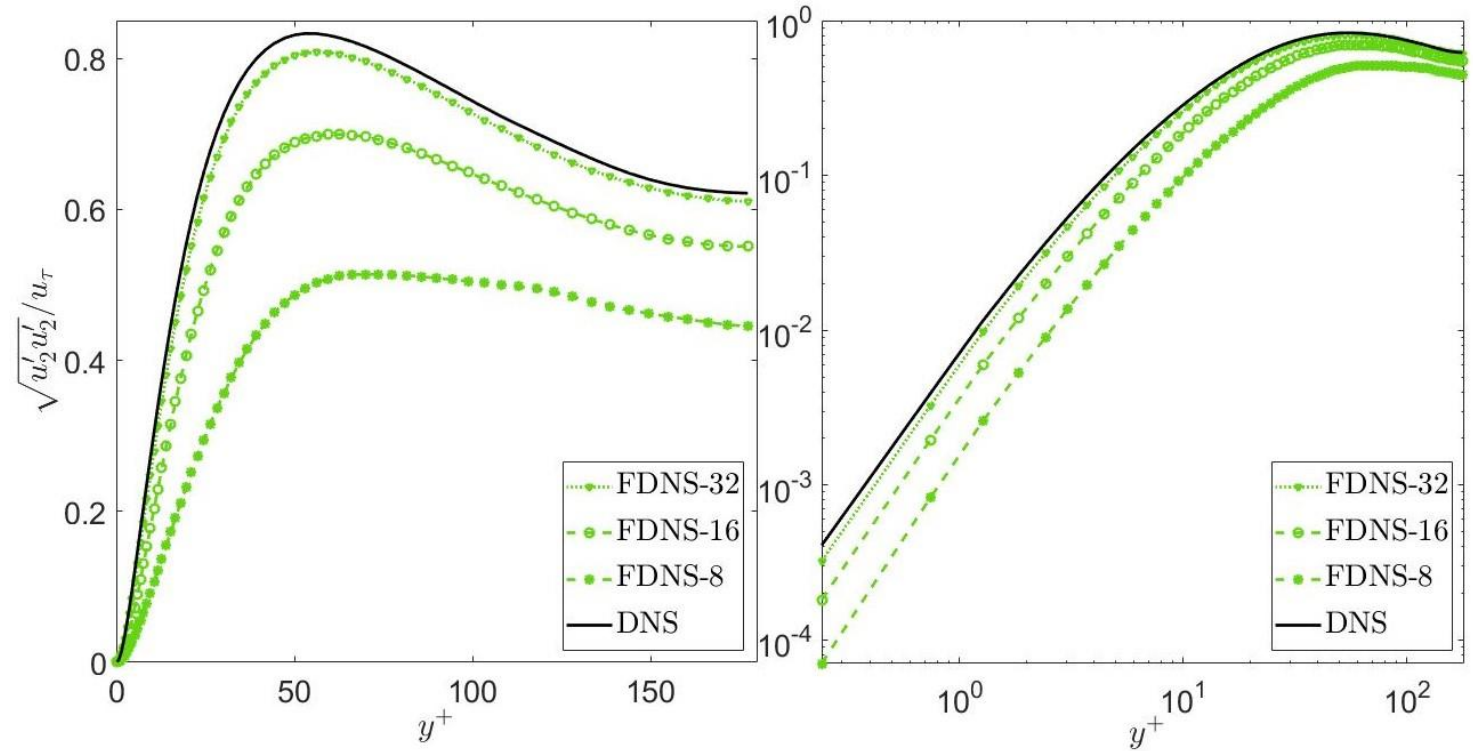


- Eulerian-Lagrangian approach
- Point-particle assumption, one-way coupling
- Channel flow with periodic boundary conditions in the streamwise and spanwise directions.
- $Re_{\tau} = 180$ - tracking 200,000 particles
- Particle-wall collisions: Fully absorbing (trap-wall)
- For DNS 128^3 grid points
- The parallel solver runs in a distributed memory environment (MPI)

- Time integration with second-order Adams–Bashforth method.
- Fourth-order central scheme in the periodic streamwise and spanwise directions.
- Second-order central scheme in the wall-normal direction, and viscous terms.
- Second-order Lagrange interpolation for the fluid velocity at the particle location.
- Spectral method with a modified wave number is used for the pressure Poisson equation in the homogeneous direction and a tridiagonal solver for the normal direction.
- Parallel mode available by dividing the computational domain into rectangular blocks in the normal direction.

Filtered DNS (FDNS)

Normal velocity fluctuations

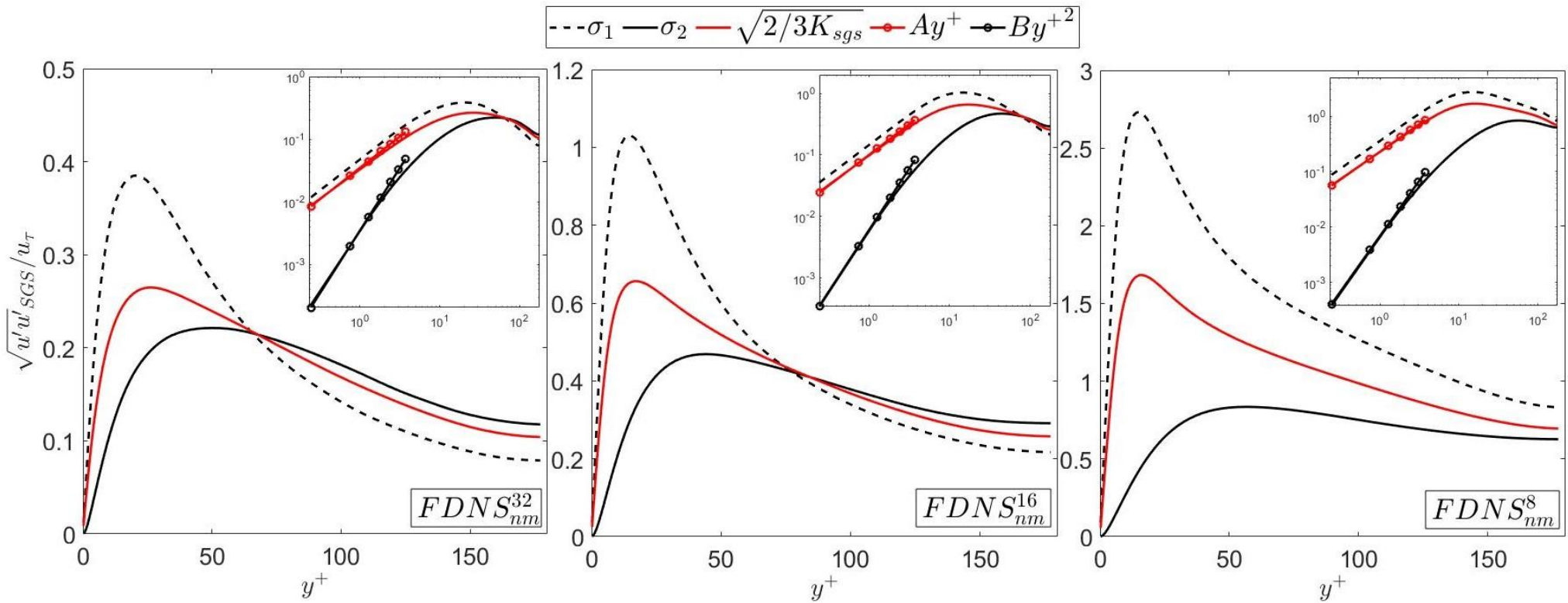


- $u_i^{\text{FDNS}}(x, y, z, t) = \text{FT}^{-1} \begin{cases} \hat{G}(\kappa_1) \cdot \hat{G}(\kappa_3) \cdot \hat{u}_i(\kappa_1, y, \kappa_3, t) & \text{if } |\kappa_j| \leq \kappa_c \text{ with } j = 1, 3 \\ 0 & \text{otherwise} \end{cases}$
- Sharp-cut off filter in Fourier space: $\hat{G}(\kappa_j) = 1$

Missed fluctuations in FDNS

SGS velocity fluctuations

DNS Grid- 128×128×128

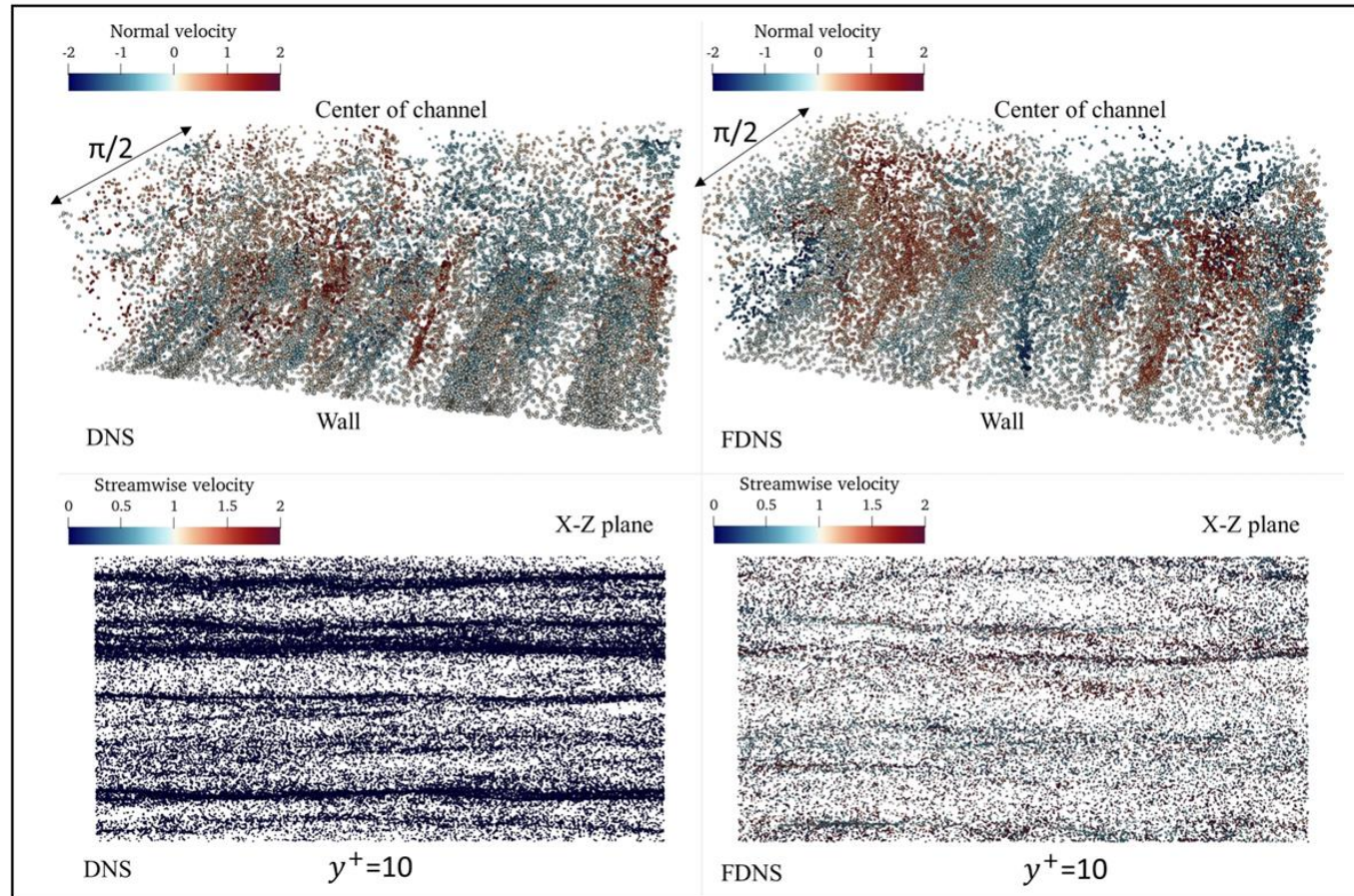


SGS velocity fluctuations are non-homogeneous and anisotropic.

Near wall flow structures

DNS

FDNS-16

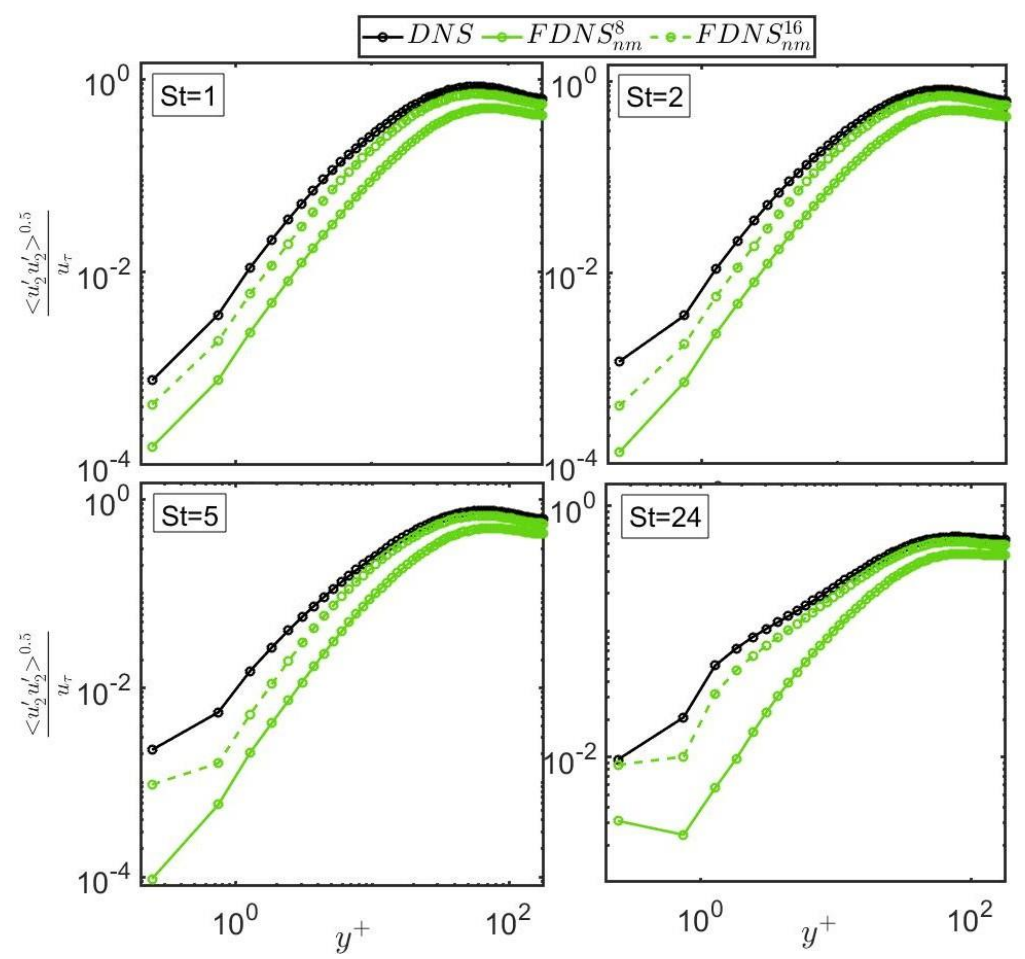
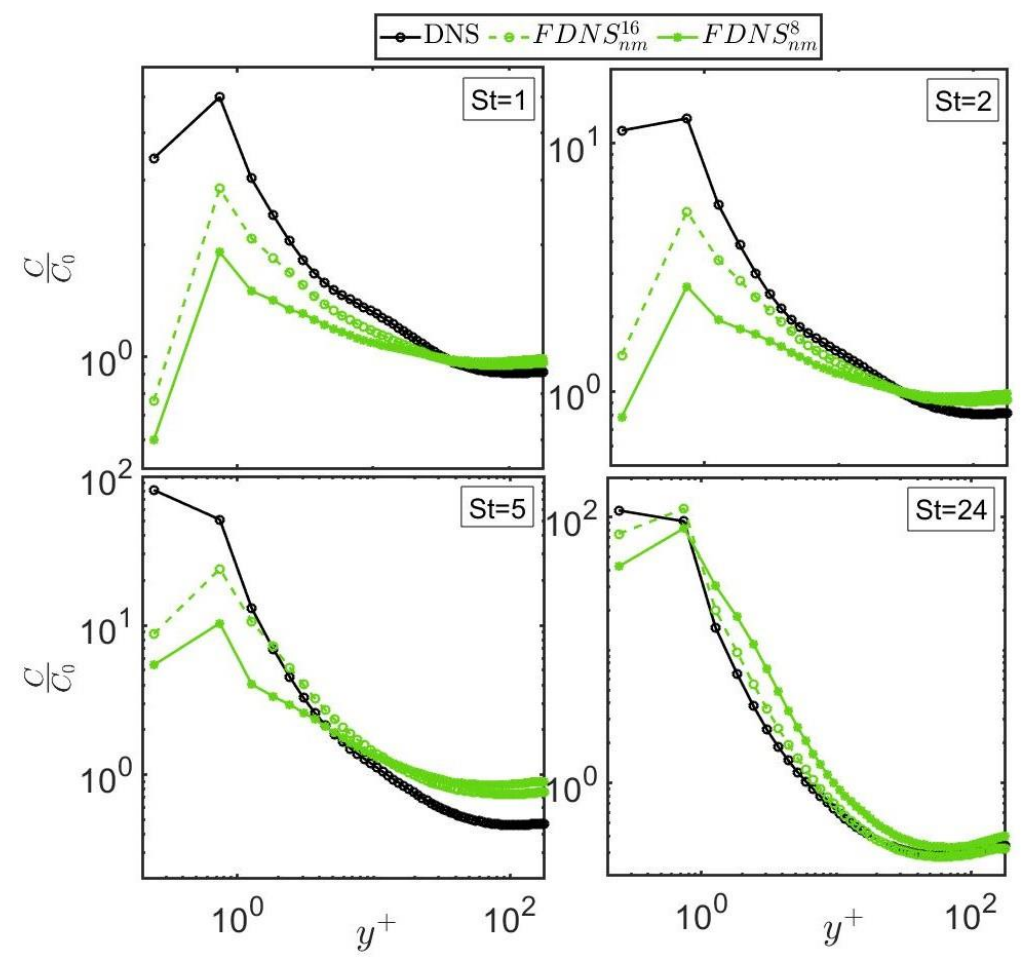


Snapshot of particle dispersion at $tu_\tau / h = 100$

Effect of filtering on particles

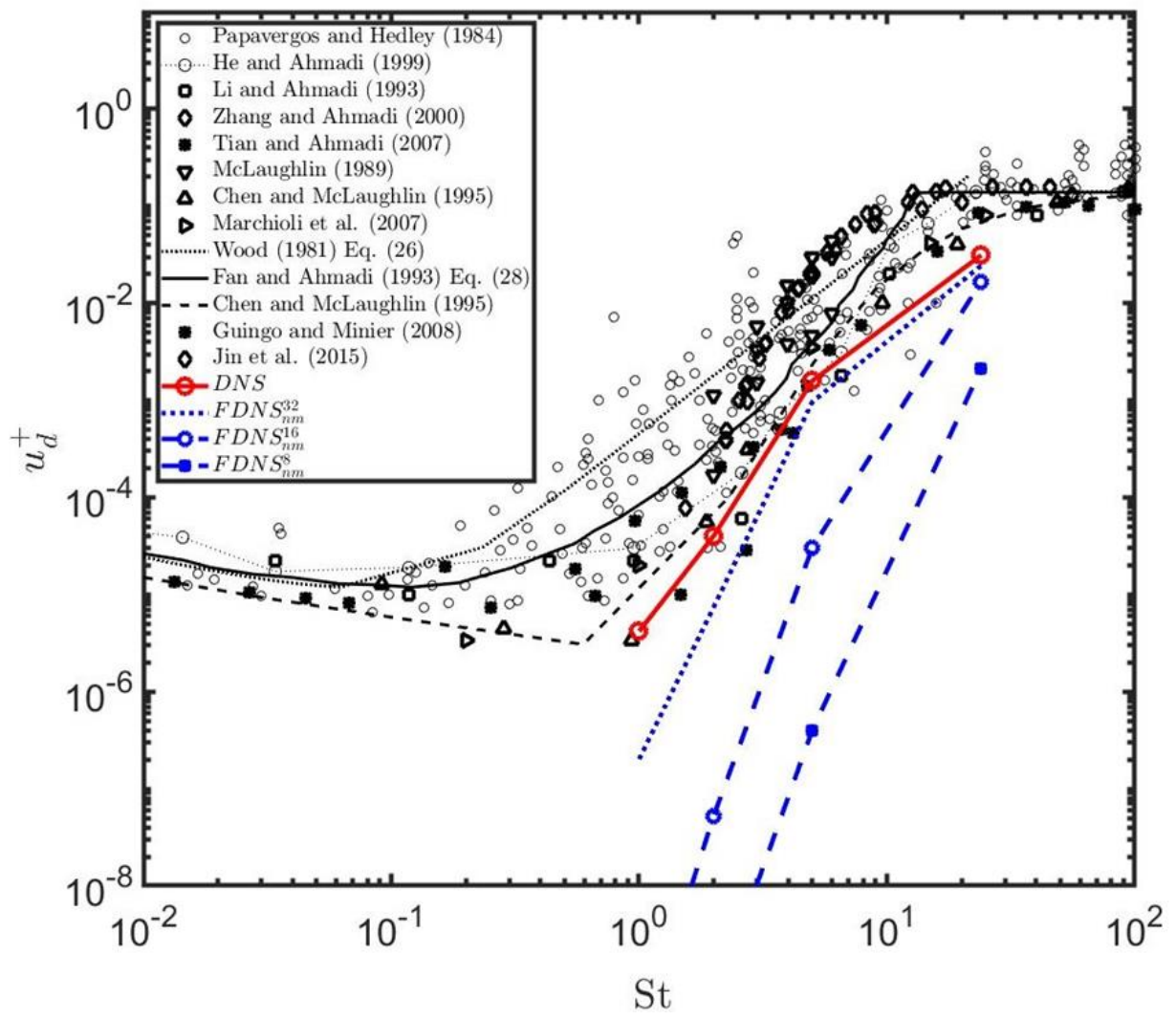
Particle concentration

Particle velocity fluctuations



Effect of filtering on particles

Particle deposition velocity



Stochastic modeling

SGS velocity fluctuation see by particles

$$d\left(\frac{u'_2}{\sigma_2}\right) = \left(\frac{\partial \sigma_2}{\partial x_2} - \frac{u'_2}{\sigma_2 \tau}\right) dt + \sqrt{\frac{2}{\tau}} dW$$

$$u_2'^{n+1} = \frac{\sigma_2^{n+1}}{\sigma_2^n} u_2'^n \exp\left(-\frac{\Delta t}{\tau_2}\right) + \sigma_2^{n+1} \left(1 - \exp\left(-2\frac{\Delta t}{\tau_2}\right)\right)^{\frac{1}{2}} \xi_2$$

$$+ \frac{\tau_2}{1 + St} \frac{\sigma_2^{n+1} \partial \sigma_2^{n+1}}{\partial y} \left(1 - \exp\left(-\frac{\Delta t}{\tau_2}\right)\right)$$

Drift term

Stokes number = $\frac{\tau_p}{\tau_f} = \frac{\rho_p d_p^2}{18\mu} \frac{v}{u_\tau^2}$

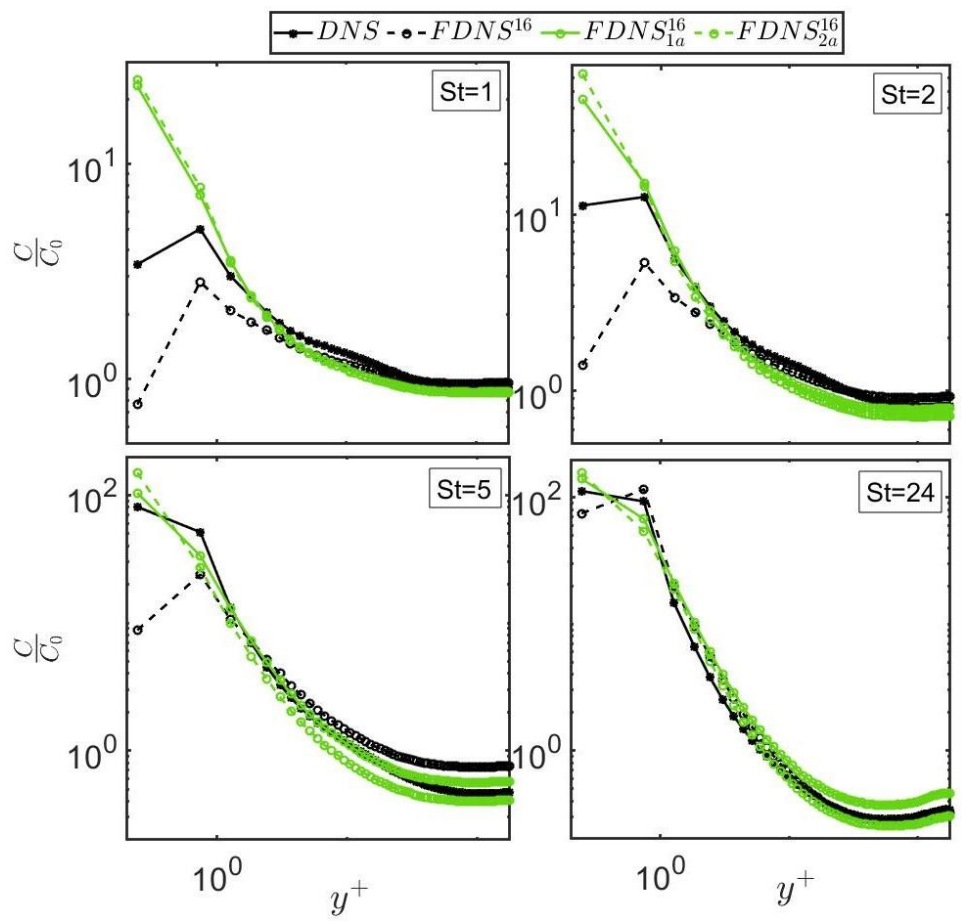
- τ is Lagrangian time scale
- σ is RMS of SGS velocity fluctuation

Isotropic Model

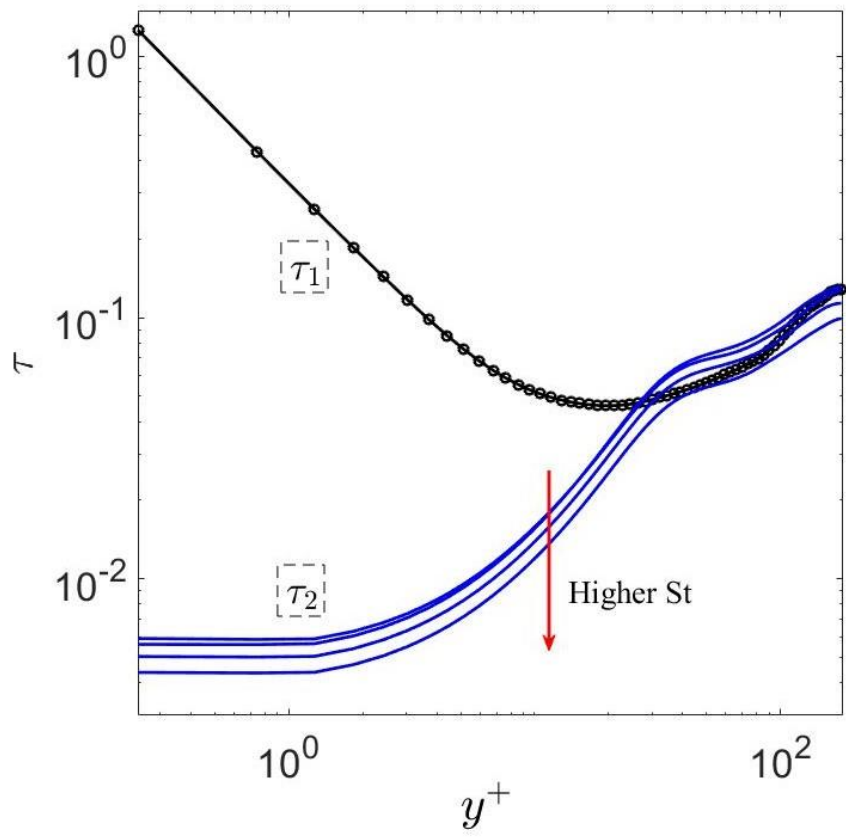
- $\tau \approx \Delta / (K_{SGS})^{1/2}$
- $\sigma = \left(\frac{2}{3} K_{SGS}\right)^{1/2}$

No Drift term

Concentration



Time scale

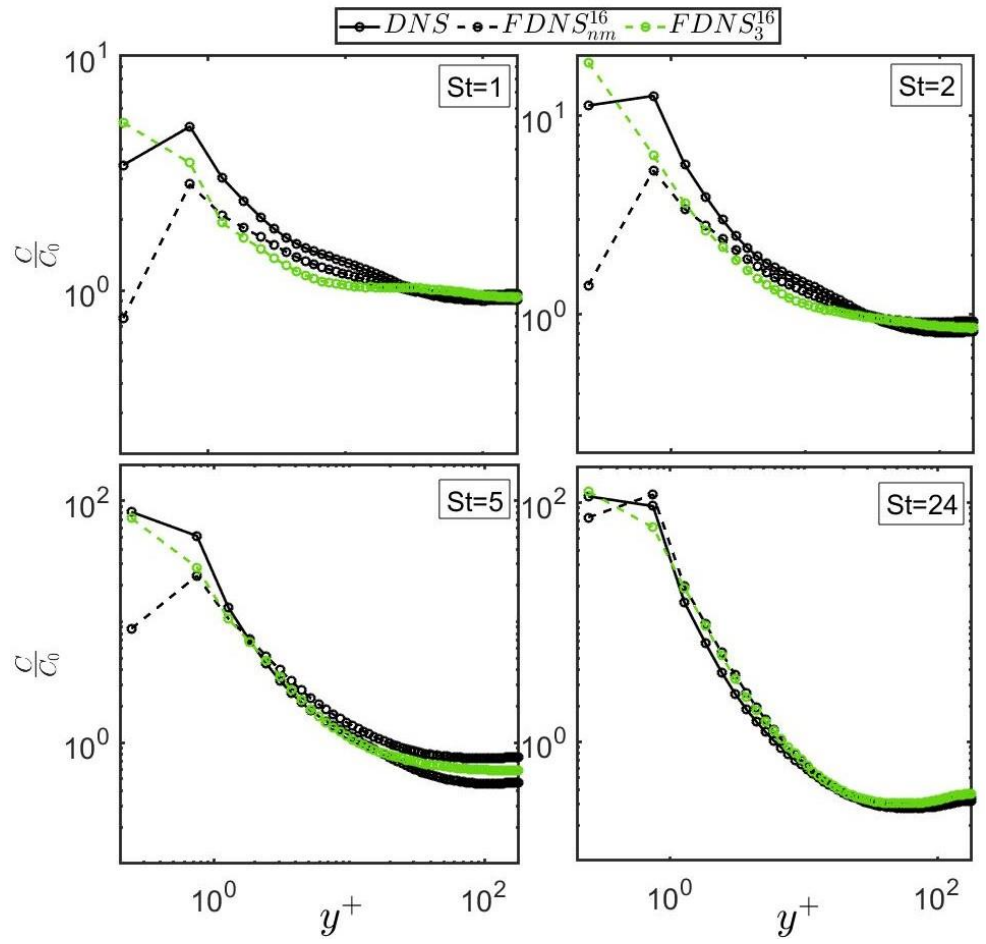


Excluding the drift term in the stochastic equation results in high concentration near the wall region, irrespective of the time scale employed in the equation (τ_1 or τ_2).

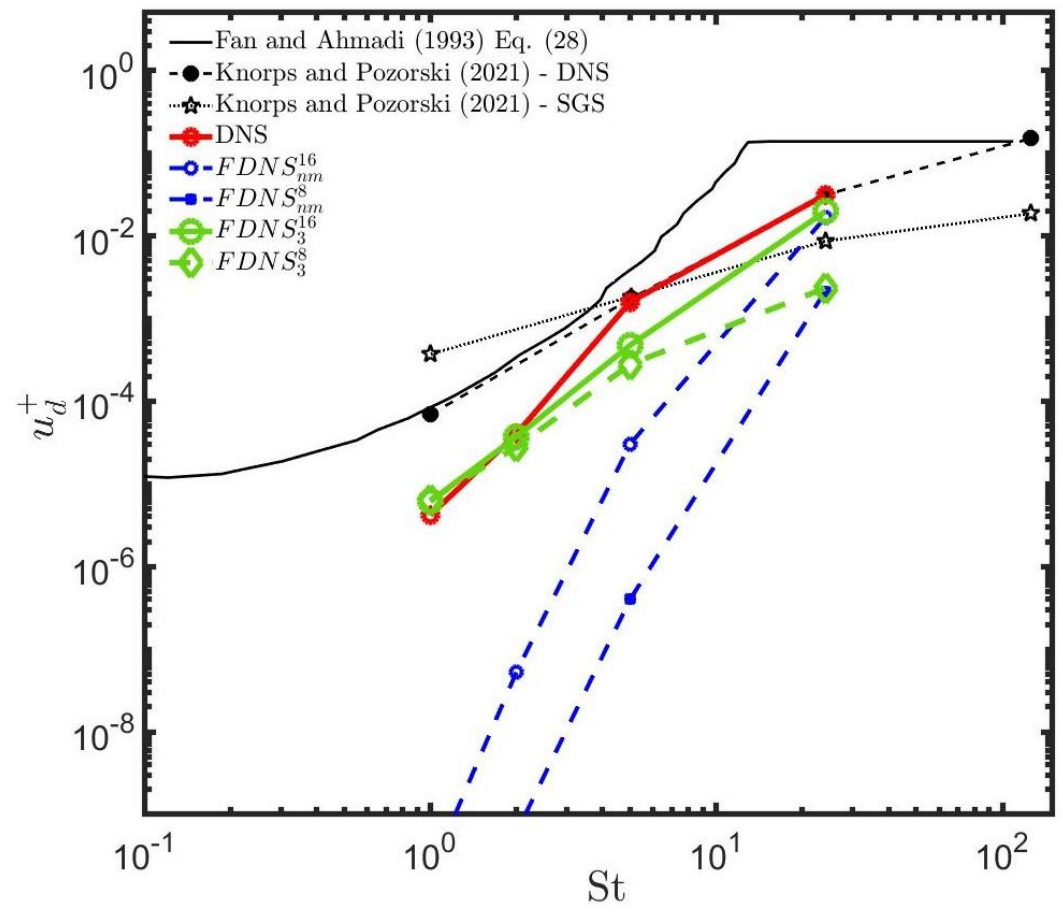
Model with drift term and modified time scale

$$\tau(\Delta, \sigma_2, St, y^+) = (1 - c_a \log(St)) \tanh(c_\tau y^{+2}) \frac{\Delta}{\sigma_2}$$

$c_a = 0.0825$
 $c_\tau = 0.001$



Particle concentration

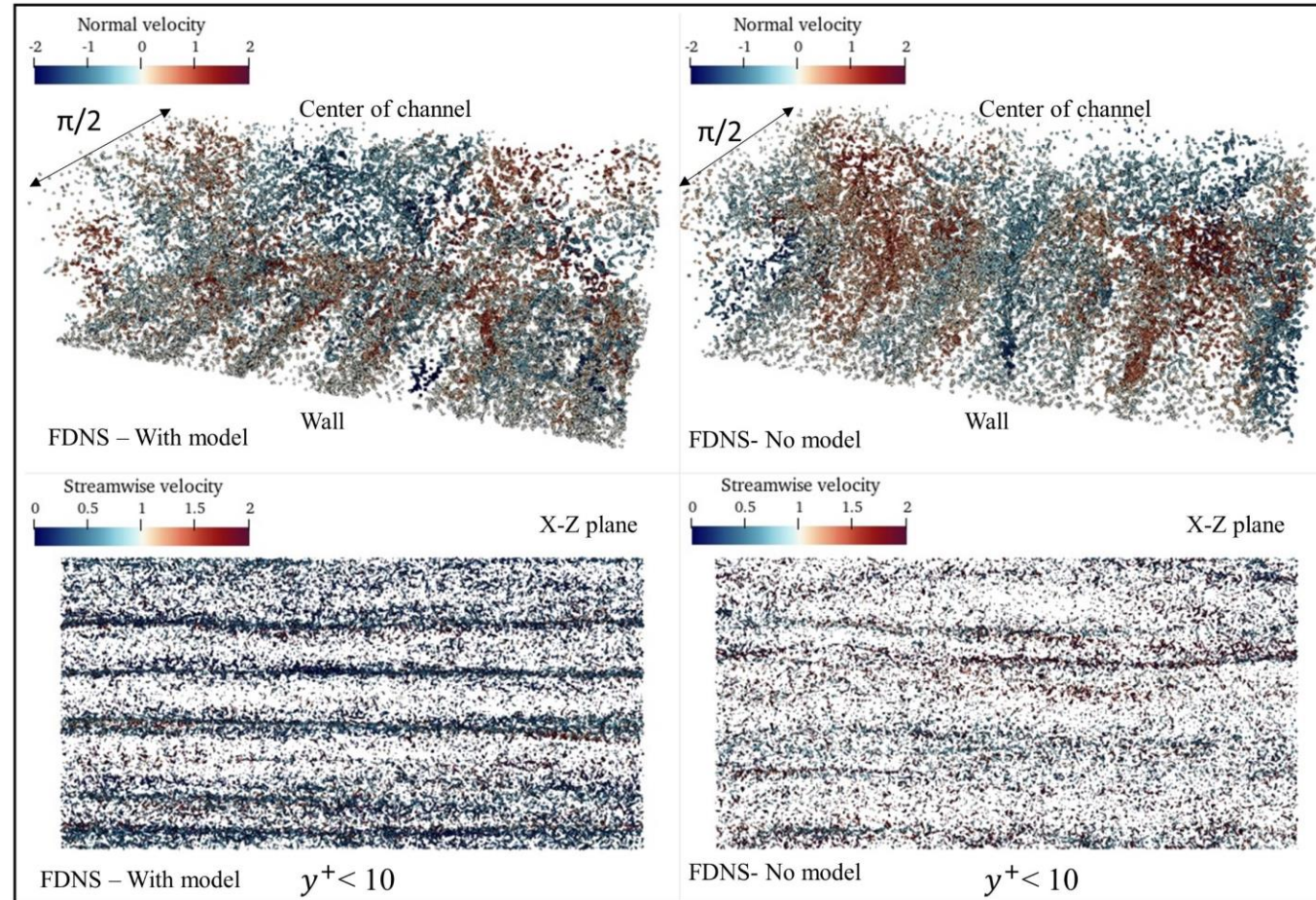


Particle deposition velocity

Near wall flow structures with model

With model

No model



Snapshot of particle dispersion $tu_\tau / h = 100$

- Filtering significantly decreases the particle deposition velocities at lower Stokes numbers ($St = 1, 2, 5$) and affects the particle dispersion in channel.
- The developed stochastic model is capable of predicting the correct deposition velocities and concentration profiles of lower inertia particles when the proper time-scale was used.
- Future Work: Evaluating the model performance for real LES scenarios.

Thank you for your attentions!

Questions?